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Supporting Information

Dual Atom Cu-Fe Ensemble Sites for Enhanced Efficiency of Green Ammonia Production from Tandem Electrochemical Nitrate Reduction Process

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Keywords

Green ammonia, Nitrate reduction, Dual atom catalyst, Tandem reaction, Synergistic effect.

1. Experimental section

1.1. Chemicals and materials

Potassium nitrite (KNO₂, Sigma Aldrich), potassium nitrate (KNO₃, Sigma Aldrich), potassium hydroxide (KOH, Sigma Aldrich), carbon paper (AvCarb P50T, NARA Cell-Tech Corp.), Iron(III) nitrate nonahydrate (Fe(NO₃)₃ 9H₂O, Sigma Aldrich), Copper(II) nitrate trihydrate (Cu(NO₃)₂ 3H₂O, Sigma Aldrich), D-(+) Glucose (C₆H₁₂O₆, JUNSEI), Melamine (C₃H₆N₆, Sigma Aldrich), sodium hypochlorite aqueous solution (NaClO 6~14%, Sigma Aldrich), sodium nitroferricyanide (Na[Fe(NO)(CN)₅], Sigma Aldrich), Sodium citrate dihydrate (C₆H₉Na₃O₉, Sigma Aldrich), N-(1-naphthyl) ethyldiamine dihydrochloride (C₁₂H₁₄N₂, Sigma Aldrich), sulfonamide (Sigma Aldrich), orthophosphoric acid (H₃PO₄, Sigma Aldrich), hydrochloric acid (HCl, Sigma Aldrich) and Nafion 212 membrane (Fuel Cell store) were purchased from the specified suppliers. Deionized water (DI water, 18 MΩ cm, Millipore) was used for entire experimental steps.

1.2 Synthesis of Activated Carbon (AC)

About 15 g of Vulcan X72R carbon was added to a round bottom flask with a heating mantle equipped with a reflux condenser, 300 mL of a solution obtained by diluting distilled water and 65% HNO₃ 1:1 was added. The prepared mixture was stirred at 60°C for 6 hours. And washing was performed using a large amount of water, and a freeze dryer was used for 3 days, and the name of the obtained black powder was AC.

1.3 Synthesis of Cu-Fe DAC

In total, 180 mg of AC, 0.45 mmol copper (II) nitrate trihydrate, 0.45 mmol Iron (III) nitrate hexahydrate, and 18 mmol of α-D-glucose were dispersed in 15 mL of distilled water and sonicated for 45 min to get a homogenous black suspension. After several washes with water using a centrifuge, the slurry was harvested and dried overnight in a vacuum oven at 60°C. The black powder and melamine were mixed at a mass ratio of 1:5. The mixed powder was placed in a tube furnace and stayed at 800°C at Ar atmosphere with ramping rate 5°C/min, naturally cooled down to the room temperature. The obtained black powder was named Cu-Fe DAC. The Cu SAC was using 0.9 mmol copper (II) nitrate trihydrate, Fe SAC was using Iron (III) nitrate hexahydrate, and the rest of procedure were same.

1.4 Catalyst characterizations

Scanning electron microscopy (SEM) images were collected using HITACHI S-4800 instrument operated at 5 kV. High-resolution transmission electron microscopy (HR-TEM) with element mapping analysis was performed using JEM-2200FS instrument operated at 200 kV. X-ray diffraction (XRD) data were collected on a Bruker-Advanced D8 diffractometer using a Cu K α (λ = 1.5418 Å) radiation operated at 40 kV and 100 mA. High-performance X-ray photoelectron spectrometer (HP-XPS, K-ALPHA+) was used in order to obtain the XPS spectra of the surface elements. The synchrotron EXAFS and XANES spectra of Cu K-edge and Fe K-edge were obtained on the 7D, 8C, 10C beamline of the Pohang Accelerator Laboratory (PLS-II), Republic of Korea.

1.5 Electrochemical measurements

The electrochemical measurements were performed in three electrodes H-type cell which was separated by Nafion 212 membrane into two compartments. Cu-Fe DAC, Cu SAC and Fe SAC catalysts deposited on carbon paper (geometric area = 1 cm x 1 cm) were used as the working electrode. Pt coil and Hg/HgO (1 M NaOH) electrode were used as the counter and reference electrodes, respectively. The potential was converted to RHE by the following equation:

$$E (vs RHE) = E (vs Hg/HgO) + 0.140 V + 0.0591 \times pH$$

A ZIVELAB potentiostat was used to record the electrochemical response. Linear sweep voltammetry (LSV) was carried out from 0 V to -1.6 V vs Hg/HgO at a scan rate of 20 mV s⁻¹. For electrocatalytic nitrate reduction, 10 mL of 1 M KOH aqueous solution was filled in the anode compartment, and 10 mL of 1 M KOH aqueous solution containing 0.1 M KNO₃ was filled in the cathode compartment. The chronoamperometry tests were conducted at constant potentials for 1 h at room temperature. For stability test, the chronoamperometry was performed 6 times at -0.53 V vs RHE for 1 h each. The products obtained from the electrochemical NO₃-reduction were detected and analyzed by UV-visible spectroscopy (Agilent Technologies Cary 8454) using indophenol blue method and Griess method.

1.6 Ammonia (NH₃) detection by Indophenol blue method

0.05 mL of electrolyte was diluted to 10 mL (200 times) using 1 M KOH solution for the detection. Then, 2 mL of 1 M NaOH solution containing 5 wt% salicylic acid and 5 wt% sodium citrate was prepared, followed by addition of 1 mL of 0.05 M NaClO and 0.01 mL of 1 wt% sodium nitroferricyanide aqueous solution. After 2 hours at room temperature, the absorbance of solution was detected by UV–visible spectroscopy (Agilent Technologies Cary 8454). The absorbance at a wavelength of 655 nm was used to calculate the ammonia concentration. The calibration curve was obtained by using the ammonium chloride aqueous solutions of known concentration.

1.7 Nitrite (NO₂-) detection by Griess method

The Griess color reagent was prepared by N-(1-naphthyl) ethylenediamine dihydrochloride (0.04 g), sulfonamide (0.8 g), and H₃PO₄ (85%, 2 mL) into DI water (10 mL). Before the test, 100 μL of electrolytes were mixed with 100 μL of HCl. The neutral solutions were diluted to 2 mL and then mixed with the 40 μL of Griess agent. After 10 minutes at room temperature, the absorbance of solution was detected by UV–visible spectroscopy (Agilent Technologies Cary 8454). The absorbance at a wavelength of 540 nm was used to calculate the nitrite concentration. The calibration curve was obtained by using the potassium nitrite aqueous solutions of known concentration.

1.8 Calculation of the NH₃ faradaic efficiency and yield

The NH₃ faradaic efficiency was calculated as follows:

$$NH_3 Faradaic \, efficiency = (n \times F \times C_{NH_3} \times V)/Q \times 100\%$$

The yield of NH₃ was calculated as follows:

$$NH_3$$
 yield $(\mu g \ cm^{-1} \ h^{-1}) = (C_{NH_2} \times V \times M_{NH_2})/(t \times A)$

 C_{NH_3} is the concentration of NH₃ (µg/mL), n is 8 which is the number of electrons transferred to generate 1 mol NH₃, F is the Faradaic constant (96485 C/mol), V is the volume of electrolyte, Q is the total electric charge passing through the electrode, M_{NH_3} is the molar mass of NH₃, t is the reaction time. A is the surface area of catalyst.

1.9 Calculation of the NO₂- faradaic efficiency

The NH₃ faradaic efficiency was calculated as follows:

$$NO_2^-$$
 Faradaic efficiency = $(n \times F \times C_{NO_2^-} \times V)/Q \times 100\%$

 ${}^{C}_{NO_2}^{-}$ is the concentration of NO_2^{-} (µg/mL), n is 2 which is the number of electrons transferred to generate 1 mol NO_2^{-} , F is the Faradaic constant (96485 C/mol), V is the volume of electrolyte, Q is the total electric charge passing through the electrode.

1.10 Computational Methods

Activated carbon-supported single-atom catalysts (SACs) containing Fe or Cu coordinated by four nitrogen atoms, as well as a dual-atom catalyst (DAC) containing Cu–Fe coordinated by six nitrogen atoms, were constructed to model the active sites for nitrate reduction reaction (NO₃RR). Spin-polarized plane-wave density-functional-theory (DFT) calculations were carried out with the Quantum ESPRESSO suite¹. The ion-electron interactions were treated using projector augmented wave (PAW) method². Exchange–correlation energies were evaluated within the generalized-gradient-approximation (GGA) using the functional Perdew–Burke–Ernzerhof (PBE), and the van der Waals interaction was included using the Grimme-D3 dispersion correction³⁻⁵. Pseudopotentials were selected from the Standard Solid-State Pseudopotential (SSSP) library⁶.

A kinetic energy cutoff of 520 eV for the plane-wave expansion was set, and The Brillouin zones were sampled by the Monkhorst–Pack k-points mesh of $3\times3\times1^7$. The convergence criteria were set to 1×10^{-5} eV atom⁻¹, 3×10^{-2} eV Å⁻¹ for the total energy and forces, respectively. A vacuum spacing of at least 15 Å was applied along the z-axis to eliminate interactions between periodic images of the slab.

The adsorption energy E_{ads} was calculated by using the following formula:

$$E_{ads} = E_{slab-molecule} - E_{slab} - E_{molecule}$$

Where $E_{\text{slab-molecule}}$ represents the total energy of adsorbed system. E_{slab} represents the calculated energies of Cu-SAC/NC, Fe-SAC/NC and Cu-Fe DAC/NC. E_{molecule} represents the calculated energy of NO₃ molecule. A more negative value of E_{ads} represents stronger adsorption.

Based on computational hydrogen electrode (CHE) model⁸, the Gibbs free energy change (ΔG) of each elementary step is defined as

$$\Delta G = \Delta E_{DFT} + \Delta ZPE - T\Delta S$$

where ΔE_{DFT} , ZPE, T and S are energy obtained from DFT calculations, zero-point energy, temperature (298.15 K), and entropy, respectively.

Here, the element steps of nitrate reduction on oreoared catalysts can be summarized by the following reaction equations.

*
$$+ NO_3^- \rightarrow *NO_3 + e^-$$

* $NO_3 + 2H^+ + 2e^- \rightarrow *NO_2 + H_2O$

* $NO_2 + 2H^+ + 2e^- \rightarrow *NO + H_2O$

* $NO + H^+ + e^- \rightarrow *HNO$

* $HNO + H^+ + e^- \rightarrow *H_2NO$

* $H_2NO + H^+ + e^- \rightarrow *H_2NOH$

* $H_2NOH + H^+ + e^- \rightarrow *NH_2 + H_2O$

* $NH_2 + H^+ + e^- \rightarrow *NH_3$

* $NH_3 \rightarrow *+ NH_3$

To avoid calculating the energy of charged NO₃- directly, gaseous HNO₃ is chosen as a reference based on the following steps⁹.

$$HNO_3 \rightarrow H^+ + NO_3^-$$

$$* + NO_3^- \rightarrow *NO_3 + e^-$$

$$* + HNO_3 \rightarrow *NO_3 + H^+ + e^-$$

As a result, the adsorption energy of NO_3^- (ΔG_{*NO3}) can be approximated by

$$\Delta G_{*NO3} = G_{*NO3} - G_* - G_{HNO3} + 0.5G_{H2}$$

where G_{*NO3} , G_{*} , G_{HNO3} , and G_{H2} are the Gibbs free energy of NO_3^- adsorbed on SAC or DAC, SAC or DAC substrates, HNO₃ and H₂ molecules in the gas phase, respectively.

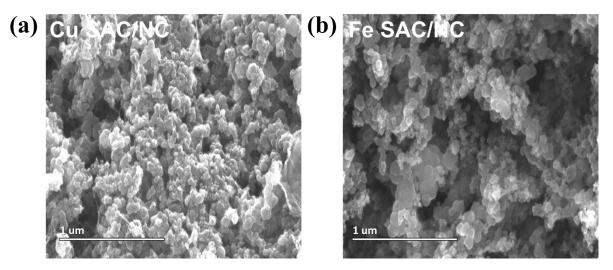


Figure S1. SEM image of (a) Cu SAC/NC. (b) Fe SAC/NC

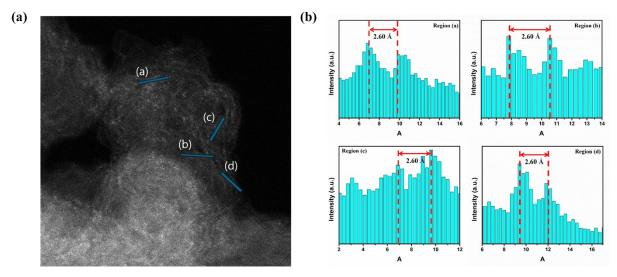


Figure S2. (a) HAADF-STEM image of Cu–Fe DAC/NC (same as Figure 1(c)), (b) Linescanning based atomic intensity profiles obtained from various regions.

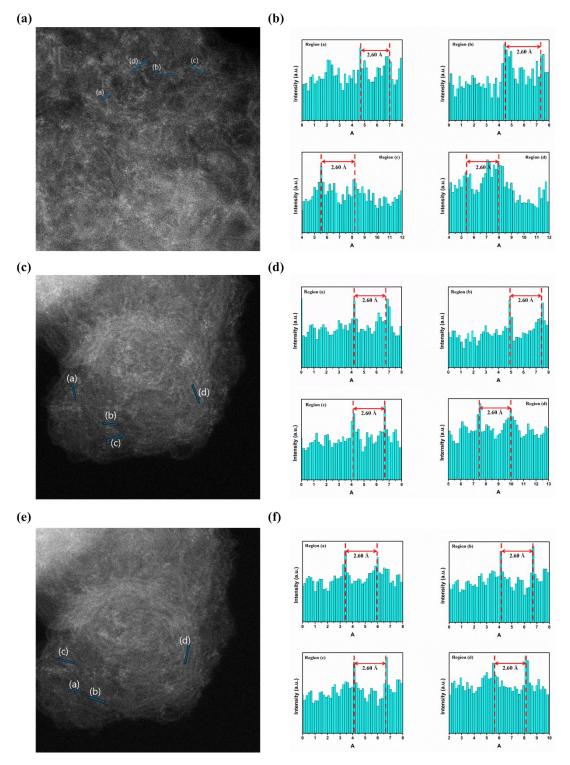


Figure S3. (a), (c), (e) Other HAADF-STEM images of Cu–Fe DAC/NC. (b), (d), (f) Linescanning based atomic intensity profiles obtained from various regions of each HAADF-STEM images.

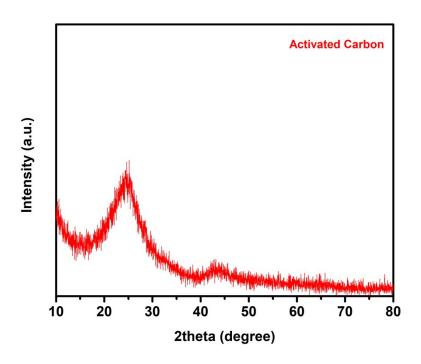


Figure \$4. XRD spectra of Activated Carbon

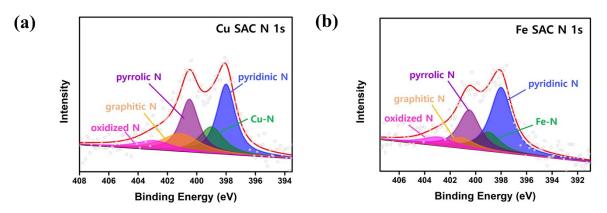


Figure S5. XPS spectra of N 1s (a) Cu SAC/NC (b) Fe SAC/NC

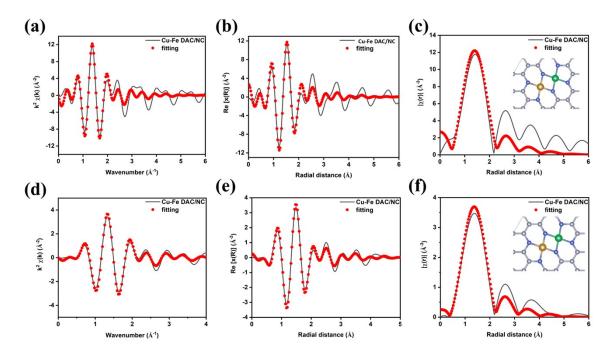


Figure S6. EXAFS fitting curves for the Cu-Fe DAC/NC of (a) *k-space* (b) *R-space* real part (c) *R-space* (inset: proposed model) of Cu K-edge. (d) *k-space* (e) *R-space* real part (f) *R-space* (inset: proposed model) of Fe K-edge.

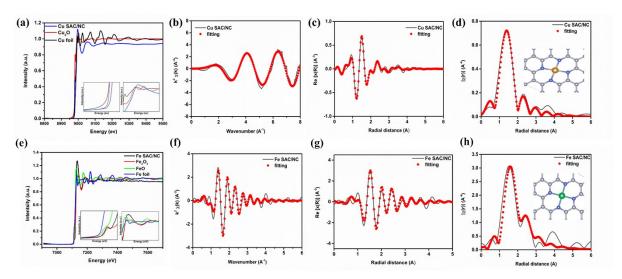


Figure S7. (a) XANES spectra, EXAFS fitting curve of (b) *k-space* (c) *R-space* real part (d) *R-space* (inset: proposed model) of Cu SAC/NC. (e) XANES spectra, EXAFS fitting curve of (f) *k-space* (g) *R-space* real part (h) *R-space* (inset: proposed model) of Fe SAC/NC

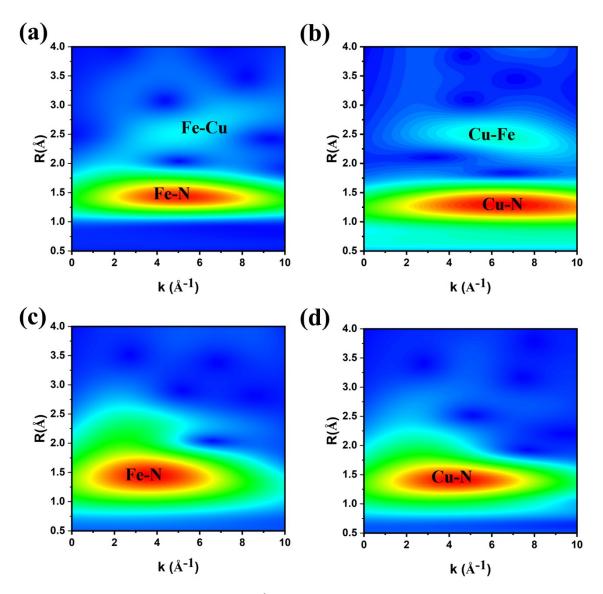


Figure S8. Wavelet transform of the k^2 -weighted EXAFS data of (a) Fe K-edge, (b) Cu K-edge of Cu-Fe DAC/NC (c) Fe K-edge of Fe SAC (d) Cu K-edge of Cu SAC

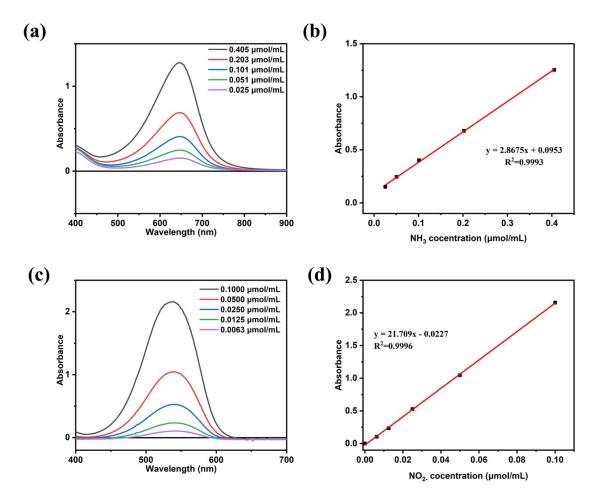


Figure S9. (a) UV-vis absorption spectra and (b) calibration curve of indophenol blue method (c) UV-vis absorption spectra and (d) calibration curve of indophenol Griess method.

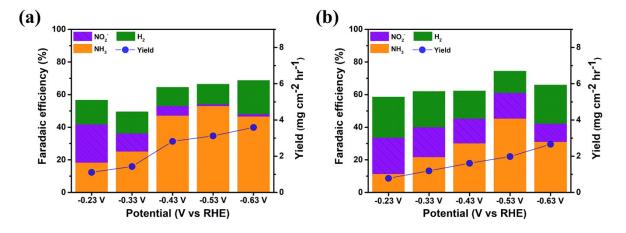


Figure S10. Faradaic efficiency and NH₃ production rate versus applied potential of (a) Fe SAC/NC (b) Cu SAC/NC

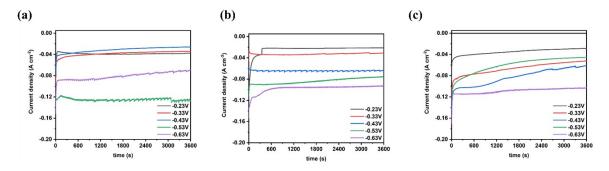


Figure S11. Current densities versus applied potential (a) Cu-Fe DAC/NC (b) Fe SAC/NC (c) Cu SAC/NC

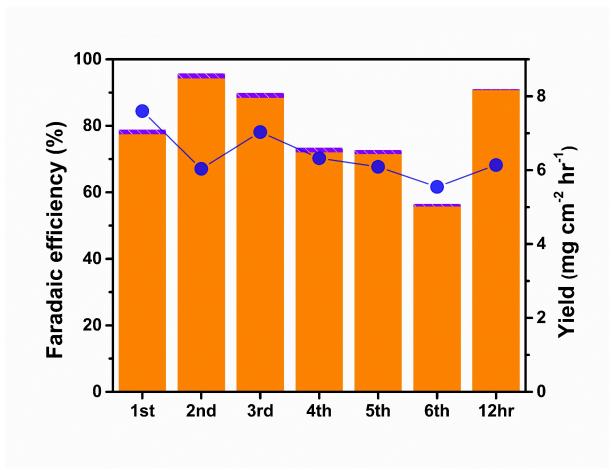


Figure S12. Faradaic efficiency and NH₃ yield during the stability tests (cycling tests & 12 h test).

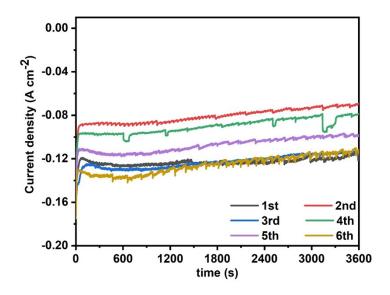


Figure S13. Current densities during the cycling tests.

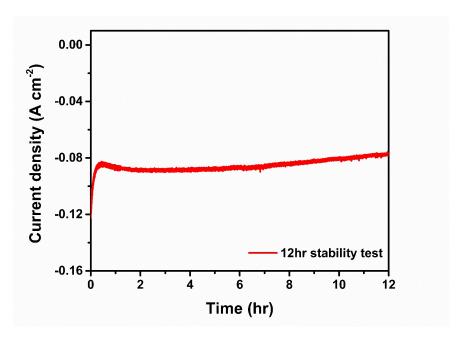


Figure S14. Current density profile measured during the 12 h stability test.

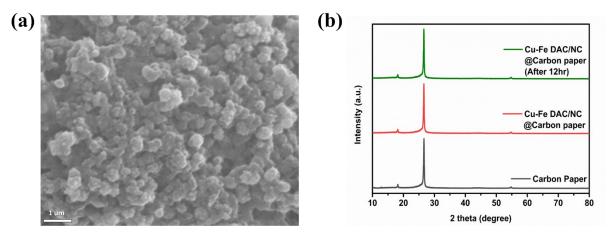


Figure S15. (a) SEM imange of Cu-Fe DAC/NC after the 12 h stability test (b) XRD spectra of Cu-Fe DAC/NC obtained after the 12 h stability test.

Table S1. The ICP-OES results of prepared catalysts.

Samples	Cu (at %)	Fe (at %)
Cu SAC/NC	0.842	-
Fe SAC/NC	-	1.178
Cu-Fe DAC/NC	0.436	0.527

Table S2. The contents of N species of prepared catalysts based on XPS results.

Samples	N (at %)	Graphitic N (%)	Pyridinic N (%)	Oxidized N (%)	Pyrrolic N (%)	M-N (%)
Cu-Fe DAC/NC	3.5	9.3	41.5	5.8	23.3	20.1
Cu SAC/NC	3.8	16.6	33.3	8.3	25.0	16.7
Fe SAC/NC	4.1	9.4	37.7	9.4	28.3	15.1

Table S3. XANES normalization condition of Athena program for prepared catalysts series.

Samples	E0	Pre-edge range	Normalization range	Normalization order
Cu SAC/NC	8987.00	-150 to -30	150 to 745.89	3
Fe SAC/NC	7126.82	-150 to -30	150 to 859.22	3
FeCu DAC/NC	8979.0	-150 to -30	150 to 850	3
FeCu DAC/NC	7125.91	-150 to -30	150 to 400.00	3

Table S4. EXAFS fitting results of Cu and Fe K-edge for the shell of catalysts series.

Samples	Shell	CN^{a}	R (Å) ^b	$\Delta E_0 (eV)^c$	$\sigma(\mathring{A}^2)^d$	R factor
Cu SAC/NC	Cu-N	3.818	1.942	-5.147	0.0030	1.8703
Fe SAC/NC	Fe-N	3.654	1.949	-7.477	0.0086	1.8703
Cu-Fe DAC/NC	Cu-N	3.917	1.805	-4.162	0.0013	2.0032
Cu-Fe DAC/NC	Fe-N	4.294	1.801	-6.358	0.0030	1.9127

^a The average coordination number for the coordination shell.

^b Interatomic distance.

 $^{^{}c}E_{0}$ shift of the path.

^d Debye-Waller factor.

Table S5. Faradaic efficiencies (%) of products and yield of NH₃ obtained from electrocatalytic NO₃RR on prepared catalysts at different potentials.

Catalyst	E (V vs RHE)	NH ₃ FE (%)	NO ₂ -FE (%)	H ₂ FE (%)	NH ₃ yield (mg·h ⁻¹ ·cm ⁻²)
	- 0.23	11.3	22.2	25.1	0.78
	-0.33	21.6	18.3	22.2	1.19
Cu SAC/NC	-0.43	30.0	15.2	17.1	1.61
	-0.53	45.3	15.7	13.5	1.98
	-0.63	30.9	11.2	23.9	2.66
Catalyst	E (V vs RHE)	NH ₃ FE (%)	NO ₂ -FE (%)	H ₂ FE (%)	NH ₃ yield (mg·h ⁻¹ ·cm ⁻²)
	-0.23	18.2	23.4	15.1	1.11
	-0.33	25.1	11.0	13.5	1.43
Fe SAC/NC	-0.43	47.1	5.9	11.5	2.82
	-0.53	52.9	1.1	12.5	3.12
	-0.63	46.5	1.4	20.9	3.59
Catalyst	E (V vs RHE)	NH ₃ FE (%)	NO ₂ -FE (%)	H ₂ FE (%)	NH ₃ yield (mg·h ⁻¹ ·cm ⁻²)
Cu-Fe DAC/NC	-0.23	23.3	36.7	15.6	0.72
	-0.33	35.6	30.5	13.4	1.08
	-0.43	61.4	18.1	5.5	1.52
	-0.53	94.3	1.5	0.6	6.04
	-0.63	57.8	1.2	28.4	5.73

Table S6. Faradaic efficiencies (%) of products and yield of NH₃ obtained from electrocatalytic NO₃RR on Cu-Fe DAC at Cycle test

Catalyst	cycle	NH ₃ FE (%)	NO ₂ -FE (%)	Total FE (%)	NH ₃ yield (mg·h ⁻¹ ·cm ⁻²)
	1	77.9	1.3	79.2	7.60
	2	94.3	1.5	95.8	6.04
Cu-Fe DAC/NC	3	88.4	1.5	89.9	7.03
	4	72.1	1.4	73.5	6.32
	5	71.5	1.2	72.7	6.09
	6	55.7	0.8	56.5	5.55
	12hr	90.76	0.23	90.99	6.14

Table S7. The electrochemical nitrate reduction reaction performance comparison with other reported catalyst recently.

Catalysts	NH ₃ Faradaic efficiency	NH ₃ yield rate	Electrolyte	Refere nce
Cu-Fe DAC/NC	94.3%	6.04 mg·h ⁻¹ ·cm ⁻²	100 mM KNO ₃ 1 M KOH	This work
Cu-N ₁ O ₂ SACs	96.5 %	3.120 mg h ⁻¹ cm ⁻²	10 mM KNO ₃ 0.1 M KOH	[10]
PR-CuNC	94.61 %	$3.74 \text{ mg h}^{-1} \text{ cm}^{-2}$	100 mM KNO ₃ 0.1 M KOH	[11]
Cu-N ₁ O ₂	96.5 %	3.12 mg h ⁻¹ cm ⁻²	100 mM KNO ₃ 0.1 M KOH	[12]
Cu-N-C	84.7 %	4.5 mg h ⁻¹ cm ⁻²	100 mM KNO ₃ 0.1 M KOH	[13]
Fe/Cu-HNG	92.51 %	4.41 mg h^{-1} cm ⁻²	100 mM KNO ₃ 1 M KOH	[14]
Fe-N/P-C	90.3 %	$4.50 \text{mg h}^{-1} \text{cm}^{-2}$	100 mM KNO ₃ 0.1 M KOH	[15]
Fe-MoS ₂	98 %	$0.51~{ m mg~h^{-1}cm^{-2}}$	$0.1~\mathrm{M~NaNO_3}$ $0.1~\mathrm{M~Na_2SO_4}$ $0.1~\mathrm{M~NaOH}$	[16]
Fe SAC	75%	4 mg h ⁻¹ cm ⁻²	0.5 M KNO ₃ 0.1 M K ₂ SO ₄	[17]
Fe SAC	92 %	4.6 mg h ⁻¹ cm ⁻²	0.5 M KNO ₃ 0.1 M K ₂ SO ₄	[18]
BCN-Cu	97.37%	$3.36~{\rm mg~h^{-1}~cm^{-2}}$	100 mM KNO ₃ 0.1 M KOH	[19]
Fe-BCN	97.48%	2.17 mg cm ⁻² h ⁻¹	0.5 mM KNO ₃ 1 M KOH	[20]

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10.1021/jacs.2c02262

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