

1 Supporting information (SI) for

2

3 **Ultrasound-Assisted Directional Freezing Enables High-Performance**
4 **Hydrogel Evaporators with Tunable Microchannels for Solar**
5 **Desalination**

6

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18 **Preparation of PVA/CS Precursor Solution (for a 100 mL Batch)**

19 To prepare the PVA/CS precursor solution (taking 100 mL as an example), a 9
20 wt% PVA aqueous solution was first prepared by dissolving 2.25 g of PVA in 22.75
21 mL of deionized water under magnetic stirring at 90 °C for 1 hour until completely
22 dissolved. Then, a 2 wt% CS solution was prepared by adding 1.5 g of low-molecular-
23 weight chitosan to 70 mL of water, followed by the addition of 3.7 mL of phosphoric
24 acid. The mixture was stirred at 80 °C for 30 minutes until fully dissolved, after which
25 0.75 mL of phytic acid (50 wt% aqueous solution) was added and stirring was continued
26 until homogeneous. The PVA and CS solutions were then mixed thoroughly in a mass
27 ratio of 1:3 (9 wt% PVA solution to 2 wt% CS solution). Subsequently, 1.0 g of
28 conductive CB powder was added to the mixed solution and stirred thoroughly,
29 followed by ultrasonic treatment to ensure uniform dispersion. Finally, 50 wt%
30 glutaraldehyde solution was added to initiate crosslinking, and the mixture was left
31 undisturbed for 30 minutes to obtain the final PVA/CS precursor solution.

32 **Characterization**

33 The surface morphology of freeze-dried hydrogel samples was characterized using
34 a scanning electron microscope (SEM, SU3800, Hitachi, Japan). Elemental analysis of
35 the hydrogels was conducted using an energy-dispersive X-ray spectrometer (EDS,
36 Oxford Ultim Max65, UK). The pore size and its distribution were analyzed with
37 ImageJ software. The wettability of the hydrogels was evaluated using a contact angle
38 goniometer (OCA15EC, Dataphysics, Germany) with 5 μ L of deionized water as the
39 test droplet. The light absorption properties of the hydrogels were precisely measured
40 using a UV-Vis-NIR spectrophotometer (SHIMADZU UV-3600i Plus, Japan)
41 equipped with an integrating sphere over the wavelength range of 250-2500 nm. Metal
42 ion concentrations in the collected water were determined by inductively coupled
43 plasma optical emission spectrometry (ICP-OES, PerkinElmer Optima 8000). Thermal
44 behaviors such as melting and evaporation of the hydrogels were studied using
45 differential scanning calorimetry (DSC, TA-Discovery, USA), where the sample was

46 heated from 25 °C to 130 °C at a rate of 5 °C /min under a nitrogen atmosphere. The
47 state of water molecules in the hydrogel was further analyzed via Raman spectroscopy
48 (HORIBA LabRAM HR Evolution, Japan) using a 532 nm excitation wavelength. The
49 compressive mechanical properties of the hydrogels were tested using a universal
50 testing machine (UTM4103, China).

51

52 **Solar Vapor Generation (SVG) Test**

53 The solar-driven water evaporation performance was evaluated under simulated
54 sunlight using a xenon lamp (PLS-SXE 300+, Perfectlight, China), which provided an
55 output power equivalent to one sun (1 kW m⁻²). The illumination intensity was
56 monitored and calibrated using a connected power meter (PLD MOPM-I, Perfectlight,
57 China). During testing, a CPC-UA hydrogel sample with a thickness of approximately
58 1 cm was placed on a polystyrene (PS) foam support within a beaker. The water in the
59 beaker was either deionized water or contaminated water (used for purification
60 experiments). A laboratory electronic balance with a resolution of 0.1 mg (JA2003,
61 Soptop) was used to record the mass loss of bulk water. All experiments were conducted
62 under controlled environmental conditions: an ambient temperature of 21 °C and
63 relative humidity of 25 %. The evaporation rate was measured after the system reached
64 a steady state under one sun illumination for 30 minutes. Outdoor evaporation
65 experiments were performed at the Binhai Campus of Tianjin University of Science
66 and Technology from July 7 to July 9. The solar-to-vapor energy conversion efficiency
67 (η , %) was calculated using the following equation:

$$68 \quad \eta = \frac{mh_{water}}{3600I} \quad (S1)$$

69 where m (kg m⁻² h⁻¹) is the net evaporation rate after subtracting the dark evaporation
70 rate, h_{water} (kJ kg⁻¹) is the enthalpy of water evaporation, and I (kW m⁻²) is the incident
71 solar irradiance.

72

73 **Contact Angle (CA) Measurement**

74 The wettability of the hydrogel samples was evaluated using an optical contact
75 angle goniometer (Dataphysics, Germany). A 5 μ L droplet of deionized water was
76 deposited onto the hydrogel surface, and the spreading and absorption processes were
77 recorded by a high-speed camera. The reported contact angle (CA) values represent the
78 average of three measurements taken at different positions on each hydrogel surface.
79

80 **Photothermal Performance Test**

81 The photothermal properties of different samples were evaluated under one sun
82 irradiation using a xenon lamp (PLS-SXE 300+, Perfectlight, China). During
83 illumination, the surface temperature of each sample was monitored in real time using
84 an infrared thermal imaging camera (H10, HIKVISION).
85

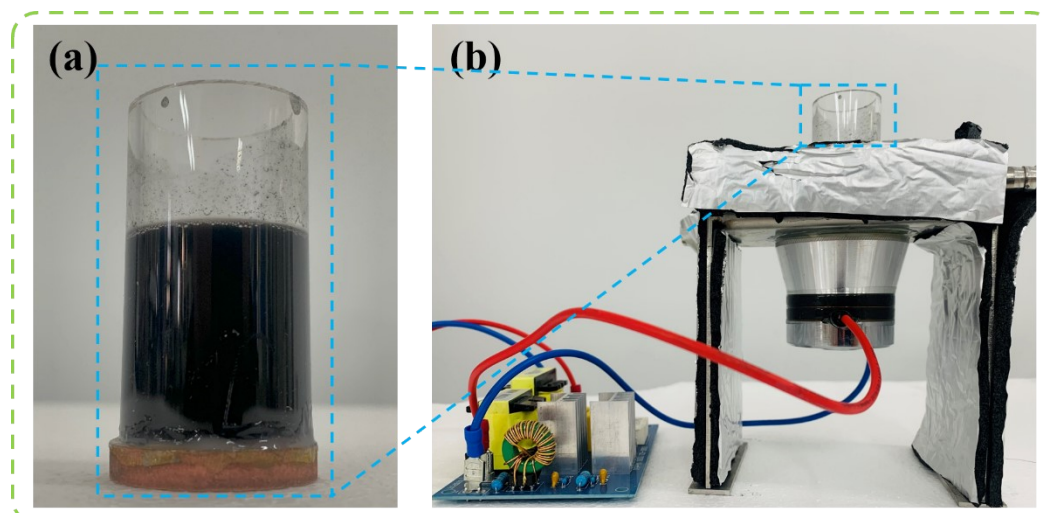
86 **Mechanical Compression Test**

87 The compressive properties of the hydrogel samples were evaluated using a
88 universal testing machine (UTM4103, China) at a loading rate of 1 mm/s. The stress-
89 strain behavior was recorded under varying strain conditions.
90

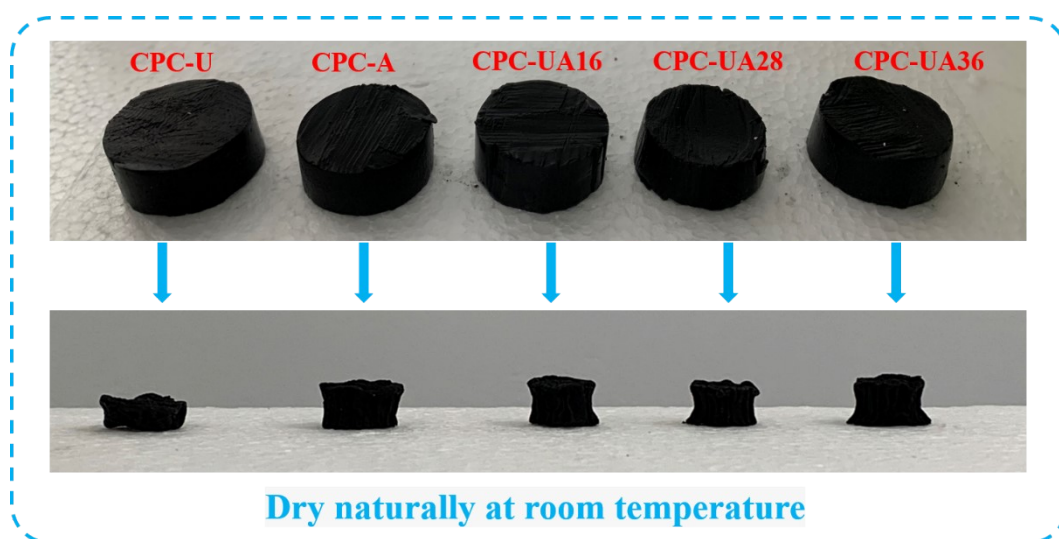
91 **Salt Tolerance and Performance in Dye and Acid/Base Solutions**

92 To simulate seawater with different salinities, NaCl solutions with varying
93 concentrations (3.5, 7, 10, 15, 20, and 25 wt%) were prepared. The evaporation devices
94 containing different hydrogel samples were placed in these solutions for testing.

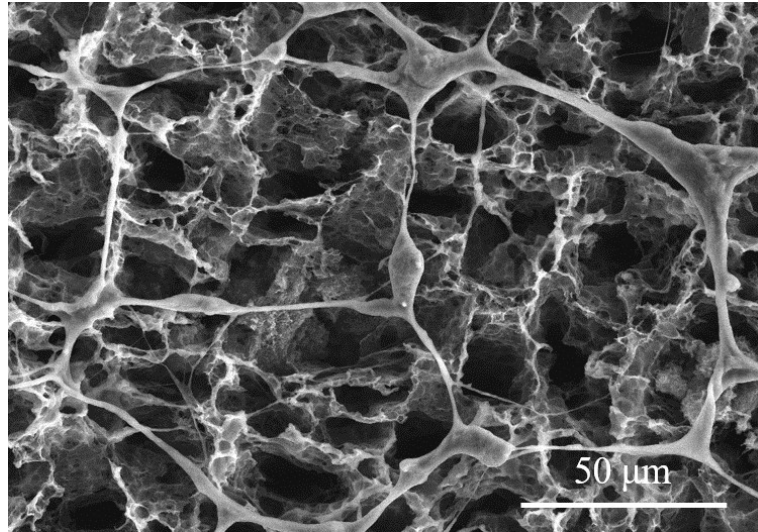
95 For organic pollutant removal tests, three typical industrial dyes—methylene blue
96 (MB), methyl orange (MO), and rhodamine B (RhB) were each dissolved to form 2
97 vol% solutions. Additionally, 1 mol/L NaOH and 1 mol/L HCl solutions were prepared
98 to evaluate the chemical stability of the hydrogels under strong alkaline and acidic
99 conditions. The evaporation performance was tested following the same procedures as
100 described above, with the saline solution replaced by the corresponding test liquids.



102
 103 **Figure S1.** (a) Photograph of the mold containing hydrogel. (b) Photograph of the
 104 directional freezing apparatus.

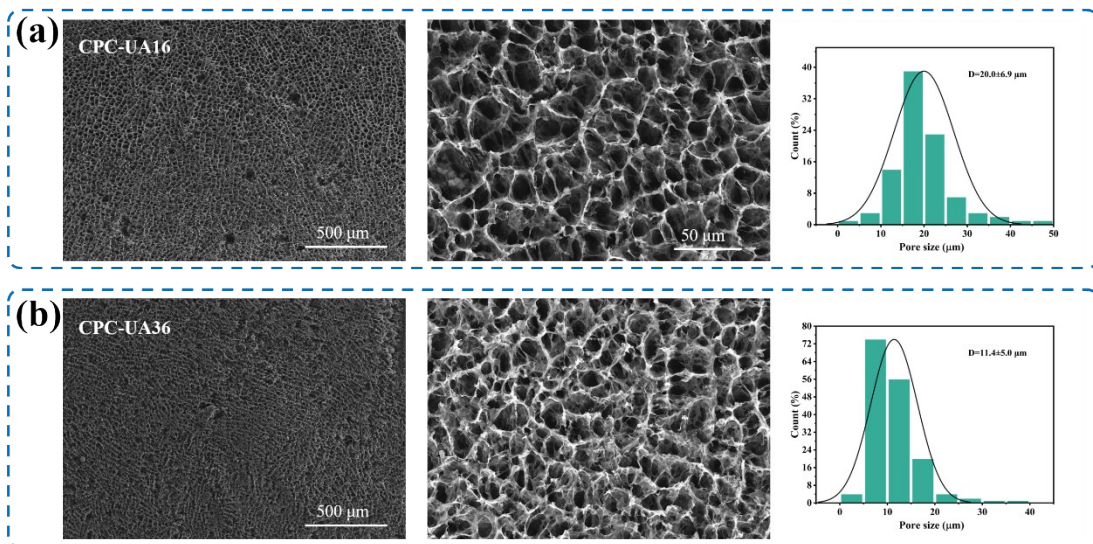


105
 106 **Figure S2.** Photographs of hydrogel samples before and after drying at room
 107 temperature.



108

109 **Figure S3.** SEM images of hydrogels prepared by ultrasound-assisted directional
110 freezing.

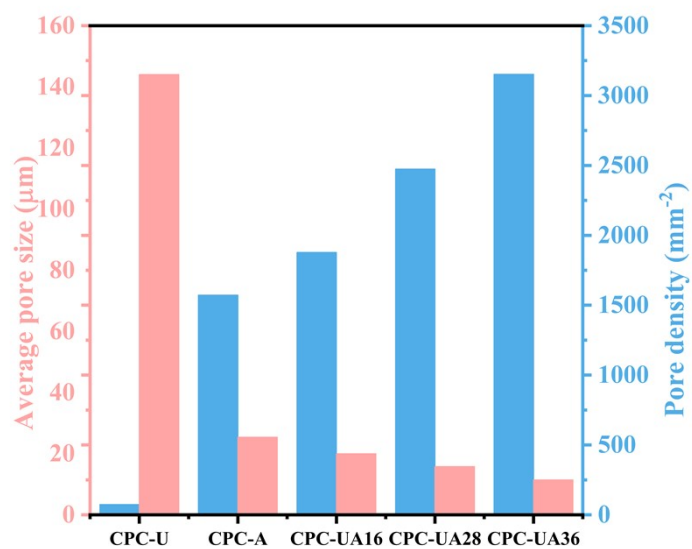


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112 **Figure S4.** (a) SEM micrograph and pore size distribution of CPC-UA16. (b) SEM

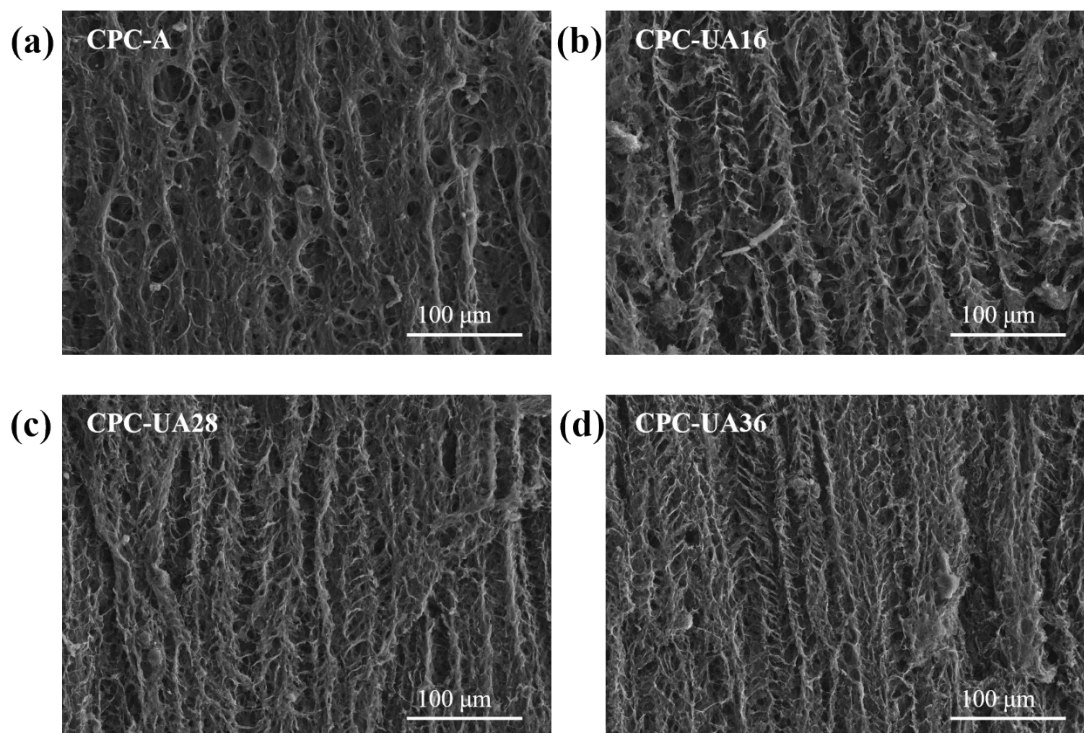
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micrograph and pore size distribution of CPC-UA



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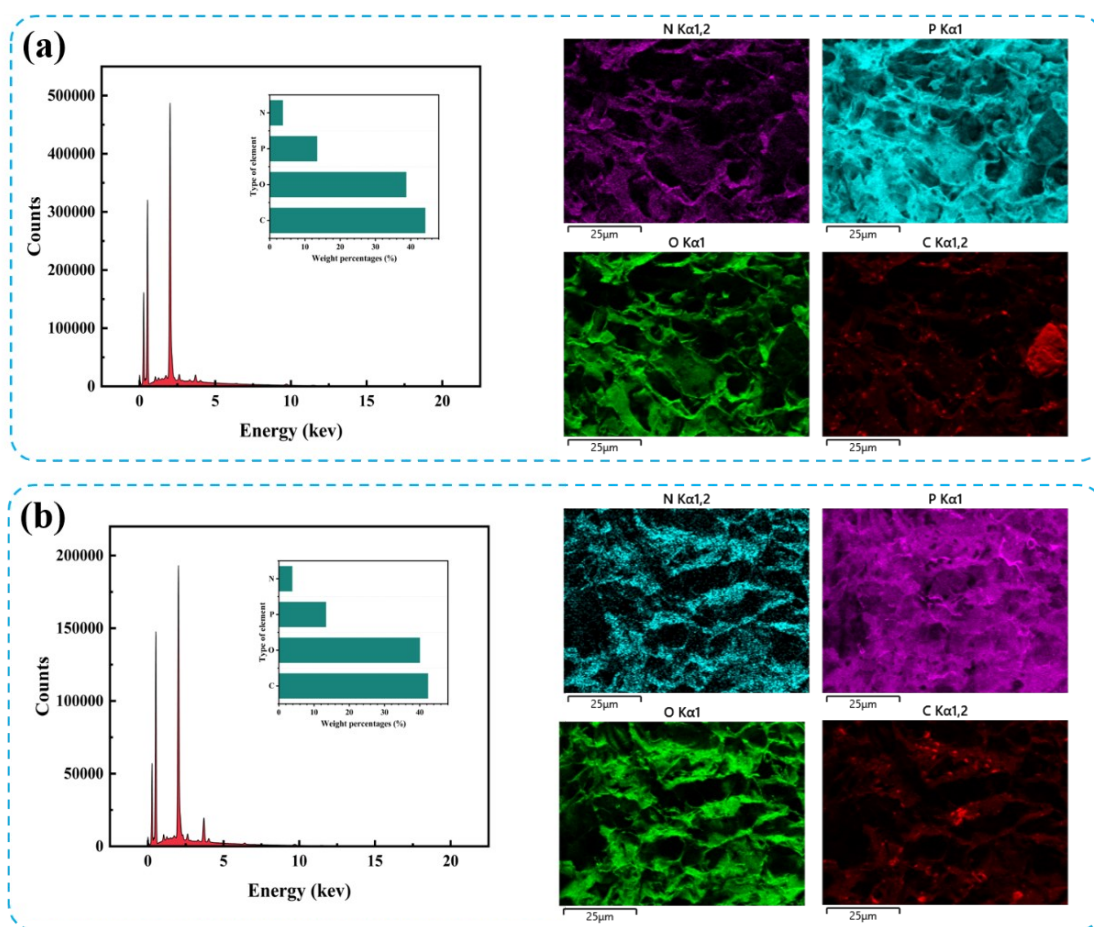
115 **Figure S5.** Pore size distribution and pore density of the hydrogels.



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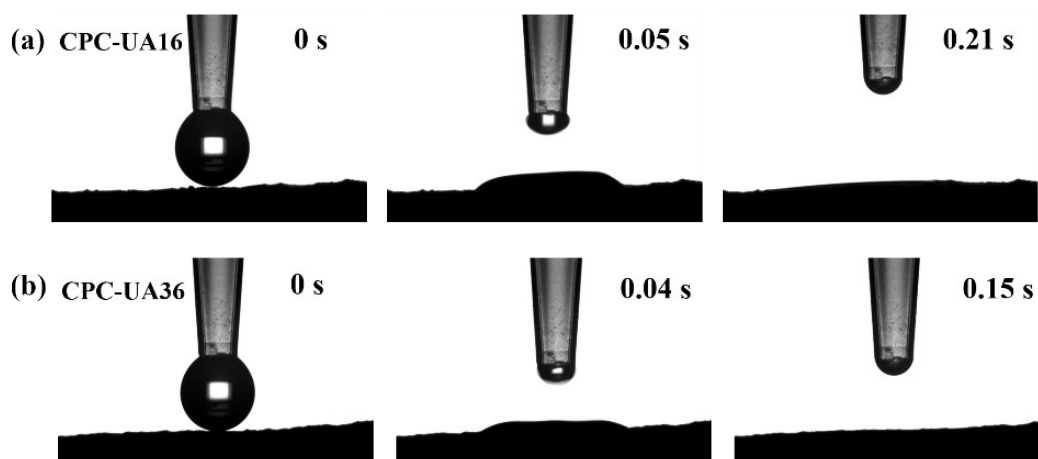
117 **Figure S6.** SEM cross-sectional images of vertically sliced hydrogels: (a) CPC-A, (b)

118 CPC-UA16, (c) CPC-UA28, (d) CPC-UA36.



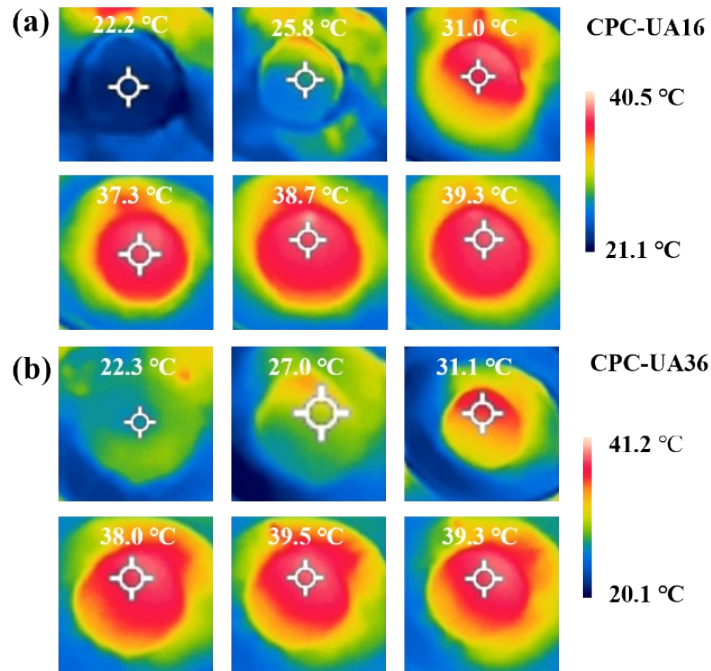
119

120 **Figure S7.** (a) EDS mapping and elemental distribution of CPC-A. (b) EDS mapping
121 and elemental distribution of CPC-UA28.



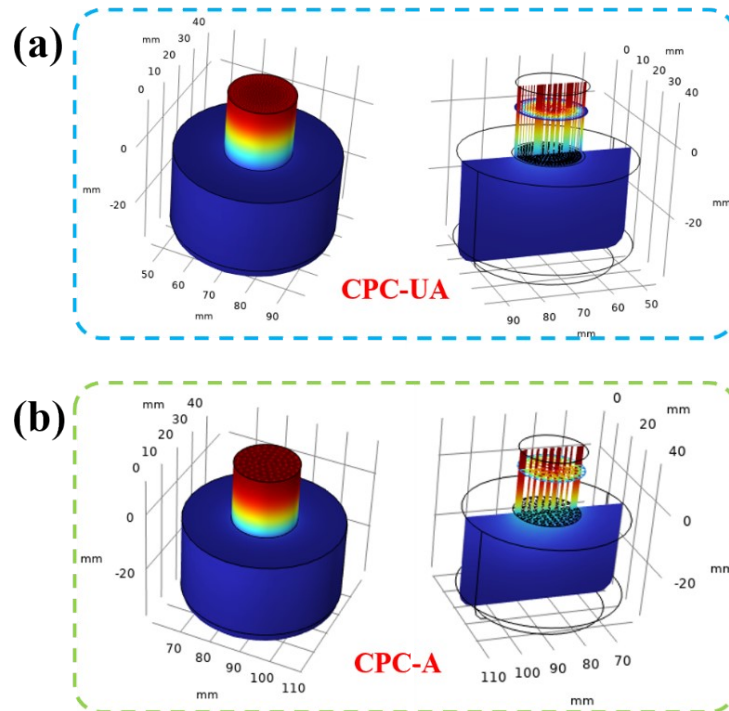
122

123 **Figure S8.** Contact angle images of: (a) CPC-UA16, (b) CPC-UA36.



124

125 **Figure S9.** Infrared thermographic images of: (a) CPC-UA16, (b) CPC-UA36.



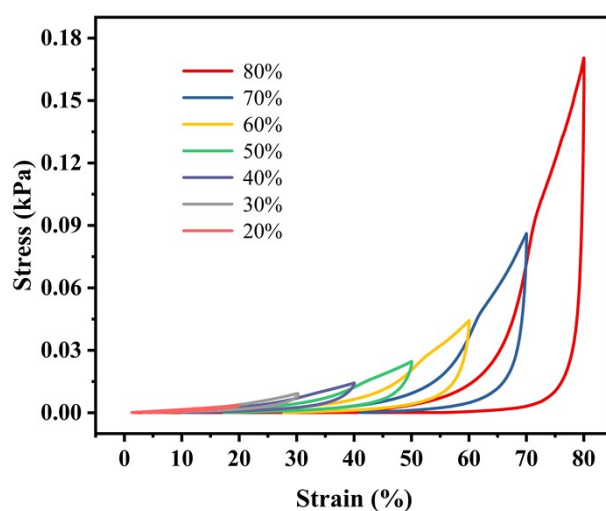
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127 **Figure S10.** (a, b) Simulated temperature distribution and cross-sectional view of CPC-
128 UA and CPC-A by COMSOL.



129

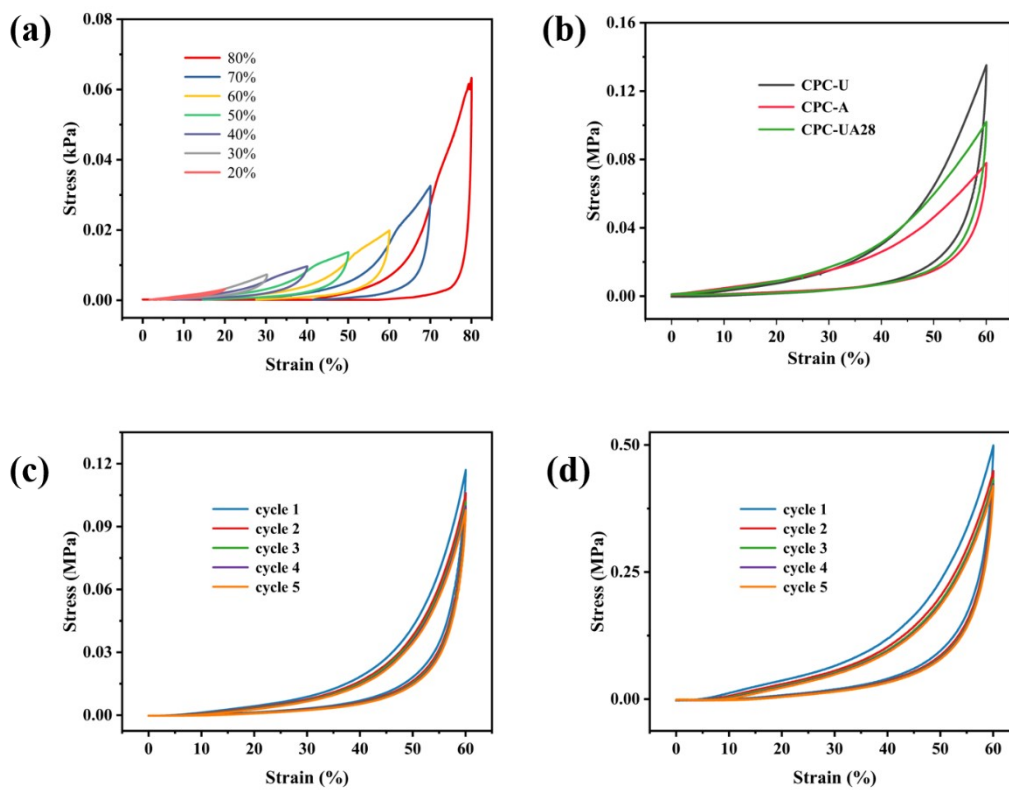
130 **Figure S11.** Macroscopic compression images of CPC-U, CPC-A, and CPC-UA28.



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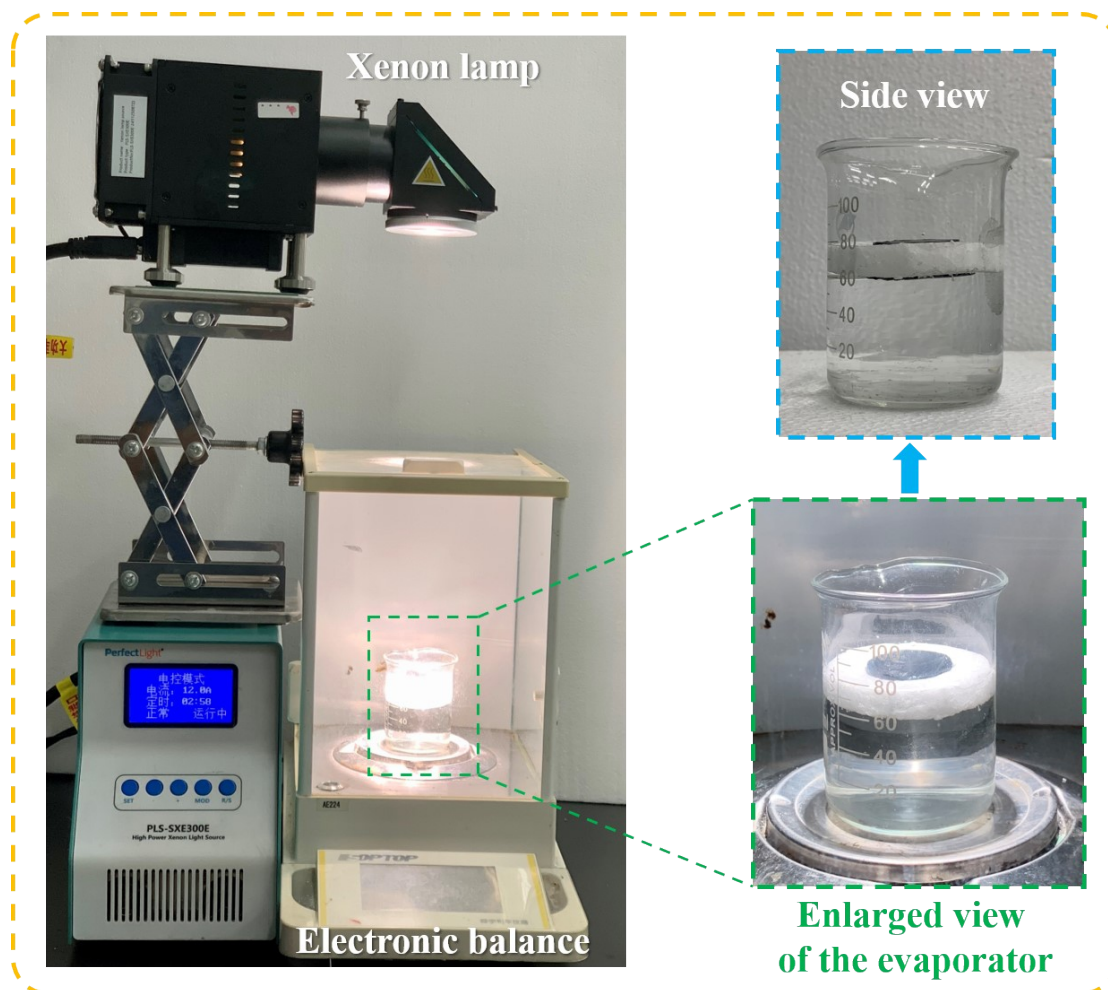
132 **Figure S12.** Stress–strain curves of CPC-UA28 under loading and unloading with

133 strain increments of 10% up to 80%.



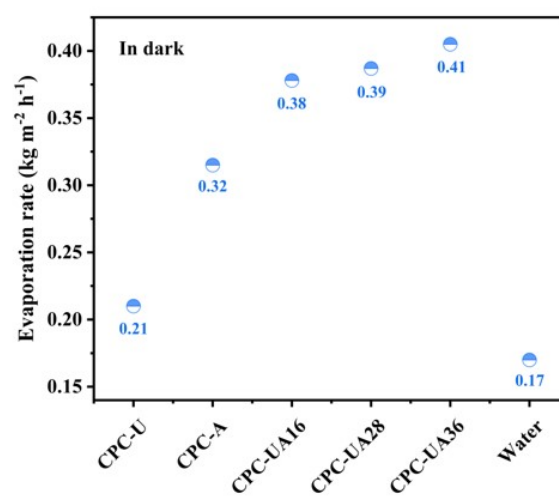
134

135 **Figure S13.** (a) Stress–strain curves of CPC-A under stepwise loading/unloading from
 136 10% to 80% strain. (b) Comparison of compressive stress–strain curves of CPC-U,
 137 CPC-A, and CPC-UA28 under 0-60% strain. (c) Cyclic compressive stress–strain
 138 curves of CPC-U at a fixed strain of 60%. (d) Cyclic compressive stress–strain curves
 139 of CPC-A at a fixed strain of 60%.



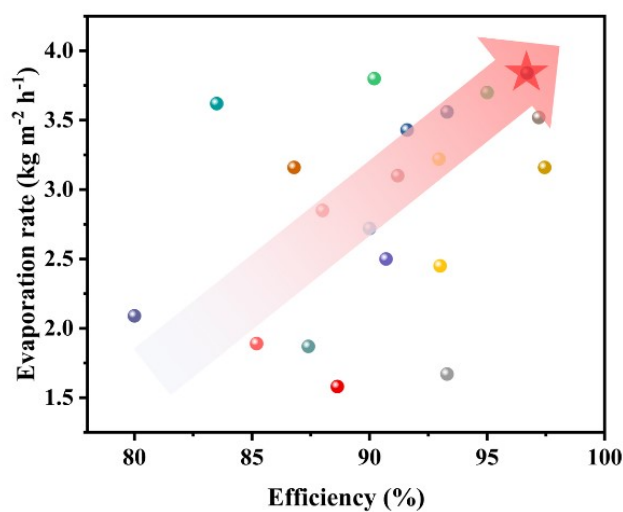
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141 **Figure S14.** Photographs of the indoor test setup and interfacial evaporation system.



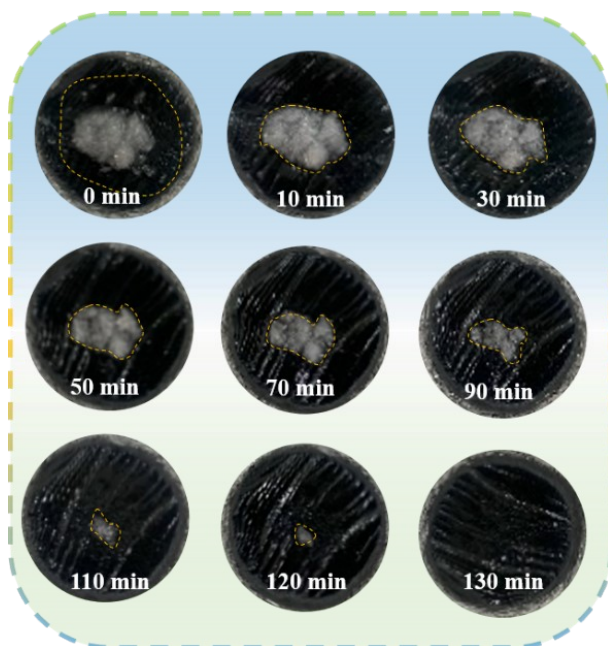
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143 **Figure S15.** Evaporation rates of various hydrogels under dark conditions.



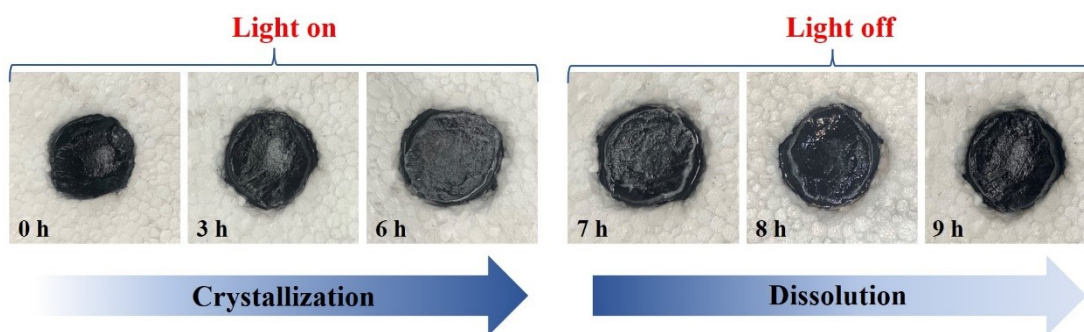
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145 **Figure S16.** Comparison of evaporation rate and solar evaporation efficiency of
 146 different hydrogels under 1 sun illumination.



147

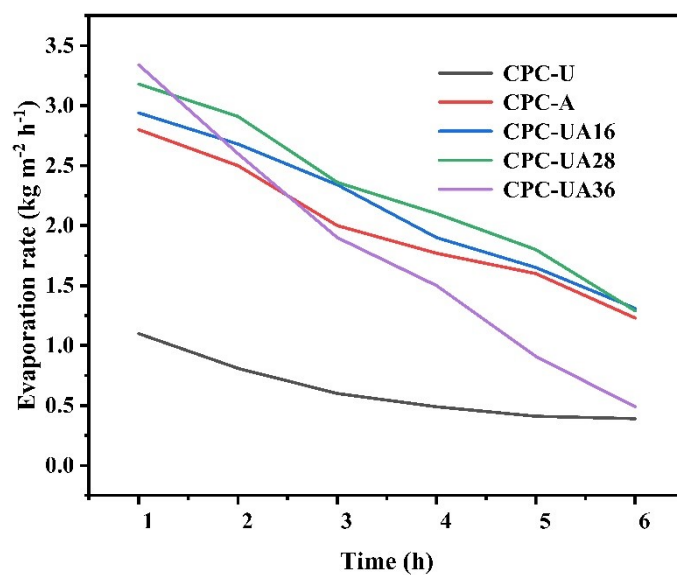
148 **Figure S17.** Dissolution process of 1 g NaCl on the surface of CPC-UA28 hydrogel.



149

150 **Figure S18.** Photographs of salt crystallization and dissolution on CPC-UA36 during

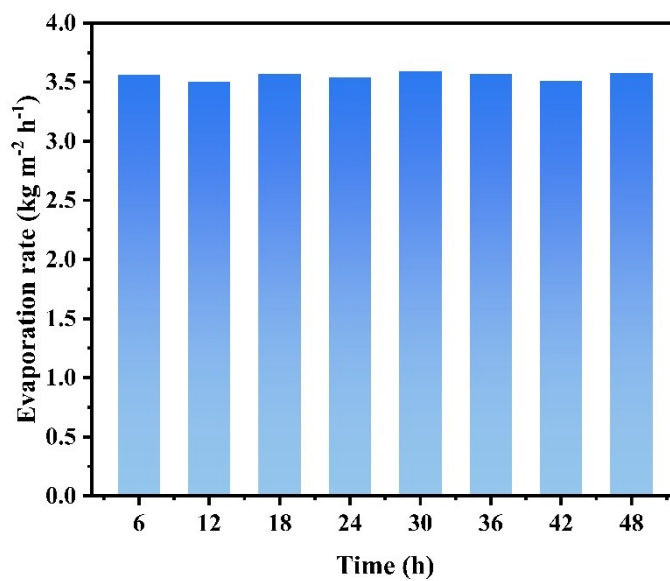
151 evaporation in 25 wt% saline water under one-sun illumination.



152

153 **Figure S19.** Variation of evaporation rates of different hydrogels in 25 wt% saline

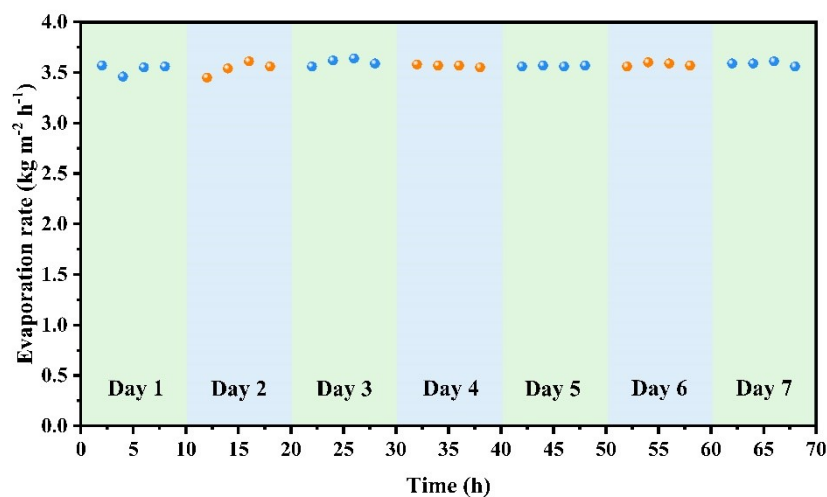
154 water under one-sun illumination.



155

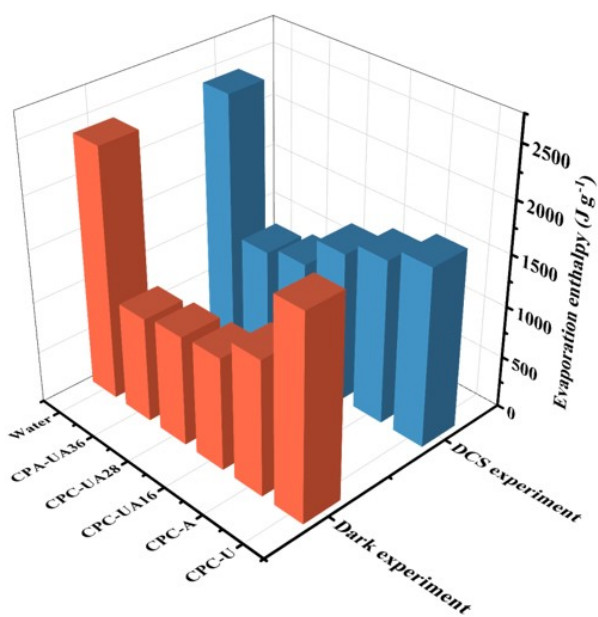
156 **Figure S20.** Evaporation rate variation of CPC-UA28 during continuous 48 h

157 seawater evaporation under one-sun illumination.



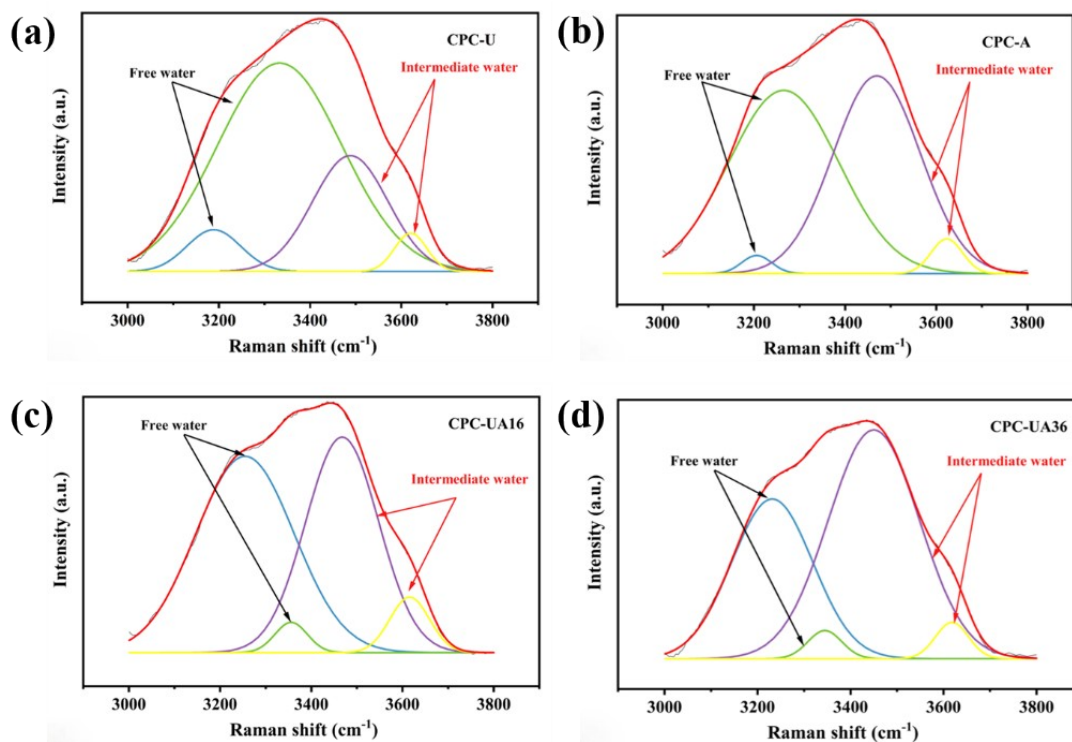
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159 **Figure S21.** Seven-day cycling stability test of CPC-UA28 in seawater under one-sun
 160 illumination, with each cycle lasting 8 h.



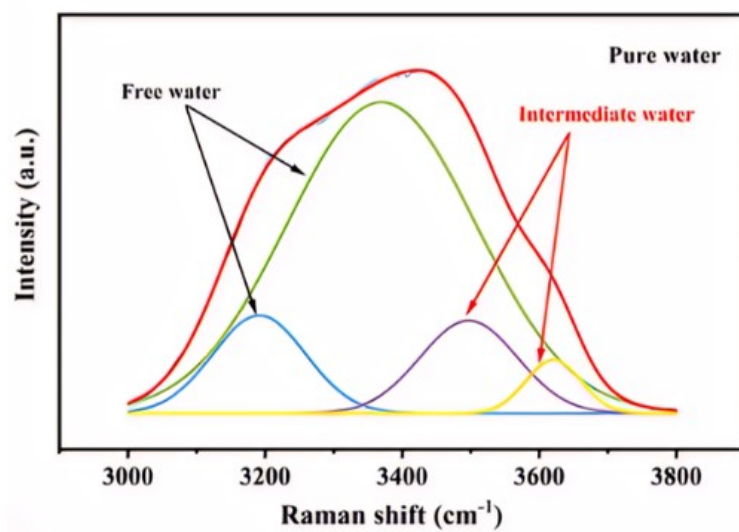
161

162 **Figure S22.** Comparison between DSC-derived evaporation enthalpy and dark-
 163 condition-derived evaporation enthalpy of various hydrogels.



164

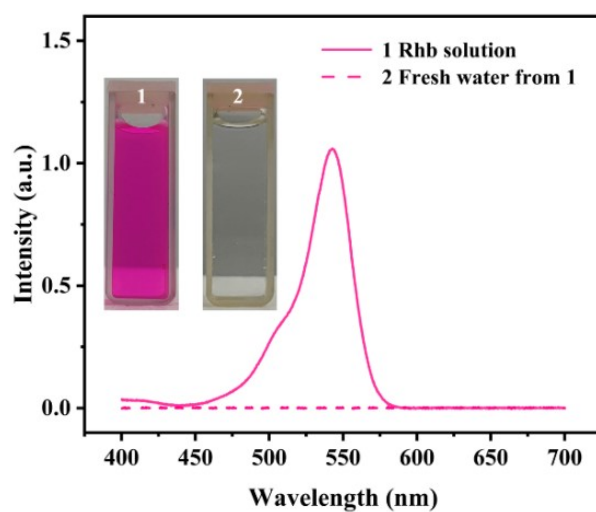
165 **Figure S23.** Raman spectra of: (a) CPC-U, (b) CPC-A, (c) CPC-UA16, (d) CPC-UA36.



$$\text{IW/FW} = 0.1768$$

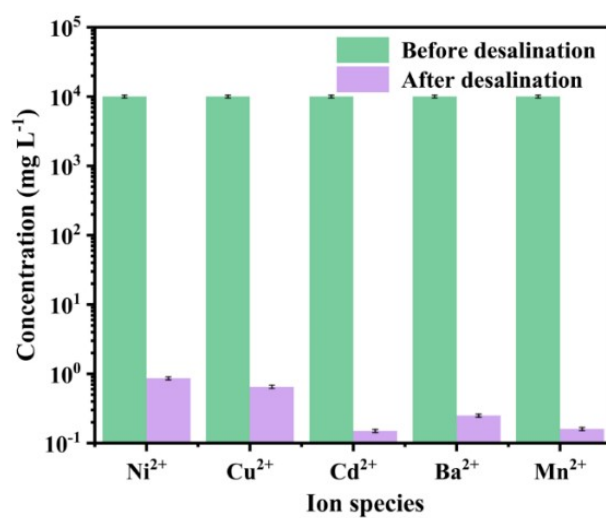
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167 **Figure S24.** Raman spectrum of pure water and the IW/FW ratio.



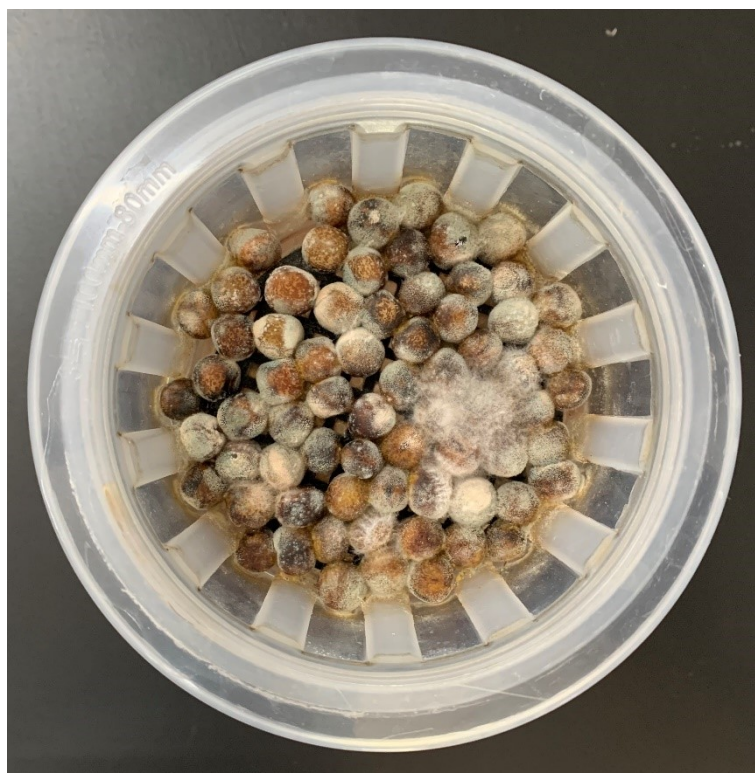
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169 **Figure S25.** UV-vis absorption spectra of Rhodamine B (RhB) contaminated water and
 170 the collected distilled water.



171

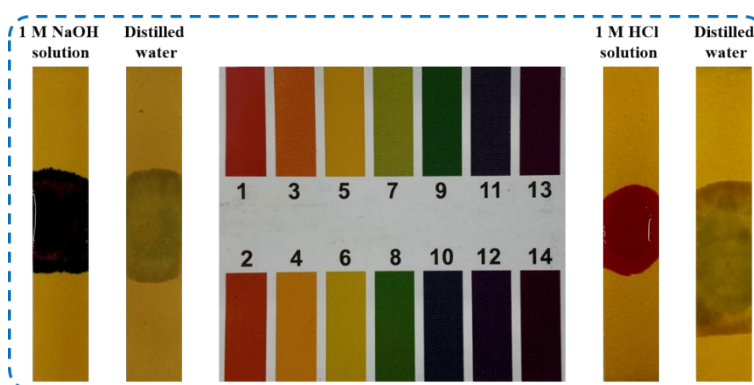
172 **Figure S26.** Heavy metal ion concentrations in simulated wastewater before and after
 173 solar desalination.



174

175 **Figure S27.** Photograph of mildew in peas farmed with seawater.

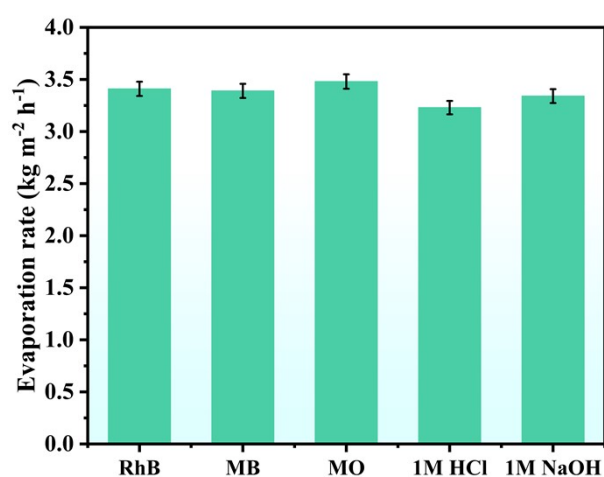
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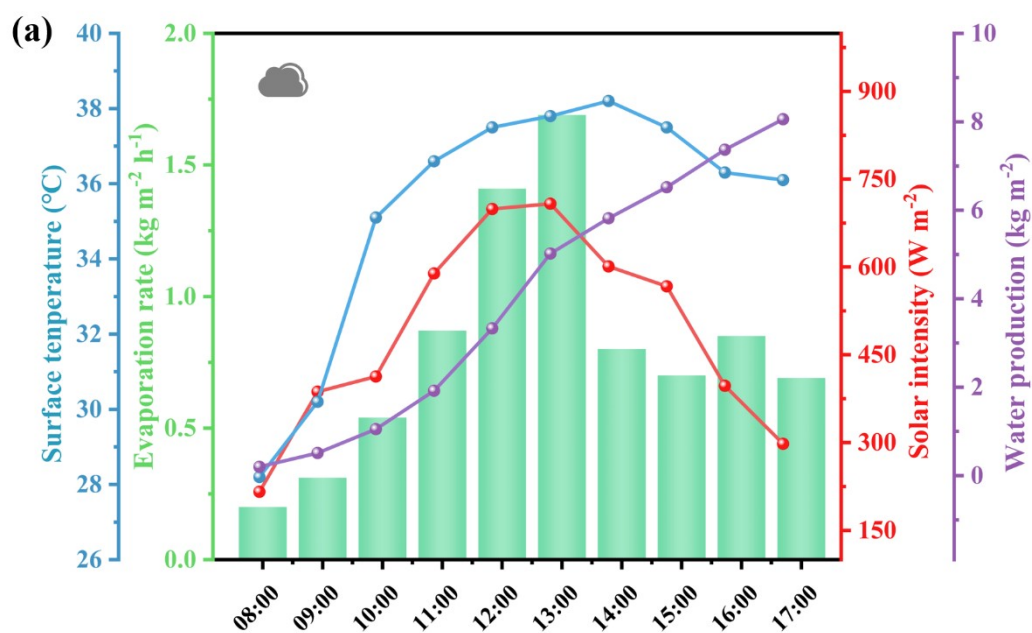
178 **Figure S28.** Photographs showing the pH values of 1 M NaOH, 1 M HCl, and distilled

179 water.



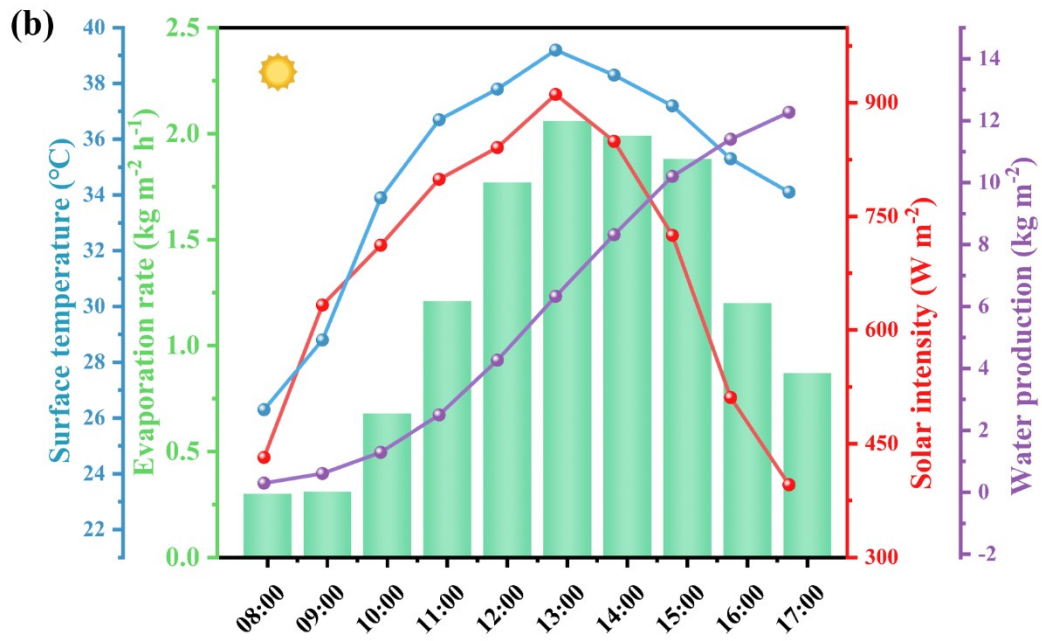
180

181 **Figure S29.** Evaporation rates of CPC-UA28 in different dye wastewater and acid/base
182 solutions.



183

184



185

186 **Figure S30.** In the outdoor experiments on July 8 (a) and 9 (b), 2025, CPC-UA28

187 recorded freshwater production, cumulative freshwater production, surface

188 temperature, evaporation rate, and light intensity.

189

190 **Table S1 Tensile mechanical properties of hydrogels.**

191

Name	Tensile strength(MPa)	Elastic modulus(MPa)	Elongation at break(%)
CPC-U	0.08	0.06	135.2
CPC-A	0.11	0.08	176.4
CPC-UA28	0.13	0.09	181.9

192

193 **Table S2 Comparison of Evaporation Rate and Efficiency of CPC-UA28 with**
 194 **Reported Hydrogel-Based Evaporators under One Sun Irradiation.**

195





Entry	Photothermal material	Evaporation rate (kg m ⁻² h ⁻¹)	Efficiency (%)	Reference in SI
1	Directed ultrasound freezing of CB/PVA-CS hydrogels	3.84	96.7	This work
2	CB/Nano-silica PVA-CS	1.58	88.63	[1]
3	AC/Janus PVA-AG	3.56	93.3	[2]
4	3D LSC5/PVA-CS	2.45	93.0	[3]
5	CNTs-PVA/TOCNFs/SLS	3.70	95.0	[4]
6	Carbon nanotube PVA/SLS	2.09	80.0	[5]
7	PVA/CS/GO-Ag-4%EfMs	1.67	93.3	[6]
8	PVA biochar hydrogels	1.89	85.2	[7]
9	Janus PSPH@CP	2.72	90.0	[8]
10	CNTs and Chinese ink cellulose/PVA	3.16	86.79	[9]
11	MXene/rGO-embedded	3.62	83.5	[10]

	hybrid hydrogels			
	δ -MnO ₂ -PVA composite			
12	hydrogels	2.5	90.7	[11]
13	PVA-CB	3.52	97.2	[12]
14	MWCNTs/PVA-agar	3.1	91.2	[13]
15	3D-GO/PVA	1.87	87.4	[14]
16	3D PVA/PDA	3.16	97.45	[15]
	PVA fabric interpenetrating			
17	composite hydrosponges	2.85	88	[16]
18	ACNTs-PDA/PVA PPCHs	3.43	91.6	[17]
19	MoS ₂ -PVA/P(SA)	3.22	92.95	[18]
20	CNPs-PVA/CS	3.80	\	[19]

196

197 **Table S3 Average pore size and salt crystallization rate of different hydrogels.**

198

Name	Pore structure	Average pore size(μ m)	Salt Accumulation
CPC-U	Random Porous Network	144	
CPC-A	Vertical Channel	25.36	
CPC-UA16		19.97	
CPC-UA28		15.79	



199

200 **Table S4 Comparison of Enthalpy of Vaporization Measured by DSC and**
 201 **Estimated from Dark Evaporation Experiments.**

202

Evaporation enthalpy(J/g)	CPC-U	CPC-A	CPC- UA16	CPC- UA28	CPC- UA36	Pure water
DSC measurement	1726.1	1588.2	1447.7	1148.6	1069.9	2375
Dark experiment	1956.6	1304.4	1087	1061.7	1014.5	2417

203

204 **Note S1 Calculation of Dark Evaporation Enthalpy**

205 Since all CPC-series hydrogels are nearly fully hydrated during the solar-driven
 206 interfacial evaporation process, the energy required for water evaporation primarily
 207 includes the vaporization enthalpy of free water and intermediate water, which is
 208 theoretically lower than the value for bulk water. To determine the dark evaporation
 209 enthalpy, we designed a control experiment in which each hydrogel sample and pure
 210 water (with identical exposed evaporation areas) were placed in sealed, completely dark
 211 containers. The environmental conditions were maintained at a constant humidity of
 212 25% and temperature of 21°C. The dark evaporation rate of each sample was then used
 213 to estimate the equivalent evaporation enthalpy. As the total energy input into the pure
 214 water and hydrogel systems is assumed to be equal in the dark environment, the dark
 215 evaporation enthalpy of the hydrogels can be calculated using the following equation:

216
$$U_{in} = h_1 m_1 = h_2 m_2 \quad (S2)$$

217 Where h_1 and m_1 are the evaporation enthalpy and mass loss of pure water, respectively,
 218 m_2 is the mass loss of the hydrogel sample, h_2 is the calculated dark evaporation
 219 enthalpy of the hydrogel.

220

221 **Note S2 Calculation of Heat Loss**

222 In general, heat loss during the interfacial evaporation process consists of three
223 components: conductive heat loss, convective heat loss, and radiative heat loss. The
224 calculations are as follows:

225 **(1) Conductive heat**

$$226 \quad Q_{cond} = Cm\Delta T_b \quad (S3)$$

227 Where Q_{cond} is the conductive heat loss, C is the specific heat capacity of water (4.2 kJ
228 $^{\circ}\text{C}^{-1} \text{ kg}^{-1}$), m is the mass of water (fixed at 60 g), ΔT_b is the temperature rise of the bulk
229 water.

230 **(2) Convective heat**

231 Convective heat loss is calculated based on Newton's law of cooling:

$$232 \quad Q_{conv} = hA\Delta T_c \quad (S4)$$

233 Where Q_{conv} is the convective heat flux, h is the convective heat transfer coefficient
234 (assumed to be $\sim 5 \text{ W m}^{-2} \text{ K}^{-1}$), A is the evaporation area (fixed at $0.314 \times 10^{-3} \text{ m}^2$),
235 ΔT_c is the temperature difference between the material's evaporating surface and the
236 ambient air just above the absorber.

237 **(3) Radiative heat**

238 Radiative heat flux is calculated using the Stefan–Boltzmann equation:

$$239 \quad \Phi = \varepsilon A \sigma (T_1^4 - T_2^4) \quad (S5)$$

240 Where Φ is the radiative heat flux, ε is the surface emissivity (assumed to be 1 during
241 evaporation), σ is the Stefan–Boltzmann constant ($5.67 \times 10^{-8} \text{ W m}^{-2} \text{ K}^{-4}$), T_1 is the
242 steady-state surface temperature of the hydrogel under one sun irradiation, T_2 is the
243 ambient temperature above the absorber.

244

245 **Note S3 COMSOL simulation**

246 The heat transfer process during evaporation in CPC-UA and CPC-A was
247 simulated using the Heat Transfer Module in COMSOL Multiphysics 6.3. A three-
248 dimensional model was first constructed in SolidWorks based on the actual dimensions

of the laboratory evaporation device and then imported into COMSOL Multiphysics 6.3 for simulation. A constant solar irradiance of 1 kW m^{-2} was applied to the top surface of the evaporator to drive the evaporation process. The inflow water flux into the evaporator was set equal to the outflow caused by evaporation. The boundary conditions were defined as follows: ambient temperature and initial water temperature were both set to $20 \text{ }^{\circ}\text{C}$ (293.15 K); the natural convective heat transfer coefficient was set to $5 \text{ W m}^{-2} \text{ K}^{-1}$; and the solar absorption efficiency was set at 95%. The density, specific thermal conductivity of CPC-UA were 0.2163 g cm^{-3} , $3.137 \text{ J g}^{-1} \text{ K}^{-1}$ and $0.5097 \text{ W m}^{-1} \text{ K}^{-1}$, respectively. The density, specific thermal conductivity of CPC-A were 0.2011 g cm^{-3} , $3.206 \text{ J g}^{-1} \text{ K}^{-1}$ and $0.4835 \text{ W m}^{-1} \text{ K}^{-1}$, respectively. Based on these boundary and material parameters, the temperature distribution in the 3D COMSOL model was simulated using the following governing equations:

$$Q_{in} = \rho C_p \frac{\partial T}{\partial t} + \rho C_p u \nabla T + \nabla q \quad (\text{S6})$$

$$q = -k \nabla T \quad (\text{S7})$$

Where Q_{in} is the heat input from solar radiation, ρ , C_p , and k are the material's density, specific heat capacity, and thermal conductivity, respectively, $T(x, t)$ is the local temperature distribution as a function of space and time, u is the fluid velocity vector, q is the heat flux vector. The simulation was carried out under a steady-state analysis mode in COMSOL Multiphysics 6.3. Heat convection at the top surface of the evaporator in contact with air was corrected using Newton's law of cooling.

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