

## Supporting Information

### **Medium-entropy iron-series metal sulfide for energy-saving hydrogen production and highly-efficient direct hydrazine borane fuel cell**

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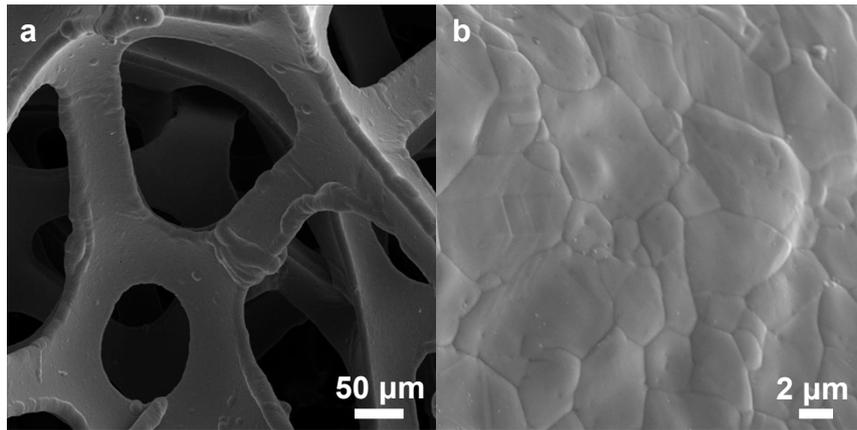
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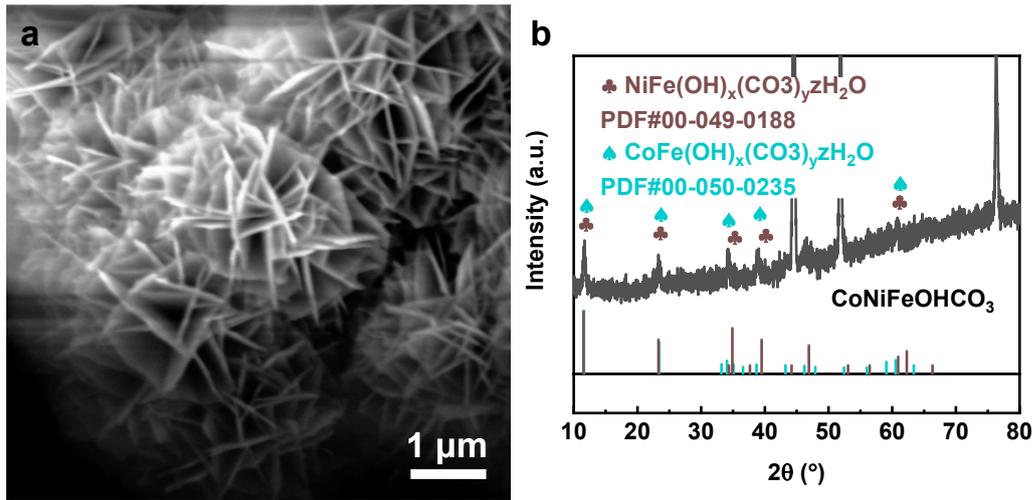
## **Experimental section**

### **Materials and reagents**

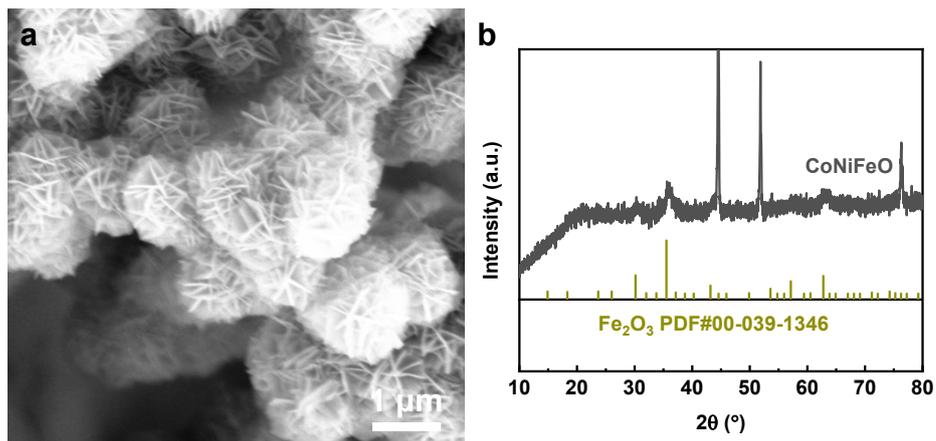
All chemicals were obtained from commercial sources. Hydrazine hemisulfate salt ( $\text{N}_2\text{H}_4 \cdot 1/2\text{H}_2\text{SO}_4$ , Aldrich, 98%), sodium borohydride ( $\text{NaBH}_4$ , Aladdin, 99.5%), nickel nitrate hexahydrate ( $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ , Aladdin, 98%), cobalt nitrate hexahydrate ( $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ , Aladdin, 99.9%), ammonium fluoride ( $\text{NH}_4\text{F}$ , Macklin), Iron nitrate nonahydrate ( $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ , Aladdin, 98%), urea ( $\text{H}_2\text{NCONH}_2$ , Aladdin, 98%), hydrochloric acid ( $\text{HCl}$ , Aladdin, 37%), Pt/C (TEC10E20E, Tanaka), nickel foam (1.0 mm, Kunshan Lv Chuang), carbon paper (TGP-H-060, Toray) were used as received without further treatment. Hydrazine borane ( $\text{N}_2\text{H}_4\text{BH}_3$ ) was synthesized according to our previous reported study.<sup>S1</sup> Ultrapure water used in the experiment was purified using a Millipore system. The anion ion exchange member (FAA-3-50, Fumasep) was treated with 1 M KOH solution for 24 h prior to utilization.



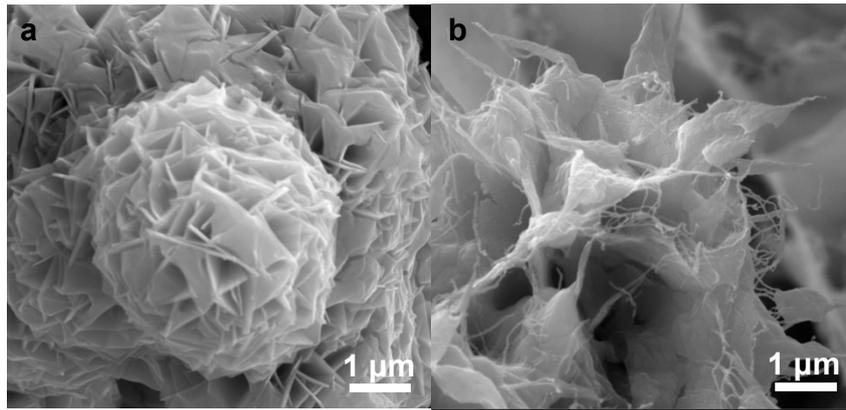
**Figure S1.** SEM images of NF.



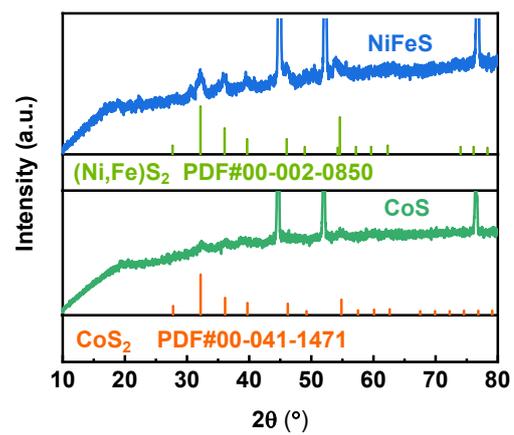
**Figure S2.** (a) SEM image and (b) XRD pattern of  $\text{CoNiFeOHCO}_3$ .



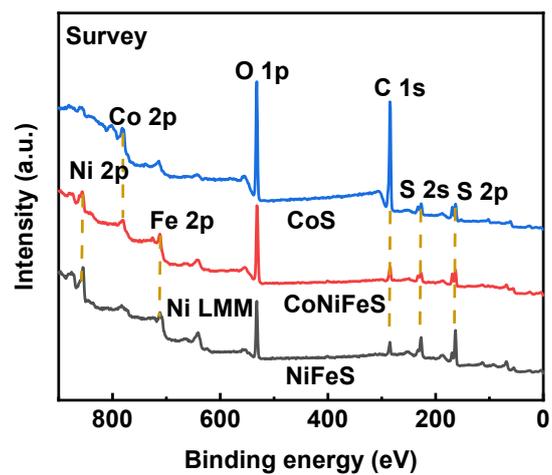
**Figure S3.** (a) SEM image and (b) XRD pattern of CoNiFeO.



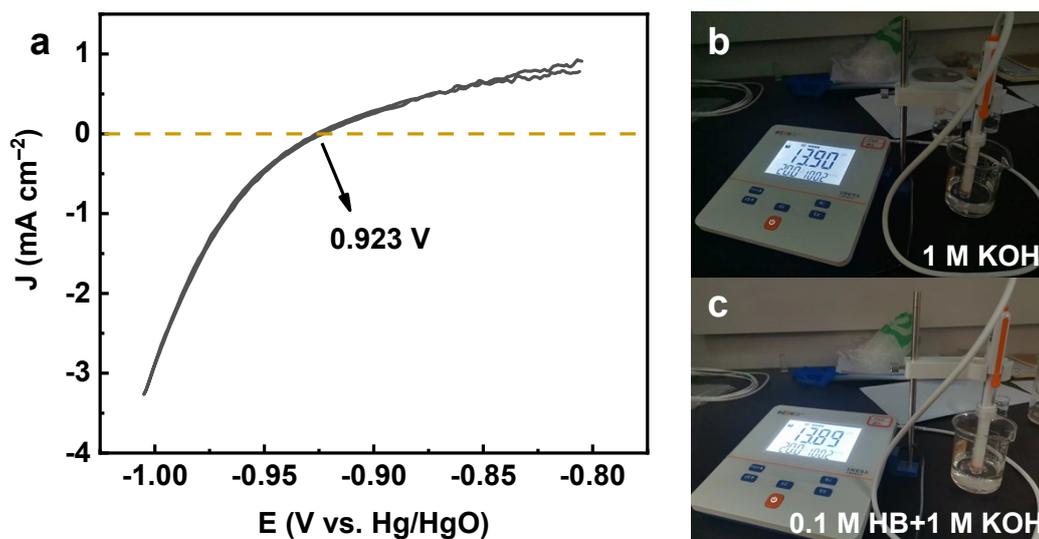
**Figure S4.** SEM images of (a) NiFeS and (b) CoS.



**Figure S5.** XRD patterns of NiFeS and CoS.

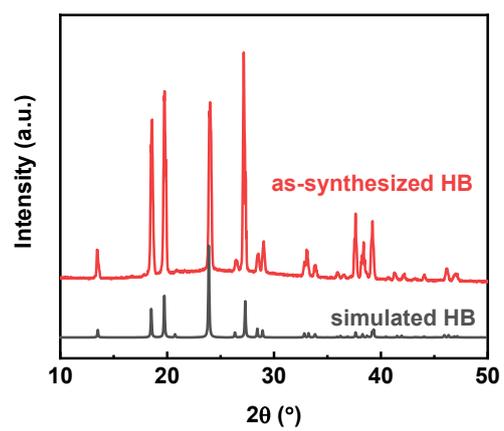


**Figure S6.** XPS survey spectra of CoNiFeS, NiFeS, and CoS.

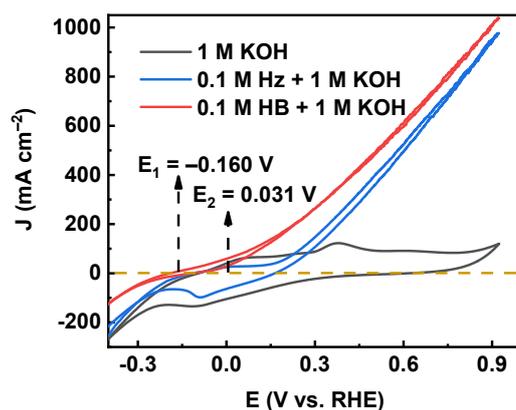


**Figure S7.** (a) Calibration of Hg/HgO reference electrode in 1 M KOH. The corresponding digital photographs of *pH* value in (b) 1 M KOH solution and (c) 1 M KOH + 0.1 M HB solution. All the potentials were calculated to the reversible hydrogen electrode (RHE) by the equation:  $E_{\text{RHE}} = E_{\text{Hg/HgO}} + 0.923 \text{ V}$ .

Calibration of the Hg/HgO reference electrode was performed in H<sub>2</sub> saturated 1 M KOH using a three electrodes system: two 1.0 cm<sup>2</sup> Pt electrode served as working and counter electrodes, respectively. The Hg/HgO electrode acted as the reference. Cyclic voltammetry was recorded at 5 mV s<sup>-1</sup>.

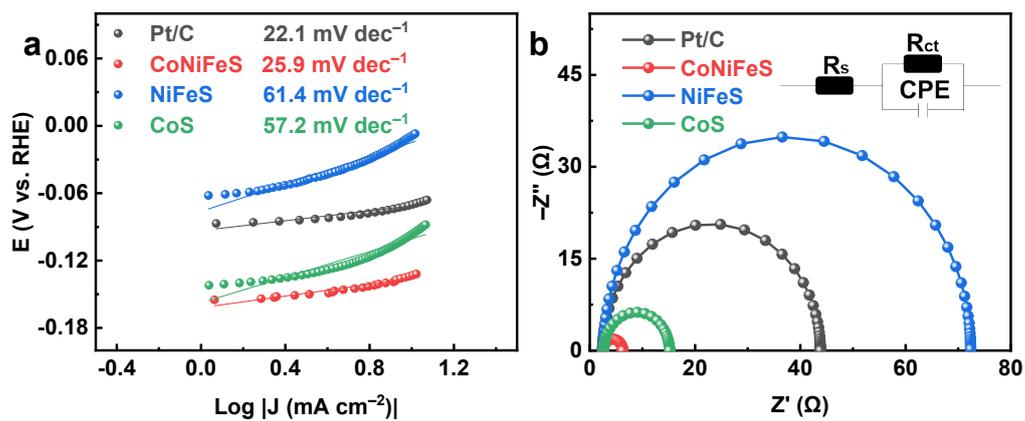


**Figure S8.** XRD patterns of home-made HB and simulated HB.

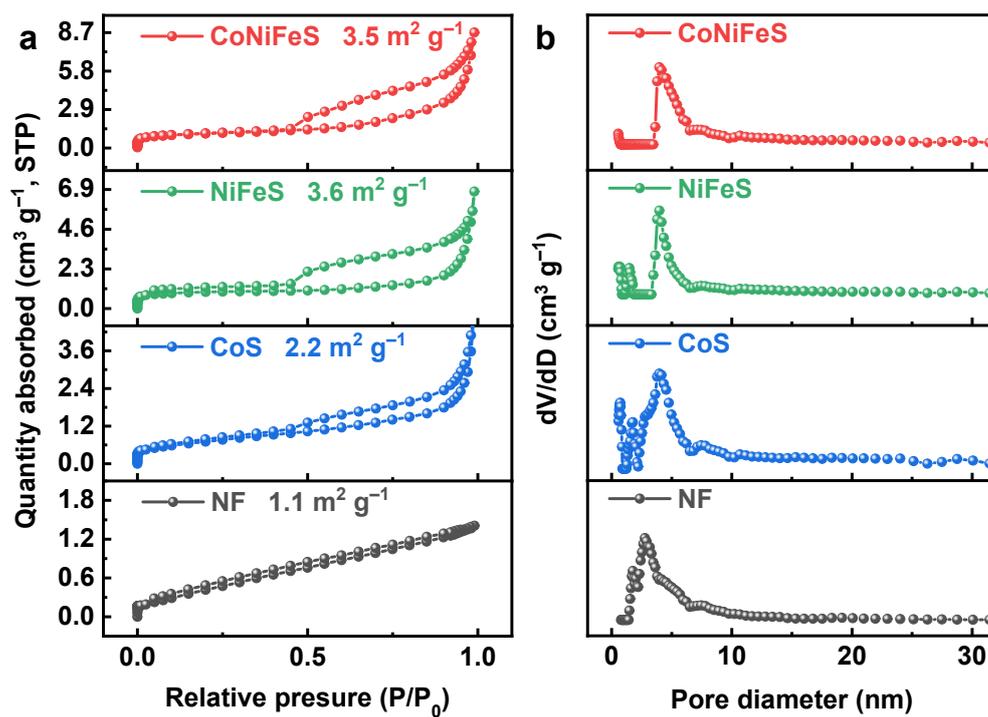


**Figure S9.** CV curves of HBOR and HzOR.

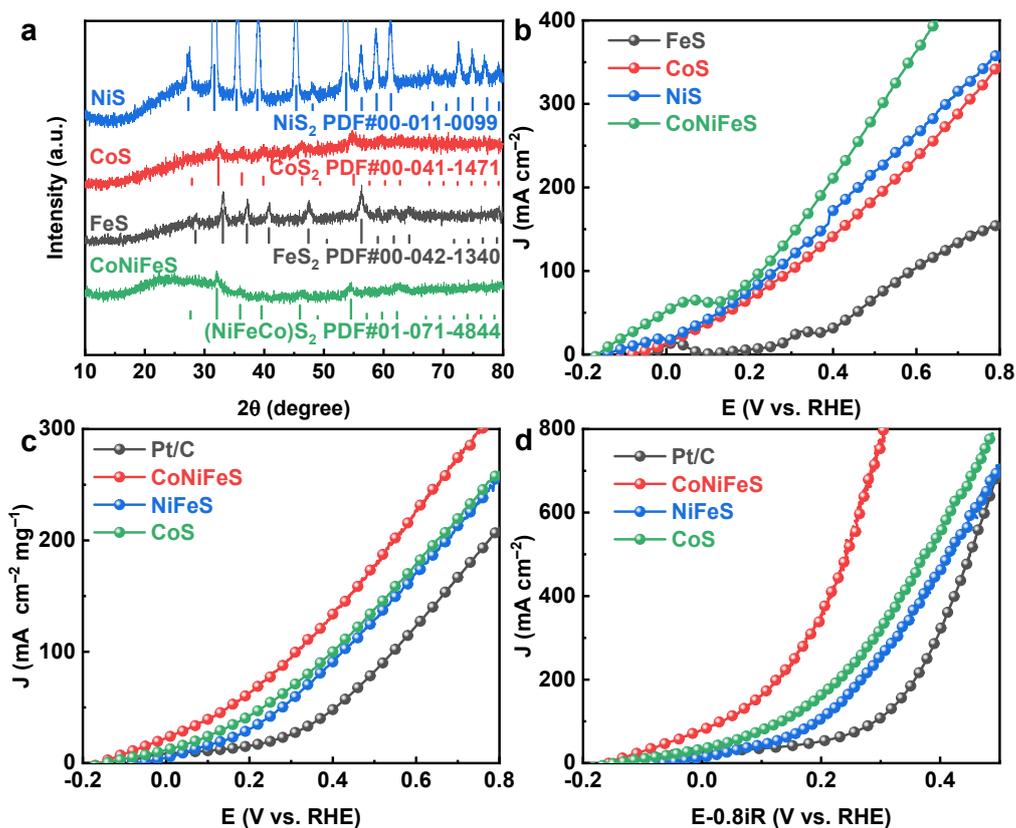
As shown in **Figure S9**, CV tests were conducted in 0.1 M HB + 1 M KOH and 0.1 M Hz + 1 M KOH, respectively. Compared to HzOR ( $E_{\text{onset}} = 0.031$  V), the HBOR ( $E_{\text{onset}} = -0.160$  V) exhibits a much lower onset potential and delivers much larger oxidation currents across the same potential range. All these results indicate that the HBOR is more thermodynamically favorable on the CoNiFeS catalyst, which is greatly beneficial for the practical applications in both energy-saving hydrogen production and direct liquid fuel cell systems.



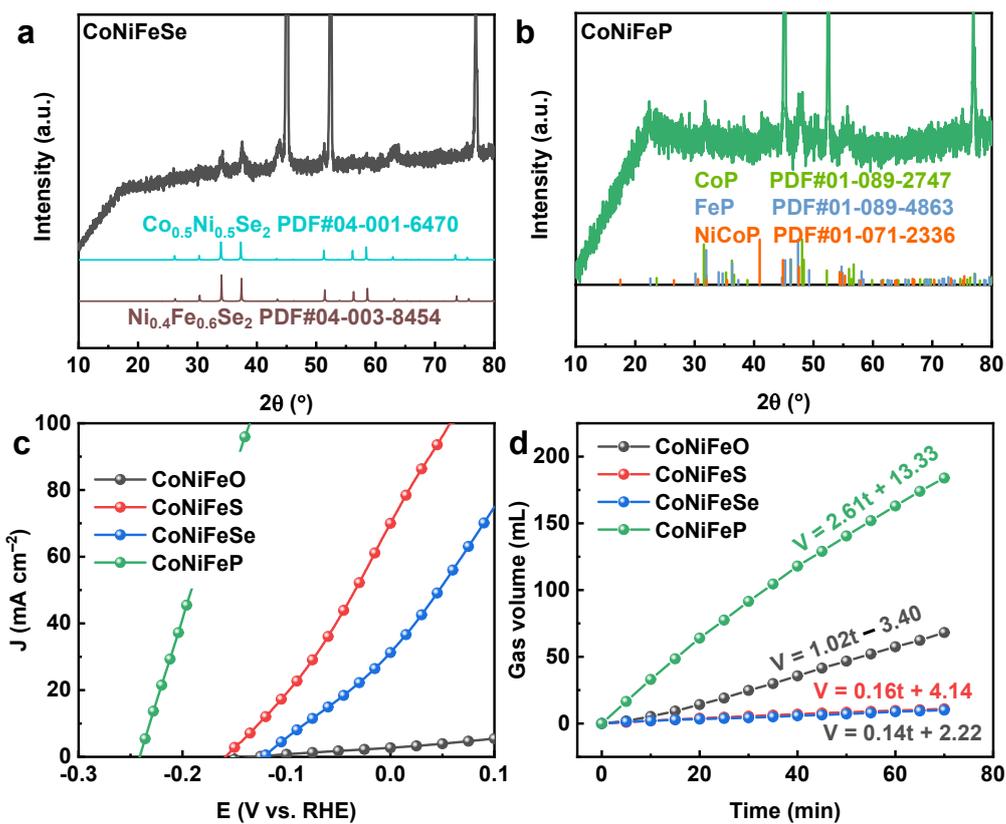
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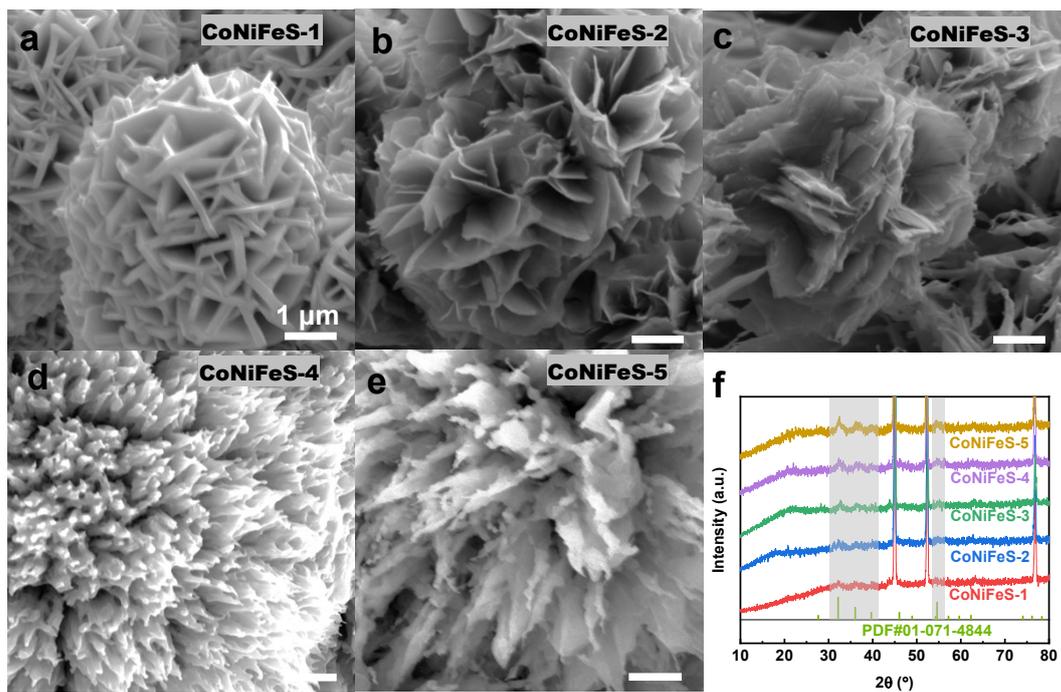
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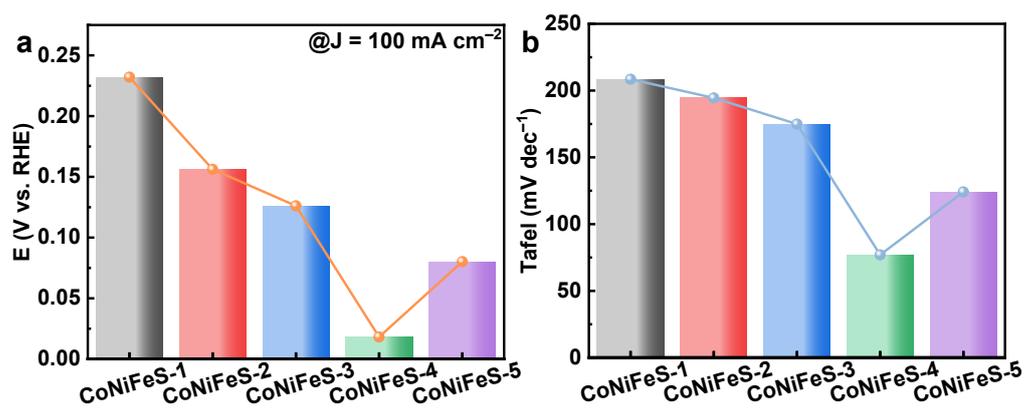
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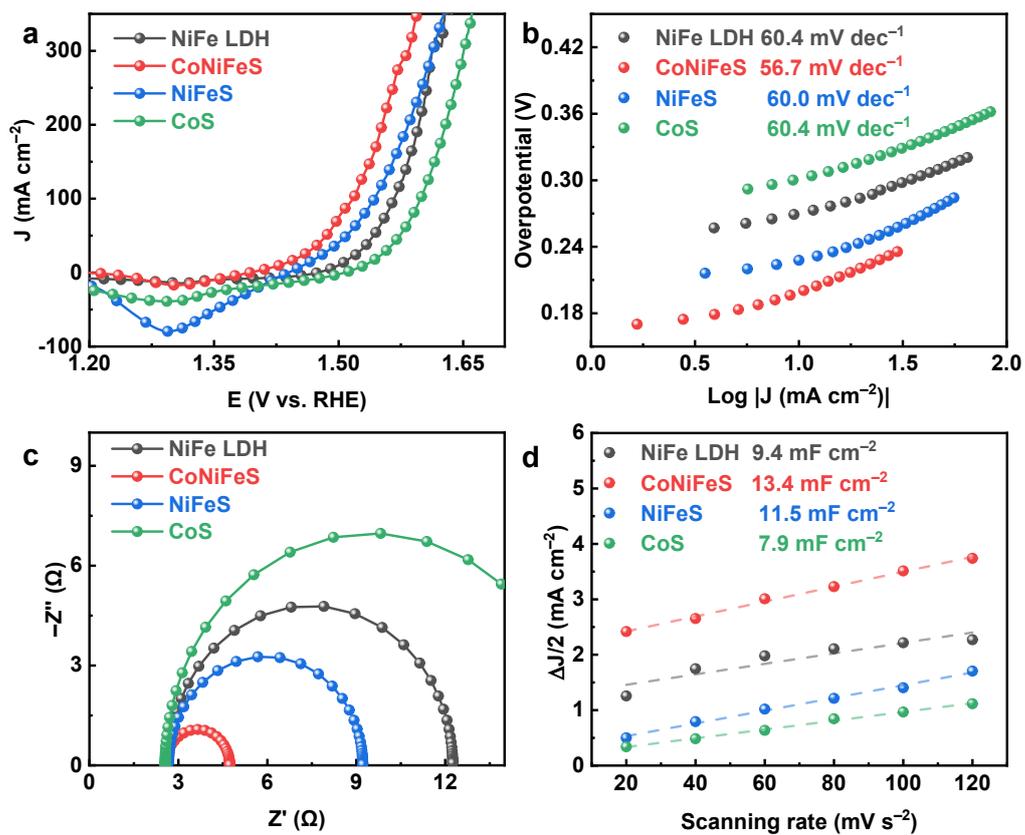
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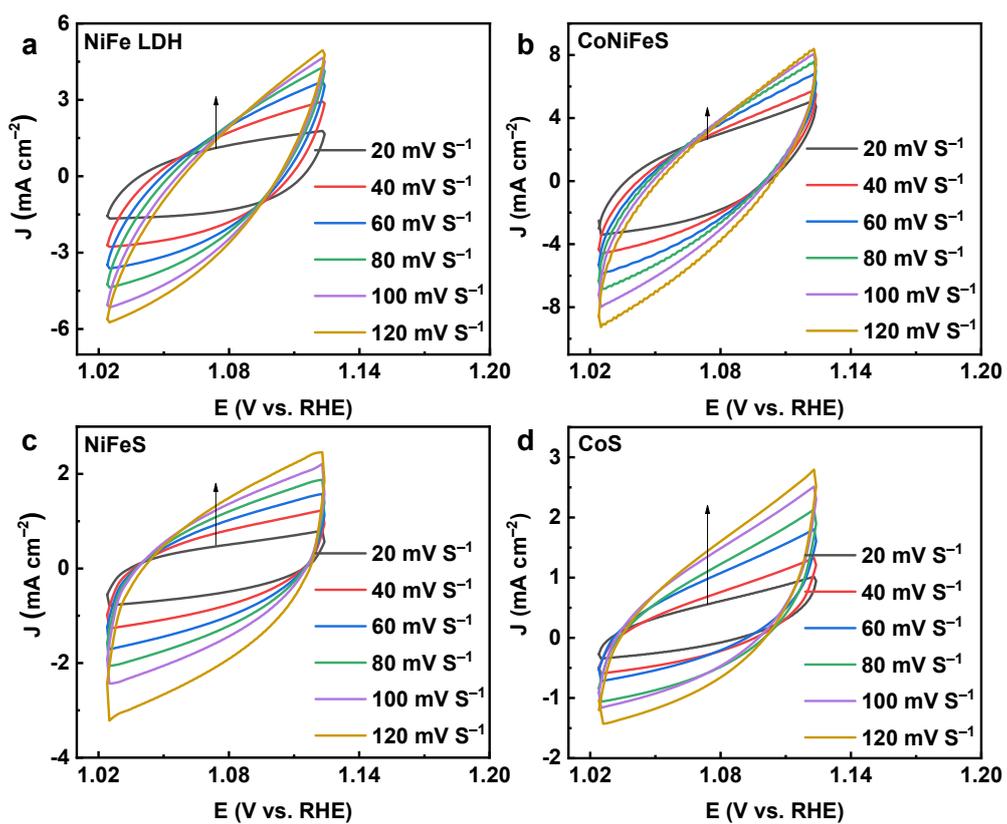
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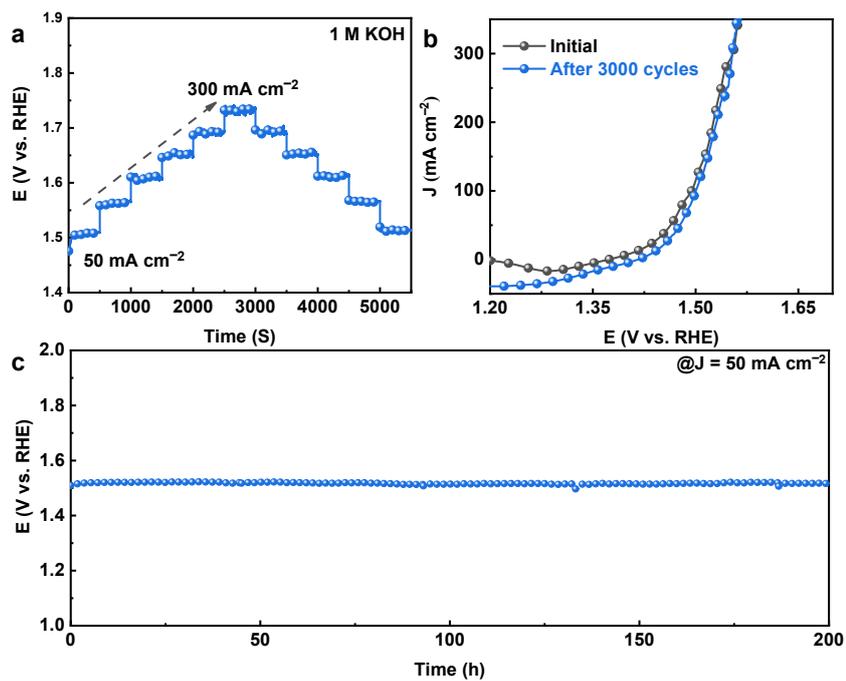
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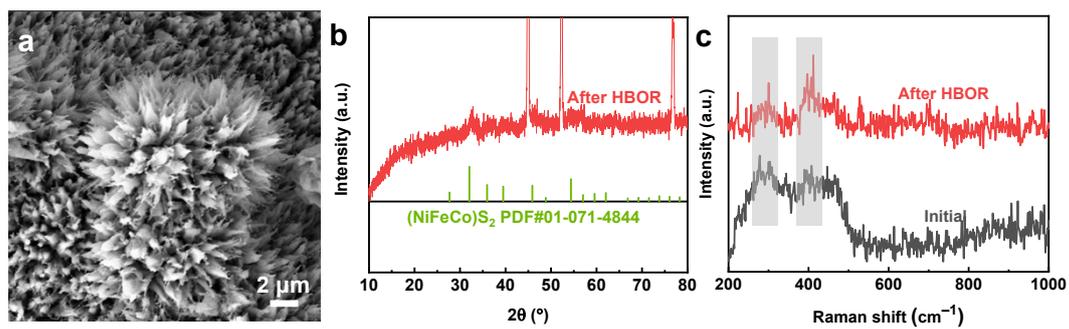
**Figure S16.** Electrochemical performance of CoNiFeS, NiFeS, CoS, and NiFe LDH: (a) LSV curves with 80%  $iR_s$  compensation for OER, (b) Tafel slopes, (c) Nyquist plots, and (d) Double-layer capacitance  $C_{dl}$ .



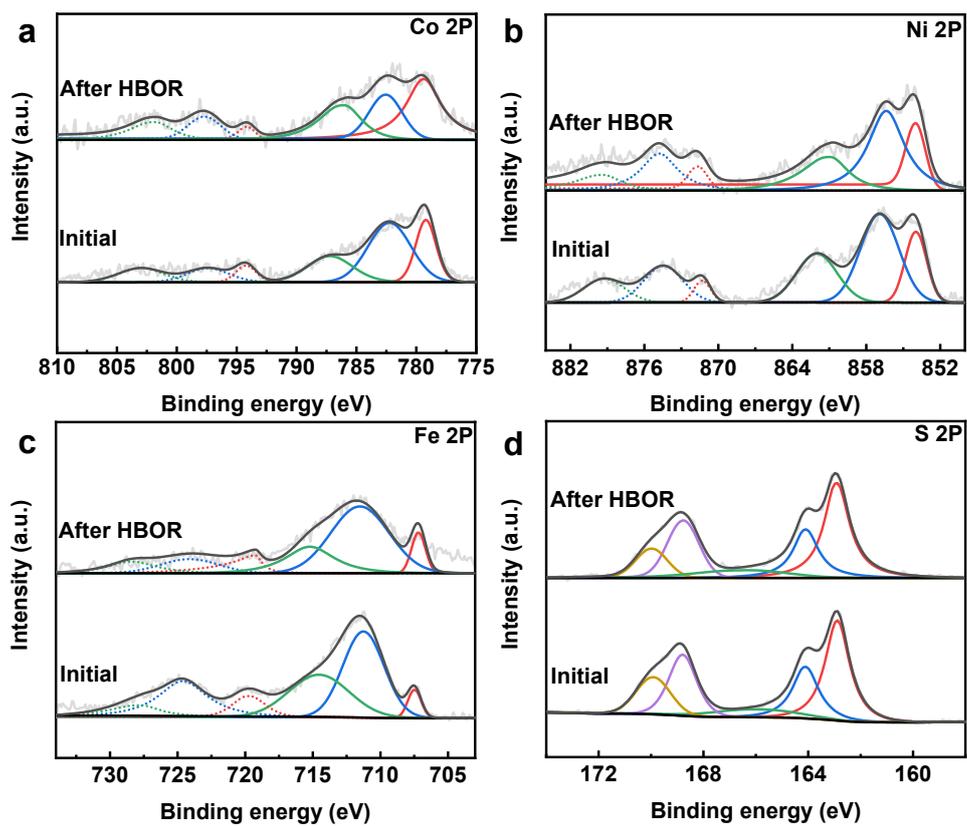
**Figure S17.** CV curves of (a) NiFe LDH, (b) CoNiFeS, (c) NiFeS, (d) NiFe LDH measured in the potential range of 1.024–1.124 V vs. RHE at different scan rates in 1 M KOH.



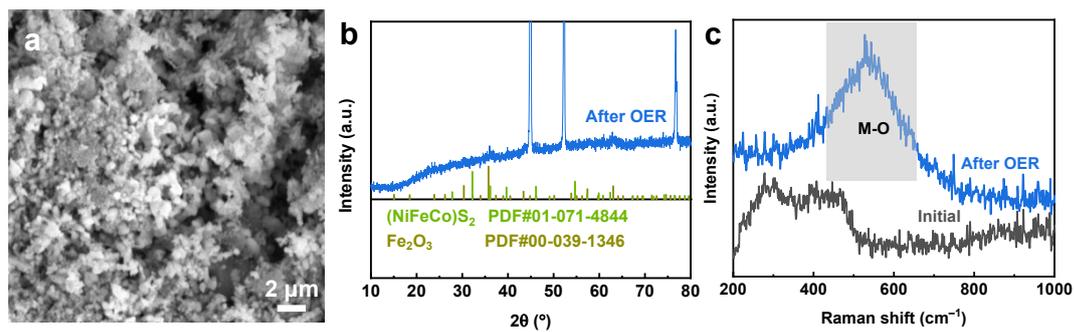
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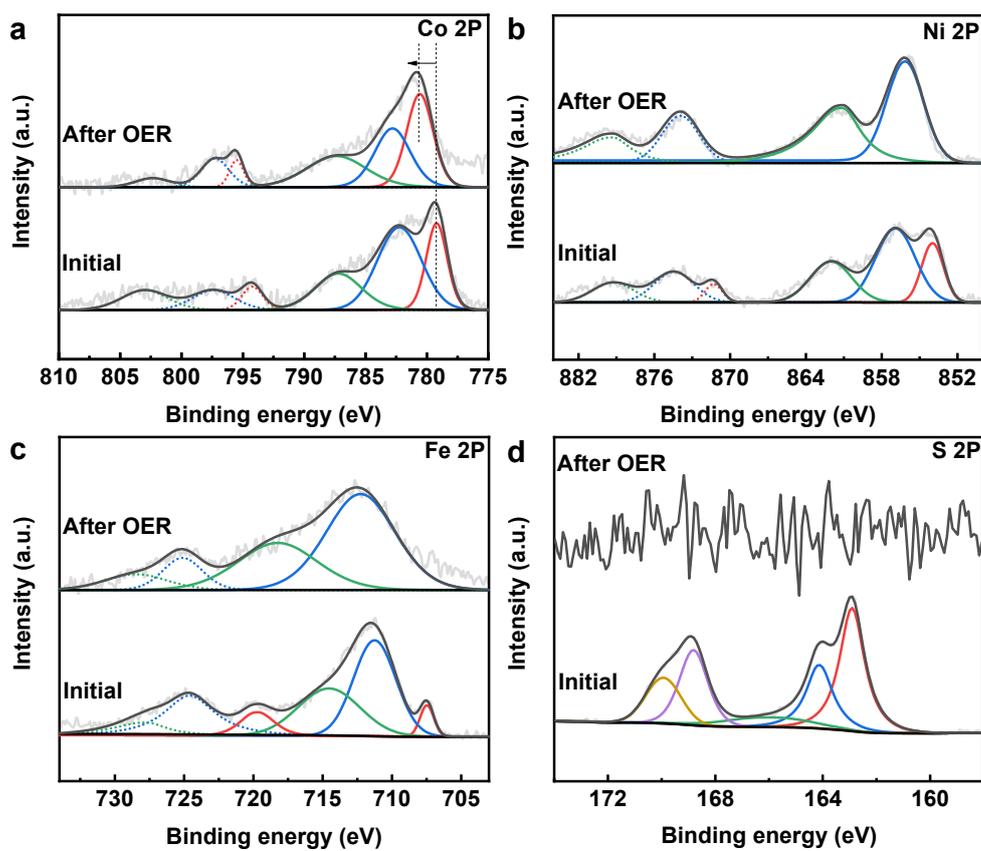
**Figure S19.** Characterizations of CoNiFeS after HBOR stability test: (a) SEM image, (b) XRD pattern, and (c) Raman spectra.



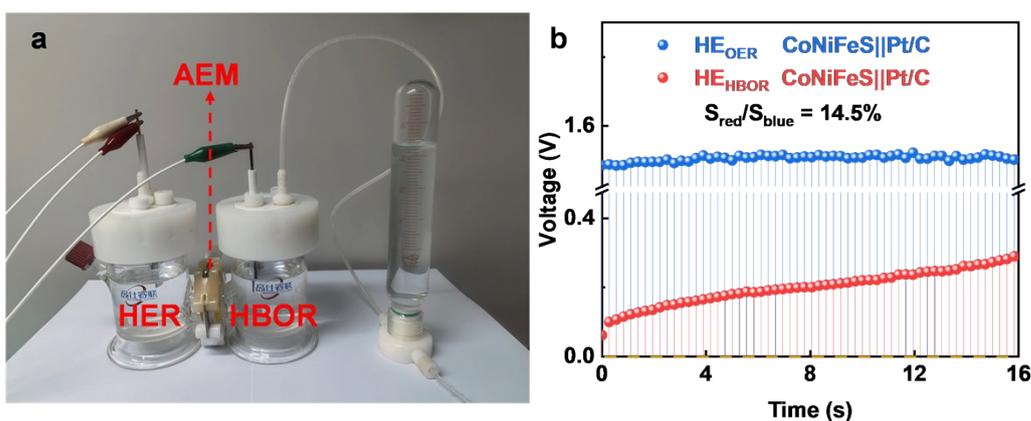
**Figure S20.** Comparison of XPS characterizations before and after HBOR stability test.



**Figure S21.** Characterizations of CoNiFeS after OER stability test: (a) SEM image, (b) XRD pattern, and (c) Raman spectra.



**Figure S22.** Comparison of XPS characterizations before and after OER stability test.

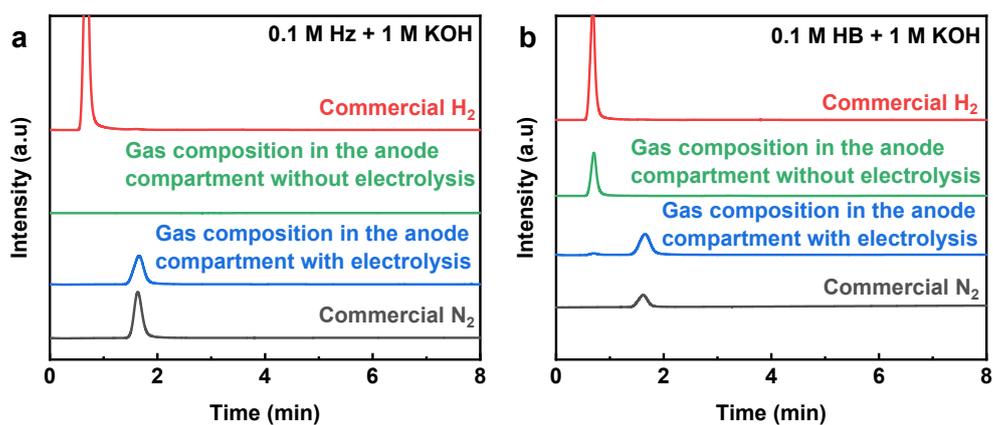


**Figure S23.** (a) Photograph of H-type cell for  $\text{HE}_{\text{HBOR}}$  and  $\text{HE}_{\text{OER}}$  tests, (b) Schematic diagram of integral area under the voltage–time curve for relative energy consumption calculation.

The relative energy consumption and the HBOR selectivity were calculated based on the electrochemical measurements in a standard H-type cell (**Figure S23**).

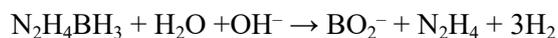
The energy consumption ( $W$ ) is the integral of power ( $P$ ) over time ( $t$ ), where  $P = V \propto I$ . Since the current ( $I$ ) is constant and same for both the HBOR||HER system ( $\text{HE}_{\text{HBOR}}$ ) and the OER||HER system ( $\text{HE}_{\text{OER}}$ ), the energy consumption is directly proportional to the integral of the voltage over time ( $W = I \propto \int V dt$ ). The term  $\int V dt$  represents the area under the voltage–time curve. Therefore, the ratio of the areas under the voltage–time curves represent the relative energy consumption. The relative energy consumption of  $\text{HE}_{\text{HBOR}}$  was calculated to be 14.5% compare to  $\text{HE}_{\text{OER}}$ , confirming the substantial energy–saving achieved by the novel  $\text{HE}_{\text{HBOR}}$  system.

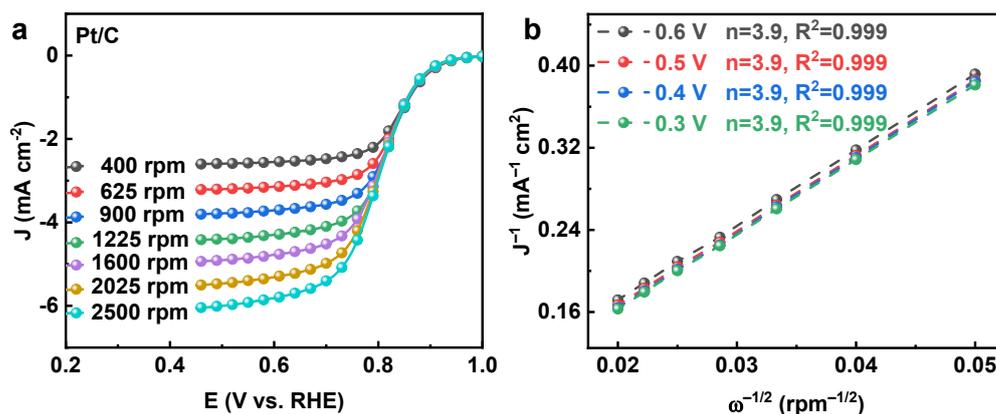
The HBOR selectivity ( $\alpha$ ) was determined by quantifying the volume of evolved gases at the anode and cathode using a gas collection method. The volume of gas generated at the anode is denoted as  $V_{\text{A}}$ , while denoted as  $V_{\text{C}}$  at the cathode. The anode gas consists of nitrogen produced from electrochemical HB oxidation and hydrogen generated from partial HB hydrolysis, while the cathode undergoes the hydrogen evolution reaction (HER) to produce hydrogen. Therefore, the theoretical volume of nitrogen produced by the electrochemical reaction at the anode is  $V_{\text{C}}/5$ , and the volume of hydrogen correspondingly generated from hydrolysis is  $V_{\text{A}} - V_{\text{C}}/5$ . Accordingly, the selectivity ( $\alpha$ ) can be calculated according to the following formula:  $\alpha = 3V_{\text{C}}/(2V_{\text{C}} + 5V_{\text{A}})$ .



**Figure S24.** (a) Gas chromatography (GC) analysis results of anode gas products: The electrolyte consists of (a) 0.1 M Hz + 1 M KOH and (b) 0.1 M HB + 1 M KOH.

When the electrolytes are different, the gas phase detection results are similar, except that hydrogen gas is present in the electrolyte containing HB. This indicates that the sulfide catalyst can induce partial slow hydrolysis of  $\text{BH}_3$ , while  $\text{N}_2\text{H}_4$  does not undergo spontaneous decomposition.





**Figure S25.** ORR performance of commercial Pt/C.

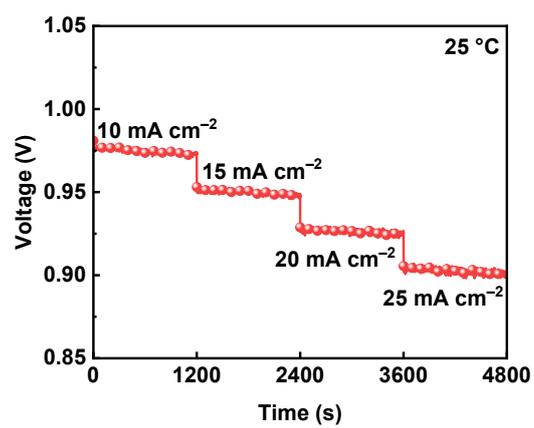
The electron transfer number ( $n$ ) is calculated by the Koutecky–Levich equation as follow:<sup>S2</sup>

$$\frac{1}{j} = \frac{1}{j_k} + \frac{1}{j_d}$$

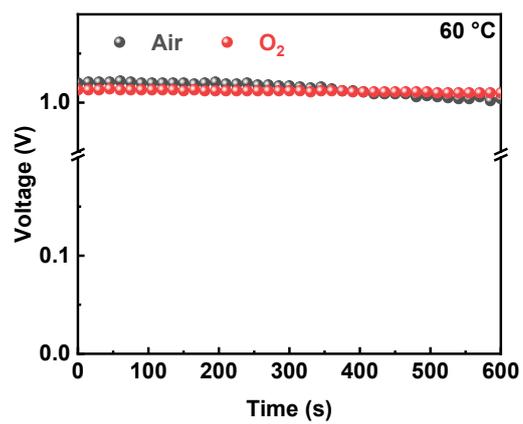
$$j_d = 0.20nFCD^{\frac{2}{3}}\nu^{\frac{1}{6}} \cdot \omega^{\frac{1}{2}}$$

$j_k = nkFC_{O_2}$  where  $j$  is the measured current density ( $\text{mA cm}^{-2}$ ),  $j_d$  is the diffusion limited current density ( $\text{mA cm}^{-2}$ ),  $j_k$  is the kinetic current densities ( $\text{mA cm}^{-2}$ ).  $F$  is the Faraday constant ( $96485 \text{ C mol}^{-1}$ ).  $D_{O_2}$  is the diffusion coefficient of  $O_2$  ( $1.93 \times 10^{-5} \text{ cm}^2 \text{ s}^{-1}$ ),  $\nu$  is the kinetic viscosity ( $1.13 \times 10^{-2} \text{ cm}^2 \text{ s}^{-1}$ ),  $\omega$  is the rotation speed of electrode (rpm), and  $C_{O_2}$  is the bulk concentration of  $O_2$  dissolved in 0.1 M KOH ( $1.2 \times 10^{-6} \text{ mol mL}^{-1}$ ).  $\nu$  ( $0.01 \text{ cm}^2 \text{ s}^{-1}$ ) is the viscosity of the 0.1 M KOH electrolyte solution, and  $k$  is the electron–transfer rate constant.

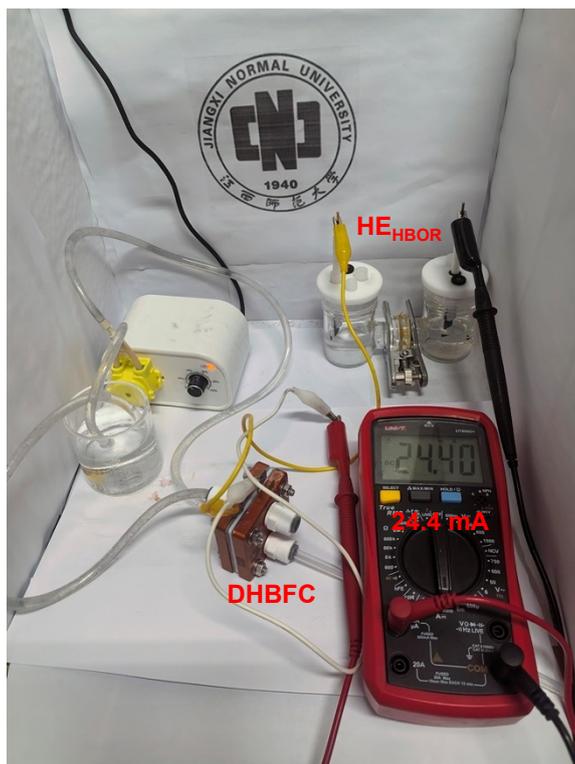
LSV measurements display that the Pt/C exhibits a half–wave potential ( $E_{1/2}$ ) and diffusion limited current density ( $j_L$ ) of  $E_{1/2} = 0.808 \text{ V}$  and  $j_L = 5.06 \text{ mA cm}^{-2}$  at 1600 rpm (room temperature).



**Figure S26.** Stability measurements at different current densities of the DHBFC with CoNiFeS (+) || Pt/C (-).



**Figure S27.** The open-circuit voltage of DHBFC performed at 60 °C.



**Figure S28.** Digital photograph of HE<sub>HBOR</sub> (CoNiFeS||Pt/C) system for H<sub>2</sub> production self-powered by DHBFC (CoNiFeS||Pt/C).

**Table S1.** ICP–OES results of CoNiFeS electrocatalyst.

CoNiFeS	No.	wt (%)	average wt (%)	at (%)
Co	1	12.4	12.4	20.6
	2	12.5		
	3	12.4		
Ni	1	24.3	24.3	39.1
	2	24.4		
	3	24.3		
Fe	1	22.1	22.4	40.3
	2	22.5		
	3	22.6		

The value of mole–fraction mixing entropy ( $S_{\text{mix}}$ ) can be used to classify the materials.

The  $S_{\text{mix}}$  can be calculated according to the follow equation.

In the as-prepared CoNiFeS catalyst, Co:Ni:Fe  $\approx$  1:2:2.

$$S_{\text{mix}} = -R \sum_{i=1}^n x_n \ln x_n = 1.06R$$

where  $n$  is the number of elemental species,  $x_n$  is the mole fraction of component  $n$ , and  $R$  is the universal gas constant ( $R = 8.314 \text{ J K}^{-1} \text{ mol}^{-1}$ ).

Materials with  $S_{\text{mix}} \geq 1.5R$  are considered to be high–entropy (HE) systems, materials with  $1.5R > S_{\text{mix}} \geq 1R$  are considered to be medium–entropy (ME) systems, and materials with  $S_{\text{mix}} < 1R$  are considered to be low–entropy (LE) systems.

**Table S2.** Binding energies of Co 2p in CoNiFeS and its comparative electrocatalysts.

	<b>CoNiFeS</b>	<b>NiFeS</b>	<b>CoS</b>
Co-S	779.2/794.2	—	779.1/794.2
Co <sup>2+</sup>	782.2/797.4	—	782.7/798.7
Sat.	787.2/803.0	—	787.5/803.9

**Table S3.** Binding energies of Ni 2p in CoNiFeS and its comparative electrocatalysts.

	<b>CoNiFeS</b>	<b>NiFeS</b>	<b>CoS</b>
Ni-S	854.0/871.3	854.1/871.3	—
Ni <sup>3+</sup>	856.9/874.5	856.5/874.6	—
Sat.	862.0/879.3	861.4/879.3	—

**Table S4.** Binding energies of Fe 2p in CoNiFeS and its comparative electrocatalysts.

	<b>CoNiFeS</b>	<b>NiFeS</b>	<b>CoS</b>
Fe-S	707.5/720.3	707.5/719.7	—
Fe <sup>3+</sup>	711.3/724.6	710.8/723.9	—
Sat.	714.6/727.7	713.2/727.1	—

**Table S5.** Binding energies of S 2p in CoNiFeS and its comparative electrocatalysts.

	<b>CoNiFeS</b>	<b>NiFeS</b>	<b>CoS</b>
S <sup>2-</sup>	162.9/164.1	162.9/164.1	162.6/163.7
S-O	168.8/169.9	169.0/170.0	169.3/170.4
Sat.	166.1	165.2	164.4

**Table S6.** OER performance comparison with recently reported electrocatalysts.

No.	Catalyst	Overpotential (mV, J=10 mA cm <sup>-2</sup> )	Tafel (mV dec <sup>-1</sup> )	Ref.
1	CoNiFeS	199	56.7	This work
2	Fe <sub>0.8</sub> Ni <sub>0.15</sub> S <sub>1.05</sub>	228	53.0	S3
3	Ni-Fe disulfide@ox hydroxide heterostructure	230	42.6	S4
4	Fe <sub>3</sub> O <sub>4</sub> /FeS <sub>2</sub> /NF	253	48.0	S5
5	Fe <sub>x</sub> Ni <sub>1-x</sub> S <sub>2</sub> nanosheets	260	46.0	S6
6	Fe-Ni <sub>3</sub> S <sub>2</sub> /AF	267	36.0	S7
7	Co-NC@CoFeS <sub>2</sub>	275	62.9	S8

**Table S7.** Recently reported small-molecule-based coupled electrolyzers.

Anodic catalyst	Electrolyte (substrate + 1 M KOH)	Coupled electrolyzer	$V_{\text{cell@J}}$ (V, mA cm <sup>-2</sup> )	Ref.
<b>CoNiFeS</b>	<b>0.1 M HB</b>	<b>HBOR  HER</b>	<b>0.051@10</b> <b>0.08@20</b> <b>0.176@50</b>	<b>This work</b>
NiCoP@CoFeP	0.1 M HB	HBOR  HER	0.078@10	S9
Zn <sub>0.08</sub> Co <sub>0.92</sub> P	0.5 M urea	UOR  HER	1.38@10	S10
Ni <sub>3</sub> N nanosheets/CC	0.33 M urea	UOR  HER	1.44@10	S11
Cu- $\alpha$ -Ni(OH) <sub>2</sub> /NF	0.33 M urea	UOR  HER	1.49@10	S12
V-Ni <sub>3</sub> N/NS	0.1 M hydrazine	HzOR  HER	0.264@50	S13
Ni-SN@C	0.1 M hydrazine	HzOR  HER	0.366@10	S14
Cu <sub>1</sub> Ni <sub>2</sub> -N	0.5 M hydrazine	HzOR  HER	0.24@10	S15
CoSe <sub>2</sub> nanosheet	0.5 M hydrazine	HzOR  HER	0.164@10	S16
Co(OH) <sub>2</sub> @HOS/CP	0.5 M methanol	MOR  HER	1.497@10	S17
SA In-Pt NWs/C	0.5 M ethanol	EOR  HER	0.62@10	S18
PtCu nanoframe	0.5 M ethanol	EOR  HER	0.58@10	S19
MoO <sub>x</sub> /Pt	0.1 M glycerol	GOR  HER	0.70@10	S20
RhIr/Ti//HEA- CoNiCuMnMo	0.1 M glycerol	GOR  HER	0.55@10	S21
Pt/C//Fe <sub>2</sub> P/SS	0.5 M glucose	GOR  HER	1.22@10	S22
Fe <sub>0.1</sub> -CoSe <sub>2</sub> /CC	0.5 M glucose	GOR  HER	0.72@10	S23

**Table S8.** Recently reported direct liquid fuel cells.

Anodic catalyst	DLFC	OCV (V)	$P_{\max}$ (mW cm <sup>-2</sup> )	Ref.
<b>CoNiFeS</b>	<b>DHBFC</b>	<b>1</b>	<b>156</b>	<b>This work</b>
6W–O–CoP/NF	DHzFC	1.1	142	S24
Fe–CoS <sub>2</sub>	DHzFC	1.03	125	S25
Ni–Co–P	DHzFC	~1	96	S26
Ni <sub>3</sub> N–Co <sub>3</sub> N PNAs/NF	DHzFC	~1	60.3	S27
FeNiP–NPHC	DHzFC	0.98	31	S28
RuFe–Ni <sub>2</sub> P	DHzFC	~1	60.1	S29
Ru/PNC	DHzFC	1.5/H <sub>2</sub> O <sub>2</sub>	76.5	S30
Pd–nanoarray@CP	DFAFC	~0.98	35.8	S31
PtRu/C	DFAFC	~0.94	64	S32
Pd <sub>0.64</sub> Pt <sub>0.36</sub> NPs	DMFC	<0.5	99.6	S33
PtRu/C	DMFC	<0.7	22	S34
H–PtNi@PtSn NWs/C	DMFC	~0.6	65.1	S35
PtAu <sub>1</sub> SAAs	DMFC	~0.7	155	S36
PtPdAu/BiTe	DMFC	<0.8	87.2	S37
PtPdAu/BiTe	DEFC	<0.8	72.9	S37

\* The cathode component is assumed to be O<sub>2</sub> with further notation.

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