

## Electrochemical CO<sub>2</sub> Reduction to Alcohols Using Flexible and Rigid MOF Electrocatalysts

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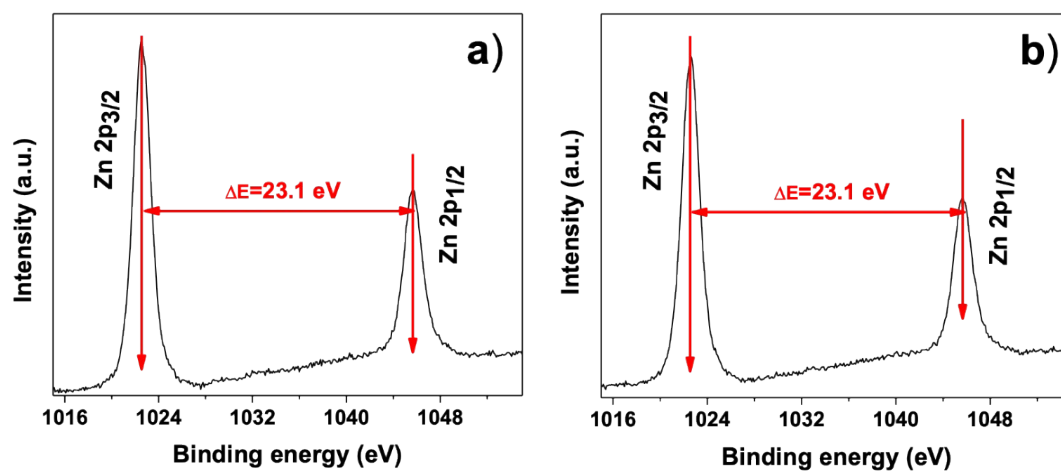
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## 1. XPS



**Fig. S1.** Core XPS spectra of Zn 2p. (a) H<sub>4</sub>DOBDC MOF and b) Oxalic acid MOF.

## 2. Calculation of specific capacitance and ECSA

For a given capacitor, it is found that the amount of charge  $Q$  acquired by each plate is proportional to the magnitude of the potential difference  $V$  between them:

$$Q = CV \quad (1-1)$$

The constant of proportionality,  $C$ , in the above equation is called the capacitance of the capacitor. The following equation can determine the capacitance of a given capacitor:

$$C = \frac{Q}{V} \quad (1-2)$$

By dividing by the mass of active material in grams,  $m$ , we obtain the specific capacitance,  $C_s$ , given by,

$$C_s = \frac{Q}{mV} \quad (1-3)$$

The average current,  $I$ , is defined as,

$$I = \frac{Q}{t} \quad (1-4)$$

Or,

$$Q = I * t \quad (1-5)$$

Replacing equation (1-5) in equation (1-3) we get,

$$C_s = \frac{I * t}{mV} \quad (1-6)$$

Dividing the numerator and denominator by  $t$ ,

$$C_s = \frac{I}{m\left(\frac{V}{t}\right)} \quad (1-7)$$

In equation (1-7),  $(V/t)$  represents cyclic voltammetry scan rate, which will be abbreviated as a constant,  $k$ .

$$C_s = \frac{I}{mk} \quad (1-8)$$

Or,

$$I = C_s * m * k \quad (1-9)$$

Considering the cyclic voltammetry experiments, the current in the range potential from  $V_a$  to  $V_b$ . Therefore, equation (1-9) can be written in its integral form as,

$$\int_{V_a}^{V_b} I(V) dV = \int_{V_a}^{V_b} (C_s * m * k) dV \quad (1-10)$$

Or,

$$Area = \int_{V_a}^{V_b} (C_s * m * k) dV \quad (1-11)$$

The values of  $C_s$ ,  $m$ , and  $k$  are constant for a specific material. Therefore, the integral of equation (1-11) can be solved as,

$$Area = (V_b - V_a) * C_s * m * k \quad (1-12)$$

When the capacitor is charging, then  $Area=A_1$  and equation (1-12) can be written as,

$$A_1 = (V_b - V_a) * C_s * m * k \quad (1-13)$$

Similarly, when the capacitor is discharging, then  $Area=A_2$  and equation (1-12) can be written as,

$$A_2 = (V_a - V_b) * C_s * m * k \quad (1-14)$$

For the calculation of the Area inside the cyclic voltammetry curve, equation (1-14) must be subtracted from equation (1-13),

$$\begin{aligned} Area &= A_1 - A_2 = [(V_b - V_a) * C_s * m * k] - [(V_a - V_b) * C_s * m * k] \\ Area &= A_1 - A_2 = [(V_b - V_a) * C_s * m * k] + [(V_b - V_a) * C_s * m * k] \\ Area &= A_1 - A_2 = 2[(V_b - V_a) * C_s * m * k] \quad (1-15) \end{aligned}$$

Solving the equation (1-15) ultimately involves isolating  $C_s$  to determine its equation.

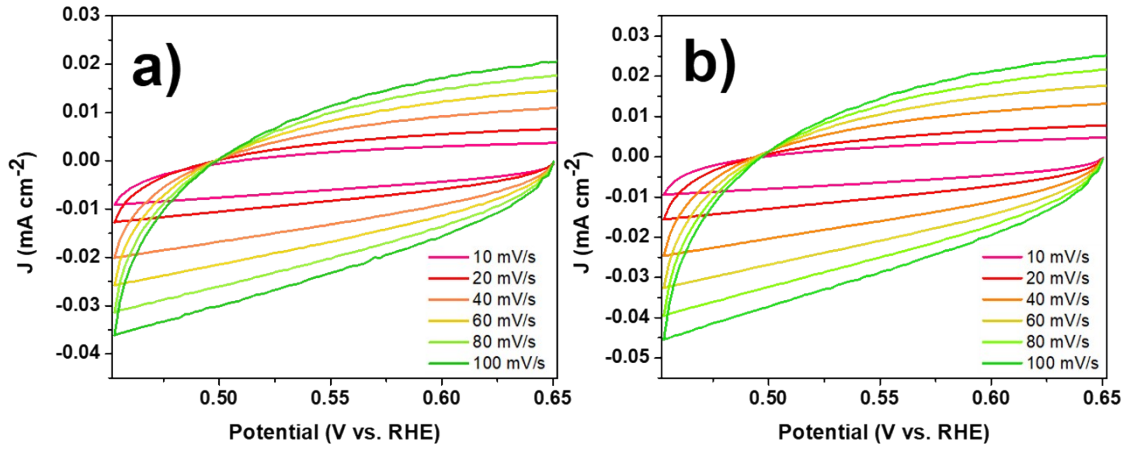
$$C_s = \frac{Area}{2(V_b - V_a) * m * k} \quad (1-16)$$

Where  $C_s$  is the specific capacitance in F/g, Area has units in  $A^*V$ ,  $m$  is the mass of active materials,  $k$  is the scan rate in volts per second, and  $V_b - V_a$  is the potential window of cyclic voltammetry.

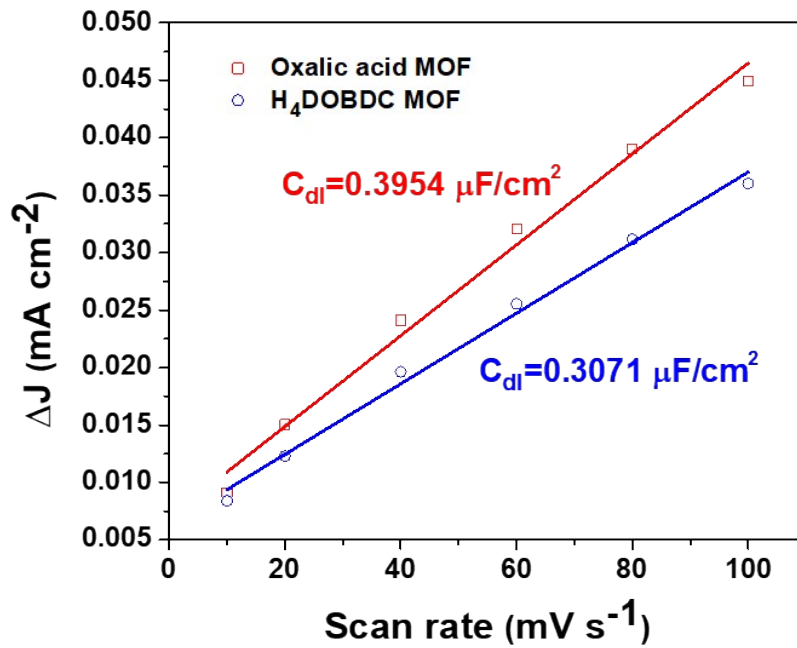
The respective  $C_s$  and the corresponding ECSA calculation for  $H_4DOBDC$  MOF and oxalic acid MOF are shown below, respectively. Given  $m=10$  mg (0.01 g) and  $k=10$  mV $\times$ s $^{-1}$  (0.01 V $\times$ s $^{-1}$ ),

$$C_s = \frac{1.3295 A * V}{2 * (0.1973 V) * 0.01 g * 0.01 V \times s^{-1}} = 33,700.01 \frac{A \times s}{V \times g} = 33,700.01 \frac{F}{g}$$

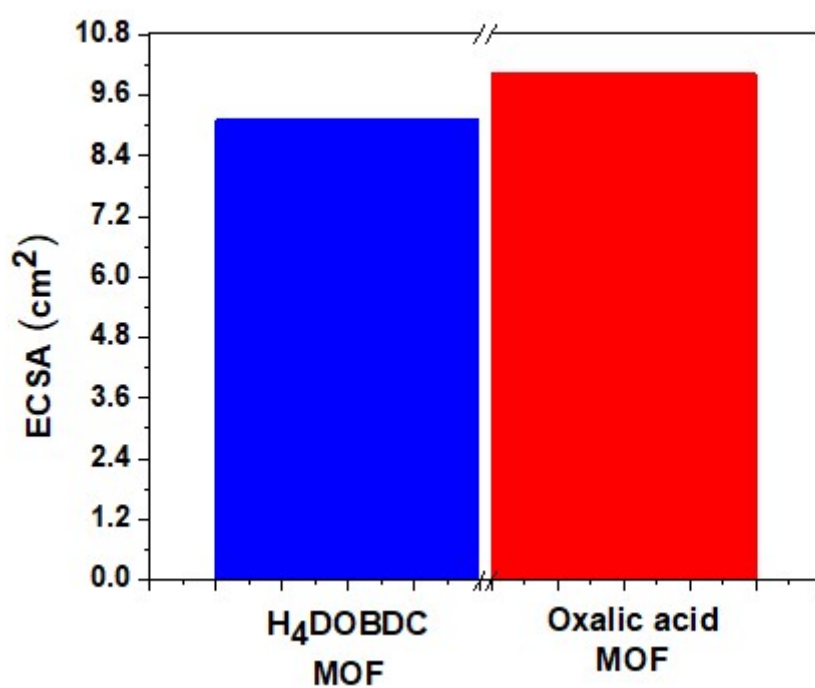
$$C_s = \frac{1.5365 \text{ A} \cdot \text{V}}{2 * (0.1949 \text{ V}) * 0.01 \text{ g} * 0.01 \text{ V} \times \text{s}^{-1}} = 39,419.03 \frac{\text{A} \times \text{s}}{\text{V} \times \text{g}} = 39,419.03 \frac{\text{F}}{\text{g}}$$



**Fig. S2.** Cyclic voltammograms (CVs) of a)  $\text{H}_4\text{DOBDC}$  MOF and b) Oxalic acid MOF in  $\text{CO}_2$ -saturated 0.1 M KOH electrolyte at various scan rates.

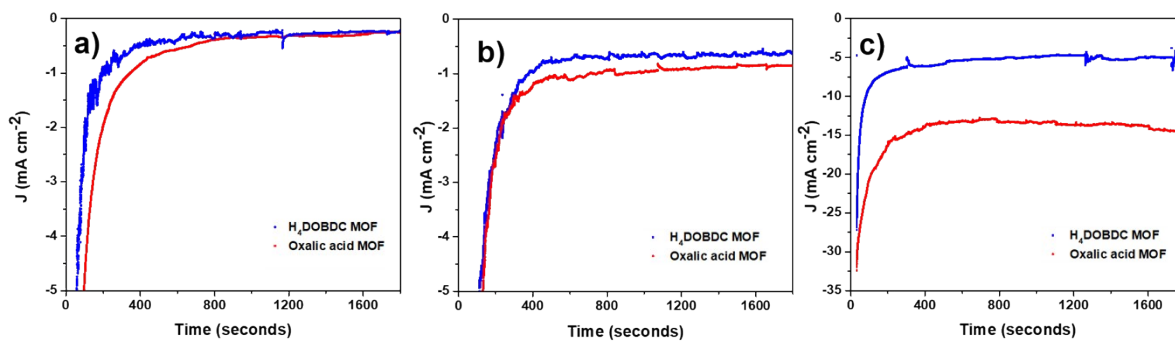


**Fig. S3.** Average current density against the scan rate showing the double-layer capacitance ( $C_{dl}$ ) extracted from the corresponding CVs presented in Fig. S2.



**Fig. S4.** The estimated electrochemical surface area for H<sub>4</sub>DOBDC MOF and Oxalic acid MOF.

### 3. Chronoamperometry



**Fig. S5.** Chronoamperometry curves recorded in  $\text{CO}_2$ -saturated  $0.1 \text{ M KOH}$  electrolyte for the MOFs at: a)  $-0.19 \text{ V vs RHE}$ , b)  $-0.59 \text{ V vs RHE}$ , and c)  $-1.01 \text{ V vs RHE}$ .

**Table S1.** Comparison of the faradic efficiency (FE) of the present work, oxalic acid MOF, and other materials in the literature.

| Electrocatalysts<br>Metals/Metal<br>Oxides | Reaction<br>product | Electrolyte                                          | Faradic<br>efficiency | Potential<br>(V vs.<br>RHE) | Ref.      |
|--------------------------------------------|---------------------|------------------------------------------------------|-----------------------|-----------------------------|-----------|
| Cu <sub>4</sub> Zn                         | EtOH                | 0.1 M<br>KHCO <sub>3</sub>                           | 30%                   | −1.05                       | [1]       |
| ZnO-CuO                                    | EtOH                | 0.1 M<br>KHCO <sub>3</sub>                           | 32%                   | −1.15                       | [2]       |
| Cu-ZnO                                     | iPrOH               | 0.1 M<br>KHCO <sub>3</sub>                           | 33.65%                | −0.99                       | [3]       |
| CuAg alloy                                 | iPrOH               | CO <sub>2</sub> -<br>saturated<br>CsHCO <sub>3</sub> | 39.6%                 | −0.73                       | [4]       |
| MOFs                                       | Reaction<br>product | Electrolyte                                          | Faradic<br>efficiency | Potential<br>(V vs.<br>RHE) | Ref.      |
| Carbonized<br>HKUST-1 (OD<br>Cu/C-1000)    | EtOH                | 0.1 M<br>KHCO <sub>3</sub>                           | 34.8%                 | −0.5                        | [5]       |
| Cu-based MOF                               | EtOH                | 0.5 M<br>KHCO <sub>3</sub>                           | 82.5%                 | −1.0                        | [6]       |
| CuSn-based<br>MOF (CuSn-<br>HAB)           | EtOH                | 1 M KOH                                              | 56%                   | −0.57                       | [7]       |
| Oxalic acid MOF                            | EtOH                | 0.1 M KOH                                            | 15.02%                | −0.19                       | This work |
| Oxalic acid MOF                            | iPrOH               | 0.1 M KOH                                            | 29.09%                | −0.19                       | This work |



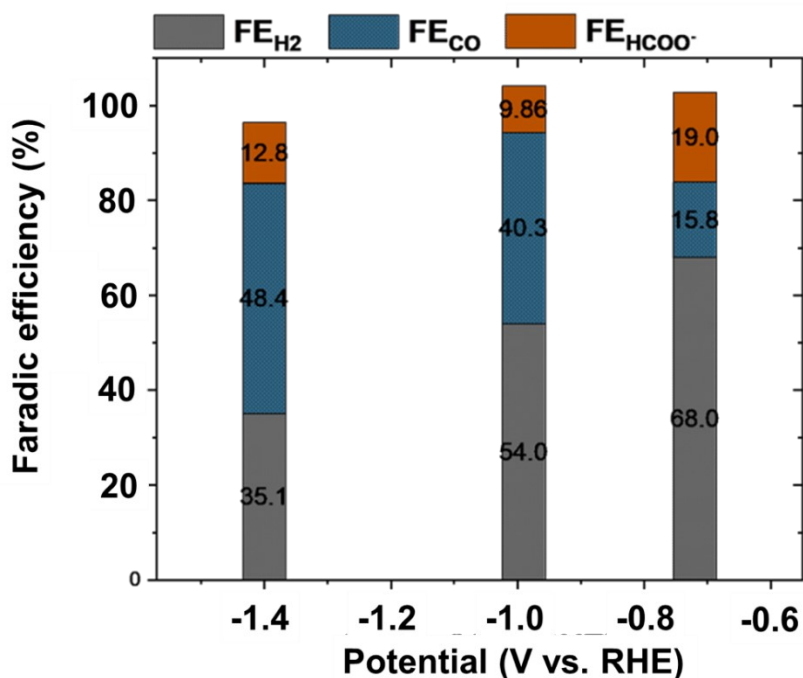
#### 4. Product distribution from an H-cell

For the analysis of gaseous products, an H-cell with two compartments (cathode, anode) and a water jacket for temperature control was used. A Pt mesh cylinder served as a counter electrode in the anode compartment, while an XR300 Ag/AgCl reference electrode (Radiometer Analytical) and a CT carbon cloth with MPL (W1S1011) gas diffusion electrode with the painted catalyst acted as the reference and working electrodes, respectively, in the cathode compartment. The gas diffusion electrode was prepared by spray painting a catalyst ink containing ca. 12 mg of MOF catalyst and 220  $\mu\text{L}$  of 5 wt.% Nafion ionomer (1:1 MOF catalyst-to-ionomer ratio by weight) in 400  $\mu\text{L}$  of isopropanol plus 100  $\mu\text{L}$  of MQ- $\text{H}_2\text{O}$ . The ink was prepared by 15 minutes of ultrasonication in an ultrasound bath and overnight stirring. The ink was sprayed on a 4 cm diameter area using a PTFE template using a Badger model 100G airbrush. The painted electrode was left to dry overnight in a desiccator. The loading of MOF catalyst was consistently  $0.7 \pm 0.01 \text{ mg cm}^{-2}$ , determined by weighing the electrode before and after painting. The active area of the working electrode was  $12.56 \text{ cm}^2$ .

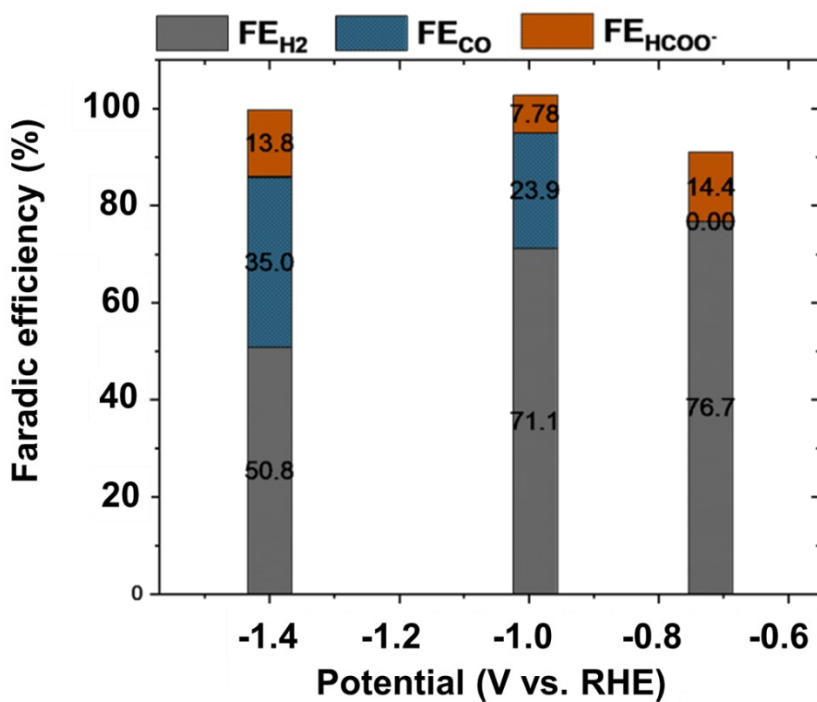
For each cell compartment, 80 mL of 0.1 M  $\text{KHCO}_3$  aqueous solution served as both anolyte and catholyte. The temperature was maintained at  $25^\circ\text{C}$  with water circulation in the water jacket whilst the electrolyte was stirred in the cathode compartment at 350 rpm with a magnetic stirrer. A Nafion 115 membrane separated the two liquid compartments.  $\text{CO}_2$  was bubbled into the cathode compartment at  $10\text{--}13 \text{ mL min}^{-1}$  and directed to analysis in micro gas chromatography (Agilen 990) through the catholyte compartment and a rotameter. Before  $\text{CO}_2$  reduction, the system was stabilized for 30 minutes under  $\text{CO}_2$  flow before running 1 baseline GC chromatogram to ensure removal of residual  $\text{H}_2$ ,  $\text{O}_2$ , and  $\text{N}_2$  and to ensure the system was not leaking.  $\text{CO}_2$  reduction was performed by chronoamperometry (CA) at desired applied potential ( $-0.72 \text{ V}$ ,  $-0.99 \text{ V}$ , and  $-1.40 \text{ V}$  vs. RHE) for 4 h, and gas chromatograms were recorded every 30 minutes. Electrochemical impedance spectroscopy (EIS) was recorded between 20 kHz and 1 Hz at 10 mV amplitude before and after bulk  $\text{CO}_2$  reduction to determine solution resistance for  $iR$  correction. The potentials reported for gaseous products analysis were corrected by the  $iR$  drop, and the potentials were reported versus RHE according to the following formula:  $E_{\text{RHE}} = (E_{\text{Ag/AgCl}} - iR) + 0.2 + 0.059 \cdot \text{pH}$ ;

Where  $E_{\text{Ag/AgCl}}$  is the applied potential (V),  $i$  is the current (A), and  $R$  is the solution resistance determined by EIS ( $\Omega$ ). The gaseous products were monitored online with an Agilent 990-micro GC. The Faradaic efficiency of gaseous products was determined using the following formula:  $\text{FE}_{\text{Gas}} = (z \cdot F \cdot \phi_{\text{Gas}} \cdot u_{\text{m}} / i_{\text{tot}}) \cdot 100\%$ , where  $z$  is the number of electrons transferred to produce a particular gaseous product (for  $\text{H}_2 = 2e^-$ , and  $\text{CO} = 2e^-$ ),  $F$  is Faraday's constant ( $96485.3 \text{ C mol}^{-1}$ ),  $\phi_{\text{Gas}}$  is the volume of the gas product determined by GC,  $u_{\text{m}}$  is the molar

flow rate of CO<sub>2</sub> gas determined with the rotameter (mol s<sup>-1</sup>). The liquid products (HCOO<sup>-</sup>) were quantified with HPLC using the following formula:  $FE_{\text{Liquid}} = (z \cdot F \cdot c_{\text{Liquid}} \cdot V / i_{\text{tot}} \cdot t) \cdot 100\%$ .

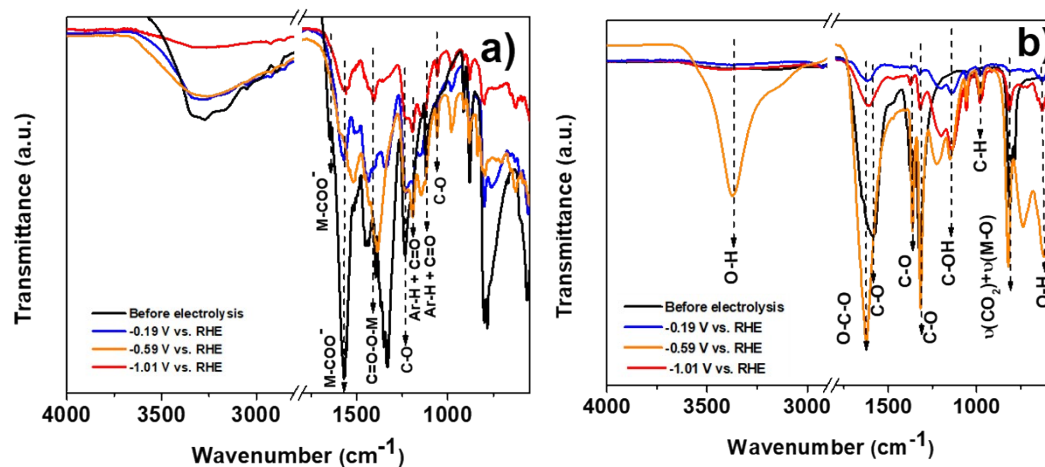


**Fig. S6.** Faradic efficiency (%) in CO<sub>2</sub>-saturated 0.1 M KHCO<sub>3</sub> using the H-cell with H<sub>4</sub>DOBDC MOF at -0.72 V vs RHE, -0.99 V vs RHE, and -1.40 V vs RHE.

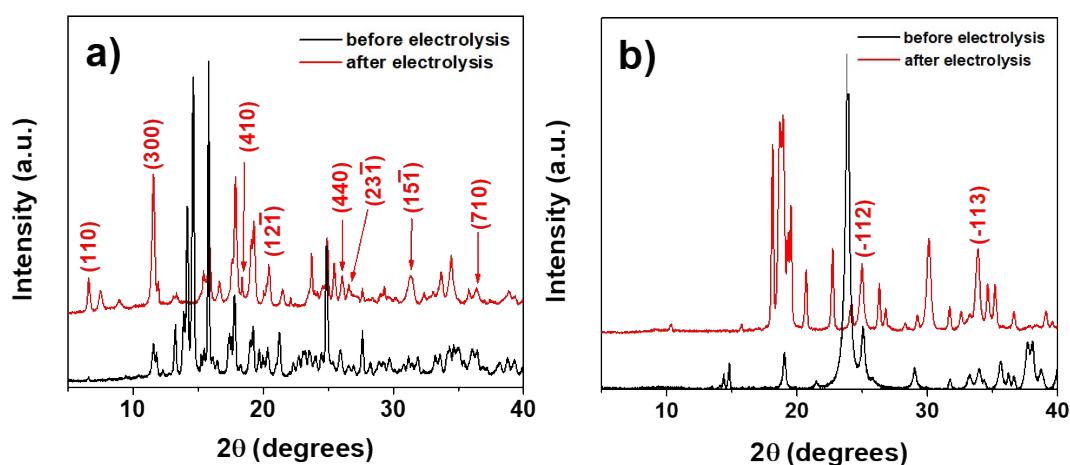


**Fig. S7.** Faradic efficiency (%) in CO<sub>2</sub>-saturated 0.1 M KHCO<sub>3</sub> using the H-cell with oxalic acid MOF at -0.72 V vs RHE, -0.99 V vs RHE, and -1.40 V vs RHE.

## 4. Electrocatalyst Stability

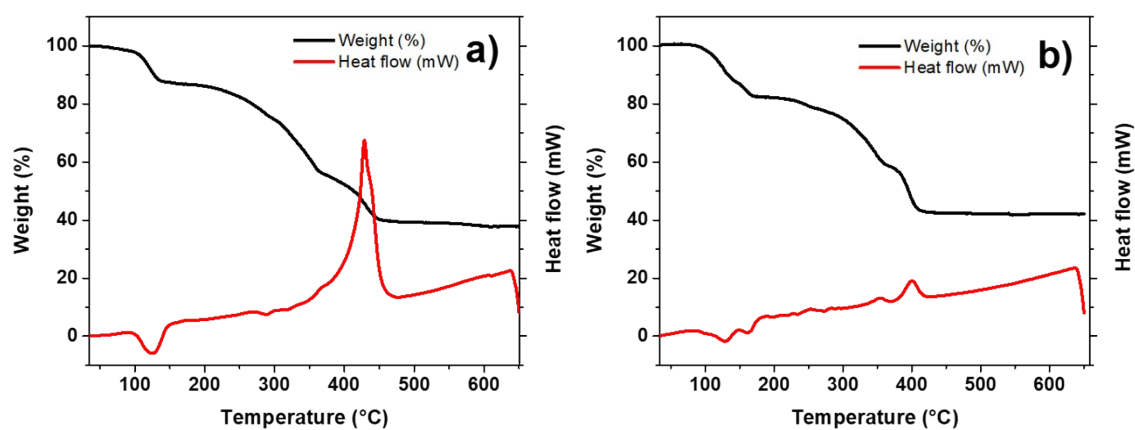


**Fig. S8.** FTIR spectra comparison for the MOFs before and after the chronoamperometric tests (at -0.19 V, -0.59 V, and -1.01 V vs. RHE). a)  $\text{H}_4\text{DOBDC}$  MOF and b) Oxalic acid MOF.



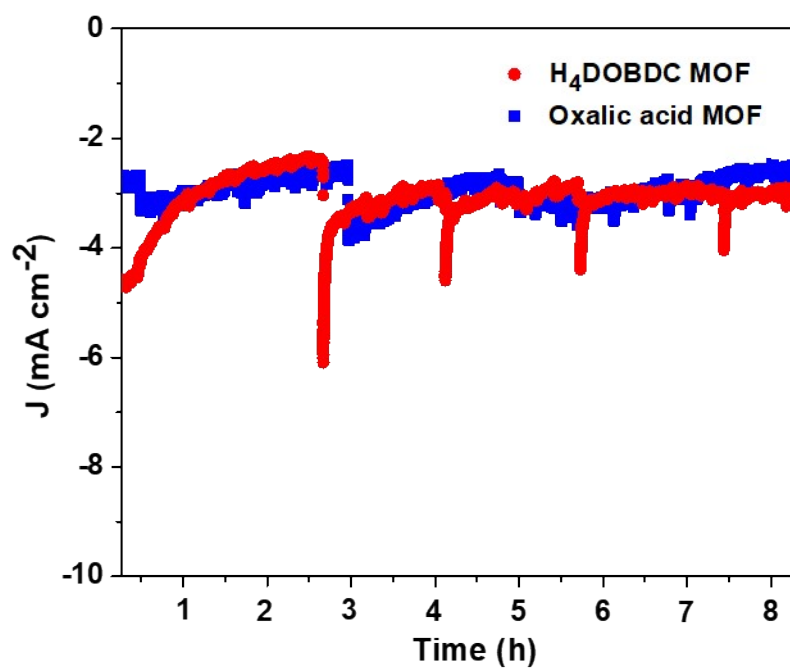
**Fig. S9.** MOF XRD patterns before and after electrolysis at -0.19 V vs. RHE. a)  $\text{H}_4\text{DOBDC}$  MOF and b) Oxalic acid MOF.

## 5. TGA



**Fig. S10.** TGA curves of: a) H<sub>4</sub>DOBDC MOF and b) Oxalic acid MOF.

## 6. Electrocatalyst Stability: Chronoamperometry



**Fig. S11.** Chronoamperometry stability tests in  $\text{CO}_2$ -saturated 0.1 M KOH electrolyte for 8h at  $-1.01$  V vs. RHE. a)  $\text{H}_4\text{DOBDC MOF}$  and b) Oxalic acid MOF.

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