

Supporting Information of
Engineering a FeOOH/g-C₃N₄/CA Composite Photocatalytic
Membrane for Enhanced Water Treatment: Synergistic
Photocatalysis and Fenton-like Processes

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Text S1. Chemicals and materials.

Isopropanol (IPA), polyvinylpyrrolidone (PVP), hydrochloric acid (HCl), ethylenediaminetetraacetic acid disodium salt (EDTA-2Na), and tert-butanol (TBA) were purchased from Tianjin Damao Chemical Reagent Factory. Melamine and ammonium bicarbonate were purchased from China National Pharmaceutical Chemical Reagent Co., Ltd. Rhodamine B (RhB) and p-benzoquinone (p-BQ) were purchased from Xiya Chemical Reagent Co., Ltd. Ferric chloride (FeCl₃) was purchased from Macklin Biochemical Co., Ltd. (Shanghai). Humic acid (HA) was purchased from Maya Reagent (USA). All chemicals mentioned above were of analytical reagent grade. In addition, cellulose acetate membranes (pore size 0.45 μm) were purchased from Haining Defu New Material Technology Co., Ltd.

Text S2. Theoretical calculations.

Models of FeOOH, g-C₃N₄ (denoted as C₃N₄), the FeOOH/g-C₃N₄ heterojunction, RhB, and RhB adsorbed on FeOOH/g-C₃N₄ (at Fe and N sites) were constructed in Materials Studio. All calculations were performed based on ground-state structures. Geometry optimization was carried out using the Dmol³ module, followed by electronic property analysis within the same module. The results were visualized on molecular surfaces with a color-coded electrostatic potential map (red for positive and blue for negative). The adsorption energy (E_{ads}) was calculated as:

$$E_{\text{ads}} = E_{\text{ad/sub}} - E_{\text{ad}} - E_{\text{sub}}$$

where $E_{\text{ad/sub}}$, E_{ad} , and E_{sub} denote the total energy of the optimized adsorbate-substrate system, the isolated adsorbate, and the clean substrate, respectively.



Fig. S1. Water treatment performance of the FeOOH/g-C₃N₄/CA catalytic membrane system under sunlight.

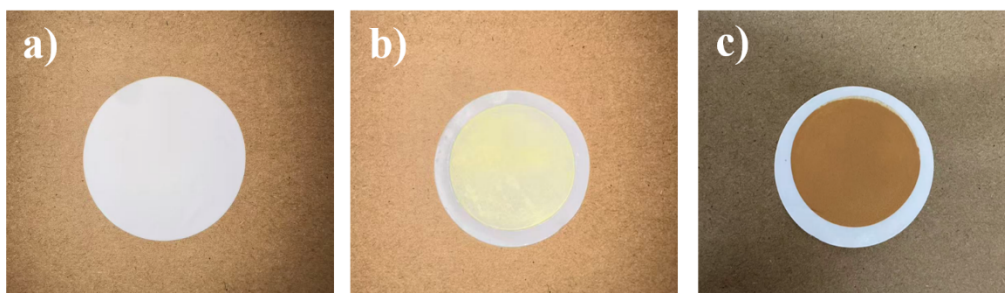


Fig. S2. a-c) Photographs of the CA membrane, g-C₃N₄/CA membrane, and FeOOH/g-C₃N₄/CA membrane

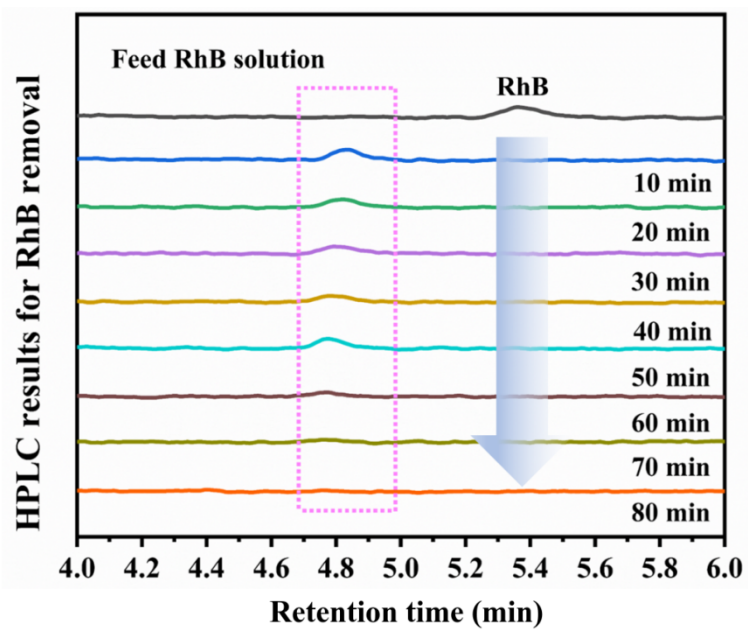


Fig. S3. HPLC analysis of RhB intermediates.

Table S1. EDS mapping elemental distribution of FGCM.

Element	Wt%
C	32.01
N	43.43
O	10.55
Fe	14.01

Table S2. Comparison of different catalytic membrane systems for RhB removal.

Catalytic membrane system	RhB (mg·L⁻¹)	RhB removal (%)	Flux (L·m⁻²·h⁻¹)	Reference
SSC700 membrane	20	91	368	[1]
Ti/SnO ₂ -Sb membrane	50	90.29	2.17	[2]
g-C ₃ N ₄ /Ag ₃ PO ₄ /PVDF membrane	10	97	1083	[3]
g-C ₃ N ₄ /FeOCl/PVDF membrane	50	90	1100	[4]
FGCM	10	93.2	30012	This work

Table S3. The peak area of FeOOH/g-C₃N₄ evaluated by XPS.

Price trend	XPS (%)	
	Fe(II)	Fe(III)
Before	23.2	76.8
After	38.5	40.3

References

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