

Supporting Information

Sintering Resistant CuO/CeO₂ Catalysts Prepared by Reversed Impregnation Method for Ethyl Acetate Oxidation

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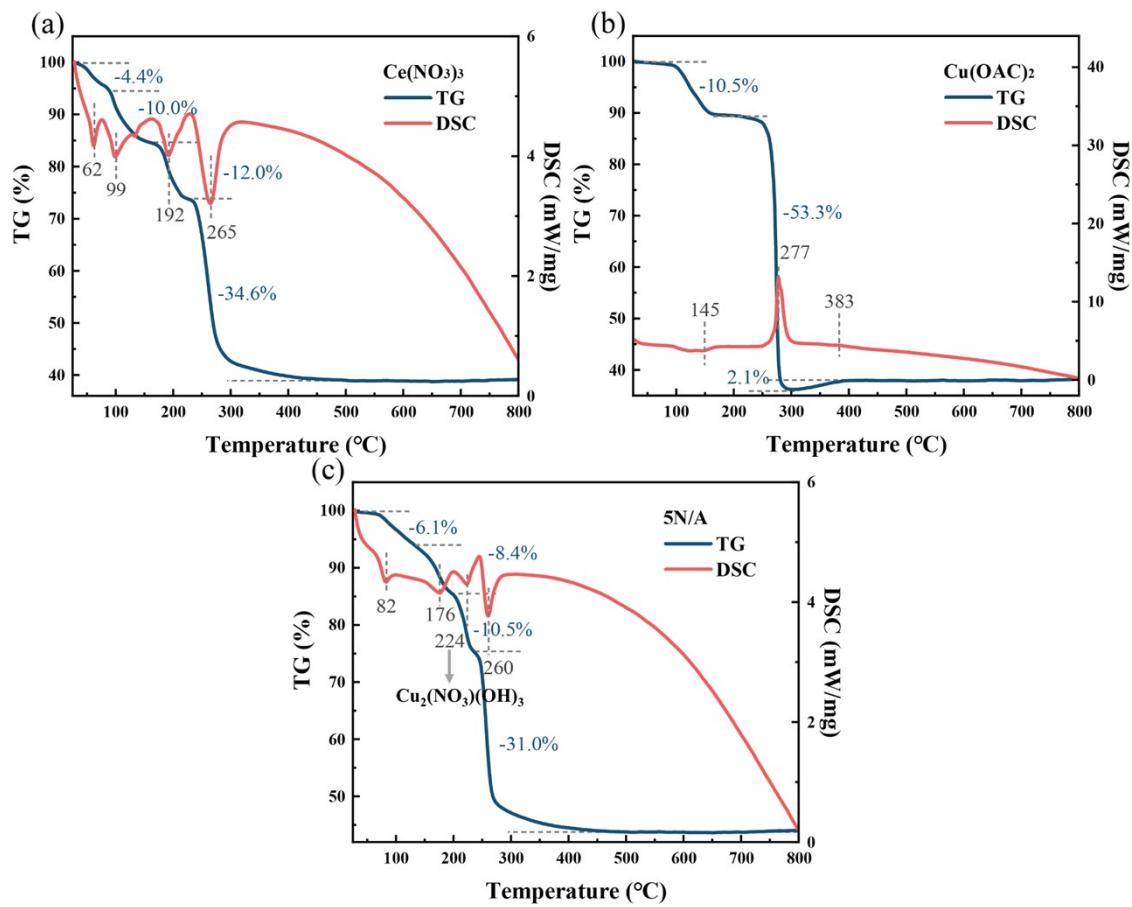


Figure S1. TG-DSC curves of (a) $\text{Ce}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$; (b) $\text{Cu}(\text{OAc})_2 \cdot \text{H}_2\text{O}$ and (c) uncalcined 5N/A catalyst.

5N/A catalyst.

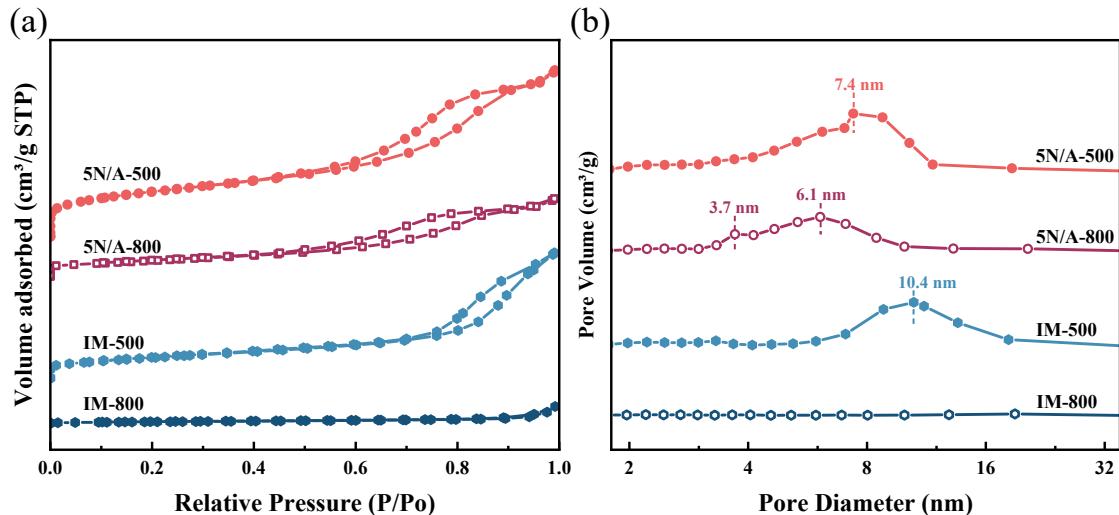


Figure S2. (a) Nitrogen adsorption-desorption isotherms and (b) Pore distributions of the 5N/A-Y and IM-Y catalysts.

5N/A-Y catalyst.

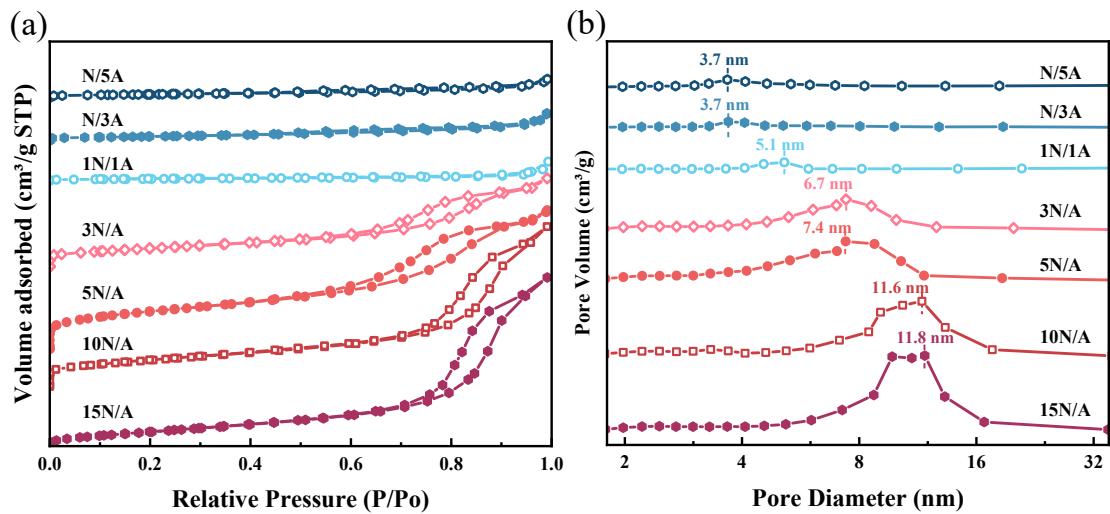


Figure S3. (a) Nitrogen adsorption-desorption isotherms and (b) Pore distributions of the XN/A-500 catalysts.

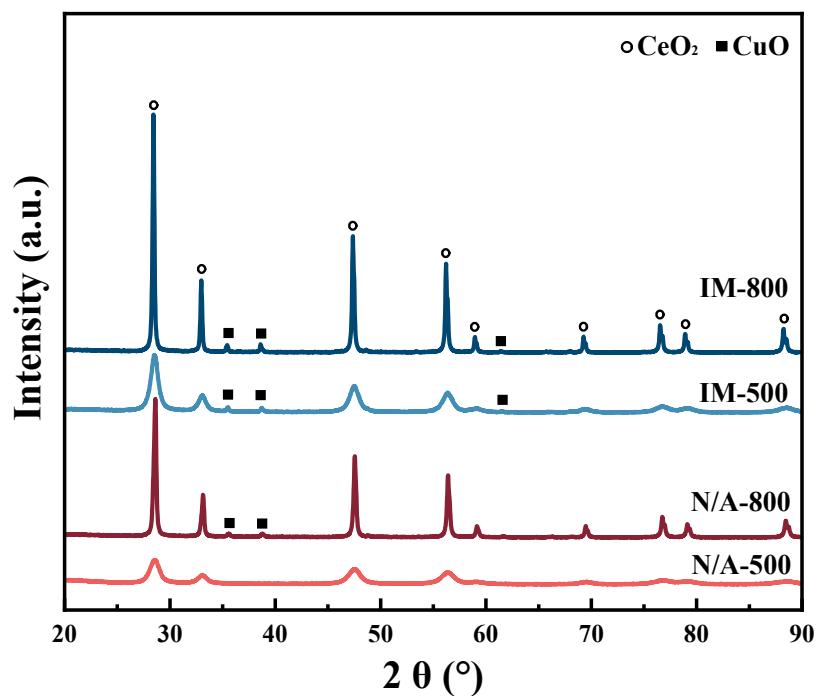


Figure S4. XRD patterns of 5N/A-Y and IM-Y catalysts.

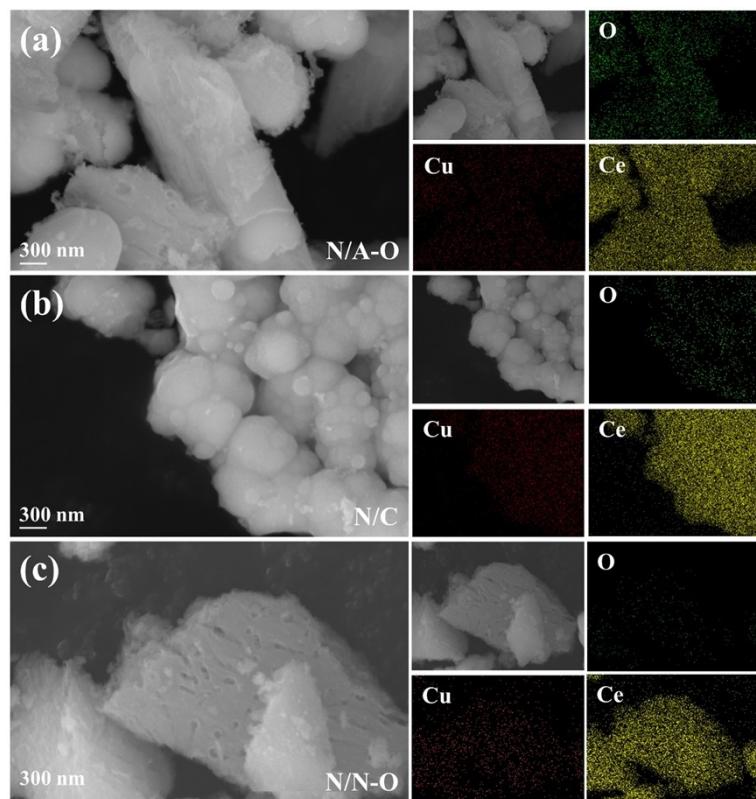


Figure S5. SEM mapping images of (a)N/A-O-500, (b)N/C-500 and (c)N/N-O-500 catalysts.

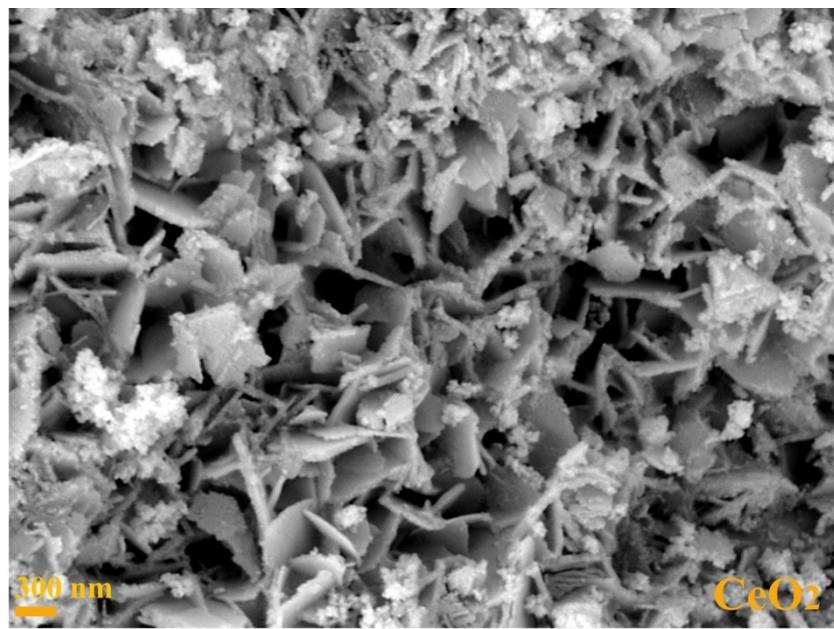


Figure S6. SEM image of CeO₂ sample obtained by calcination of Ce(OAc)₃ at 300 °C for

4h.

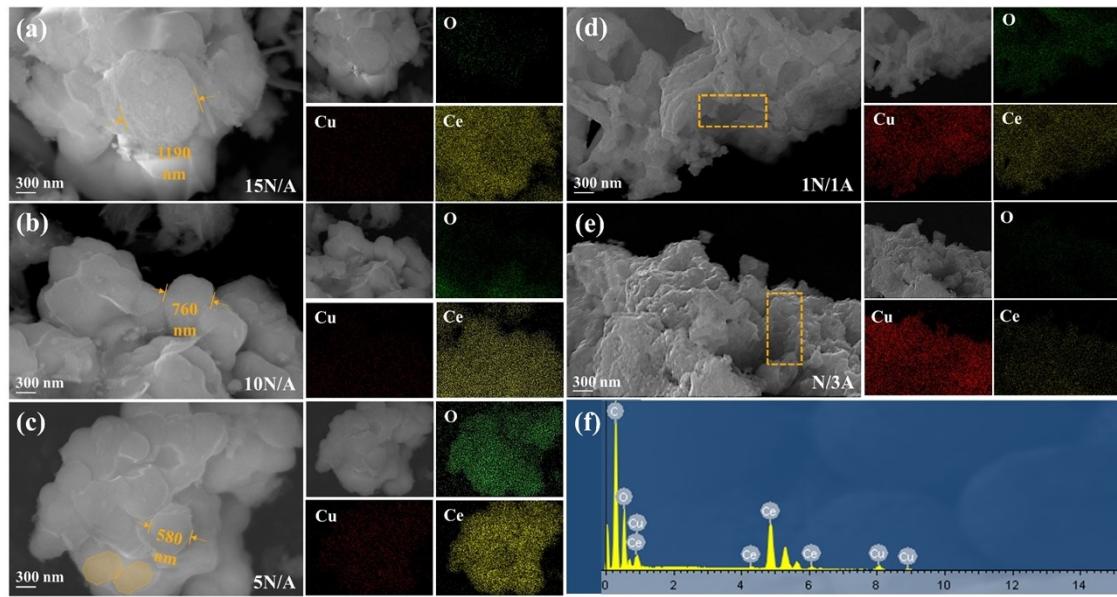


Figure S7. SEM mapping images of XN/A-500 catalysts.

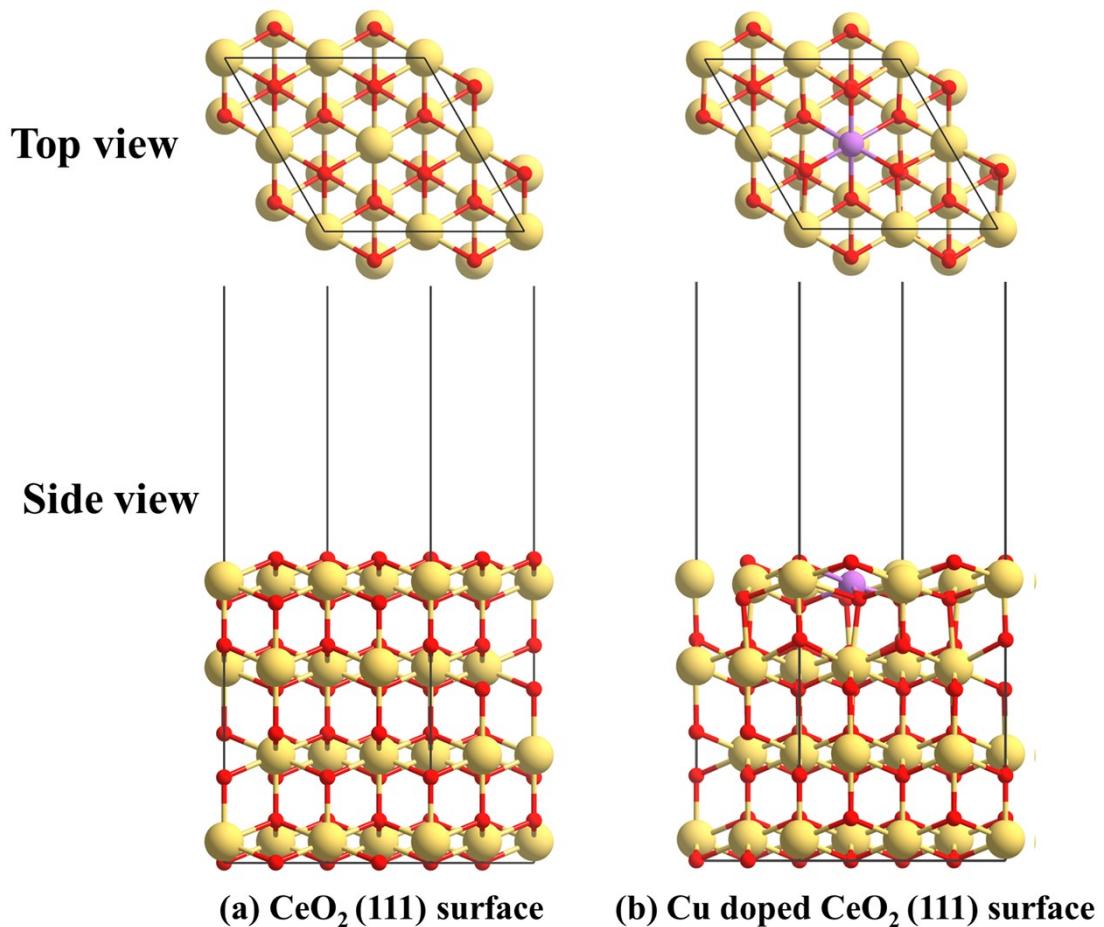


Figure S8. The optimized structures of (a) CeO_2 (111) and (b) Cu doped CeO_2 (111) surfaces.

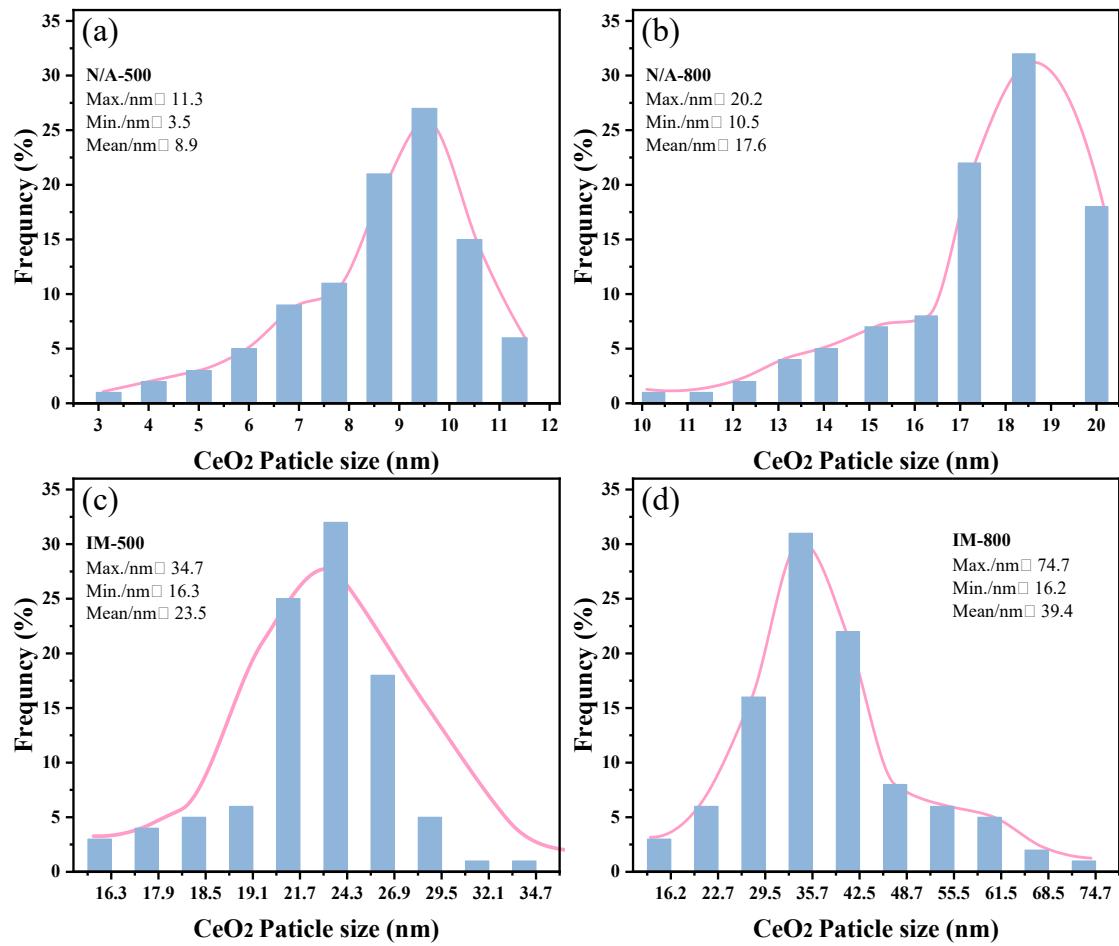


Figure S9. The CeO_2 particle size histograms of 5N/A-Y and IM-Y catalysts.

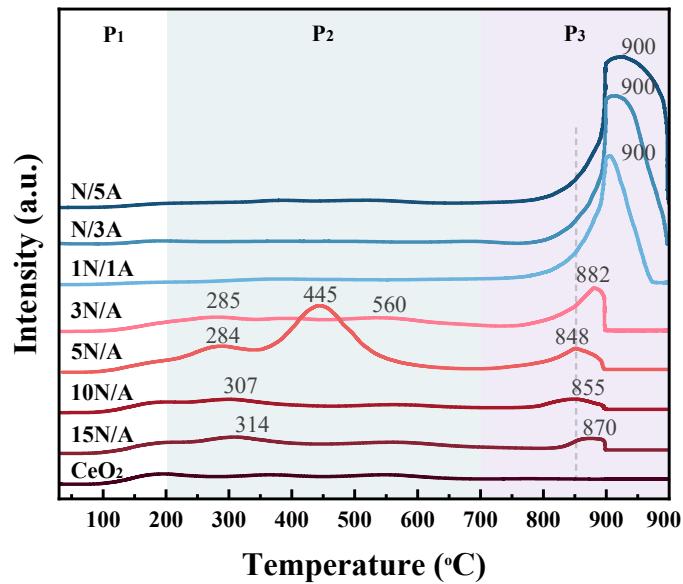


Figure S10. O_2 -TPD profiles of the XN/A-500 catalysts.

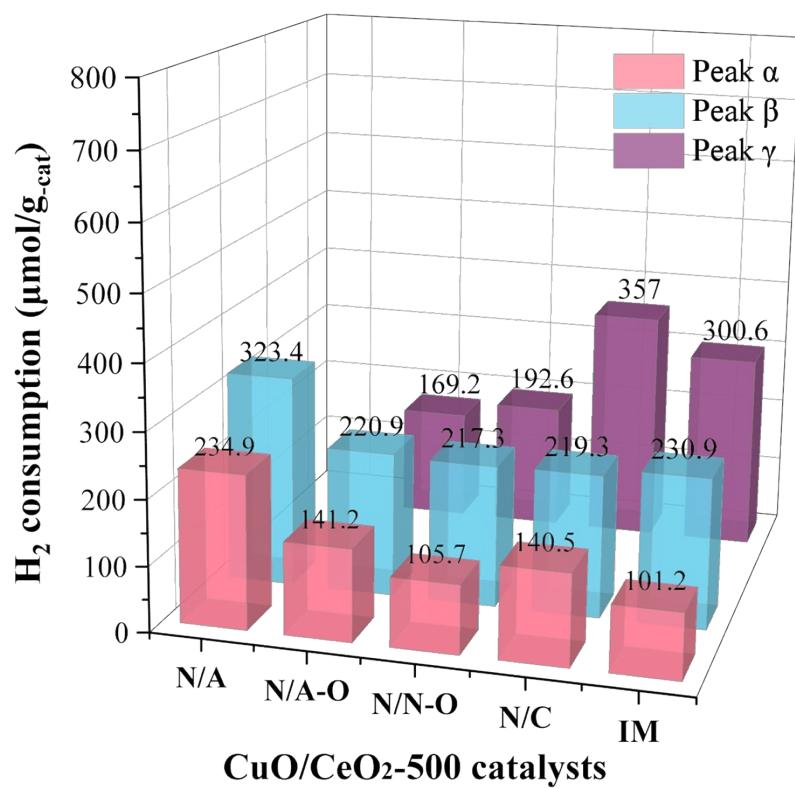


Figure S11. H₂ consumption of three reduction peaks on the 5Ce/1Cu-500 and IM-500 catalysts.

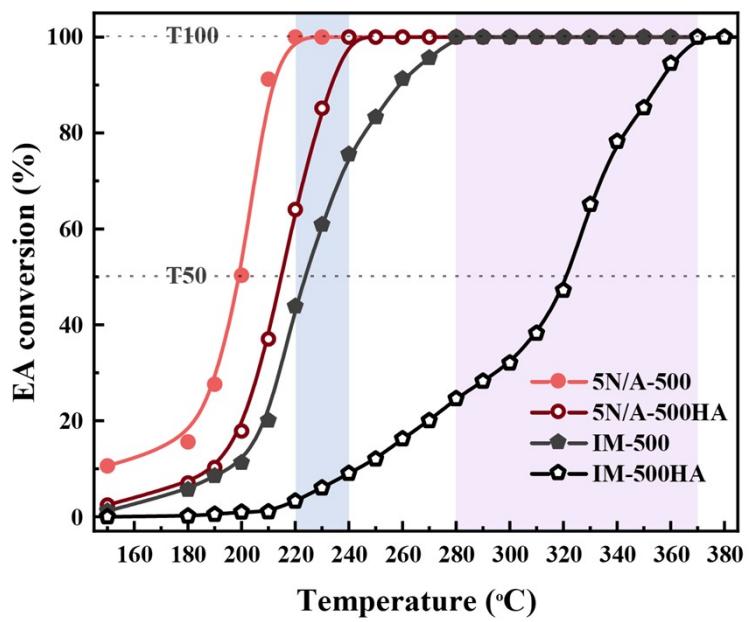


Figure S12. Catalytic activities for fresh 5N/A-500, IM-500 and hydrothermal ageing 5N/A-500HA, IM-500HA catalysts.

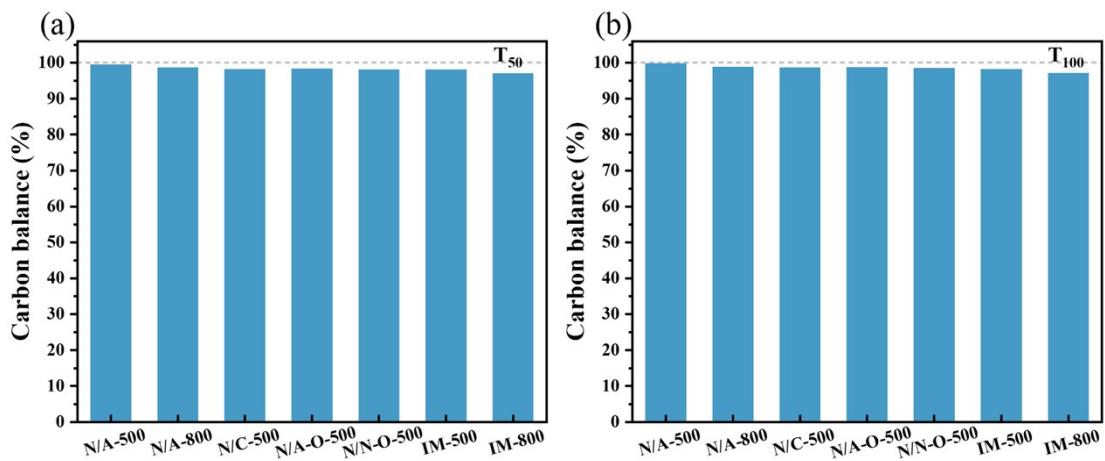


Figure S13. Carbon balance of CuO/CeO₂-Y catalysts at (a) T₅₀ and (b) T₁₀₀ during EA oxidation.

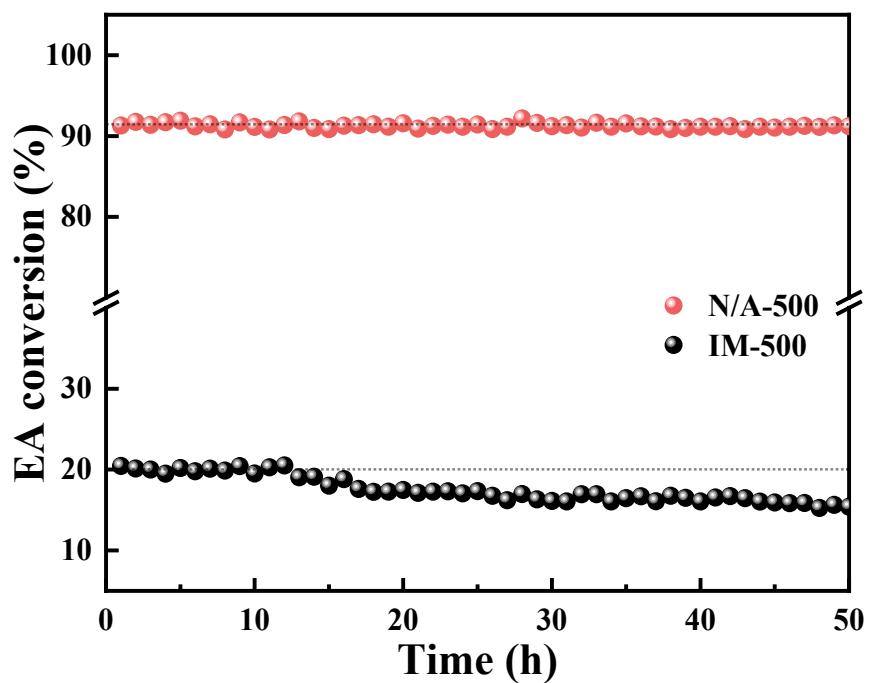


Figure S14. Durability test of 5N/A-500 and IM-500 catalysts at 210 °C.

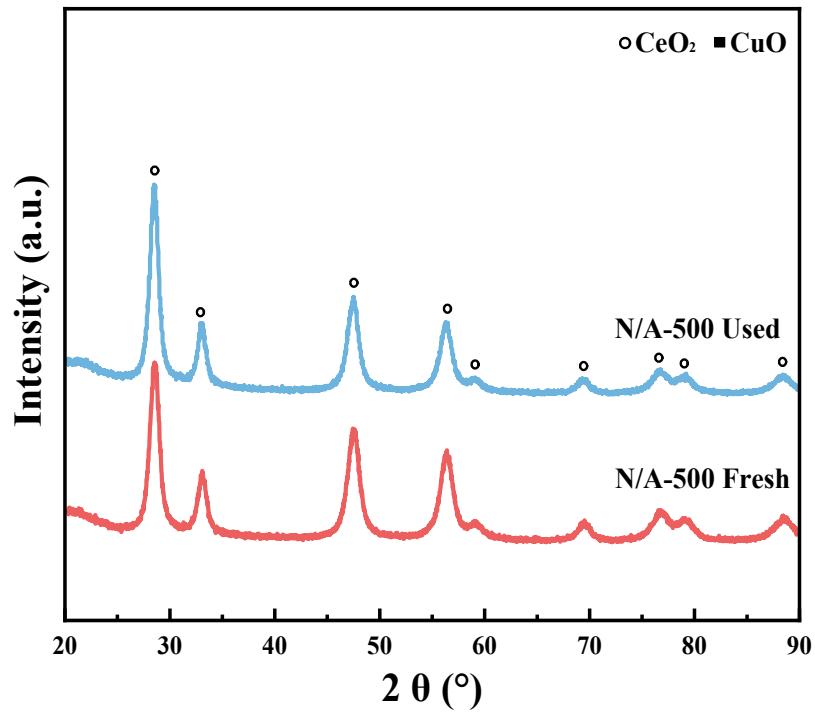


Figure S15. XRD patterns of the 5N/A-500 catalysts fresh and after durability test.

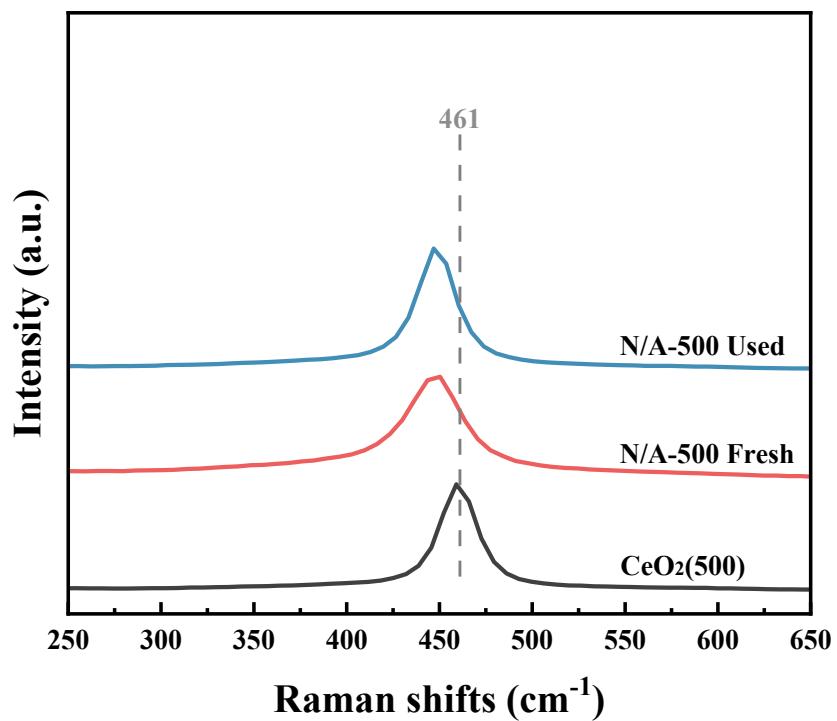


Figure S16. Raman spectra of the 5N/A-500 catalysts fresh and after durability test.

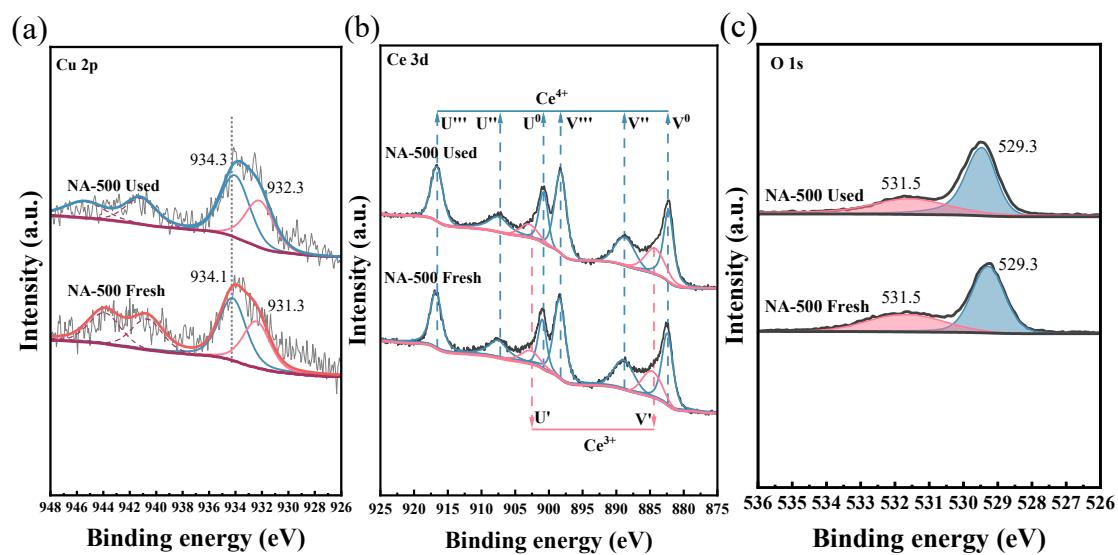


Figure S17. XPS spectra of (a) Cu 2p, (b) Ce 3d and (c) O 1s for the 5N/A-500 catalysts fresh and after durability test.

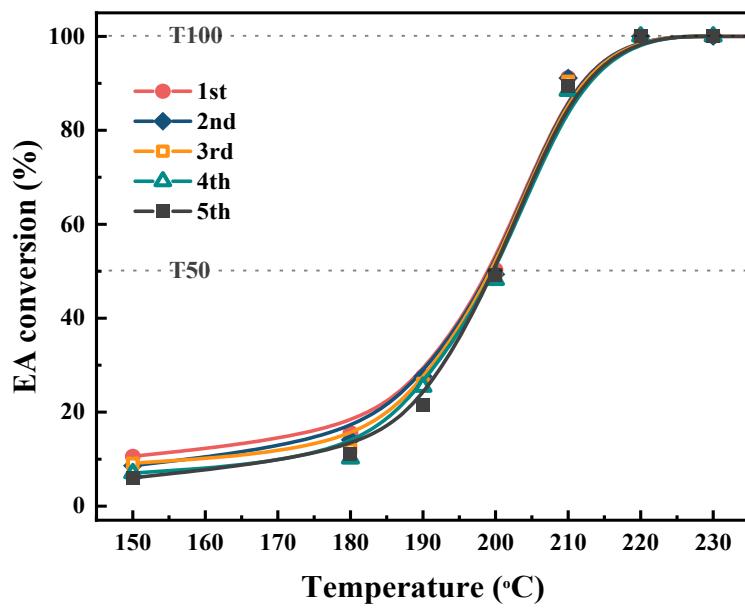


Figure S18. Five-cycle catalytic activity of the 5N/A-500.

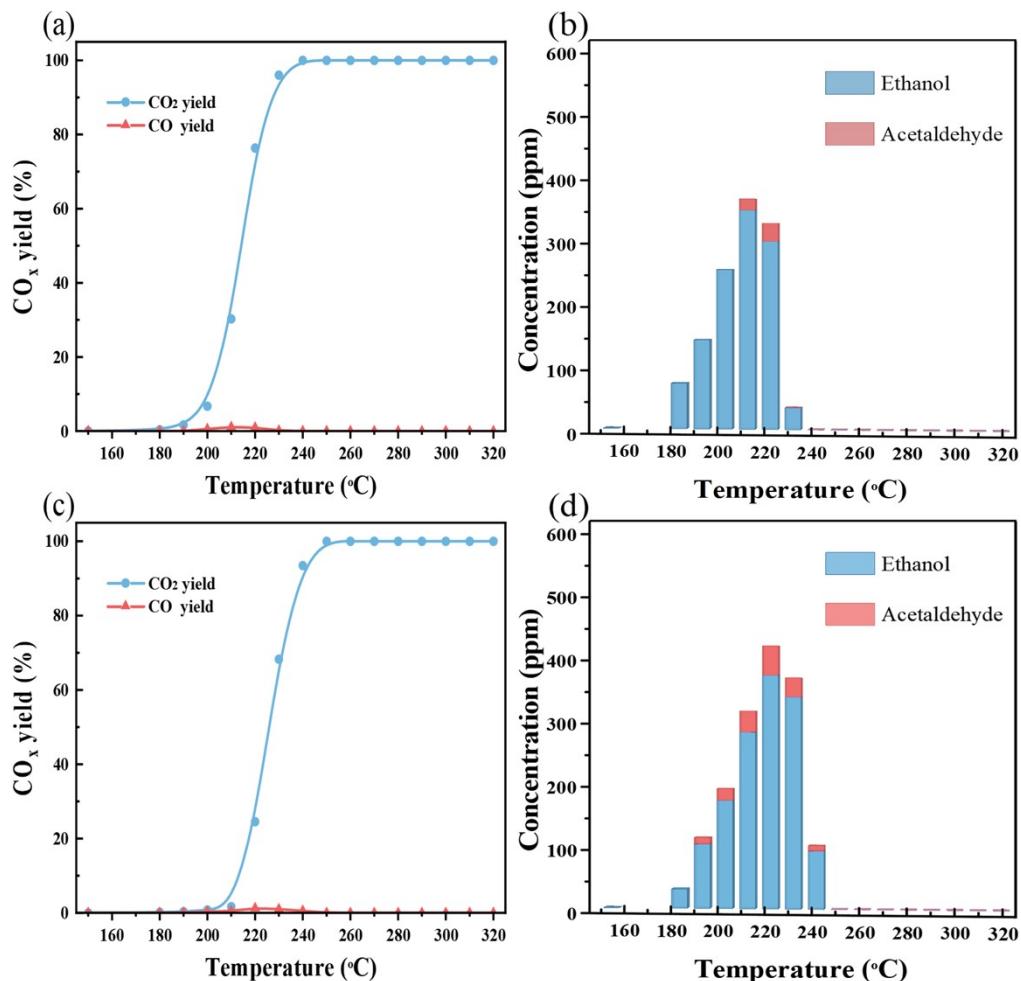


Figure S19. CO_x yields and distributions of by-products over the 5N/A-500 under 20 vol.% O₂ (a, b) and without O₂ (c, d) atmosphere.

O₂ (a, b) and without O₂ (c, d) atmosphere.

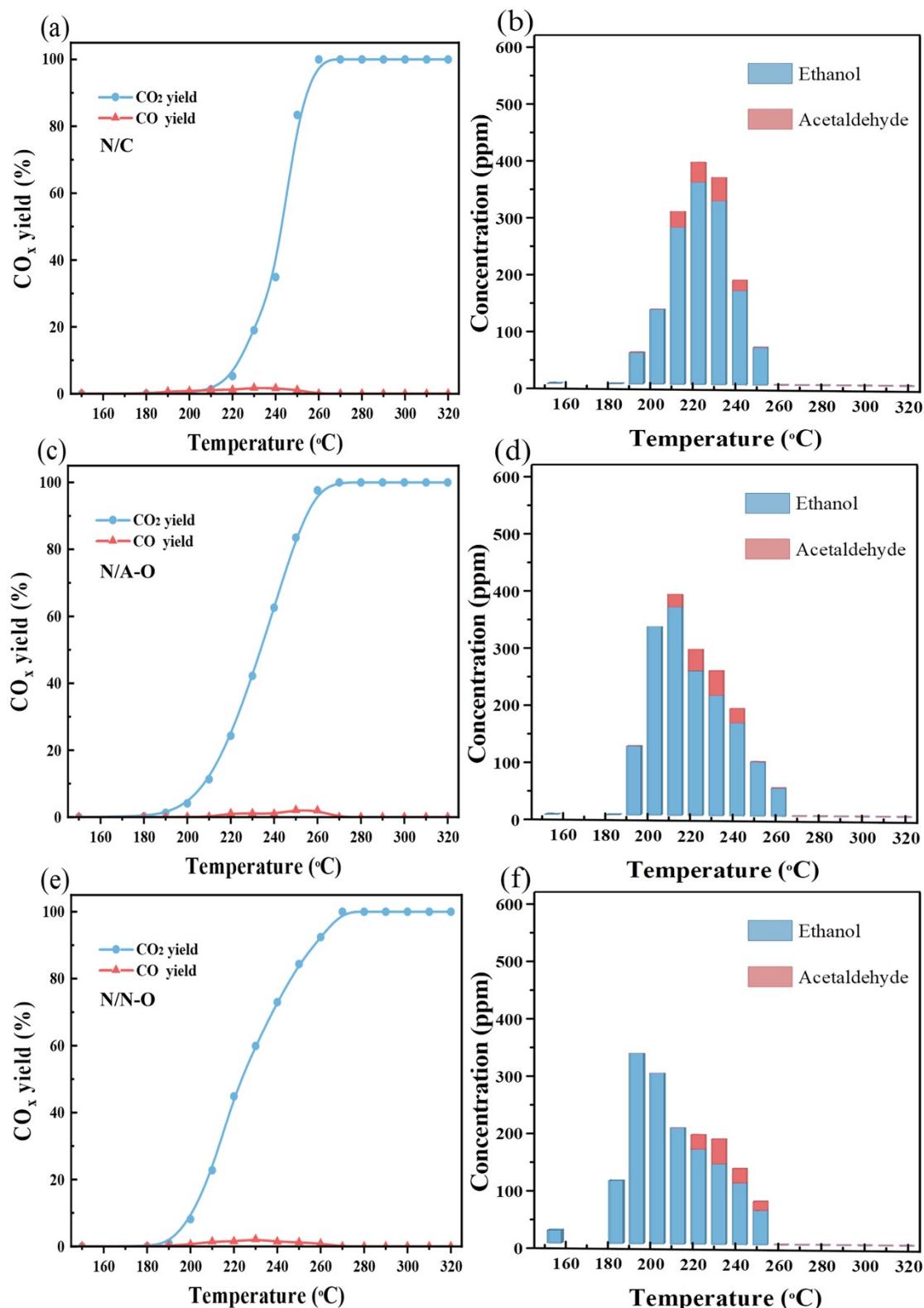


Figure S20. CO_x yields and distributions of by-products over the 5N/C-500 (a, b), 5N/A-O-500 (c, d) and 5N/N-O-500 (e, f) catalysts.

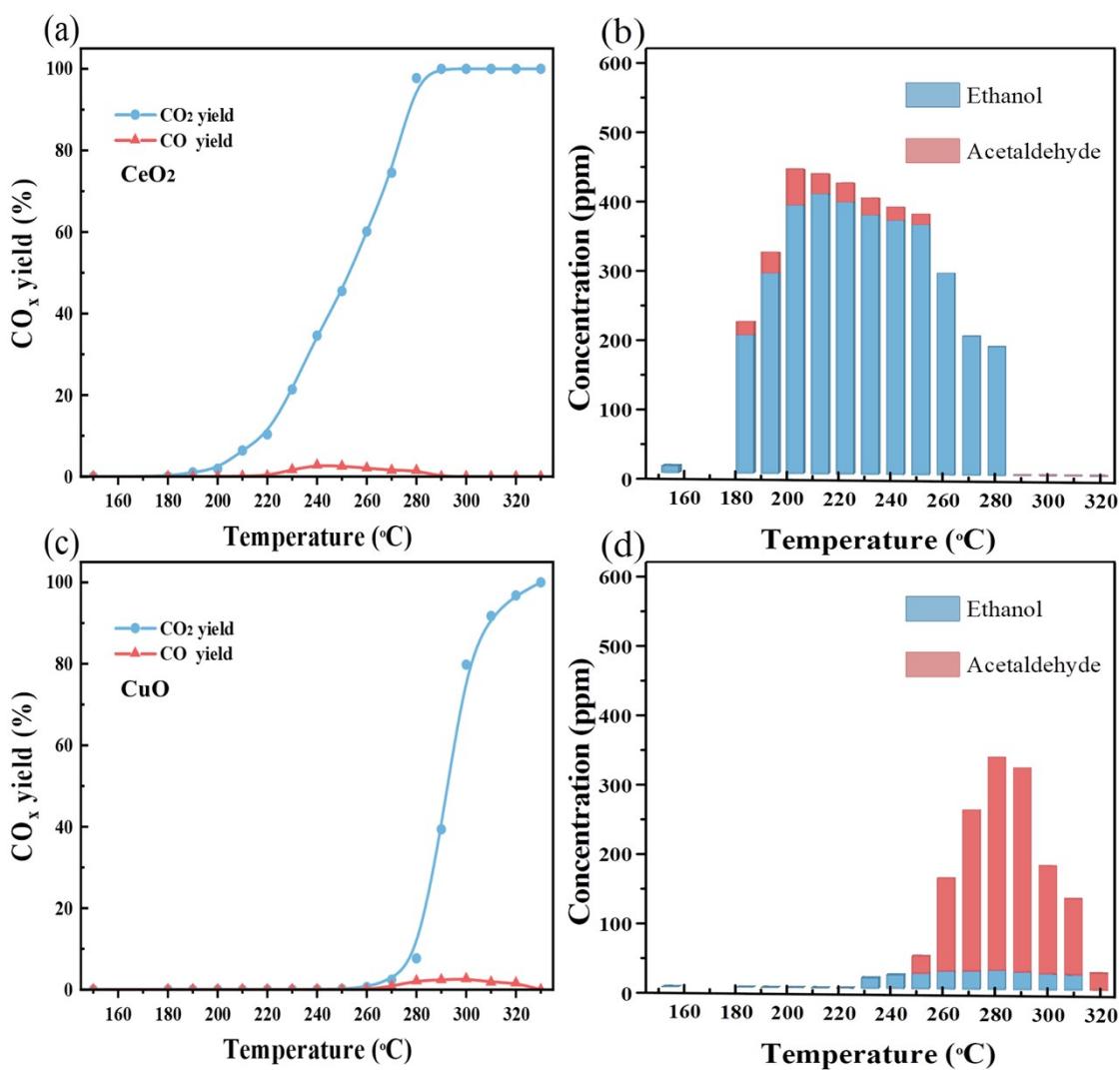


Figure S21. CO_x yields and distributions of by-products over the $\text{CeO}_2(500)$ (a, b) and CuO (A-O) (c, d) catalysts.

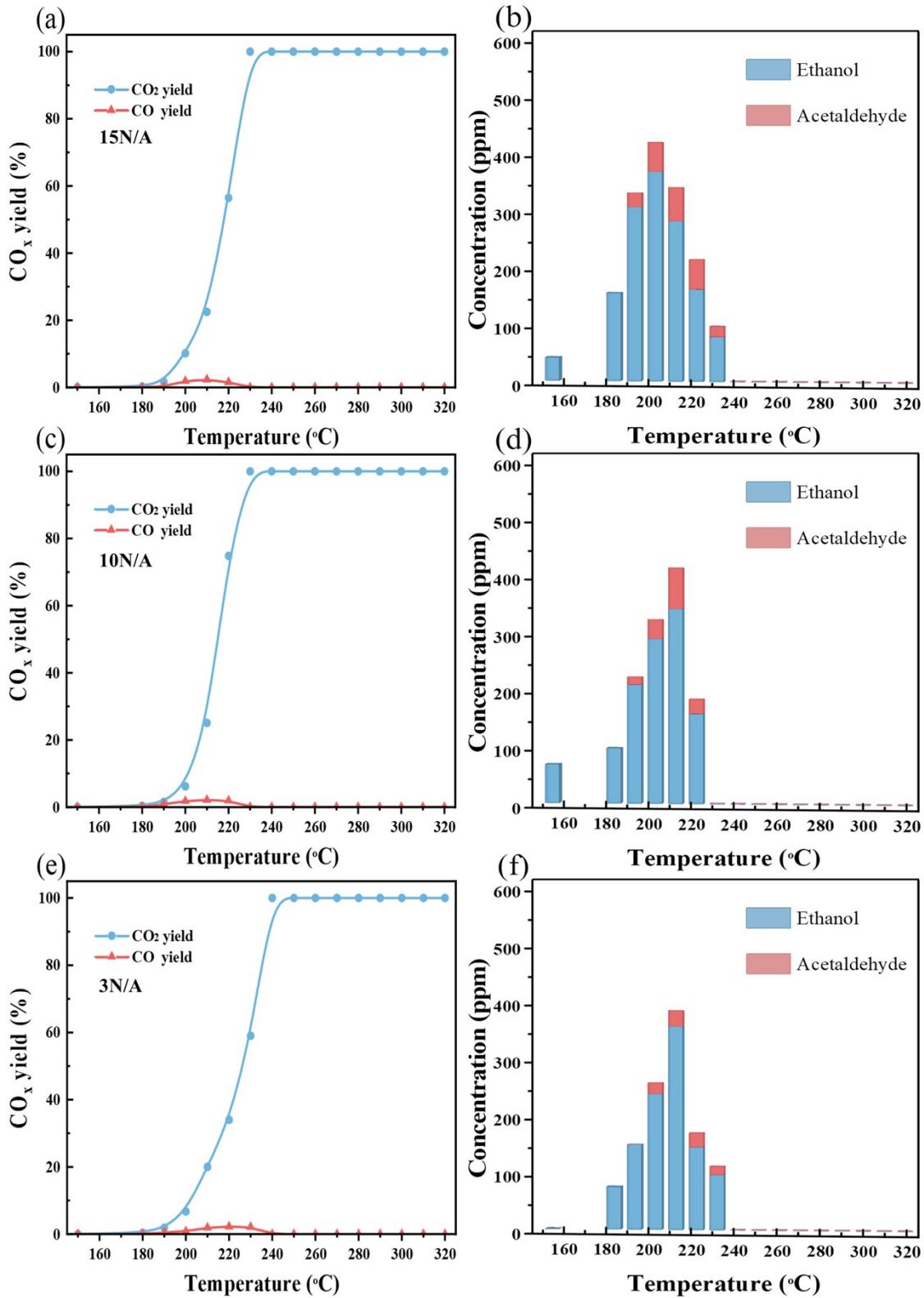


Figure S22. CO_x yields and distributions of by-products over the 15N/A-500 (a, b), 10N/A-

500 (c, d) and 3N/A-500 (e, f) catalysts.

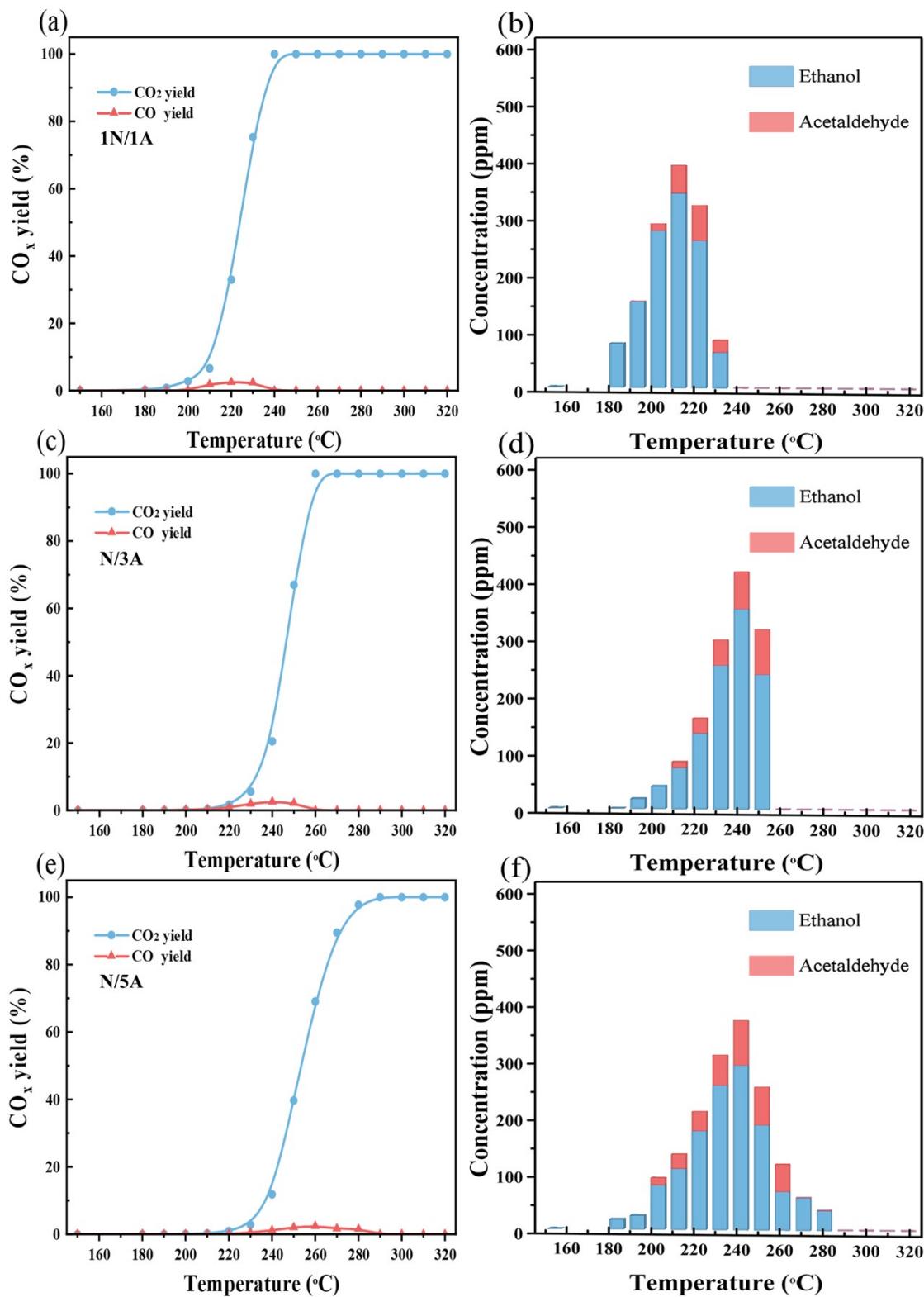


Figure S23. CO_x yields and distributions of by-products over the 1N/1A-500 (a, b), N/3A-500 (c, d) and N/5A-500 (e, f) catalysts.

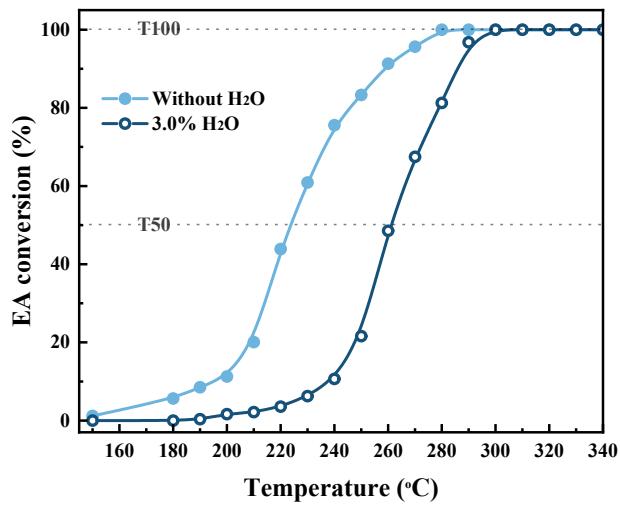


Figure S24. Catalytic activities of IM-500 catalyst with 3.0 vol.% water vapor contents.

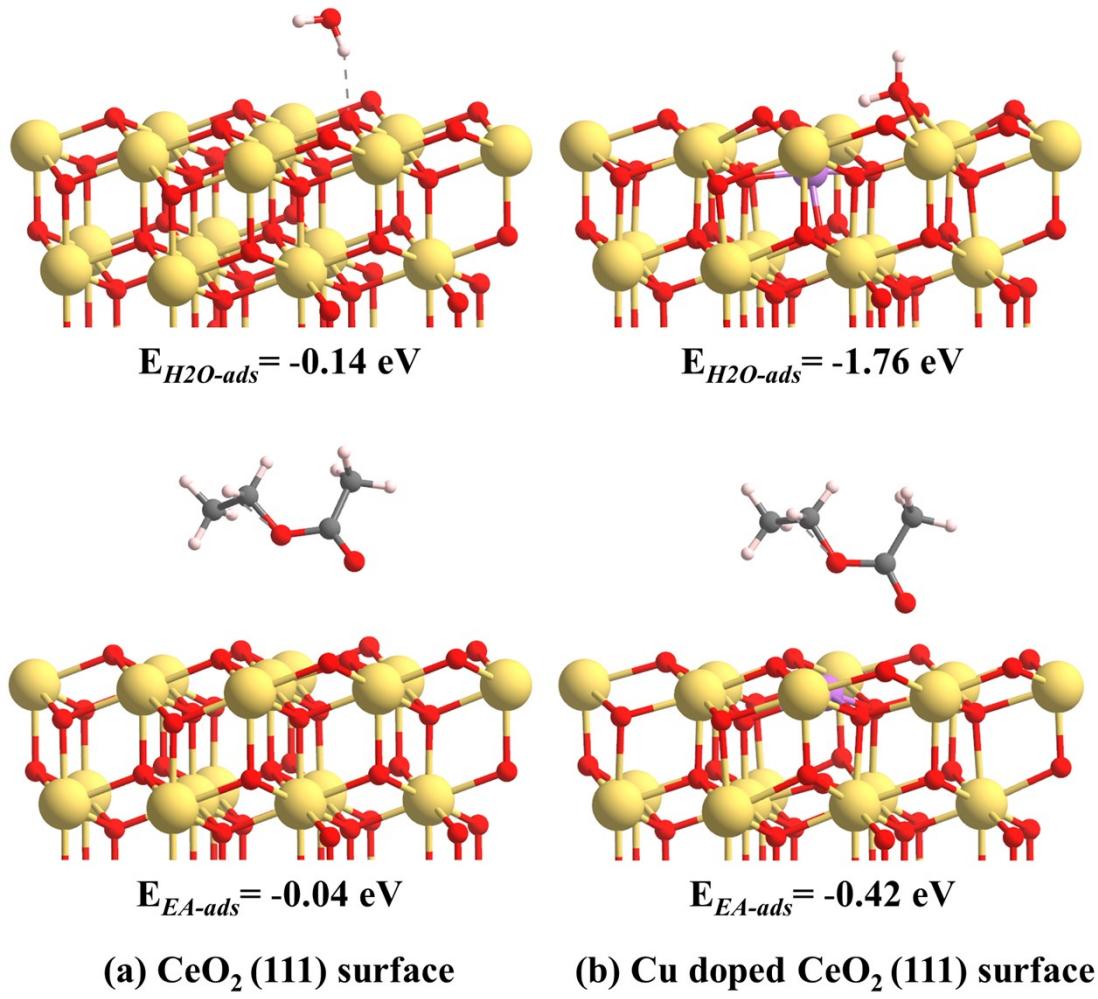


Figure S25. Optimized structures of H₂O and EA molecules adsorbed on the surfaces of (a) CeO₂(111) and (b) Cu doped CeO₂(111). (Yellow, purple, and red colors is Ce, Cu, and O, respectively).

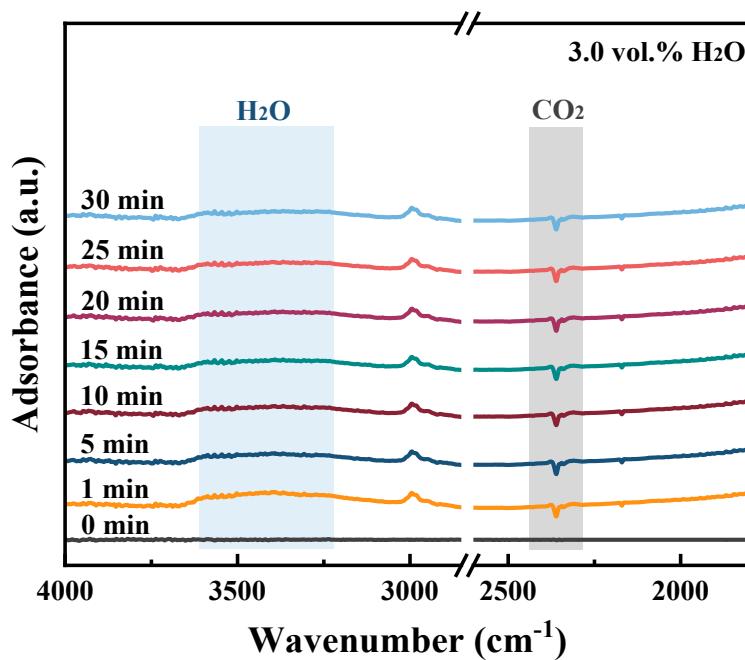


Figure S26. In situ FTIR spectra of EA adsorption at different time over 5N/A-500 catalyst under 1000 ppm EA/20% O₂/He/3.0 vol.% water vapor content.

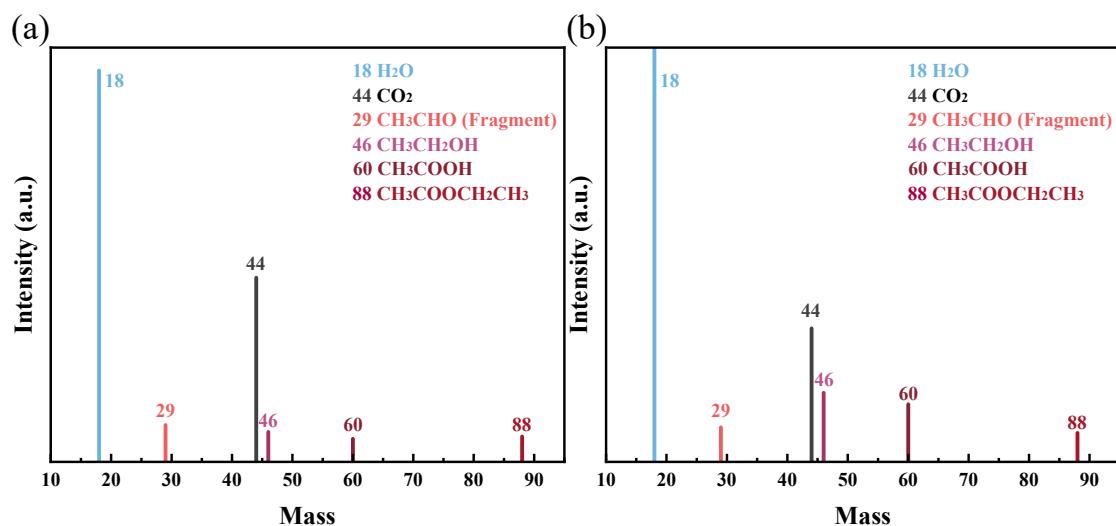


Figure S27. MS signal of EA catalytic oxidation over 5N/A-500 catalyst under 1000 ppm (a) EA/20% O₂/He and (b) 3.0 vol.% water vapor content atmospheres at 80 °C.

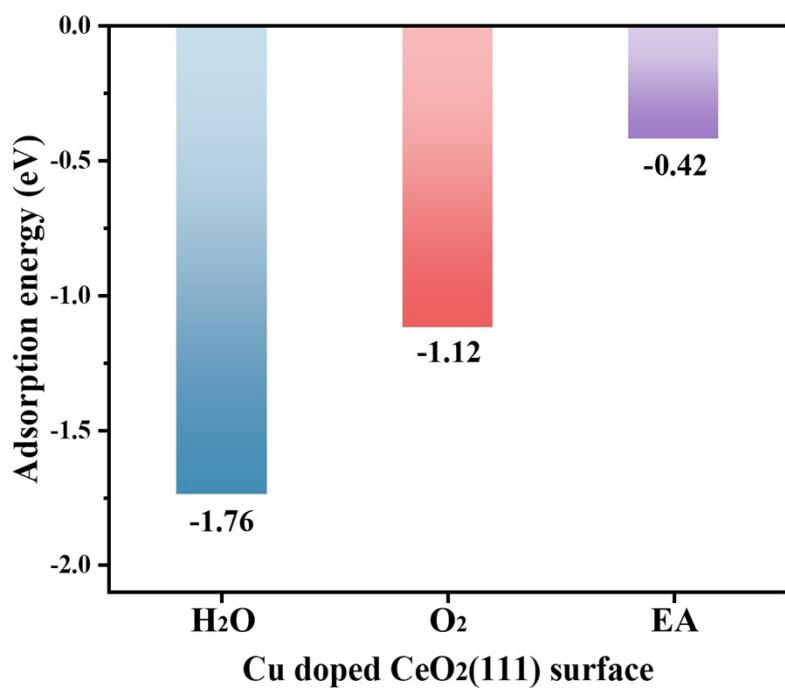


Figure S28. Comparison of adsorption energies of H₂O, O₂ and EA on the Cu doped CeO₂(111) surface.

Table S1 Specific surface areas, crystallite sizes and cell parameters of the CuO/CeO₂ catalysts.

Catalysts	SA (m ² /g)	Pore diameter (nm)	Pore volume (cm ³ /g)	CeO ₂ crystallite size ^a (nm)	CuO crystallite size ^a (nm)	Cell parameter (nm)
CeO ₂ (500)	74	10.8	0.16	18.2	-	0.5401
CuO(A-O)	1	17.3	0.01	-	34.1	-
IM-500	49	10.4	0.13	23.4	7.9	0.5392
5N/C-500	20	5.9	0.03	13.1	2.1	0.5389
5N/N-O-500	62	10.7	0.17	14.9	-	0.5385
5N/A-O-500	64	9.6	0.19	13.7	-	0.5382
5N/A-500	106	7.9	0.20	9.4	-	0.5370
15N/A-500	74	11.9	0.22	12.6	-	0.5381
10N/A-500	74	10.5	0.19	10.9	-	0.5379
3N/A-500	53	8.2	0.11	11.8	-	0.5375
1N/1A-500	12	10.7	0.03	15.3	3.2	0.5383
N/3A-500	10	9.1	0.02	15.3	4.7	0.5387
N/5A-500	5	6.8	0.02	12.9	8.1	0.5391
5N/A-300	58	10.2	0.16	10.3	-	0.5401
5N/A-400	65	9.4	0.15	9.8	-	0.5387
5N/A-600	105	6.8	0.20	9.6	-	0.5373
5N/A-700	75	6.2	0.16	14.7	1.4	0.5378
5N/A-800	38	6.1	0.08	18.7	2.6	0.5380
IM-800	5	14.7	0.02	42.5	18.7	0.5408

^a The crystallite sizes were calculated by the Scherrer equation.

Table S2 The Cu, Ce and O contents of energy dispersion spectrum (EDS) over the CuO/CeO₂ catalysts

	Catalysts	Cu (wt.%)	Ce (wt.%)	O (wt.%)
Different preparation methods	IM-500	7.84	52.11	40.05
	5N/C-500	6.95	51.17	41.88
	5N/A-O-500	6.87	51.84	41.29
	5N/N-O-500	7.12	52.65	40.23
	5N/A-500	6.34	49.19	44.47
Different calcination temperatures	5N/A-300	7.56	51.61	40.83
	5N/A-400	7.32	50.33	42.35
	5N/A-500	6.34	49.19	44.47
	5N/A-600	6.47	49.65	43.88
	5N/A-700	6.52	50.17	43.31
	5N/A-800	6.78	50.35	42.87
	IM-800	8.36	54.5	37.14

Table S3 H₂-TPR analysis of the 5N/A-Y catalysts

Catalysts	Peak temperature (°C)			H ₂ consumption (μmol/g _{cat})			H ₂ consumption ratio of α/(α+β+γ)
	α	β	γ	α	β	γ	
5N/A-300	-	202	225	-	306.8	380.9	-
5N/A-400	173	198	216	243.3	197.9	180.1	0.39
5N/A-500	164	195	-	234.9	323.4	-	0.42
5N/A-600	163	195	-	201.4	302.2	-	0.40
5N/A-700	160	192	225	56.3	297.3	28.6	0.14
5N/A-800	160	190	225	21.3	233.1	42.5	0.07

Table S4 XPS analysis of the 5N/A-500 catalysts fresh and after durability test

Catalysts	Surface composition (at.%)			Surface element molar ratio		
	Cu	Ce	O	Cu ⁺ /Cu ²⁺	Ce ³⁺ /Ce ⁴⁺	O _{ads} /O _{latt}
Fresh	7.79	12.00	50.94	0.65	0.29	0.65
Used	7.81	12.16	50.72	0.65	0.28	0.64

Table S5 Comparison of the conversion temperature for EA with other catalysts

Catalysts	T ₁₀₀	GHSV (h ⁻¹)	Loading (wt.%)	Treatment t (°C, h)	Preparation method	Rf.
5N/A-500	220	60,000	8.5%Cu	500, 4	Reversed Impregnation	This work
5N/A-800	230	60,000		800, 4		
Cu/Al ₂ O ₃ /COR	255	32,000	1.9%Cu	550, 4	Impregnation	1
Cu–Mn–La(NH ₄) ₂ CO ₃)	240	12,500	35.6%Cu	550, 4	Co-precipitation	2
Cu-Ce	240	120,000	29.3%Cu	400, 3	Impregnation	3
15Cu/OMS-2	240	120,000	15%Cu	400, 4	Pre-incorporation	4
CeCuY ₂ O ₃ -S5	250	15,000	-	500, 4	Sol-Gel	5
CeCuY ₂ O ₃ -S8	260			800, 4		
Cu/CeO ₂	275	60,000	20%Cu	550, 2	Impregnation	6
Cu/CeO ₂	260	60,000	20%Cu	550, 2	Impregnation	7
Cu _{0.15} Ce _{0.85}	240	50,000	15%Cu	550, 2	Urea–nitrate Combustion	8
CuO/CeO ₂ -800	260	60,000	5%Cu	800, 4	Modified Impregnation	9
Cu10/Al ₂ O ₃ -SiO ₂	300	5,000	10%Cu	600, 4	Impregnation	10
Ce _{0.8} Sn _{0.2} O ₂ -500	235	60,000	-	500, 6	Combustion	11
Ce _{0.8} Sn _{0.2} O ₂ -800	250			800, 4		
0.37AuPd _{2.72} /TiO ₂	260	40,000	0.37%AuPd	450, 4	Impregnation	12
Pt/CeMnO _X	240	20,000	0.5%Pt	500, 4	Impregnation	13
Pd/CeCuO-Y ₂ O ₃ -500	260	40,000	0.28%Pd	500, 4	Impregnation	14
Pd/CeCuO-Y ₂ O ₃ -800	270			800, 4		
Pt/ZrO ₂	230	30,000	1%Pt	600, 4	Impregnation	15
Pt/Al ₂ O ₃	250	30,000	1%Pt	600, 4	Impregnation	15
Pt/Co ₃ O ₄ -CeO ₂	220	30,000	2%Pt	400, 1	Hydrothermal	16
Pt/Al ₂ O ₃	240	30,000	2%Pt	400, 1	Hydrothermal	16
Pt/Al ₂ O ₃	340	105,000	0.5% Pt	500, 2	Impregnation	17

References

1. M. Ma, R. Yang, Z. Jiang, C. Chen, Q. Liu, R. Albilali and C. He, *Fuel*, 2021, **303**, 121244.
2. R. Xiao, R. Qin, C. Zhang, S. Chen and J. Wang, *Journal of Rare Earths*, 2021, **39**, 817-825.
3. L. Lv, Z. Zhang, S. Wang, Y. Shan, L. Wang, T. Xu and P. He, *Catalysis Communications*, 2024, **186**, 106832.
4. Z. Fu, M. Chen, Q. Ye, N. Dong and H. Dai, *Catalysts*, 2021, **11**, 713.
5. R. Ma, X. Su, L. Jin, J. Lu and M. Luo, *Journal of Rare Earths*, 2010, **28**, 383-386.
6. M. Konsolakis, S. A. C. Carabineiro, G. E. Marnellos, M. F. Asad, O. S. G. P. Soares, M. F. R. Pereira, J. J. M. Órfão and J. L. Figueiredo, *Inorganica Chimica Acta*, 2017, **455**, 473-482.
7. M. Konsolakis, S. A. C. Carabineiro, P. B. Tavares and J. L. Figueiredo, *Journal of Hazardous Materials*, 2013, **261**, 512-521.
8. D. Delimaris and T. Ioannides, *Applied Catalysis B: Environmental*, 2009, **89**, 295-302.
9. Y. Ye, J. Xu, L. Gao, S. Zang, L. Chen, L. Wang and L. Mo, *Chemical Engineering Journal*, 2023, **471**, 144667.
10. T. Pei, L. Liu, L. Xu, Y. Li and D. He, *Catalysis Communications*, 2016, **74**, 19-23.
11. Y. Jiang, Q. Wang, J. Xu, S. Zang, L. Chen, L. Wang and L. Mo, *Catalysts*, 2023, **13**, 1400.
12. M. Bao, Y. Liu, J. Deng, L. Jing, Z. Hou, Z. Wang, L. Wei, X. Yu and H. Dai, *Catalysts*, 2023, **13**, 643.
13. L. Li, Y. Liu, J. Deng, L. Jing, Z. Hou, R. Gao and H. Dai, *Catalysts*, 2023, **13**, 676.
14. X.-W. Su, L.-Y. Jin, J.-Q. Lu and M.-F. Luo, *Journal of Industrial and Engineering Chemistry*, 2009, **15**, 683-686.
15. W. Zhang, S. Xia, C. Chen, H. He, Z. Jin, M. Luo and J. Chen, *New Journal of Chemistry*, 2021, **45**, 11352-11358.
16. K. Inoue and S. Somekawa, *Chemical Engineering & Technology*, 2019, **42**, 257-260.
17. H. Rotter, M. Landau, M. Carrera, D. Goldfarb and M. Herskowitz, *Applied Catalysis B: Environmental*, 2004, **47**, 111-126.