

Supporting Information

Gaseous CO₂ Electrolysis: Latest Advances in Electrode and Electrolyzer Technologies toward Abating CO₂ Emissions

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Table S1. Compilation of previous studies on CO₂ electroreduction in MEA-based electrolyzers.

Year	FE [%] of CO ₂ RR products							E	j_{total}	Single-pass conversion for C ₂ H ₄ [%]	Stability			Cathode		Membrane	Anode	Anolyte	Electrode size	CO ₂ flow rate	Ref.
	C ₂ H ₄	EtOH	PrOH	AcOH	CO	HCOOH	H ₂	[V]	[mA cm ⁻²]		Time [h]	j_{total} [mA cm ⁻²]	E [V]	Catalyst	Ionomer				[cm ²]	[sccm]	
2019	48	15	3	7	20	1	5	4.2	200	1.5	100	120	3.8	Cu ^a	Nafion	Sustainion or Aemion	IrO ₂ /Ti	0.1 M KHCO ₃	5	80	1
2020	64	No Data	No Data	No Data	5	No Data	8	3.9	170	1.7	190	120	3.6	Cu	aryldihydropyridine oligomer	Sustainion	IrO ₂ /Ti	0.1 M KHCO ₃	5	80	2
2020	66	8	2	0	10	5	10	3.9	300	3.1	100	220	3.9	Cu ^b	Aquivion	Sustainion	IrO ₂ /Ti	0.1 M KHCO ₃	5	80	3
2021	57	16	2	5	11	2	6	3.8	175	1.6	236	175	3.8 ⇌ 2	Cu	Nafion	Sustainion	IrO ₂ /Ti	0.1 M KHCO ₃	5	80	4
2021	65	10	2	2	7	1	13	4.1	330	3.4	55	300	4.1	Cu-SiO _x	Aquivion	Sustainion	IrO ₂ /Ti	0.1 M KHCO ₃	5	80	5
2021	55	9	0	15	10	1	15	3.3	281	3.9	6	200	7.0 ^c	Cu-KOH	Nafion	Sustainion	IrO ₂ /Ti	1 M KOH	10	100	6
2021	63	5	2	1	10	2	12	3.8	150	— ^d	180	90	3.6	Cu ^e	Nafion	Sustainion	IrO ₂ /Ti	0.1 M KHCO ₃	No Data	50	7
2021	56	16	5	0	7	2	15	4.5	325	18.5	100	400	4.5	Ag-Cu ^f	Not in use	Fumasep	IrO ₂ /Ti	0.1 M KHCO ₃	4	10	8
2022	49	6	0	14	14	0	9	3.3	700	2.3	5	200	2.9	porous Cu	QAPEEK ^g	QAPEEK ^g	IrO ₂ /Ti	pure water	1.6	60	9
2022	48	No Data	No Data	No Data	12	No Data	16	5.4	300	3.7	52	200	4.0	Cu	Nafion	SC-BPMA ^h	IrO ₂ /Ti	0.1 M KHCO ₃	4	40	10
2023	40	3	2	4	10	0	17	3.7	500	— ^d	2	300	3.9	Cu	<i>p</i> TPN-Beim ⁱ	No Data	IrO ₂ /Ti	pure water	No Data	100	11
2023	44	44	0	3	2	1	10	2.7	300	4.5	400	200	3.2	Cu dendrites ^j	Nafion	Sustainion	IrO ₂ /Ti	1 M KOH ^k	4	30	12
2024	52	19	3	4	9	1	14	3.5	252	2.6	194	70	4.1	Cu	Nafion	PiperION	IrO ₂ /Ti	0.1 M KHCO ₃ ^l	6.25	80	13
2024	86	6	0	0	3	1	2	3.0	368	26.8	200	370	3.0	MP-Cuf20 ^m	Not in use	Sustainion	Ni form	0.1 M KHCO ₃	5	15	14
2024	43	6	2	1	10	1	30	4.3	300	1.1	1000	333	25 ^c	surface-step-rich Cu	Sustainion	Sustainion +Nafion	Pt/Ti	pure water	1	30	15
2024	63	8	1	2	3	5	20	4.1	150	20.0	65	150	4.1	porous Cu	Nafion	PiperION +Nafion	IrO ₂	0.1 M KHCO ₃	1	1.2	16
2025	66	1	0	0	10	1	17	3.0	500	6.7	56	300	3.5	amorphous-rich Cu	Nafion	Sustainion	IrO ₂ /Ti	1 M KOH ⁿ	4	50	17

^awith carbon nanoparticle and graphite powder

^bwith tetrahydro-phenanthroline

^cCell voltage measured in the stacked-cell configuration.

^dNot calculated owing to the lack of electrode dimension data.

^equasi-graphitic C shell-protected Cu doping with N

^fN₂S functionalized Ag-Cu

^gquaternary ammonia poly(ether ether ketone)

^hPVDF+TiO₂-coated Nafion+PiperION

ⁱterphenyl-trifluoroheptan-2-one-1-methyl-benzimidazolium

^jCu dendrites with ultrastable Cu^{δ+} sites and hydrophobicity

^k0.02 M KHCO₃ was used for the stability test.

^lSwitching between 0.1 M KHCO₃ and dilute K⁺ solution

^melectrochemically depositing mesoporous Cu films on Cu foam

ⁿ1 M KHCO₃ was used for the stability test.

Note S1. Details of the experimental conditions for the data used in Table 1.¹³

Materials and Chemicals

CuONPs (copper(II) oxide, nanopowder, <50 nm particle size (TEM)) were purchased from Sigma-Aldrich. 5 wt% Nafion dispersion, 2-propanol, dimethyl sulfoxide (DMSO), potassium hydrogen carbonate (KHCO₃) and D₂O were purchased from Wako Pure Chemical. Carbon-based GDE (GDS2130, AvCarb) was purchased from the Fuel Cell Store. IrO₂/Ti mesh (porosity: 56%, wire diameter: 20 mm, thickness: 3 mm) was purchased from Tanaka Kikinzoku Kogyo. Anion-exchange membrane (Sustainion X37-50 Grade RT) was purchased from Dioxide Materials.

Fabrication of cathode electrode

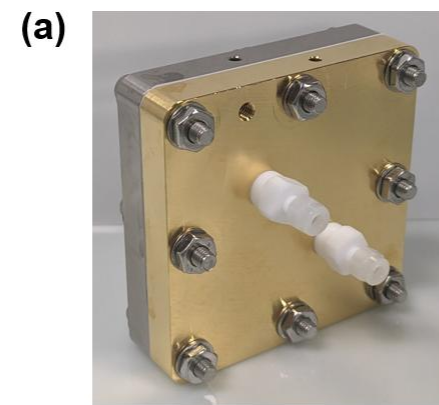
Cathode electrodes were fabricated by spray-coating a Cu catalyst ink onto a GDE. The catalyst ink was prepared by dispersing 100 mg of CuNPs in a mixture of 200 μ L 5 wt% Nafion ionomer solution and 6800 μ L 2-propanol. The catalyst ink mixtures were sonicated for 30 min and then sprayed onto a carbon-based GDE (electrode area: 6.25 cm²) at room temperature. The mass loading of Cu catalyst on the GDE was controlled at $\sim$ 0.2 mg cm⁻².

Electrochemical measurements

All electrochemical experiments were performed using an MEA-based electrolyzer (Figure S1). IrO₂/Ti mesh (electrode surface area: 6.25 cm²) was used as an anode. Sustainion AEM was used as a solid electrolyte for the electrolysis. In all of the experiments, humidified CO₂ was set at a flow rate of 80 mL min⁻¹ and was supplied to the cathode flow channel at room temperature using a mass flow controller (8500 MC, Kofloc, Japan). At the anode side, 90 mL of 0.1 M KHCO₃ was placed in a reservoir as an anode solution and was circulated in the anode flow channel at 10 mL min⁻¹ using a diaphragm pump. An electrochemical workstation (HZ-Pro, Hokuto Denko, Japan) was used to conduct all of the electrochemical experiments.

Analysis of CO₂RR products

Liquid products such as ethanol, propanol, acetic acid, and formic acid were collected in a liquid trap and an anode solution reservoir at the cathode and anode side, respectively. Vaporized liquid products in the cathode outlet gas were collected by bubbling into a liquid trap filled with deionized water. The liquid products transported from the cathode surface to the anode through solid electrolyte membrane were collected in an anode solution reservoir. The liquid products captured in the liquid trap and in the anode solution reservoir were analyzed using ¹H nuclear magnetic resonance (¹H NMR) spectroscopy (JNM ECS-400, 400 MHz, JEOL, Japan). ¹H NMR spectra of freshly acquired samples were collected using the water suppression mode reported elsewhere.¹⁸ A 500 mL sample of the electrolyte after electrolysis was mixed with 100 μ L of D₂O containing DMSO as an internal standard. The gas products downstream of the liquid trap were analyzed using a gas chromatograph (GC 2030, Shimadzu, Japan), which was equipped with both a thermal conductivity detector (TCD) and a flame ionization detector (FID). The gas chromatograph, in which He was used as the carrier gas, was equipped with a MICROPACKED ST column.



(b)

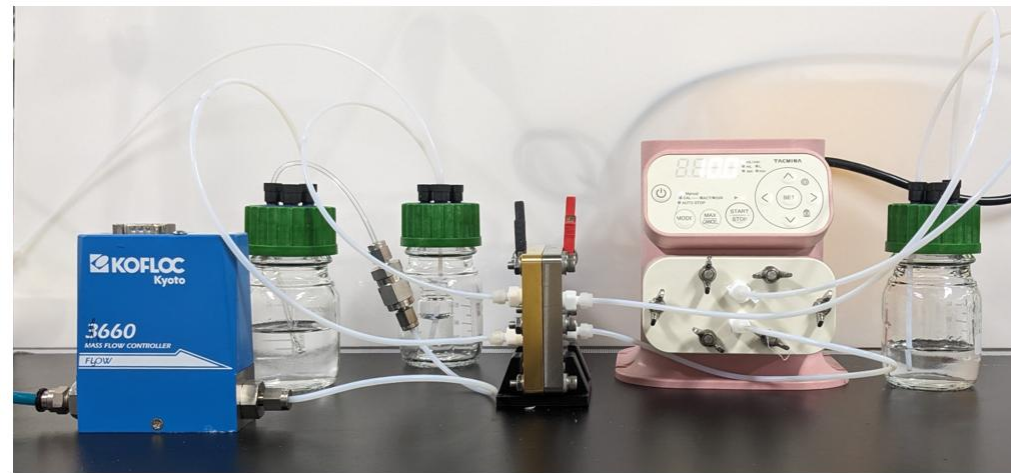


Fig. S1. Photographs of (a) MEA-based cell and (b) MEA system for CO₂RR used used for the data presented in Table 1.¹³

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