

Electronic supplementary information

Interface Strain Engineering of Ru-RuO_x/Graphene Aerogel Composite Boost HER, OER and ORR Applications

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1. Experimental Section

1.1 Electrochemical measurements

The electrochemical measurements (HER and OER) performance were evaluated using a three-electrode system on the CHI 760E electrochemical station. The Hg/HgO (1 M KOH) was used as the reference electrode, while the counter and the working electrodes were Pt foil and the self-supported electrode, respectively. All the measured potentials vs Hg/HgO were converted to the reversible hydrogen electrode (RHE). In 1 M KOH, $E_{\text{RHE}} = E_{\text{Hg/HgO}} + 0.0977 \text{ V} + 0.059 \cdot \text{pH}$. The working electrodes were first activated using the cyclic voltammetry (CV) test at a scan rate of 50 mV s^{-1} several times, and then linear sweep voltammetry (LSV) tests were conducted. The Tafel slope was obtained from the LSV curves. To test the electrochemical stability of Ru/GA and other samples in 1 M KOH, a long-term chronopotentiometry was performed at the current density of 10 or 100 mA cm^{-2} . The electrochemically active surface area (ECSA) was determined by measuring the CV scan rate dependence with respect to the capacitive current associated with the double-layer charging. The ECSA was evaluated by the following equation:

$$\text{ECSA} = C_{dl} / 0.04 \text{ mF cm}^{-2}$$

The ORR was conducted under basic conditions (0.1 M KOH). Differences from the HER and OER tests are the reference electrode is Ag/AgCl, $E_{\text{RHE}} = E_{\text{Ag/AgCl}} + 0.197 \text{ V} + 0.059 \cdot \text{pH}$. For comparison, commercial Pt/C and other samples were used as the contrast catalysts.

1.2 Overall Water Splitting measurements

A two-electrode cell was fabricated to conduct the assisted OER/HER electrocatalysis Overall Water Splitting test (1 M KOH). The cathode and anode materials were both the Ru-RuO_x/GA-2 electrode. For comparison, commercial RuO₂ and 20%Pt/C were used as the OER/HER electrocatalysis Overall Water Splitting test (1 M KOH). The cathode and anode materials were first activated using the CV test at a scan rate of 50 mV s^{-1} several times, and then linear sweep voltammetry (LSV) tests were conducted. To test the electrochemical stability of Overall Water Splitting in 6 M KOH, a long-term chronopotentiometry was performed at 500 mA cm^{-2} . The O₂/H₂ produced by the cathode was collected by the drainage and gas-collecting method for quantitative analysis.

1.3 Zinc-air battery tests

The prepared air electrode and a polished Zn plate (thickness 5 mm) were assembled in 6.0 M KOH and

0.2 M $\text{Zn}(\text{CH}_3\text{COO})_2$ electrolyte. For air electrode preparation: 4 mg catalyst powders were dispersed into an ethanol solution containing 760 μL ethanol and 40 μL Nafion solution (5 wt%) under sonication for 1 h. Then the obtained homogeneous catalyst inks were uniformly dropcast onto carbon paper ($2 \times 2 \text{ cm}^2$) to reach a loading of 1 mg cm^{-2} and the effective area (S) exposed to the electrolyte was 1 cm^2 , and a Ni mesh was used as the current collector. For the assembly of the battery for comparison, a commercial catalyst (20 wt % Pt/C: $\text{RuO}_2 = 1:1$, mass ratio) was used with the same loading amount. For the Zn-air batteries test: the discharge/charge tests were conducted on a CHI 760E electrochemical working station at a scan rate of 5 mV s^{-1} . The galvanostatic discharge-charge curves were recorded using a LAND testing system at a current density of 10 mA cm^{-2} with 10 min per cycle (charge 5 min and discharge 5 min). The specific capacity and energy density were calculated from the galvanostatical discharge results, normalized to the mass of consumed Zn. The mass of consumed Zn was determined by the mass difference between the fresh Zn and resultant anode after discharging. The energy density, specific capacity and power density of primary Zn-air battery were calculated based on the applied current (I), average discharge voltage (V), service hours (t), the weight of zinc consumed (m_{Zn}) and the effective area (S) exposed to the electrolyte for the air electrode.

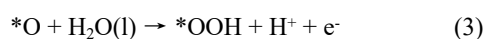
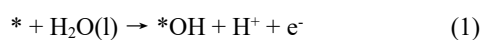
$$\text{Specific capacity (mAh g}^{-1}\text{)} = \frac{I \times t}{m_{\text{Zn}}}$$

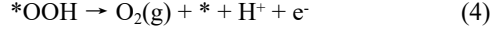
$$\text{Power density (mW cm}^{-2}\text{)} = \frac{I \times V}{S}$$

1.4 The density functional theory calculations

All the spin-polarized DFT calculations were performed using the projector augmented wave method (PAW)^[1] as implemented in the Vienna Ab initio Simulation Package (VASP)^[2]. The generalized gradient approximation (GGA) with the Perdew-Burke-Ernzerhof functional (PBE)^[3] was used to describe the exchange-correlation interactions, and the van der Waals (vdW) correction proposed by Grimme (DFT-D3)^[4] was included in describing the long-range interactions. The cutoff energy of the plane-wave was set to 500 eV. Ab initio molecular dynamics (AIMD) simulations in constant temperature and volume with a Nose-Hoover thermostat^[5] were adopted to evaluate the thermodynamic stability of the materials. All the structures were relaxed until the residual atomic forces on each atom were less than 0.02 eV/\AA , and the total energy was less than 10^{-6} eV for self-consistent field (SCF) calculations. To improve the accuracy and efficiency, the Brillouin zone integration was performed on the $3 \times 3 \times 1$ Monkhorst-Pack k-point mesh.^[6] The vacuum space was set to 15 \AA in the z-direction to avoid interactions between periodic images.

The 4e⁻ OER mechanism in acidic media is listed as follows:





The adsorption energies of three reaction intermediates (*OH, *O, and *OOH) in OER are calculated as follows:

$$\Delta E_{\text{DFT}}(*\text{OH}) = E_{\text{DFT}}(*\text{OH}) - E(*) - [E_{\text{DFT}}(\text{H}_2\text{O}) - 1/2 * E_{\text{DFT}}(\text{H}_2)] \quad (5)$$

$$\Delta E_{\text{DFT}}(*\text{O}) = E_{\text{DFT}}(*\text{O}) - E(*) - [E_{\text{DFT}}(\text{H}_2\text{O}) - E_{\text{DFT}}(\text{H}_2)] \quad (6)$$

$$\Delta E_{\text{DFT}}(*\text{OOH}) = E_{\text{DFT}}(*\text{OOH}) - E(*) - [2 * E_{\text{DFT}}(\text{H}_2\text{O}) - 3/2 * E_{\text{DFT}}(\text{H}_2)] \quad (7)$$

where the $E_{\text{DFT}}(*\text{OH})$, $E_{\text{DFT}}(*\text{O})$, $E(*)$, $E_{\text{DFT}}(\text{H}_2\text{O})$, and $E_{\text{DFT}}(\text{H}_2)$ indicate the total energy of *OH, *O, substrate, H₂O molecular, H₂ molecular, separately. The free energies of O₂, H₂O, and H₂ are listed in Table 1.

The free energy change (ΔG) of each elementary step is calculated as , where is the zero-point energy change, is the enthalpy-temperature correction, and is the entropy change, respectively. Gibbs adsorption free energy corrections ($\Delta G_{\text{corr}} = \Delta ZPE + \int C_p dT - T\Delta S$) for each intermediate during OER are listed in Table 2.

Table 1. The DFT energies (E_{DFT}) and corresponding free energy correction values (ΔG) of H₂(g) and H₂O(l) are calculated at 1 bar and 0.035 bar. Due to the fact that O₂ is poorly described in DFT calculations, the free energy of O₂ is calculated by $\text{GO}_2 = 2\text{GH}_2\text{O} - 2\text{GH}_2 + 4.92 \text{ eV}$. The DFT energies of H₂ and H₂O were calculated in a $10 \text{ \AA} \times 10 \text{ \AA} \times 10 \text{ \AA}$ unit cell in vacuum.

	Pressure(bar)	Temperature(K)	E(DFT)(eV)	$\Delta G(\text{eV})$	G(eV)
H₂O(l)	0.035	298.15	-14.22	0.00	-14.22
H₂(g)	1.00	298.15	-6.77	-0.044	-6.81
O₂(g)	1.00	298.15	/	/	-9.90

Table 2. Gibbs adsorption free energy corrections ($\Delta G_{\text{corr}} = \Delta ZPE + \int C_p dT - T\Delta S$) for each intermediate during OER.

Species	*OH	*O	*OOH
G_{corr}/eV	0.27	0.028	0.34

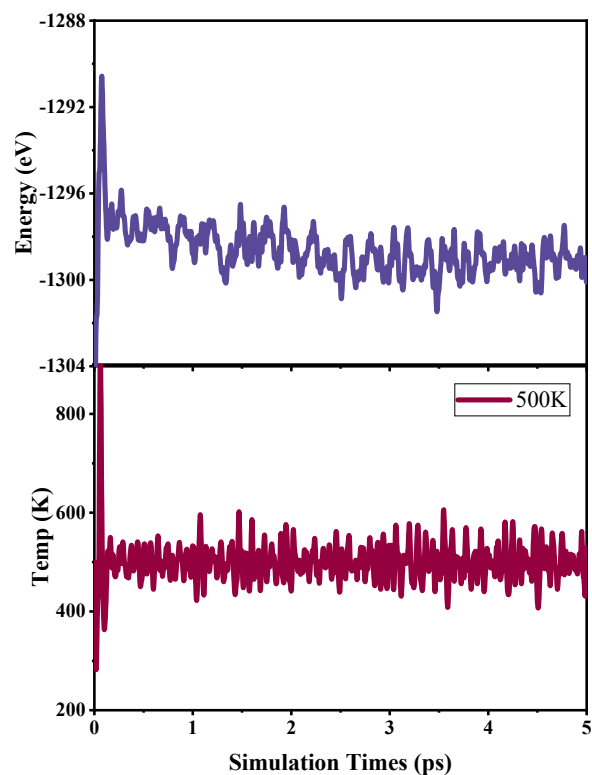


Figure S1. The atomic structure and system energy obtained by AIMD calculation for $\text{RuO}_x(110)\text{-Ru}(101)$. The fluctuation of temperature concerning the duration for AIMD simulations of $\text{RuO}_x(110)\text{-Ru}(101)$ under 500 K in 5 ps.

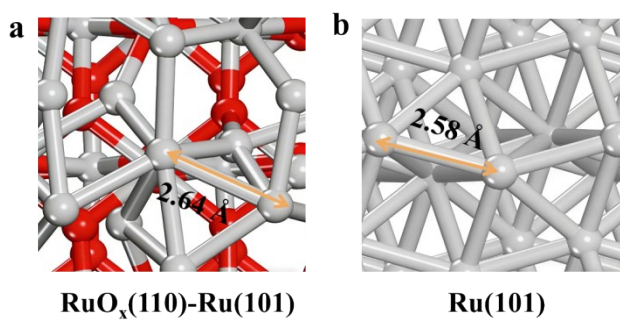


Figure S2. Simulative structural model of Ru-Ru bond in (a) $\text{RuO}_x(110)\text{-Ru}(101)$ and (b) $\text{Ru}(101)$ model.

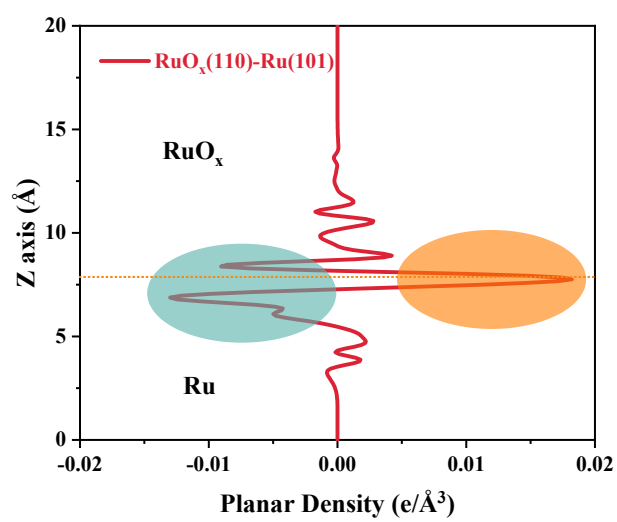


Figure S3. Planar-averaged electron density difference $\Delta\rho(Z)$ of $\text{RuO}_x(110)\text{-Ru}(101)$.

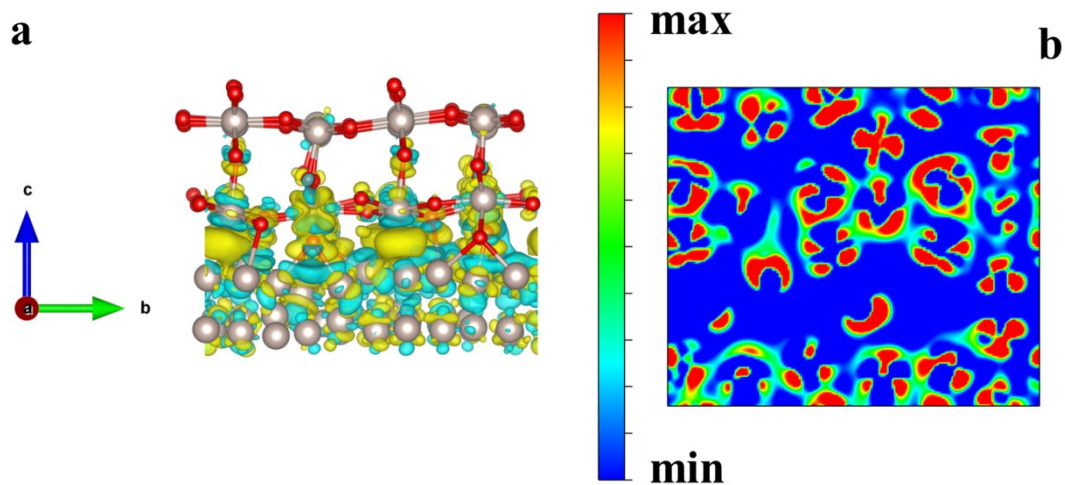


Figure S4. Differential charge density of RuO_x(110)-Ru(101). (a) Side-view. Yellow: electron accumulation, cyan: electron depletion. (b). Two-dimensional projection of the Ru site of RuO_x(110) with differential charge density at the interface.

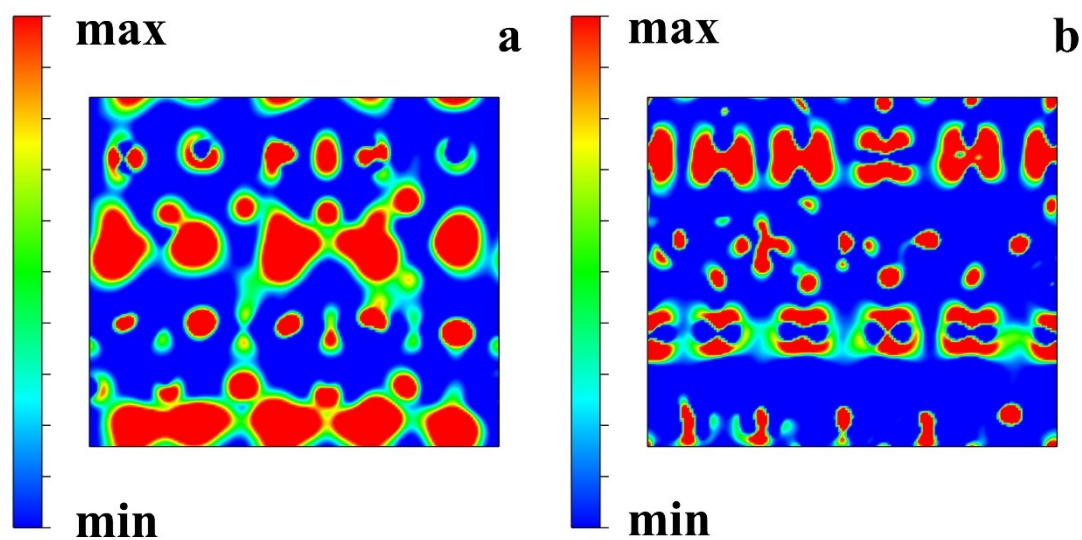


Figure S5. (a) Two-dimensional projection of the O site of RuO_x(110) with differential charge density at the interface. (b). Two-dimensional projection of the Ru site of Ru(101) with differential charge density at the interface.

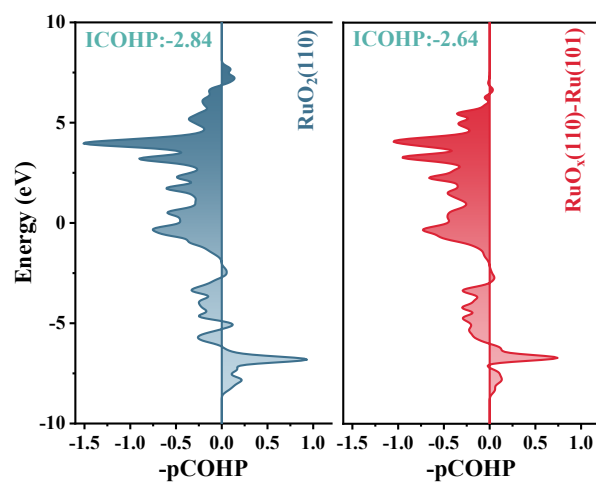


Figure S6. Calculated pCOHP diagrams for RuO₂(110) and RuO_x(110)-Ru(101).

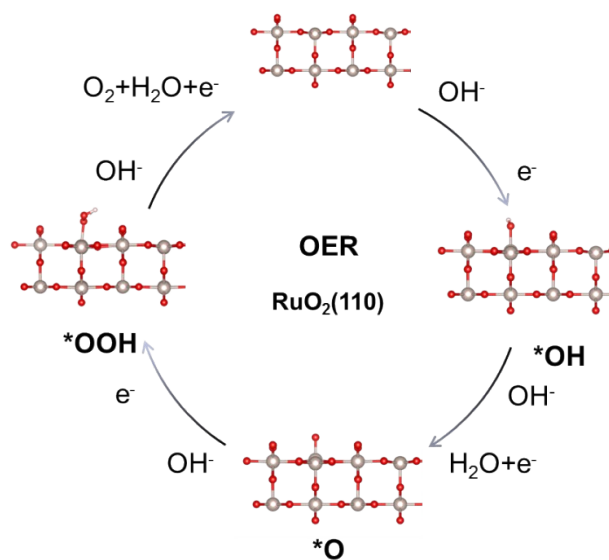


Figure S7. DFT optimized structures for OER reaction intermediates adsorbed on pristine RuO₂(110).

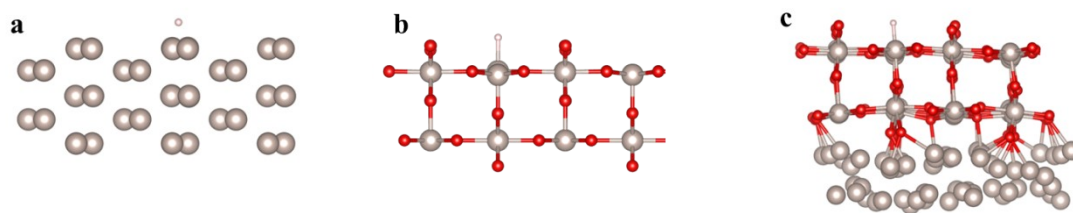


Figure S8. (a-c) The optimized structure of $\ast \text{H}$ adsorbed on the Ru site of (a) Ru(101), (b) $\text{RuO}_2(110)$, and (c) $\text{RuO}_x(110)\text{-Ru}(101)$, respectively.

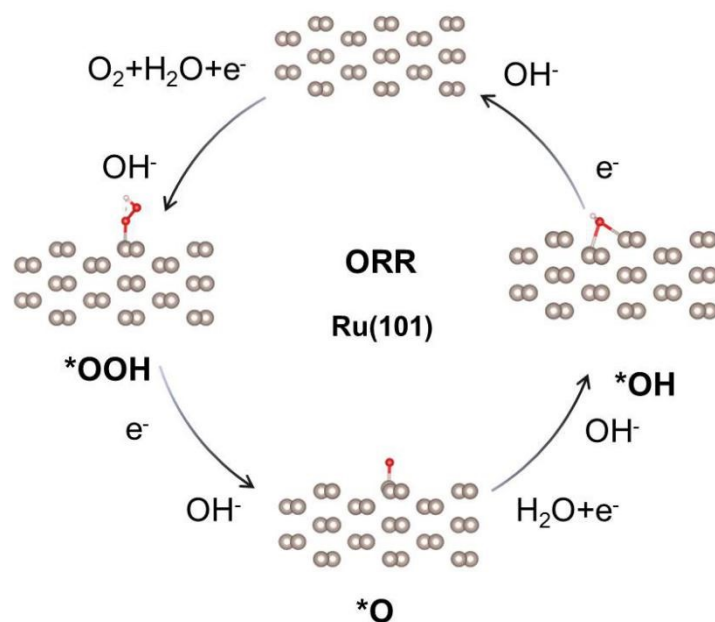


Figure S9. DFT optimized structures for ORR reaction intermediates adsorbed on pristine Ru(101).

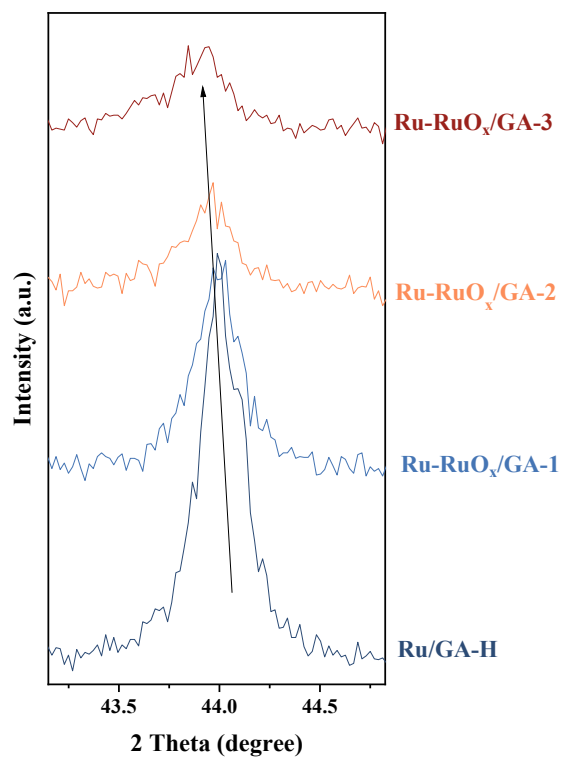


Figure S10. XRD localized magnification of Ru/GA-H and Ru-RuO_x/GA-1, 2, 3.

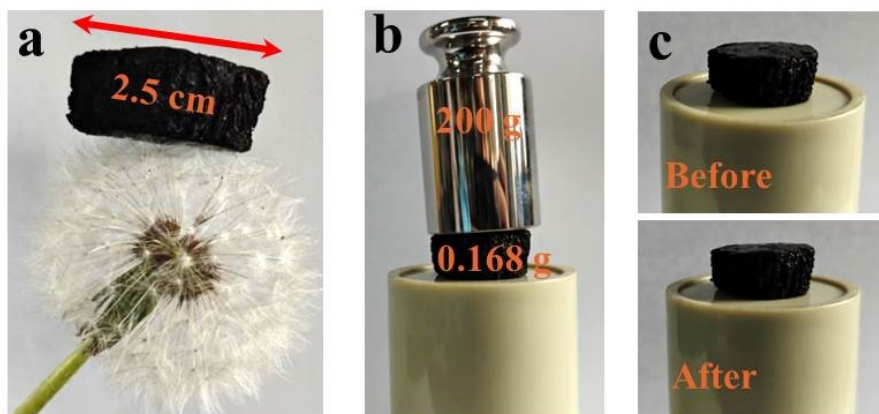


Figure S11. (a) optical image of GA. (b, c) optical photographs of GA before and after stress tests.

The porous GA precursor was obtained by using NaCl as template, and then the final sample was obtained by solution adsorption and two-step calcination processes [7]. Notably, the mass density of GA is extremely low, and the dandelion can easily bear the weight of a piece of carbon aerogel ($\sim 6 \text{ cm}^3$) without deformation of the dandelion (Fig. S11a). Moreover, the GA has excellent compressive properties and can withstand a weight of 1200 times its own weight without deformation (Fig. S11b, c). This suggests that the GA obtained by this method has a rich porous structure, which serves as a substrate material that helps to reduce the agglomeration of the catalyst [8].

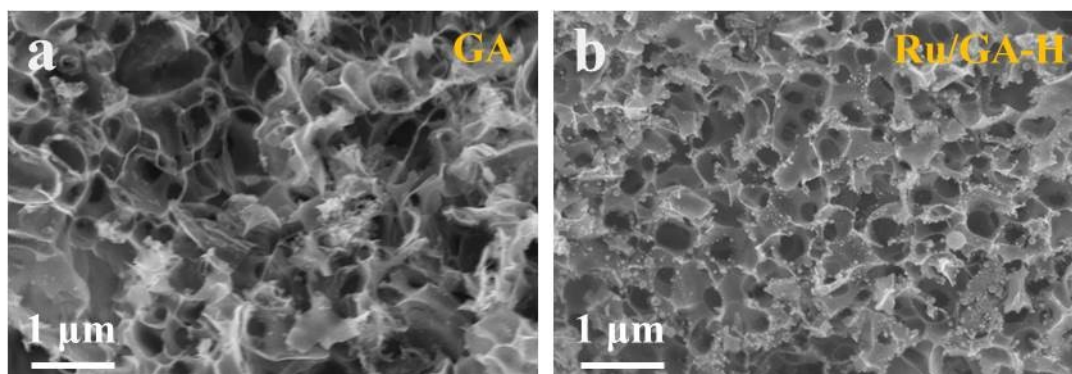


Figure S12. SEM images of (a) GA and (b) Ru/GA-H.

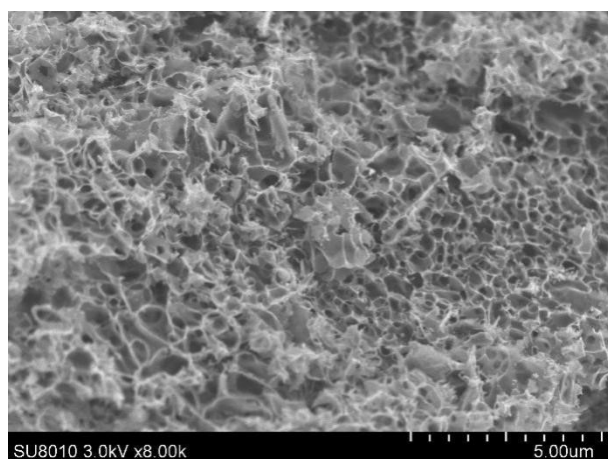


Figure S13. SEM image of Ru/GA-H.

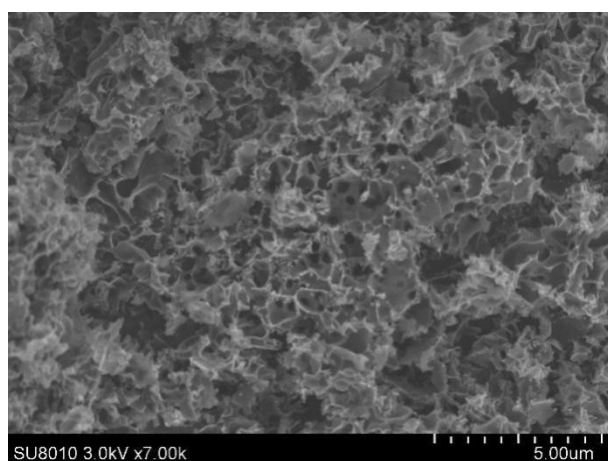


Figure S14. SEM image of Ru-RuO_x/GA-1.

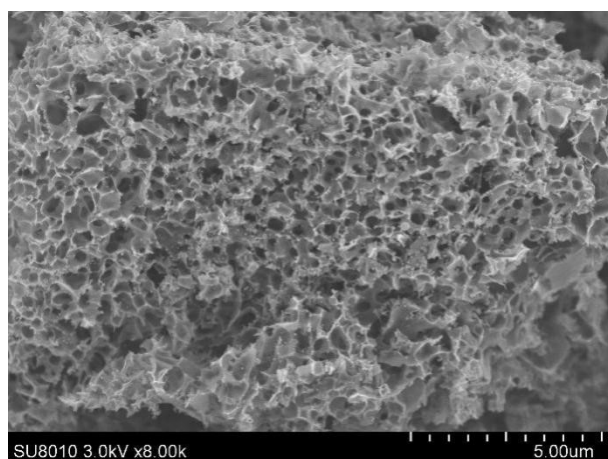


Figure S15. SEM image of Ru-RuO_x/GA-2.

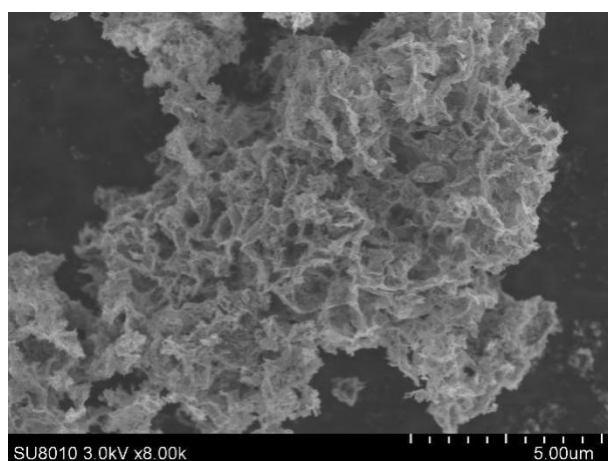


Figure S16. SEM image of Ru-RuO_x/GA-3.

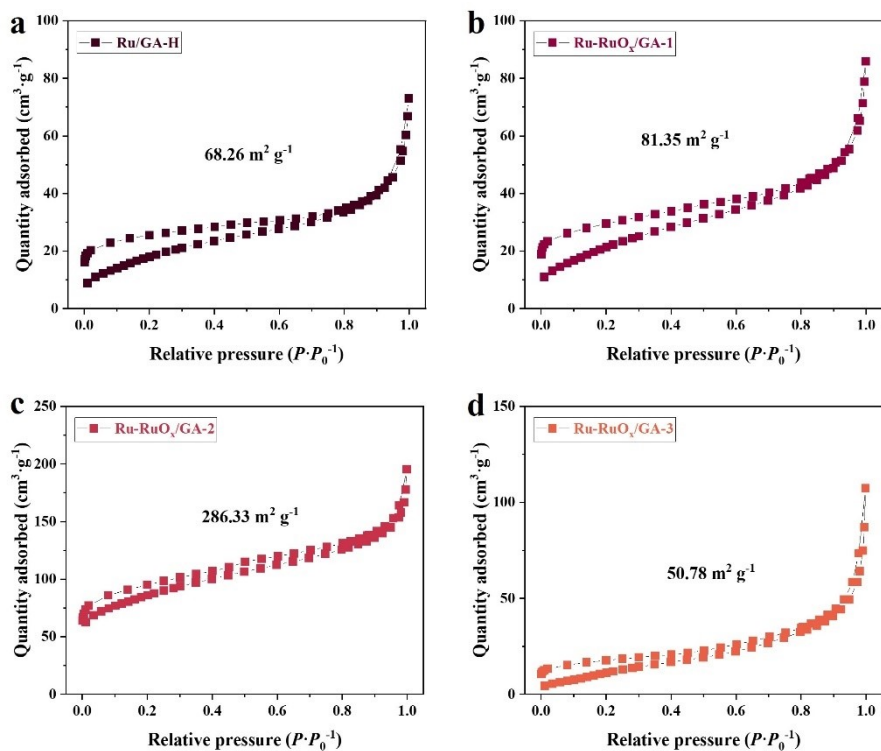


Figure S17. (a) N₂ sorption isotherms of Ru/GA-H and Ru-RuO_x/GA-1, 2, 3.

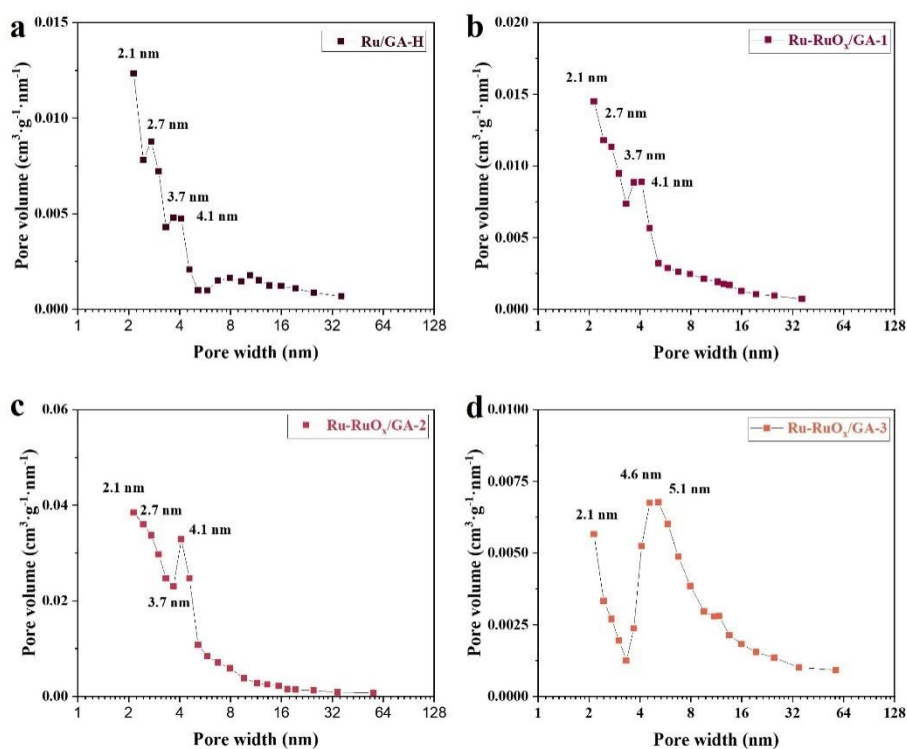


Figure S18. (a) The corresponding pore size distribution of Ru/GA-H and Ru-RuO_x/GA-1, 2, 3.

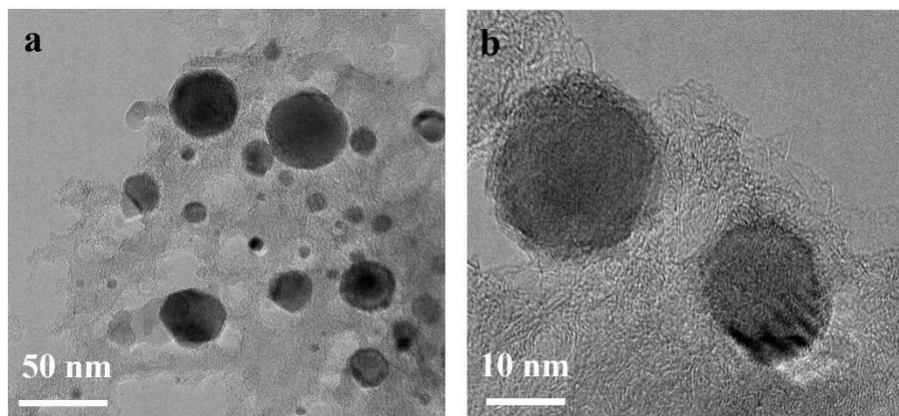


Figure S19. TEM images of Ru/GA-H.

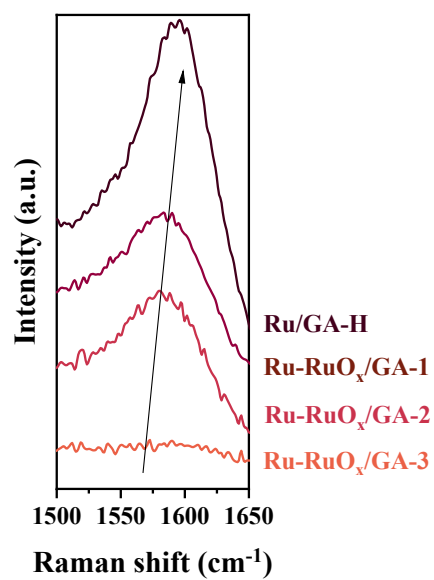


Figure S20. local magnification Raman spectra of Ru/GA-H, Ru-RuO_x/GA-1, 2, 3.

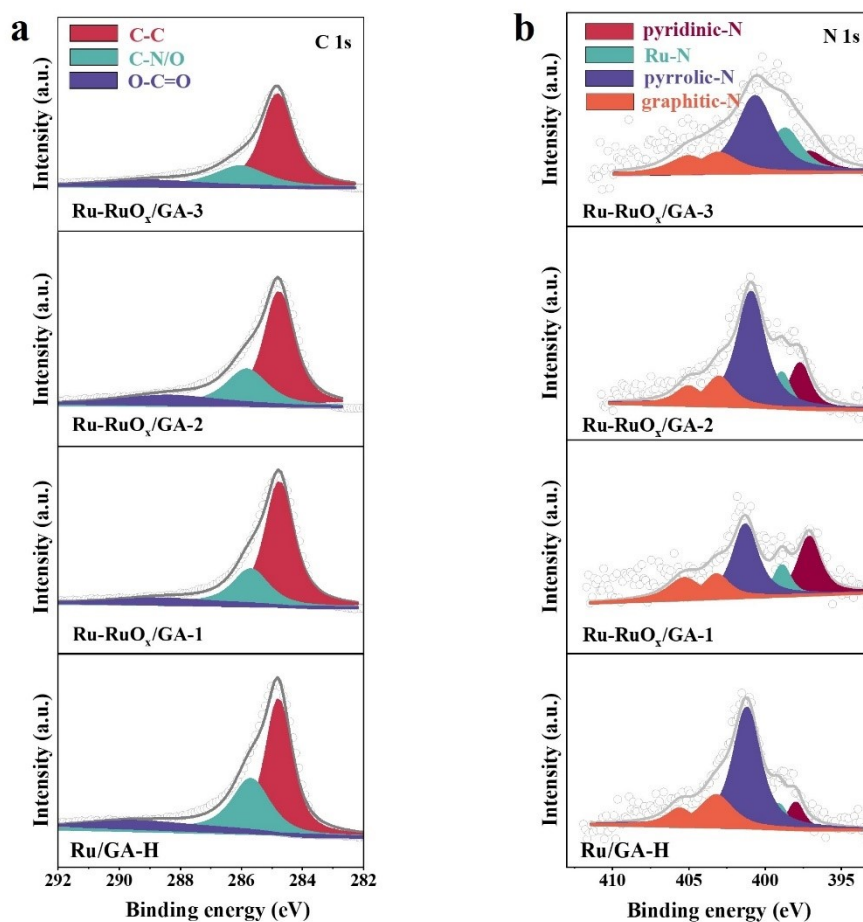


Figure S21. (a) C 1s and (b) N 1s XPS spectra of Ru/GA-H, Ru-RuO_x/GA-1, 2, 3.

In addition, the C 1s and N 1s XPS results of the catalysts were systematically analyzed as an indication of the bonding structure and changes in the substrate GA. As shown in Fig. S21a, the C 1s XPS results indicate the existence of three types of chemical bonds, C-C, C-N/O, and O-C=O, for GA [9]. Notably, the strength of these three types of chemical bonds weakened at the oxidation temperature of 450 °C, which indicated that the GA structure was damaged; the N 1s XPS results showed a similar situation, except that the Ru-N chemical bonds could be observed [9-11], and the spectral peaks of the N 1s spectrum of the 450 °C oxidation-treated Ru-RuO_x/GA-3 were weakened. This indicated that the oxidation temperature was on the high side, which was in agreement with the SEM, Raman, and BET test results, the preferred 350 °C is the suitable oxidation temperature (Fig. S21b).

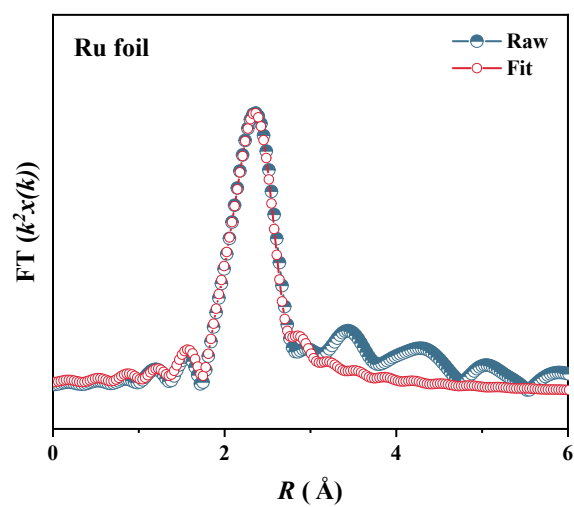


Figure S22. Ru K-edge EXAFS fitting curves of Ru foil in R space.

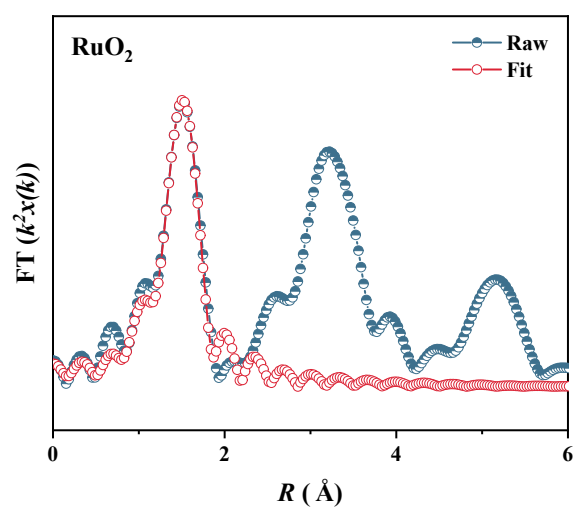


Figure S23. Ru K-edge EXAFS fitting curves of RuO₂ in R space.

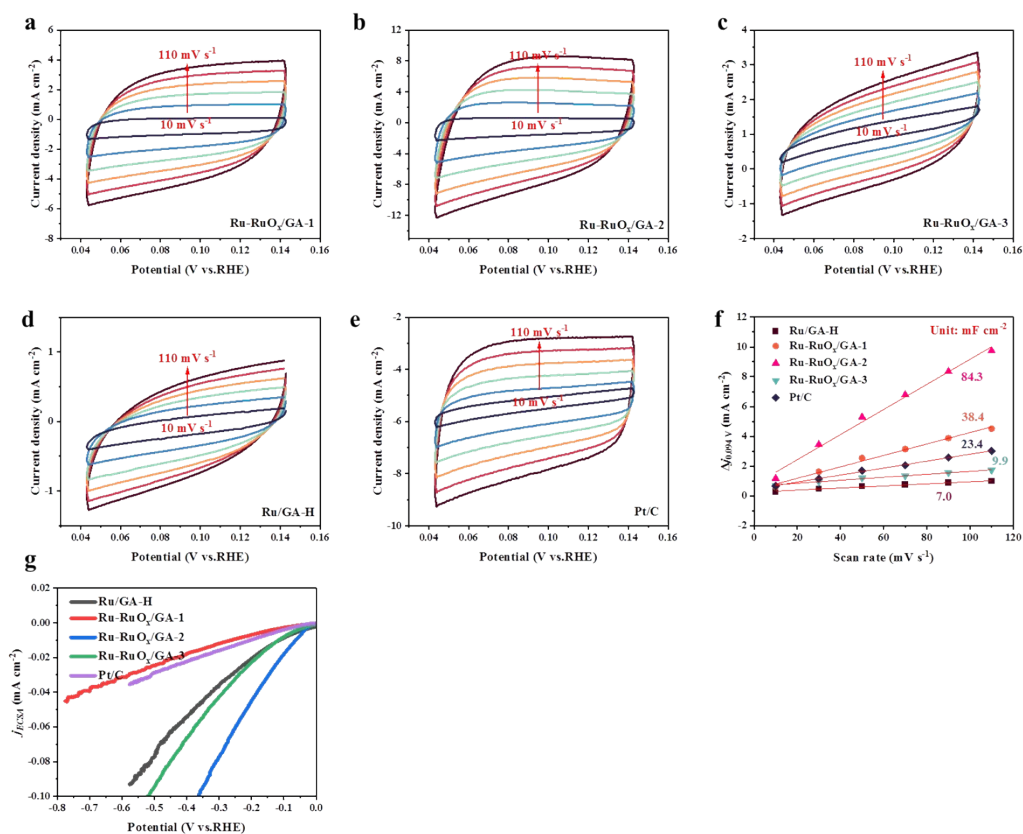


Figure S24. (a-e) CVs with different scan rates for Ru-RuO_x/GA-1, 2, 3, Ru/GA-H, and Pt/C. (f) C_{dl} values fitted according to CV curves. (g) Current densities (j_{ECSA}) normalized by ECSAs for HER.

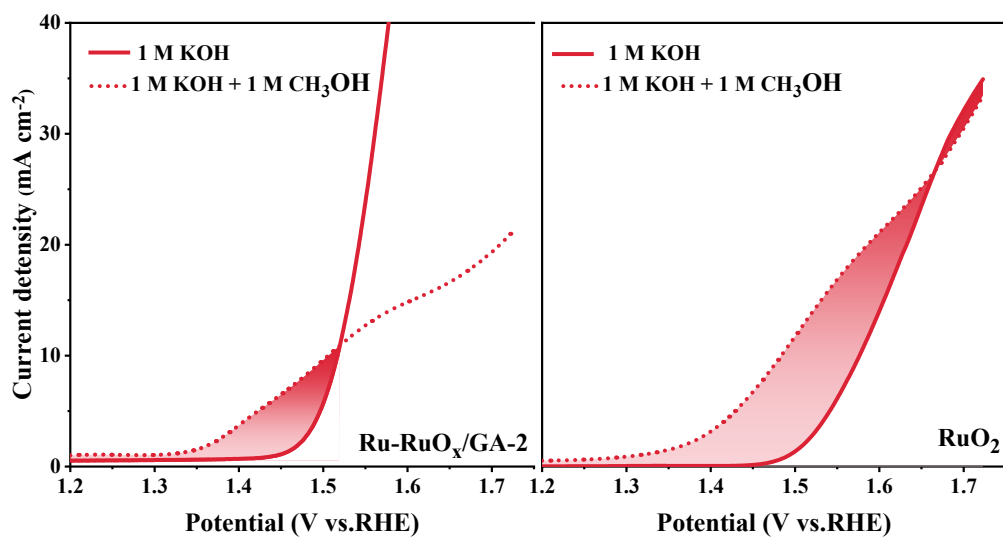


Figure S25. LSV curves for Ru-RuO_x/GA-2 and RuO₂ in 1 M KOH solution with (dashed lines) and without (solid lines) 1 M methanol.

Additionally, methanol was used as a probe to experimentally verify the weakened *OH adsorption. The

methanol oxidation reaction (MOR) follows a well-established mechanism, where the nucleophilic reagent methanol readily adsorbs onto the electrophilic reagent *OH [12, 13]. Therefore, MOR is more active on surfaces with stronger *OH adsorption. When 1.0 M methanol was introduced into a 1 M KOH solution, the current density of Ru-RuO_x/GA-2 and RuO₂ showed a significant increase compared to before adding methanol, which is attributed to the electrooxidation of methanol. The current density difference caused by MOR was quantified by calculating the filled area between the curves, which is proportional to the number of transferred charges. The current difference observed between MOR and OER on Ru-RuO_x/GA-2 is smaller than that on RuO₂, indicating weaker MOR competitive reactions, which validates the weakened *OH on Ru-RuO_x/GA-2.

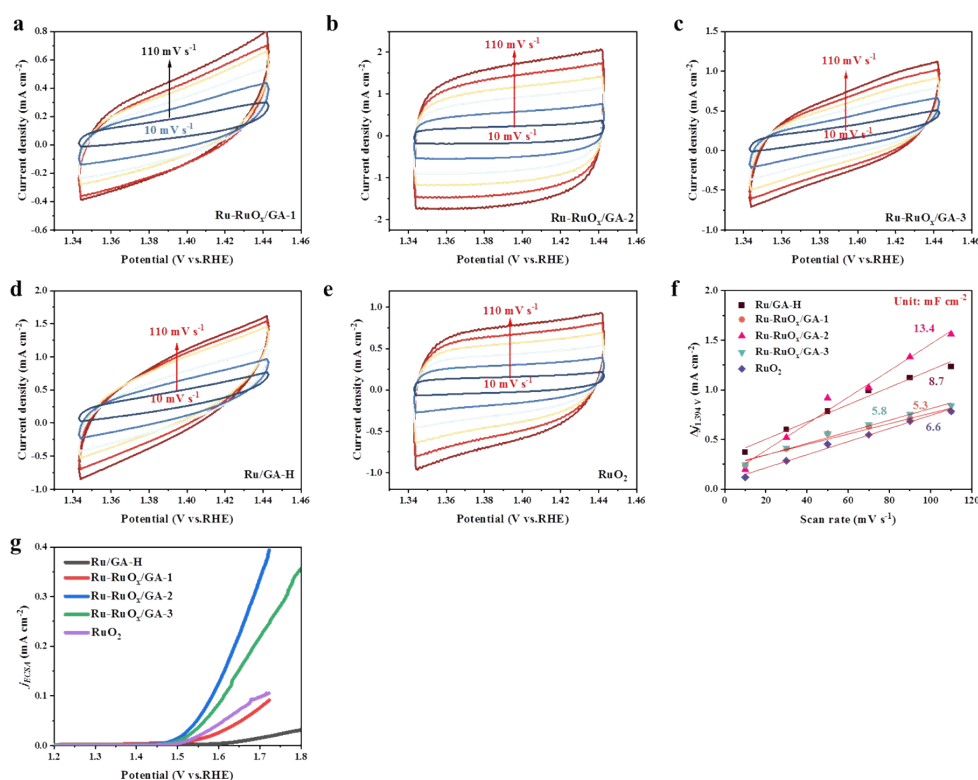


Figure S26. (a-e) CVs with different scan rates for Ru-RuO_x/GA-1, 2, 3, Ru/GA-H, and Pt/C. (f) C_{dl} values fitted according to CV curves. (g) Current densities (j_{ECSA}) normalized by ECSAs for OER.

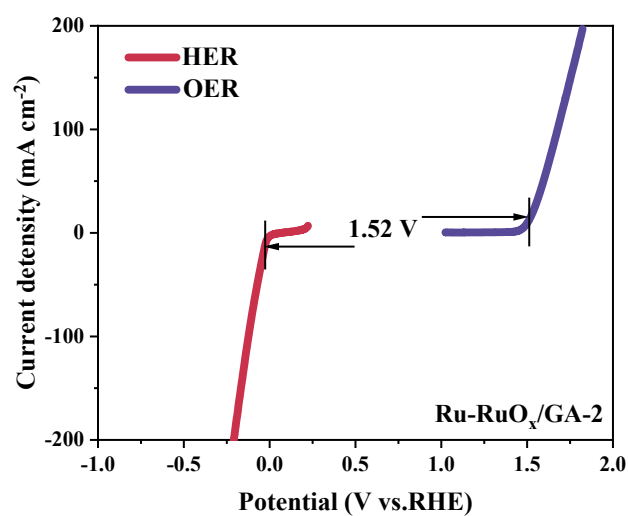


Figure S27. Theoretical electrolytic voltage to achieve a current density of 10 mA cm^{-2} .



Figure S28. (a) Optical photograph of the assembled electrolyzer. (b) Photographs of H_2 and O_2 collected at different times. (c) The amount of H_2 and O_2 varying with time.

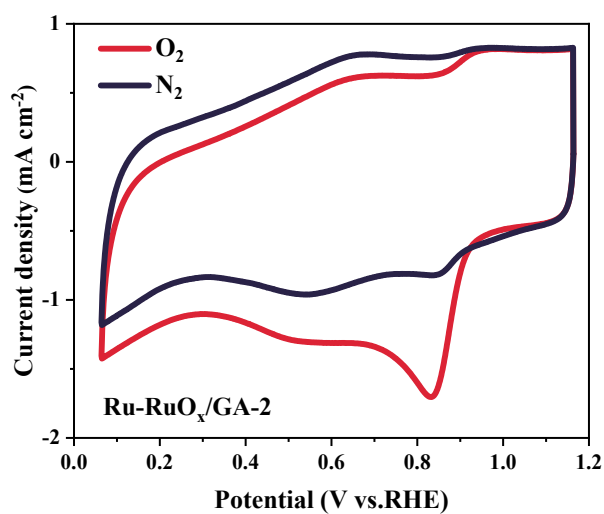


Figure S29. CV curves of Ru-RuO_x/GA-2 in both N₂-saturated and O₂-saturated 0.1 M KOH solution.

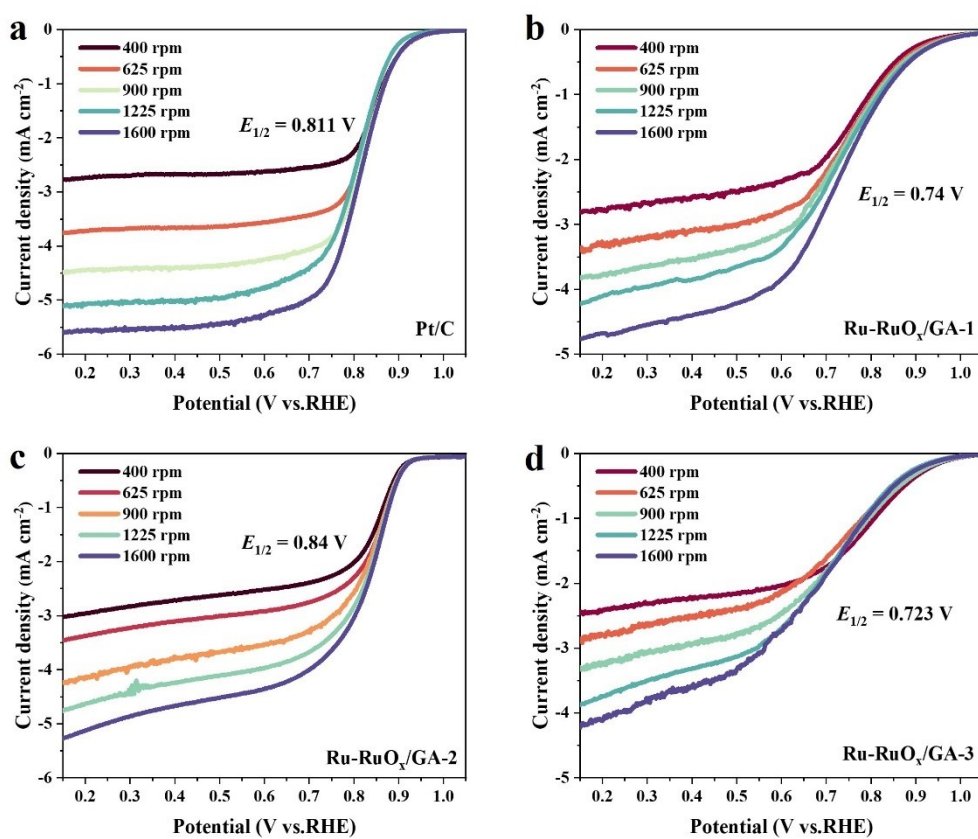


Figure S30. (a-d) ORR polarization curves in 0.1 M KOH with different rotating speed.

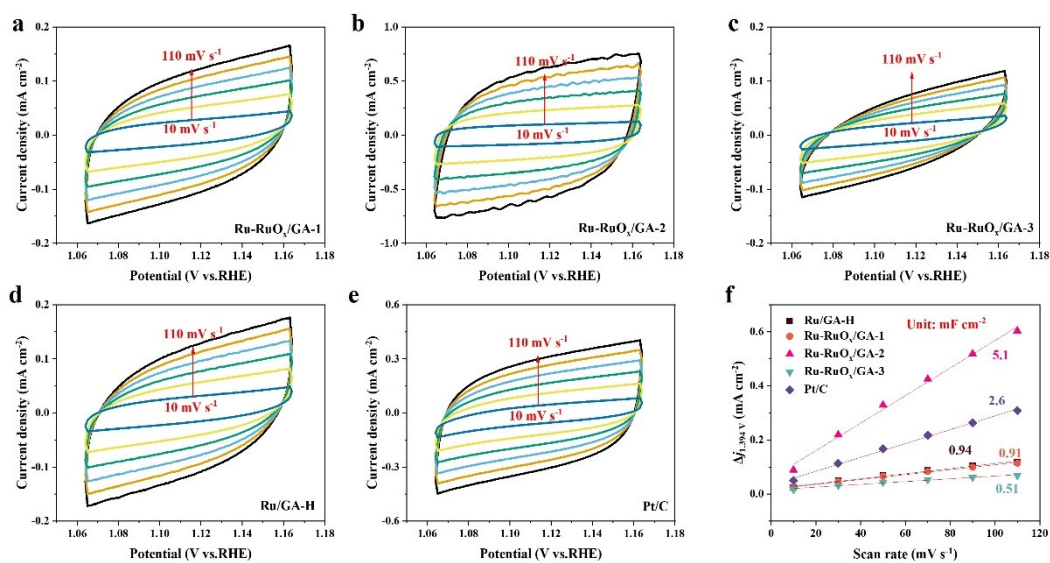


Figure S31. (a-e) CVs with different scan rates for Ru-RuO_x/GA-1, 2, 3, Ru/GA-H, and Pt/C. (f) C_{dl} values fitted according to CV curves.

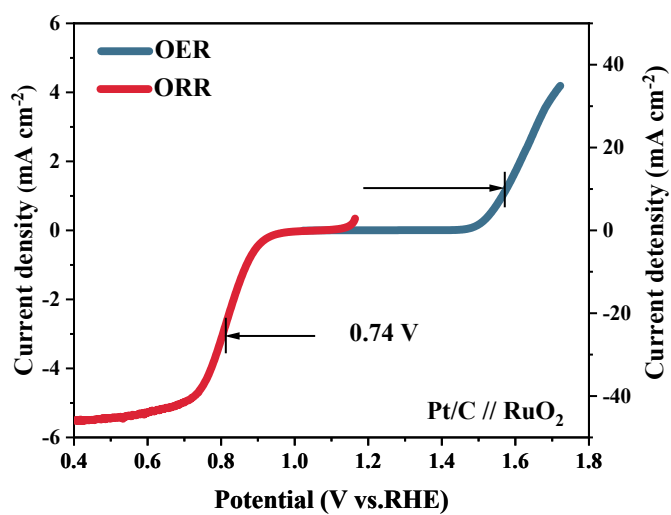


Figure S32. OER and ORR polarization curves of different electrocatalysts for Pt/C//RuO₂.

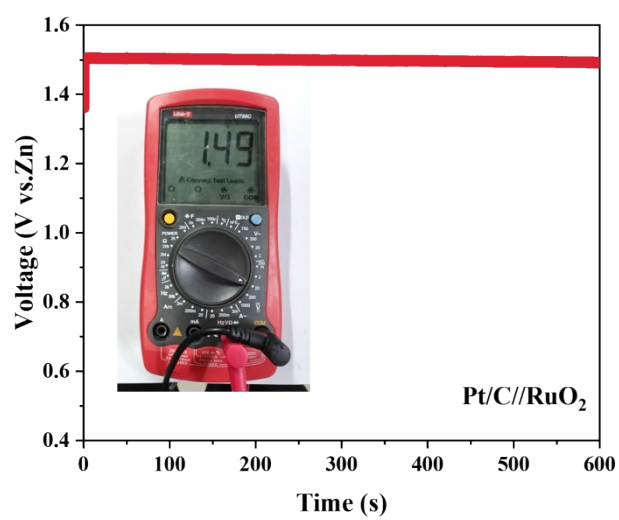


Figure S33. OCV profiles for Pt/C//RuO₂.

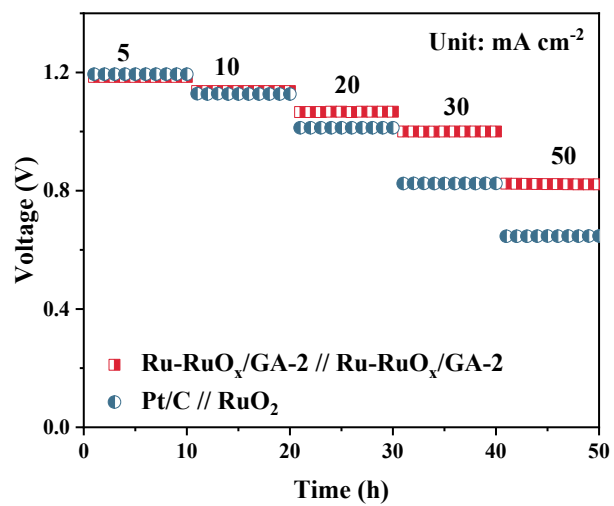


Figure S34. Galvanostatic discharge curves at various current densities of Ru-RuO_x/GA-2 and Pt/C//RuO₂ based ZABs.

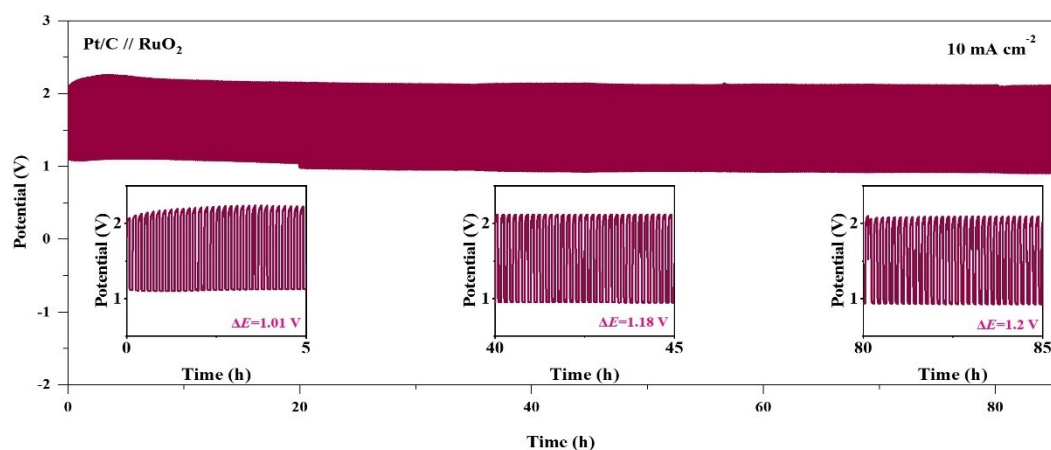


Figure S35. Long-term cycling stability of the ZABs at 10 mA cm^{-2} .

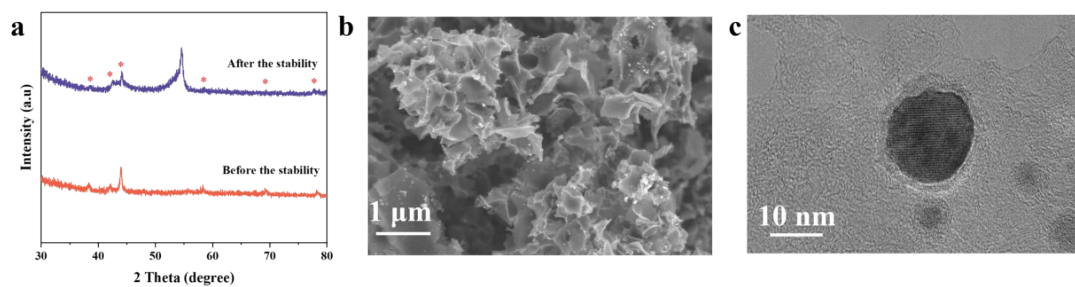


Figure S36. (a) XRD results before and after stability testing. (b-c) SEM and TEM results after stability testing.

Table S1. XPS results of Ru⁴⁺/Ru⁰ for different catalysts.

Catalysts	Ru ⁴⁺ /Ru ⁰
Ru/GA-H	0
Ru-RuO _x /GA-1	0.62
Ru-RuO _x /GA-2	0.69
Ru-RuO _x /GA-3	0.80

Table S2. The EXAFS fitting results for different Ru samples.

Sample	path	CN	R/Å	$\sigma^2/10^3$ Å	E_0	R-factor
Ru foil	Ru-Ru	1	2.67	0.00319	-8.73	0.011
Ru-RuO _x /GA-2	Ru-O	1.98	2.13	0.001	6.75	0.018
	Ru-Ru	2.08	2.83			
RuO ₂	Ru-O	2	1.97	0.00292	1.90	0.012

CN is the coordination number; S_0^2 for Ru is set as 0.829 recorded from literatures. R is interatomic distance (the bond length between central atoms and surrounding coordination atoms); σ^2 is Debye-Waller factor (a measure of thermal and static disorder in absorber-scatterer distances); E_0 is edge-energy shift (the difference between the zero kinetic energy value of the sample and that of the theoretical model).

Table S3. ECSA results of different Ru samples, Pt/C and RuO₂.

Catalysts	HER (cm ²)	OER (cm ²)	ORR (cm ²)
Ru/GA-H	175	217.5	23.5
Ru-RuO _x /GA-1	960	132.5	22.75
Ru-RuO _x /GA-2	2107.5	335	127.5
Ru-RuO _x /GA-3	247.5	145	13.25
Pt/C	585	--	65
RuO ₂	--	165	--

Table S4. Comparison of HER performance of Ru-based catalysts.

Catalysts	Overpotential @10mA cm ⁻² (mV)	Stability	Multiple electro- catalysis	References
Ru-RuO _x /GA-2	17	200 h	HER/OER/ORR	This work
fcc Ru/C-NH ₃	17	10000 cycles	HER/HOR	[14]
a/c-RuO ₂ /Ni _{0.85} Se	58	100 h	HER/OER	[15]
Ru/RuO ₂ -TiO ₂	16.4	--	HER	[16]
Pd ₂ RuO _x	14	20 h	HER/OER/ORR	[17]
Co ₁ Ru@Ru/CN _x	30	10000st	HER	[18]
Ru@WNO-C	24	10000 cycles	HER	[19]
CeO ₂ -Ru	12.9	25 h	HER	[20]
Ru/Ni-N-C	20	48 h	HER	[21]
Ru/ac-ZrO ₂	14	8000th	HER	[22]
Ru-ene	41	100 h	HER	[23]
RMNCL	19	100 h	HER/OER	[24]
RuP/Ru@CNS	15	24 h	HER	[25]
Ru/NC	21.9	1000 cycles	HER	[26]
Ru/WO ₃ -VO	21	40 h	HER	[27]

Table S5. Comparison of ZAB performance of different catalysts.

Catalysts	Open Voltage (V)	Discharge capacity (mAh g ⁻¹)	Stability	References
Ru-RuO _x /GA-2	1.56	946.4	300 h	This work
(NiFe-LDH)1/GA _{0.18}	1.50	725	220 h	[28]
CoFe-FeNC	1.447	767.5	1200 h	[29]
Mn ₂ O ₃ /RuO ₂	1.45	742.1	850 h	[30]
Co-NCS-5 Co ₂ P-NCS-60	1.50	--	60 h	[31]
RuSe ₂ CoSe ₂ /NC	1.52	--	140 h	[32]
C@Ir/CNF700	1.45	647.6	33 h	[33]
Pt@CoS ₂ -NrGO	1.41	763	55 h	[34]
MnO ₂ /Co ₂ P@SDHC	1.49	810.3	2800 h	[35]
Mo ₂ N-FeMo/HNCs	1.48	--	280 h	[36]
CoO-Mn ₃ O ₄	1.43	802	100 h	[37]
Co-N-C@mHCSs	1.41	943.1	45 h	[38]
Co-FNC	1.55	817	300 h	[39]
Co@D-NCNT/CW	1.45	785.5	500 h	[40]
SA-Fe-SNC@900	1.464	798.7	200 h	[41]
CoN-BC-0.3	1.465	776.4	330 h	[42]

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