

## Supplementary Information

### Mixture Design of Experiments to Improve Fungal Degradation of Cosmetic Pigments

Erika Ribezzi,<sup>a</sup> Fabio Fornari,<sup>a†</sup> Nicolò Riboni,<sup>a,b\*</sup> Maria Vittoria Rizzo,<sup>b,c</sup> Monica Mattarozzi,<sup>a</sup> Maurizio Piergiovanni,<sup>a</sup> Alessandra Mori,<sup>d</sup> Paolo Goi,<sup>d</sup> Corrado Sciancalepore,<sup>b,c</sup> Daniel Milanese,<sup>b,c</sup> Giuseppe Vignali,<sup>b,c</sup> Federica Bianchi,<sup>a,b\*</sup> and Maria Careri,<sup>a</sup>

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<sup>a.</sup> University of Parma, Department of Chemistry, Life Sciences and Environmental Sustainability, Parco Area delle Scienze 17/A, Parma, 43124, Italy

<sup>b.</sup> University of Parma, CIPACK (Interdepartmental Center for the Packaging), Parco Area delle Scienze 181/A, Parma, 43124, Italy

<sup>c.</sup> University of Parma, Department of Systems Engineering and Industrial Technologies, Parco Area delle Scienze 181/A, Parma, 43124, Italy

<sup>d.</sup> Davines SpA, Via Calzolari Don Angelo 55a, Parma, 43126, Italia

<sup>†</sup>Present address: Customs and Monopolies Agency, Local Directorate of Lombardy, Via Marco Bruto 14, Milan, 20138, Italy

## EXPERIMENTAL SECTION

**Materials and Reagents.** Toluene-2,5-diamine sulfate (PTD), *p*-aminophenol (PAP), 2-methylresorcinol (2MR), and 4-amino-2-hydroxytoluene (PAOC), all > 99.9% purity, were kindly provided by Huwell Chemicals S.p.A. (Milan, Italy). Lactic acid ( $\geq 88\%$  purity) and *i*-propyl alcohol ( $\geq 99.9\%$  purity) were purchased from Carlo Erba Reagents (Milan, Italy).  $\text{MgSO}_4$  (98.4% purity), NaCl (99.9% purity), and sodium citrate ( $\geq 99.0\%$  purity) were obtained from VWR International (Milan, Italy). Glacial acetic acid ( $\geq 99.8\%$  purity), sodium acetate and acetonitrile (both  $\geq 99.0\%$  purity), and ammonium acetate ( $\geq 98\%$  purity) were from Sigma-Aldrich (Milan, Italy). Methyl alcohol (> 99.8% purity) and citric acid ( $\geq 99.5\%$  purity) were from Honeywell International Inc. (Morristown, USA). Milli-Q water was produced by means of a Millipore Milli-Q Element A10 water purification system (Merk-Millipore, Milan, Italy). Mycelium of species M9911 *Trametes versicolor* (mix with  $\pm 1\%$  spawn), M2191 *Pleurotus ostreatus* (mix with  $\pm 2\%$  spawn), and M9720 *Ganoderma lucidum* (mix with  $\pm 1\%$  spawn) were acquired from Mycelia (Deinze, Belgium). Cardboard and the ingredients for the formulation of hair dyes were all kindly provided by Davines S.p.A. (Parma, Italy). QuEChERS PSA/C18 +  $\text{MgSO}_4$  and PSA/C18/GCB +  $\text{MgSO}_4$  dSPE devices were obtained from Restek (Milan, Italy), whereas the Supel<sup>TM</sup> QuE Z-Sep/C18 dSPE devices were from Supelco (Bellefonte, USA).

**Optimization of fungal growth conditions.** For each trial, a total of 9.50 g of culture was prepared in porcelain capsules and 10 mL of an aqueous lactic acid solution was added. The acid concentration was adjusted proportionally to the amount of dye present within the culture. After homogenization, each culture was covered with perforated Parafilm® (Bemis Company Inc., Wisconsin, USA). The cultures were incubated under aerobic conditions at 28 °C, at 85% relative humidity, and in the dark, using a PID system incubator (Instruments s.r.l., Milan, Italy). Prior to culture preparation, all the tools were sterilized in a POLEAX EC 10 L autoclave (Quirumed, Valencia, Spain) at 121 °C for 18 min. Between the preparation of each culture, the work surface and tools were disinfected with a 70% v/v aqueous solution of isopropyl alcohol.

**Model regression.** A first-order model was postulated for  $t_G$  and  $S_f$ :

$$y = b_1X_1 + b_2X_2 + b_3X_3 + b_{12}X_1X_2 + b_{13}X_1X_3 + b_{23}X_2X_3 + b_{123}X_1X_2X_3 + e$$

Equation 1

where the terms denoted as  $b_i$  are the regression coefficients and  $e$  represents the residuals.

A coefficient was deemed statistically significant if its absolute value exceeded the semi-amplitude of its 95% confidence interval. Model performance was evaluated in terms of the fraction of explained variance ( $R^2$ ) and predictive capability using leave-one-out cross-validation ( $Q^2$ ). Model validity was assessed by carrying out a lack-of-fit  $F$ -test ( $\alpha = 0.01$ ).

Single desirability functions ( $d_i$ ) were calculated for  $t_G$  as shown in Equation 2, and for  $S_f$  and  $m_d$ , as shown in Equation 3.

$$d_i = \begin{cases} 0, & y_i > U_i \\ \frac{U_i - y_i}{U_i - L_i}, & \text{otherwise} \end{cases}$$

Equation 2

$$d_i = \begin{cases} 0, & y_i < L_i \\ \frac{y_i - L_i}{U_i - L_i}, & \text{otherwise} \end{cases}$$

Equation 3

The optimization boundaries were defined as follows:

- $t_G$ :  $L_i$  was defined as the upper limit of the 95% confidence interval of the minimum predicted response within the experimental domain, whereas  $U_i$  was set at 240 h.
- $S_f$ :  $L_i$  was set at 2, and  $U_i$  at 6.
- $m_d$ :  $L_i$  corresponded to the minimum amount of dye used in the culture formulation (*i.e.*, 0.95 g), whereas  $U_i$  corresponded to the maximum amount (*i.e.*, 4.75 g).

The optimal conditions were those corresponding to the maximum global desirability, calculated as the weighted geometric mean of the single desirability functions.<sup>1</sup> The weights assigned to  $t_G$ ,  $S_f$ , and  $m_d$  were 3, 1, and 2, respectively.

**QuEChERS extraction.** The performance of QuEChERS extraction was evaluated by varying the extraction salts mixtures and the sorbent for dSPE. The binary mixture PTD-2MR was selected as model combination. Three different extraction salt mixtures were tested: i) unbuffered (UB): 4 g of MgSO<sub>4</sub> and 1 g of NaCl;<sup>2</sup> ii) AOAC: 6 g of MgSO<sub>4</sub> and 1.5 g of sodium acetate;<sup>3</sup> iii) EN: 4 g of MgSO<sub>4</sub>, 1 g of NaCl, 1 g of sodium citrate and 0.32 g of citric acid<sup>4</sup>. Three different sorbents were tested: i) MgSO<sub>4</sub> + PSA/C18; ii) MgSO<sub>4</sub> + PSA/C18/GCB; iii) MgSO<sub>4</sub>, Z-Sep/C18.

The extracts were diluted 1:20 with Milli-Q water and submitted to UV-vis analysis using an Evolution 260 Bio spectrophotometer (Thermo Fisher Scientific, Massachusetts, USA) in the 210–800 nm range, operating in transmittance mode. The sample was placed into a quartz semi-micro cuvette (Hellma Analytics, Milan, Italy) with a light path of 10 mm. Both bandwidth and resolution were set to 1 nm, while the integration time was set to 250 ms. For each treatment, a blank culture was also submitted to extraction for background correction. The wavelength values for each dye, used as response variable, are reported in Table S3.

A two-way ANOVA was carried out to highlight differences in the average responses for each factor under investigation. Normality and homoscedasticity of data were tested using Shapiro-Wilk test and Hartley's test, respectively. For statistically significant results, effect size was estimated using Cohen's  $\eta^2$ <sup>5</sup> and post-hoc multiple pairwise comparisons were carried out by applying Student's t-tests with Bonferroni correction ( $\alpha = 0.05$ ).

**Degradation experiments.** Ten grams of each sample (8.05 g if mycelium was absent) were weighed, followed by the addition of 2.50 mL of cold Milli-Q water (4.62 mL if mycelium was absent). Subsequently, 10 ml of cold acetonitrile were added, and the sample was vigorously shaken for 1 min. Four g of MgSO<sub>4</sub> and 1 g of NaCl were added, and the tube was shaken again for 1 min. The tubes were stored at -20 °C for 1 h to facilitate the separation of fats and proteins. Finally, it was centrifuged at 5000 rpm for 5 min at 4 °C. One milliliter of supernatant was transferred to the PSA/C18 + MgSO<sub>4</sub> dSPE clean-up tube, agitated for 30 s and centrifuged at 5000 rpm for 5 min at 4 °C. The extract was diluted 1:20 with Milli-Q water and submitted to UHPLC-DAD analysis using a

Thermo Scientific UHPLC 3000 RS (Thermo Fisher Scientific, Monza, Italy), equipped with a quaternary pump (GPL-3400RS), a WPS-3000 TRS autosampler, a TCC-3000 RS temperature controller column compartment, and a DAD 3000 RS detector. Instrument control, data acquisition and processing were performed using Chromeleon software.

Reversed phase chromatographic separation was carried out using a pentafluorophenyl Nucleodur PFP (150 mm x 2.0 mm, 3.0  $\mu$ m) column equipped with the same pre-column (both by Marcherey-Nagel, Dueren, Germany) and maintained at 30 °C. The operating conditions were as follows: solvent (A), ammonium acetate (0.1 M, pH = 5.4); and solvent (B), methanol. The flow rate was 0.3 mL min<sup>-1</sup>, and the injection volume was 5  $\mu$ L. Chromatographic separation was carried out under gradient elution as follows: 5–70% B at 5–22 min, 70–5% B at 22–25 min (total runtime: 35 min). The detection wavelength was set at 230 nm.

**Method validation.** Detection ( $y_D$ ) and quantitation limits ( $y_Q$ ) expressed as signals were calculated by performing 10 replicate measurements of the blank matrix, as follows:  $y_D = \bar{x}_b + 3 s_0'$  and  $y_Q = \bar{x}_b + 10 s_0'$ , where  $\bar{x}_b$  and  $s_0'$  are the mean and corrected standard deviation ( $s_0' = s_0/\sqrt{n}$ ) calculated on the basis of the blank responses ( $s_0$ ) and the number of replicate observations ( $n$ ) averaged when reporting results. Finally, LODs and LOQs were obtained by projection of the corresponding  $y_D$  and  $y_Q$  through a calibration plot  $y = f(x)$  onto the concentration axis.

Linearity was evaluated for each analyte on  $k = 5$  concentration levels in the LOQ–2500 mg kg<sup>-1</sup> range (LOQ, 500, 1000, 2000, 2500 mg/kg,  $n = 3$  independent replicated measurements per level). Homoscedasticity was assessed using Bartlett's test. The goodness of fit and linearity were further verified through lack-of-fit and Mandel's tests. The significance of the intercept was evaluated by running a  $t$ -test ( $\alpha = 0.05$ ). Precision was assessed in terms of repeatability and intermediate precision. Relative standard deviations (RSD%) were evaluated at three concentration levels (LOQ, 160 mg/kg<sup>-1</sup> and 2500 mg/kg<sup>-1</sup> for each analyte) by performing  $n = 6$  replicated measurements *per* level. Intermediate precision was estimated over three days verifying homoscedasticity of data and performing the analysis of variance (ANOVA) at a 95% confidence level. Trueness was evaluated in

terms of recovery rate (RR%) by spiking the blank matrix at the same concentration levels used for precision testing. RR% were calculated as follows:  $RR\% = c_1/c_2 \cdot 100$  where  $c_1$  is the observed concentration and  $c_2$  is the concentration obtained by spiking the blank sample. Ten replicate measurements per level were performed. Selectivity was assessed by analyzing blank samples spiked with potentially interfering dyes to verify the absence of interfering compounds.

Matrix effect was evaluated as follows:

i) by comparing the response of the analytes in a standard solution was compared with that of a blank matrix extract spiked with the analytes at the same concentration

$$ME = (A-B)/A \times 100$$

where A is the response (peak area) of the analyte in the standard solution, and B is the response in the blank matrix extract spiked with the analyte at the same concentration.

ii) by comparing the slopes of calibration curves obtained from standard solutions and matrix-matched standard solutions were compared. A Student's *t*-test ( $\alpha = 0.05$ ) was performed to assess the presence of significant differences between the slopes.

**Life cycle assessment.** The Ecoinvent version 3.10 database contains up to 18000 reliable processes covering a wide range of industries, including agriculture and animal husbandry, building and construction, chemicals and plastics, energy, forestry and wood, metals, textiles, transportation, tourist accommodation, waste treatment and recycling, and water supply.<sup>6</sup> In particular, processes from the “Ecoinvent, cut-off by classification, system” database were used for the SimaPro modeling.

**Goal and Scope Definition.** Consumption in terms of materials, both constituting the substrate and for laboratory equipment, energy consumption for machinery operation, and transport steps for supply of primary materials constituting the substrate were included in the analysis. According to the reference ISO, the defined Functional Unit (F.U.) is the reference unit against which inventory flows are normalized. In the present case study, the selected F.U. consists of 100 g of substrate (substrate composition; 29% hair dye, 40% mycelium and 31% cardboard) incubated for 4 days, i.e., a material

composition and period considered optimal for degradation. The reference year chose for analysis is 2024.

**Life Cycle Inventory.** Once the scope, functional unit and system boundaries of the study are established, the inventory analysis is carried out according to the ISO references for LCA methodology. This step involves quantifying the input and output streams bounded by the system boundaries and normalized to the functional unit. The data related to laboratory operations are primary data from direct on-site measurements. All material consumption related to the equipment used were quantified: ceramic capsule and pestle, steel spatula and prop, plastic tray, parafilm cover, lactic acid in the inoculation phase, and distilled water in the sterilization phase. Regarding the electricity consumption, these were quantified based on the data sheets of the machines and their operating times. The operations considered are as follows: scales for weighing the materials, autoclave for sterilization of the equipment, inoculation of the substrate for 4 days, and finally oven drying of the final substrate. The information on the final substrate constituent materials, such as the cardboard layer and hair dye, were modeled using secondary data from the Ecoinvent 3.10 library. In addition, also the mycelium production process is based on secondary data and was modeled based on the study CIT from the literature.<sup>7,8</sup> Finally, concerning the transportation of the materials, the distance for transporting the substrate material (mycelium, cardboard, hair dye and lactic acid) from the production site to the laboratory were measured.<sup>9</sup> The transport medium selected from the Ecoinvent library is “Transport, freight, lorry 16-32 metric ton, EURO6 {RER}| market for transport, freight, lorry 16-32 metric ton, EURO6 | Cut-off, S”. On the other hand, auxiliary materials used during these transport phases were not considered, due to the lack of information and to the low level of contribution of these elements. Production of equipment, buildings, and other capital goods, staff business travel, and staff commuting to work were excluded from the analysis, in line with the reference ISO.<sup>10</sup> The detailed description of the input data used in the inventory phase is provided in Table S7.

**Life Cycle Impact Assessment.** The impact assessment method used in this study is Environmental Footprint (E.F.) 3.1.<sup>11</sup> This is the environmental impact assessment method recommended by the European Commission, consisting of 16 impact categories with a midpoint approach, each of which refers to a given independent characterization model.

**Software.** Multilinear regression and multicriteria optimization were carried out by using custom scripts in MATLAB environment (v. R2022a, Mathworks, Massachusetts, USA). The evaluation of effects and iso-response curves was performed using the CAT software,<sup>12</sup> in the R development environment (v.3.1.2, The R Foundation).

**Development and characterization of bio-composite materials:** The fungal substrate powder was mixed with PBAT granules in an analytical mill and heat-treated overnight at 40 °C, before being extruded using a twin-screw extruder (Zamak MercatorRES-2 P/12A Explorer twin-screw Extruder)). Filaments obtained during extrusion were cooled, pelletized by a Scheer SGS 25-E4 pelletizer before being introduced in the Babyplast 10/12 injection molding machine (Rambaldi+Co it srl, Italy) for the injection molding process to produce 5A type dumbbell specimens. According to the UNI EN ISO 527-2:2012<sup>13</sup>, a tensile test was performed on ten replicates of each PBAT/fungal substrate mixture, including pure PBAT. The uniaxial tensile tests were performed with a TesT dynamometer (Model 112, TesT GMBH Universal Testing Machine, Germany). The specimens are clamped at both ends using hydraulic jaws approximately at the broad parallel-sided portions. Pre-tensioning of 5 N at 5 mm/min was carried out to align the specimens. The test began with an elongation rate of 10 mm/min until breakage. The engineering stress-strain curve for the determination of mechanical properties is obtained reporting the stress  $\sigma$  [MPa], defined as the ratio between the applied force (F) and the initial cross section area ( $A_0$ ), as a function of the strain  $\epsilon$  [mm/mm], derived from the displacement  $\Delta l$  (mm) of the specimen over its starting length ( $l_0$ ).



**TABLES**

Table S1. Composition of the pseudo-components expressed as weight fraction (see Fig. S1 top-left)

Pseudo-component	Cardboard	Dye	Mycelium
$X_1$	0.10	0.10	0.80
$X_2$	0.10	0.50	0.40
$X_3$	0.50	0.10	0.40

Table S2. Experimental matrix. The composition of each experiment is reported as weight fraction in the pseudo-component domain as depicted in Fig. S1 (top-right)

Experiment	$X_1$	$X_2$	$X_3$
1	1.00	0.00	0.00
2	0.00	1.00	0.00
3	0.00	0.00	1.00
4	0.67	0.33	0.00
5	0.67	0.00	0.33
6	0.33	0.67	0.00
7	0.00	0.67	0.33
8	0.33	0.00	0.67
9	0.00	0.33	0.67
10	0.67	0.17	0.17
11	0.17	0.67	0.17
12	0.17	0.17	0.67
13	0.33	0.33	0.33
14	0.33	0.33	0.33
15	0.33	0.33	0.33

Table S3. Wavelengths used for the detection of the investigated pigment

Dye	Compound	Wavelength (nm)
Primary dyes	PTD	256
	PAP	230
Couplers	2MR	279
	PAOC	230

Table S4. Single desirability values and global desirability

Response	Species	$d_i$
$t_G$	$TV$	1.00
	$PO$	0.96
	$GL$	1.00
$S_f$	$TV$	0.55
	$PO$	0.87
	$GL$	0.42
$m_d$		0.47
$D$		0.79

Table S5. LOD, LOQ, linearity range and calibration curves of precursors and couplers

<b>Pigment</b>	<b>LOD (mg kg<sup>-1</sup>)</b>	<b>LOQ (mg kg<sup>-1</sup>)</b>	<b>Linearity range</b>	<b>b<sub>1</sub> (± s<sub>e</sub>)</b>
<b>PAP</b>	2.3	7.5	LOQ-2500	$y = 0.0159 (\pm 0.0003) x$
<b>PTD</b>	4.8	16		$y = 0.0099 (\pm 0.0002) x$
<b>2MR</b>	5.6	19		$y = 0.0112 (\pm 0.0002) x$
<b>PAOC</b>	2.2	7.5		$y = 0.0256 (\pm 0.0003) x$

Table S6. Impact of each component in the substrate production process

Impact categories	Hair dye	Mycelium	Cardboard	Lactic acid	Plastic tray for mycelium	Steel spatula	Ceramic capsules	Ceramic pestle
AC [mol H <sup>+</sup> eq]	1,17E-03	2,40E-04	1,07E-04	2,22E-03	5,61E-07	1,08E-05	2,14E-05	7,24E-06
GWP [kg CO <sub>2</sub> eq]	2,53E-01	2,35E-02	2,32E-02	5,98E-01	1,48E-04	2,57E-03	6,77E-03	2,29E-03
ECF [CTUe]	7,70E+00	4,24E-01	2,22E-01	4,47E+00	6,04E-05	8,58E-02	1,90E-02	6,42E-03
PM [disease inc.]	1,16E-08	1,78E-09	1,18E-09	2,01E-08	6,27E-12	2,33E-10	7,37E-09	2,49E-09
EUm [kg N eq]	1,46E-03	5,34E-04	4,91E-05	5,73E-04	9,23E-08	2,43E-06	4,78E-06	1,62E-06
EUf [kg P eq]	5,01E-05	7,39E-06	1,35E-05	1,27E-04	1,63E-09	1,05E-06	1,37E-06	4,64E-07
EUt [mol N eq]	1,76E-03	9,08E-04	3,85E-04	4,46E-03	9,95E-07	2,50E-05	5,21E-05	1,76E-05
HTc [CTUh]	2,48E-09	1,09E-10	9,44E-11	1,66E-09	3,40E-14	2,61E-10	1,68E-11	5,66E-12
HTnc [CTUh]	1,88E-09	2,07E-09	3,72E-10	4,62E-09	1,58E-13	4,85E-11	4,65E-11	1,57E-11
IR [kBq U-235 eq]	1,06E-02	9,63E-04	2,23E-03	4,19E-02	7,20E-08	7,54E-05	3,70E-04	1,25E-04
LU [Pt]	5,12E-01	2,42E+00	1,56E+00	1,22E+00	3,75E-05	8,50E-03	2,81E-02	9,48E-03
OD [kg CFC11 eq]	2,23E-08	6,22E-10	5,62E-10	1,74E-08	8,62E-14	1,23E-11	1,17E-10	3,95E-11
POF [kg NMVOC eq]	8,78E-04	9,85E-05	1,08E-04	2,83E-03	4,10E-07	8,37E-06	1,95E-05	6,60E-06
RUf [MJ]	4,06E+00	2,37E-01	3,16E-01	1,07E+01	3,33E-03	2,62E-02	9,59E-02	3,24E-02
RUm [kg Sb eq]	1,28E-06	1,93E-07	8,55E-08	4,58E-06	2,67E-11	1,73E-08	3,32E-08	1,12E-08
WU [m <sup>3</sup> depriv.]	6,45E-02	2,92E-01	1,03E-02	2,12E-01	8,91E-05	4,85E-04	1,13E-03	3,83E-04

Table S6. Impact of each component in the substrate production process (continue)

Impact categories	Deionised water	Parafilm	Glass jar	Tin cap	Steel prop	Plastic tray for incubation	Sterilizer	Hair dye transport	Mycelium transport
AC [mol H <sup>+</sup> eq]	9,46E-07	1,21E-05	2,57E-06	1,97E-06	7,71E-06	4,02E-06	5,39E-07	1,43E-07	1,76E-05
GWP [kg CO <sub>2</sub> eq]	8,91E-05	2,66E-03	3,18E-04	1,61E-04	1,84E-03	1,06E-03	5,08E-05	6,88E-05	8,46E-03
ECF [CTUe]	1,12E-02	1,63E-02	1,74E-03	4,67E-03	6,15E-02	4,32E-04	6,39E-03	2,63E-04	3,24E-02
PM [disease inc.]	7,48E-12	1,33E-10	3,64E-11	2,26E-11	1,67E-10	4,49E-11	4,26E-12	5,07E-12	6,23E-10
EUm [kg N eq]	7,38E-08	2,37E-06	4,17E-07	4,56E-07	1,74E-06	6,61E-07	4,21E-08	3,44E-08	4,23E-06
EUf [kg P eq]	3,42E-08	5,86E-07	4,69E-08	3,76E-07	7,52E-07	1,17E-08	1,95E-08	4,66E-09	5,73E-07
EUt [mol N eq]	7,37E-07	2,49E-05	4,75E-06	6,13E-06	1,79E-05	7,12E-06	4,20E-07	3,71E-07	4,57E-05
HTc [CTUh]	6,52E-13	7,95E-12	7,95E-13	4,11E-13	1,87E-10	2,44E-13	3,72E-13	4,88E-13	6,00E-11
HTnc [CTUh]	1,30E-12	2,09E-11	3,28E-12	6,22E-12	3,47E-11	1,13E-12	7,41E-13	6,08E-13	7,47E-11
IR [kBq U-235 eq]	1,09E-05	1,21E-04	1,29E-05	1,43E-05	5,40E-05	5,16E-07	6,23E-06	1,26E-06	1,54E-04
LU [Pt]	3,84E-04	7,93E-03	2,95E-03	1,37E-03	6,09E-03	2,69E-04	2,19E-04	5,85E-04	7,19E-02
OD [kg CFC11 eq]	3,35E-11	6,38E-11	5,11E-12	1,43E-12	8,82E-12	6,18E-13	1,91E-11	1,37E-12	1,68E-10
POF [kg NMVOC eq]	2,90E-07	1,41E-05	1,52E-06	1,41E-06	5,99E-06	2,94E-06	1,65E-07	2,38E-07	2,93E-05
RUf [MJ]	1,16E-03	8,94E-02	4,07E-03	2,04E-03	1,88E-02	2,38E-02	6,59E-04	9,68E-04	1,19E-01
RUm [kg Sb eq]	1,19E-09	2,00E-08	1,60E-09	4,12E-07	1,24E-08	1,91E-10	6,80E-10	2,24E-10	2,75E-08
WU [m <sup>3</sup> depriv.]	9,73E-03	1,14E-03	5,37E-05	9,05E-05	3,47E-04	6,38E-04	5,55E-03	4,02E-06	4,94E-04

Table S6. Impact of each component in the substrate production process (continue)

Impact categories	Incubation energy consumption	Heater energy consumption	Autoclave energy consumption	Lactic acid transport	Cardboard transport	Scale energy consumption	Total
AC [mol H <sup>+</sup> eq]	1,10E-02	1,60E-03	3,74E-06	7,50E-07	1,55E-07	5,88E-05	1,65E-02
GWP [kg CO <sub>2</sub> eq]	2,62E+00	3,82E-01	8,91E-04	3,60E-04	7,46E-05	1,40E-02	3,94E+00
ECF [CTUe]	8,13E+00	1,19E+00	2,77E-03	1,38E-03	2,86E-04	4,35E-02	2,24E+01
PM [disease inc.]	5,41E-08	7,91E-09	1,85E-11	2,65E-11	5,49E-12	2,90E-10	1,08E-07
EUm [kg N eq]	1,64E-03	2,39E-04	5,58E-07	1,80E-07	3,73E-08	8,78E-06	4,52E-03
EUf [kg P eq]	5,81E-04	8,50E-05	1,98E-07	2,44E-08	5,05E-09	3,11E-06	8,73E-04
EUt [mol N eq]	1,79E-02	2,61E-03	6,09E-06	1,95E-06	4,03E-07	9,57E-05	2,83E-02
HTc [CTUh]	6,73E-09	9,83E-10	2,29E-12	2,56E-12	5,29E-13	3,60E-11	1,26E-08
HTnc [CTUh]	3,25E-08	4,74E-09	1,11E-11	3,18E-12	6,59E-13	1,74E-10	4,66E-08
IR [kBq U-235 eq]	3,11E-01	4,54E-02	1,06E-04	6,57E-06	1,36E-06	1,66E-03	4,15E-01
LU [Pt]	1,53E+01	2,23E+00	5,20E-03	3,06E-03	6,34E-04	8,18E-02	2,34E+01
OD [kg CFC11 eq]	6,01E-08	8,78E-09	2,05E-11	7,17E-12	1,48E-12	3,22E-10	1,11E-07
POF [kg NMVOC eq]	7,65E-03	1,12E-03	2,61E-06	1,25E-06	2,58E-07	4,10E-05	1,28E-02
RUf [MJ]	4,18E+01	6,11E+00	1,43E-02	5,07E-03	1,05E-03	2,24E-01	6,39E+01
RUm [kg Sb eq]	3,26E-05	4,77E-06	1,11E-08	1,17E-09	2,43E-10	1,75E-07	4,42E-05
WU [m <sup>3</sup> depriv.]	1,89E+00	2,76E-01	6,44E-04	2,10E-05	4,36E-06	1,01E-02	2,78E+00



Table S7. LCI INPUT inventory data referred to 1 kg of substrate

	<b>Inventory</b>	<b>Unit</b>	<b>Value</b>	<b>Data source process</b>	<b>Data source</b>
Materials	Hair dye	kg	0.2873	Ecoinvent 3.10	On site measurement
	Mycelium	kg	0.401	Ecoinvent 3.10	On site measurement
	Cardboard	kg	0.3115	Ecoinvent 3.10	On site measurement
	Lactic acid	kg	1.272	Ecoinvent 3.10	On site measurement
	Plastic tray for mycelius	kg	0.00039	Ecoinvent 3.10	On site measurement
	Steel spatula	kg	0.0121	Ecoinvent 3.10	On site measurement
	Ceramic capsules	kg	0.0343	Ecoinvent 3.10	On site measurement
	Ceramic pestle	kg	0.0115	Ecoinvent 3.10	On site measurement
	Deionised water	kg	2.187	Ecoinvent 3.10	On site measurement
	Parafilm	kg	0.0132	Ecoinvent 3.10	On site measurement
	Glass jar	kg	0.0029	Ecoinvent 3.10	On site measurement
	Tin cap	kg	0.00015	Ecoinvent 3.10	On site measurement
	Steel prop	kg	0.0086	Ecoinvent 3.10	On site measurement
	Plastic tray for incubation	kg	0.0028	Ecoinvent 3.10	On site measurement
	Sterilizer	kg	1.246	Ecoinvent 3.10	On site measurement
Processes	Hair dye transport	km	12.3	Ecoinvent 3.10	Calculated
	Mycelium transport	km	1110	Ecoinvent 3.10	Calculated
	Cardboard transport	km	12.3	Ecoinvent 3.10	Calculated
	Lactic acid transport	km	149	Ecoinvent 3.10	Calculated
	Incubation energy consumption	kWh	73.68	Ecoinvent 3.10	Calculated
	Heater energy consumption	kWh	10.77	Ecoinvent 3.10	Calculated
	Autoclave energy consumption	kWh	0.0251	Ecoinvent 3.10	Calculated
	Scale energy consumption	kWh	0.000375	Ecoinvent 3.10	Calculated

Table S8. Sensitivity analysis on energy sources, Scenario 1 and Scenario 2 comparison

<b>Impact categories</b>	<b>S1 Laboratory energy consumption</b>	<b>S2 Laboratory energy consumption</b>	<b>Reduction/Increase</b>
AC [mol H+ eq]	1,26E-02	4,92E-03	61%
GWP [kg CO2 eq]	3,01E+00	6,39E-01	79%
ECF [CTUe]	9,36E+00	7,66E+00	18%
PM [disease inc.]	6,24E-08	4,47E-08	28%
EUm [kg N eq]	1,89E-03	7,31E-04	61%
EUf [kg P eq]	6,70E-04	3,92E-04	41%
EUt [mol N eq]	2,06E-02	7,71E-03	63%
HTc [CTUh]	7,75E-09	5,60E-09	28%
HTnc [CTUh]	3,74E-08	3,09E-08	17%
IR [kBq U-235 eq]	3,58E-01	5,22E-02	85%
LU [Pt]	1,76E+01	2,77E+00	84%
OD [kg CFC11 eq]	6,92E-08	4,33E-08	37%
POF [kg NMVOC eq]	8,82E-03	2,82E-03	68%
RUf [MJ]	4,82E+01	7,92E+00	84%
RUm [kg Sb eq]	3,76E-05	4,41E-05	-15%
WU [m3 depriv.]	2,18E+00	6,17E-01	72%

## FIGURES

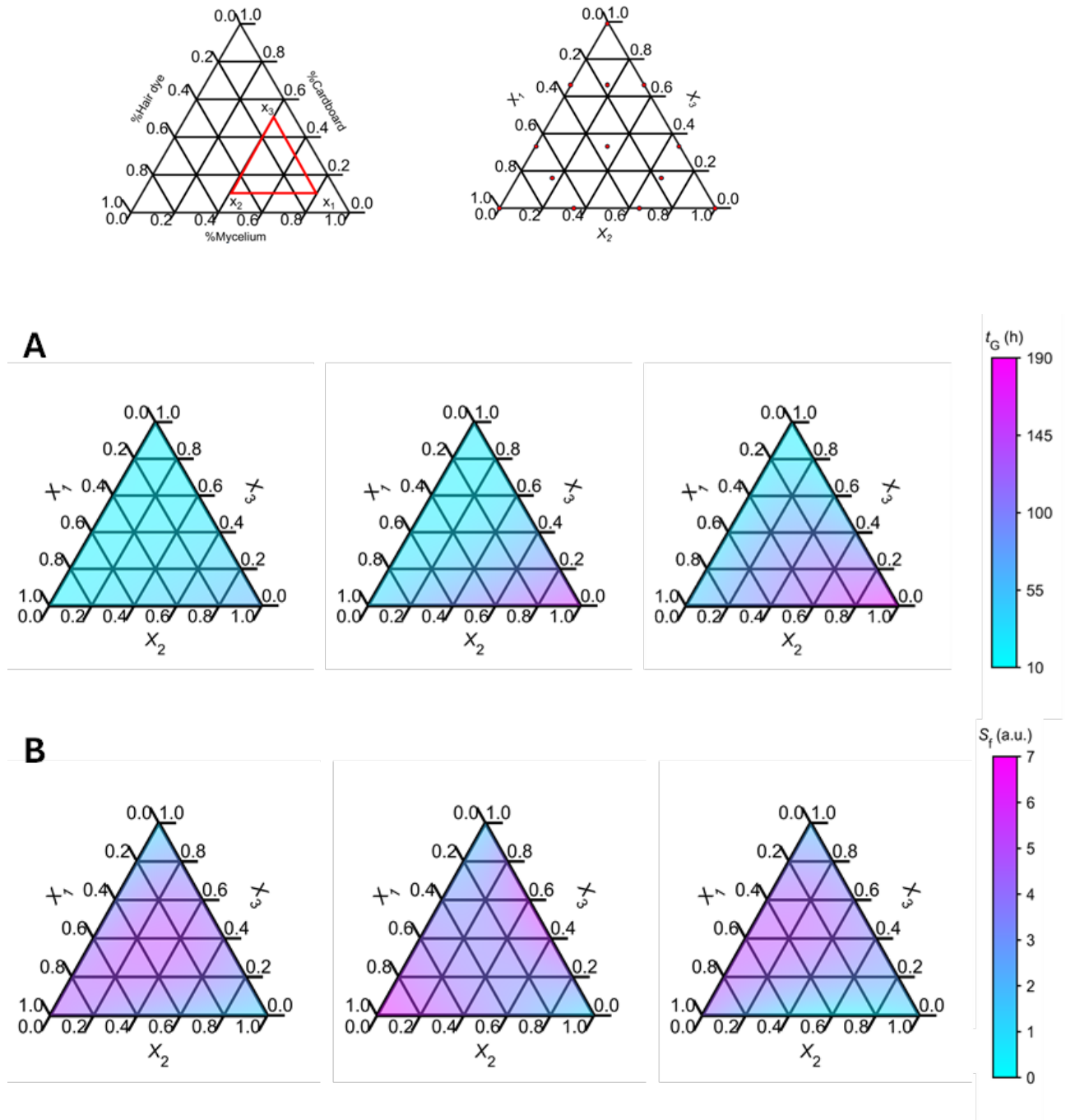


Fig. S1. The red triangle illustrates the pseudo-component domain used in this study (top-left) and the utilized experimental points are depicted in red (top-right). Ternary contour plots for: A) germination time and B) shape factor. TV is reported on the left, PO in the middle, and GL on the right. For each response variable, all the plots were rescaled to use the same color bar for comparison purposes

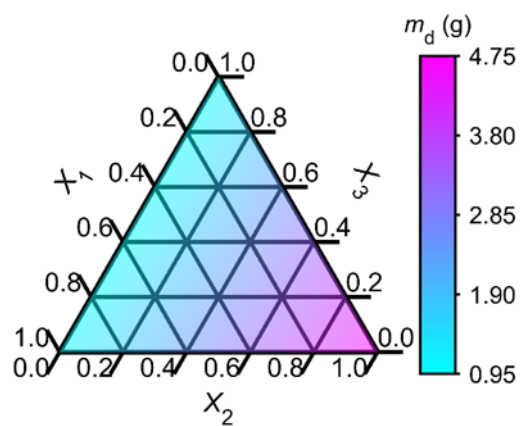


Fig. S2. Ternary contour plots for the amount of hair dye in the pseudo-component domain.

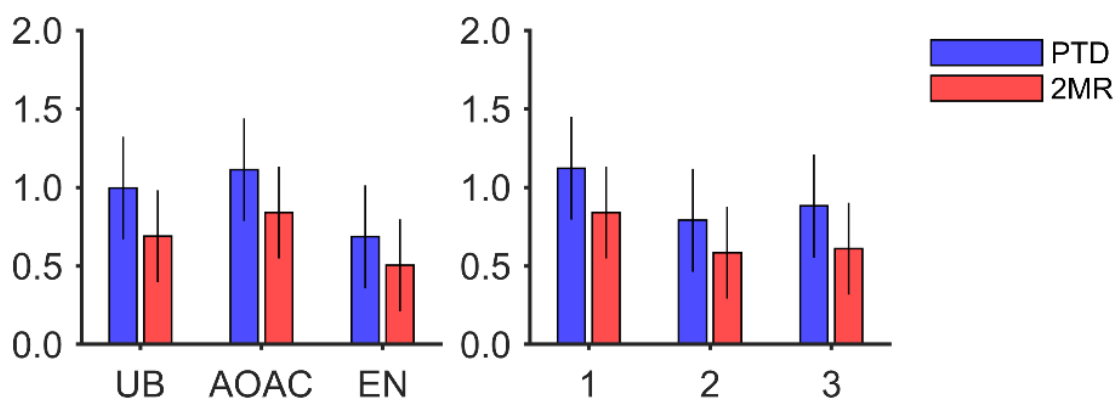


Fig. S3. Two-ways ANOVA after background correction. Left: effect of the buffer (UB: unbuffered; AOAC: acetic buffer; EN: citrate buffer). Right: effect of the dSPE clean-up (1: PSA/C18 + MgSO<sub>4</sub>; 2: Z-Sep/C18; 3: PSA/C18/GCB + MgSO<sub>4</sub>). The results are reported as means with respect to each treatment for the investigated combinations of dyes: PTD + 2MR. Absorbance values were recorded at the wavelengths reported in Table S3. The error bars show the amplitude of the 95% confidence interval estimated with respect to the residual variance.

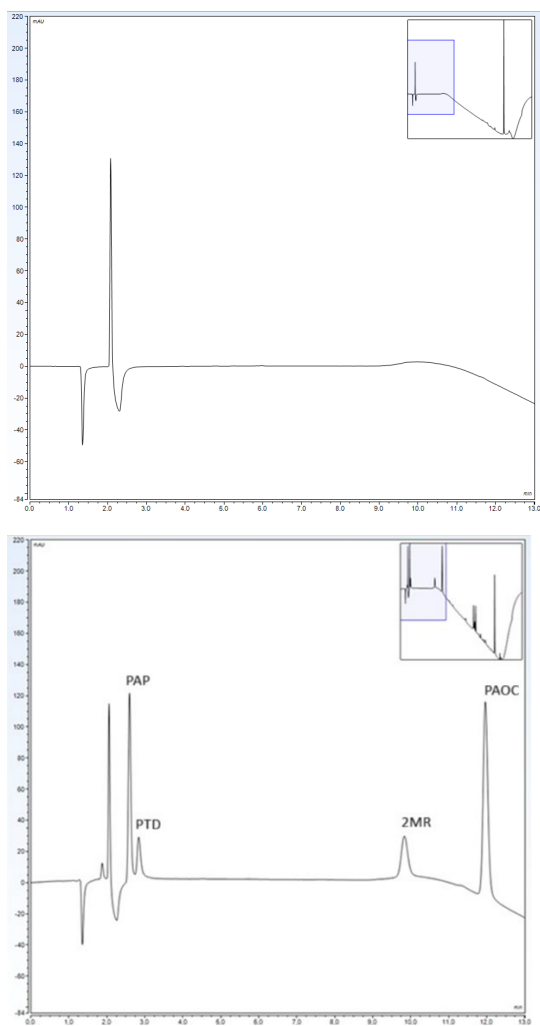


Fig. S4. QuEChERS-UHPLC-DAD chromatograms of: blank matrix (top) and blank matrix spiked with the binary mixtures PTD-2MR and PAP-PAOC at 2500 mg kg<sup>-1</sup> (bottom)

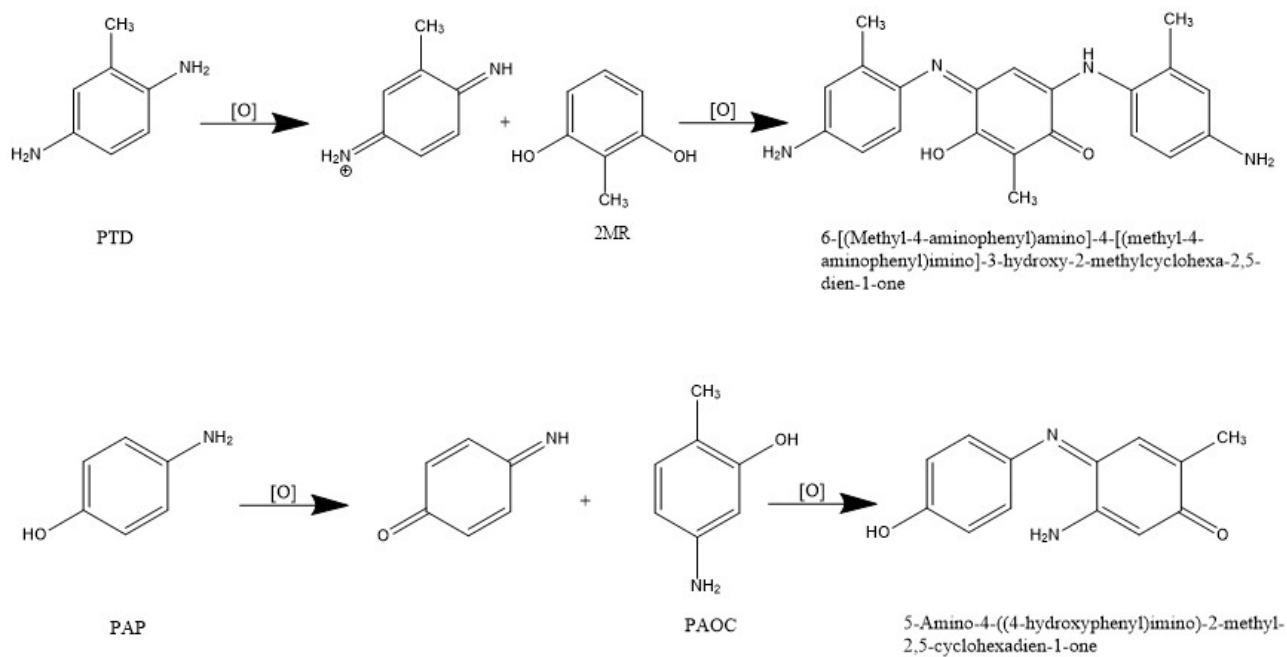


Fig. S5. Reaction scheme related to the formation of the coupling products of the binary mixtures PTD-2MR (top) and PAP-PAOC (bottom) <sup>14</sup>

## Environmental impacts of the single activities for mycelium substrate production

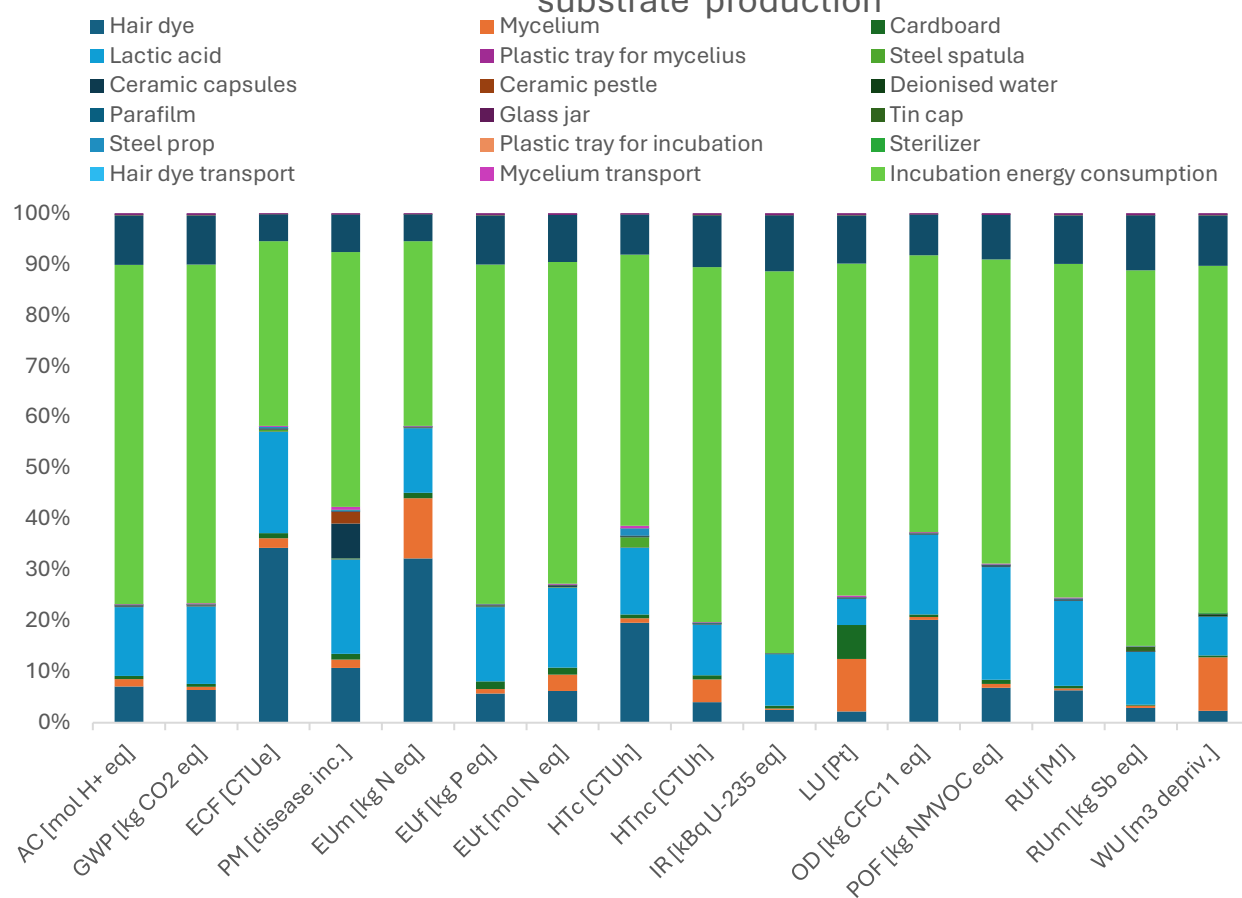


Fig. S6. Environmental impact of each activity for mycelium substrate production.



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