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Annex 1 Carbon dioxide rich side streams from sugar beet factories

This file calculates potential CO₂ streams that could be used for utilization. The SuperPro sugar factory example was taken as a starting point (Intelligen, 2024).

Get libraries

Include << .\Libraries\Mw.mcdx

Include << .\Libraries\Vm.mcdx

Include << .\Libraries\Units.mcdx

Include << .\Libraries\Molecular formulas.mcdx

The following data were taken from the SuperPro Sugar beet example.

$$\Phi_{mol} := 33.61 \cdot \frac{\text{ton}}{\text{hr}} \quad \text{mol} = \text{molasses}$$

$$f_{sucr_mol} := 43.96\%$$

$$f_{non_sucr_mol} := 28.18\%$$

$$\Phi_{pulp} := 26.18 \cdot \frac{\text{ton}}{\text{hr}} \quad \text{pulp} = \text{Sugar Beet Pulp} \quad \text{dry!}$$

$$\tau_{campaign} := 1920 \cdot \frac{\text{hr}}{\text{yr}} \quad \text{duration of campaign}$$

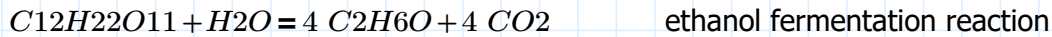
The number of Sugar beet Factories needed to process sugar from NL agriculture is calculated in Annex 6

$$N_{SBF} := 7.839$$

It is assumed that molasses is fermented to produce ethanol. The production of ethanol and CO₂ released from the ethanol fermentation is calculated from the sucrose content of molasses.

$$\eta_{eth_ferm} := 0.95 \quad \text{practical efficiency compared to theoretical efficiency}$$

$$\Phi_{sucr_mol} := f_{sucr_mol} \cdot \Phi_{mol} = 14.775 \frac{\text{ton}}{\text{hr}}$$



$$y_{eth_sucr_th} := 4 \cdot \frac{\text{mol}}{\text{mol}} \quad \text{theoretical ethanol yield}$$

$$Y_{eth_sucr} := y_{eth_sucr_th} \cdot \frac{Mw(\text{ethanol})}{Mw(\text{sucrose})} \cdot \eta_{eth_ferm} = 0.511 \frac{kg}{kg}$$

$$\Phi_{eth_mol} := Y_{eth_sucr} \cdot \Phi_{sucr_mol} = 7.556 \frac{ton}{hr}$$

$$y_{CO_2_sucr_th} := 4 \cdot \frac{\text{mol}}{\text{mol}} \quad \text{theoretical CO}_2 \text{ yield}$$

$$Y_{CO_2_sucr} := y_{CO_2_sucr_th} \cdot \frac{Mw(CO_2)}{Mw(\text{sucrose})} \cdot \eta_{eth_ferm} = 0.489 \frac{kg}{kg}$$

$$\Phi_{CO_2_mol} := Y_{CO_2_sucr} \cdot \Phi_{sucr_mol} = 7.219 \frac{ton}{hr}$$

Sugar beet pulp is assumed to be digested to produce biogas. The yield of methane and CO₂ is estimated from literature (Muzik et al., 2012).

$$Y_{CH_4_pulp_vol} := 330.9 \cdot \frac{\text{liter}}{kg} \quad \rho_{methane} := \frac{Mw(\text{methane})}{V_m(p_s, T_s)} = 0.716 \frac{kg}{m^3}$$

$$Y_{CH_4_pulp} := Y_{CH_4_pulp_vol} \cdot \rho_{methane}$$

$$Y_{CH_4_pulp} = 0.237 \frac{kg}{kg}$$

$$\Phi_{CH_4_pulp} := Y_{CH_4_pulp} \cdot \Phi_{pulp} = 6.201 \frac{ton}{hr}$$

The literature value can be checked assuming that the pulp contains only cellulose.



$$y_{CH_4_pulp_th} := 3 \cdot \frac{\text{mole}}{\text{mole}}$$

$$Y_{CH_4_pulp_th} := y_{CH_4_pulp_th} \cdot \frac{Mw(\text{methane})}{Mw(\text{pulp})}$$

$$Y_{CH_4_pulp_th} = 0.297 \frac{kg}{kg} \quad \text{Check OK! (Y}_{CH_4_pulp_th} \text{ should be larger than Y}_{CH_4_pulp} \text{)}$$

The methane content of biogas was taken from Hutnan et al. (2000)

$$f_{CH_4_biogas} := 0.60$$

$$f_{CO_2_biogas} := 1 - f_{CH_4_biogas} = 0.4$$

Carbon dioxide from pulp fermentation

$$Y_{CO_2_pulp} := \frac{Y_{CH_4_pulp}}{Mw(\text{methane})} \cdot \frac{f_{CO_2_biogas}}{f_{CH_4_biogas}} \cdot Mw(CO_2) = 0.433 \frac{kg}{kg}$$

$$\Phi_{CO_2_pulp} := Y_{CO_2_pulp} \cdot \Phi_{pulp} = 11.34 \frac{ton}{hr}$$

Total carbon dioxide production

$$\Phi_{CO_2} := \Phi_{CO_2_mol} + \Phi_{CO_2_pulp} = 18.558 \frac{ton}{hr} \quad \text{During campaign!}$$

Both molasses and pulp could be preserved (and fermented/digested) over longer periods. If the production of CO₂ is averaged over one year, the production rate is:

$$\tau_{campaign} = 80 \frac{day}{yr} \quad \text{Campaign is less than 3 months per year!}$$

Ethanol, methane and carbon dioxide from the Dutch sugar beet industry is calculated below (as reported in Table 3).

Ethanol fermentation

$$\Phi_{sucr_mol} \cdot \tau_{campaign} \cdot N_{SBF} = 222.376 \frac{kton}{yr}$$

$$\Phi_{eth_mol} \cdot \tau_{campaign} \cdot N_{SBF} = 113.731 \frac{kton}{yr} \quad \Phi_{CO_2_mol} \cdot \tau_{campaign} \cdot N_{SBF} = 108.645 \frac{kton}{yr}$$

Anaerobic digestion

$$\Phi_{pulp} \cdot \tau_{campaign} \cdot N_{SBF} = 394.032 \frac{kton}{yr}$$

$$\Phi_{CH_4_pulp} \cdot \tau_{campaign} \cdot N_{SBF} = 93.324 \frac{kton}{yr} \quad \Phi_{CO_2_pulp} \cdot \tau_{campaign} \cdot N_{SBF} = 170.671 \frac{kton}{yr}$$

Total

$$\Phi_{CO_2} \cdot \tau_{campaign} \cdot N_{SBF} = 279.316 \frac{kton}{yr}$$

Literature

Hutnan et al., 2000 [27]

Intelligen, 2024 [26]

Muzik et al., 2012 [28]