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## Supplementary Information

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4 **Achieving Stable Syngas Production during Photothermal synergistic**

5 **Dry Reforming of Methane over Layered Double Hydroxides-Based**

6 **Catalysts with anti-coking Performance**

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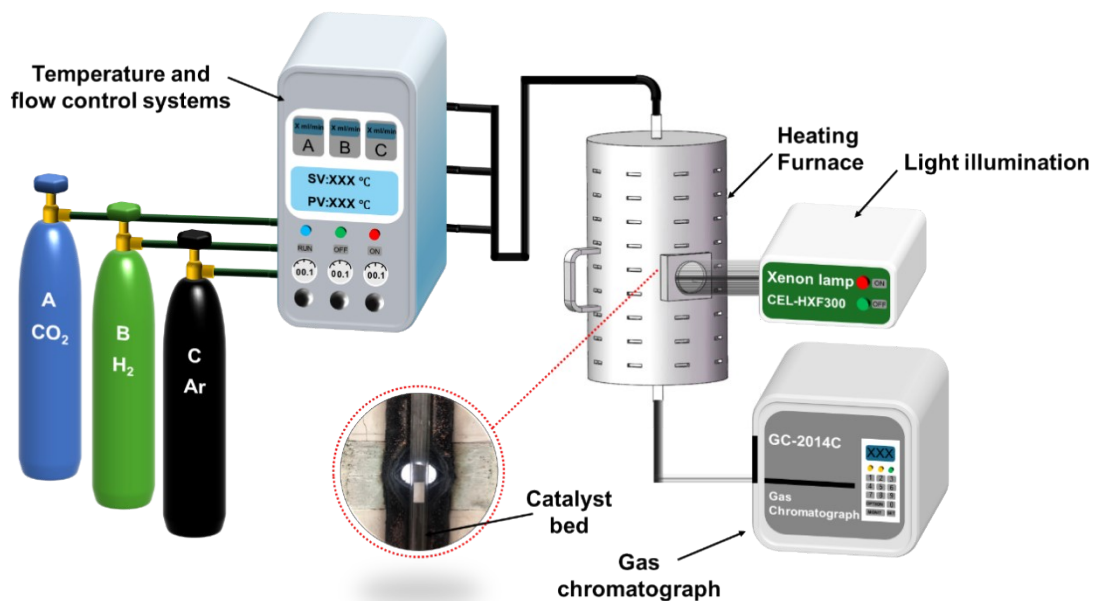
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## 18 Contents

19	<b>Supplementary data</b> .....	3
20	Figure S1. Overall Process Flow Diagram of the System.....	3
21	Figure S2. EDS image of MgAl-LDH. ....	4
22	Figure S3. EDS image of CuAl-LDH. ....	5
23	Figure S4. EDS image of Ni/MgAl <sub>2</sub> O <sub>4</sub> . ....	6
24	Figure S5. TEM characterization of the Ni/CuAl <sub>2</sub> O <sub>4</sub> catalyst. ....	7
25	Figure S6. Gas chromatography sample diagram of the reaction product.....	8
26	Figure S7. Effect of xenon lamp current on the temperature of different catalysts. ....	9
27	Table S1. Mass fraction of Ni in the catalyst.....	10
28	Table S2. The specific surface area, pore volume, and average pore diameter of different catalysts. ....	11
29	Table S3. Relative amounts of oxygen vacancies in different catalysts calculated from XPS results. ....	12
30	Table S4. Reaction rates of different catalysts in the TC-DRM and PTSC-DRM reactions. ....	13
31	Table S5. Selectivity of different catalysts in TC/PTSC-DRM reactions.....	14
32	Table S6. Carbon deposition of Ni/MgAl <sub>2</sub> O <sub>4</sub> and Ni/CoAl <sub>2</sub> O <sub>4</sub> after TC and PTSC reactions. ....	15
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35 **Supplementary data**

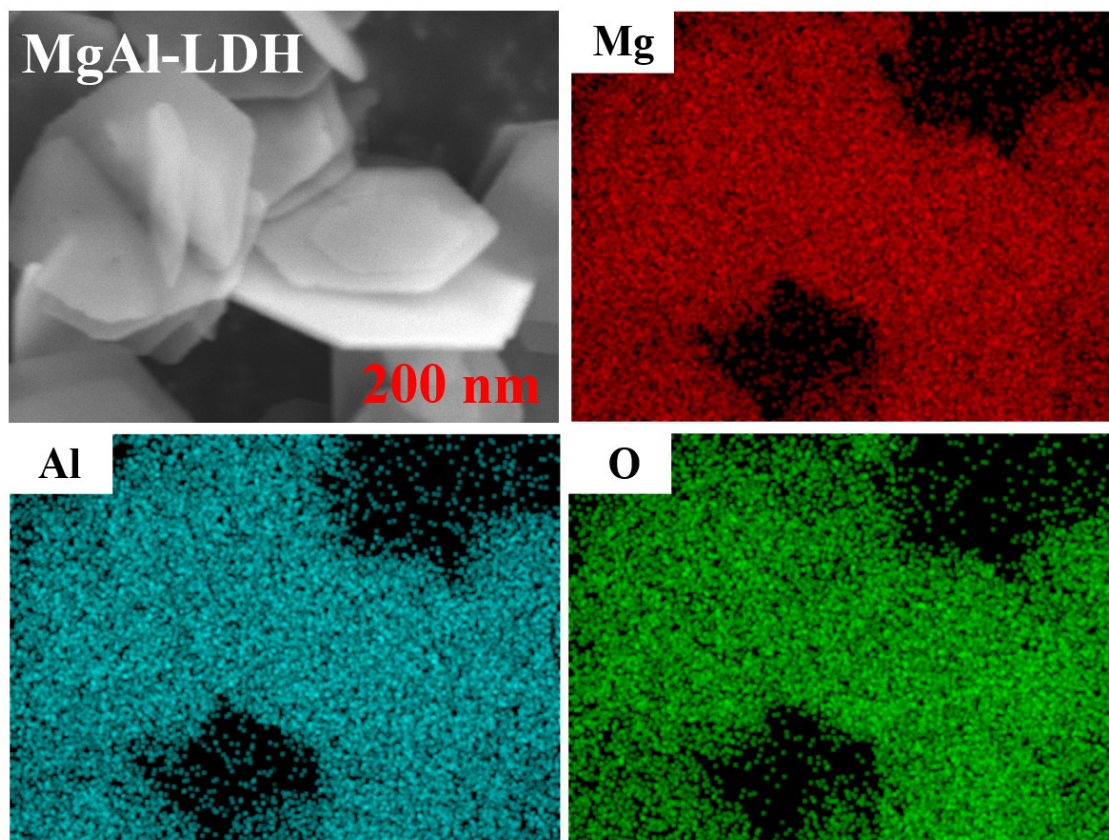


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**Figure S1.** Overall Process Flow Diagram of the System.



**Figure S2.** EDS image of MgAl-LDH.

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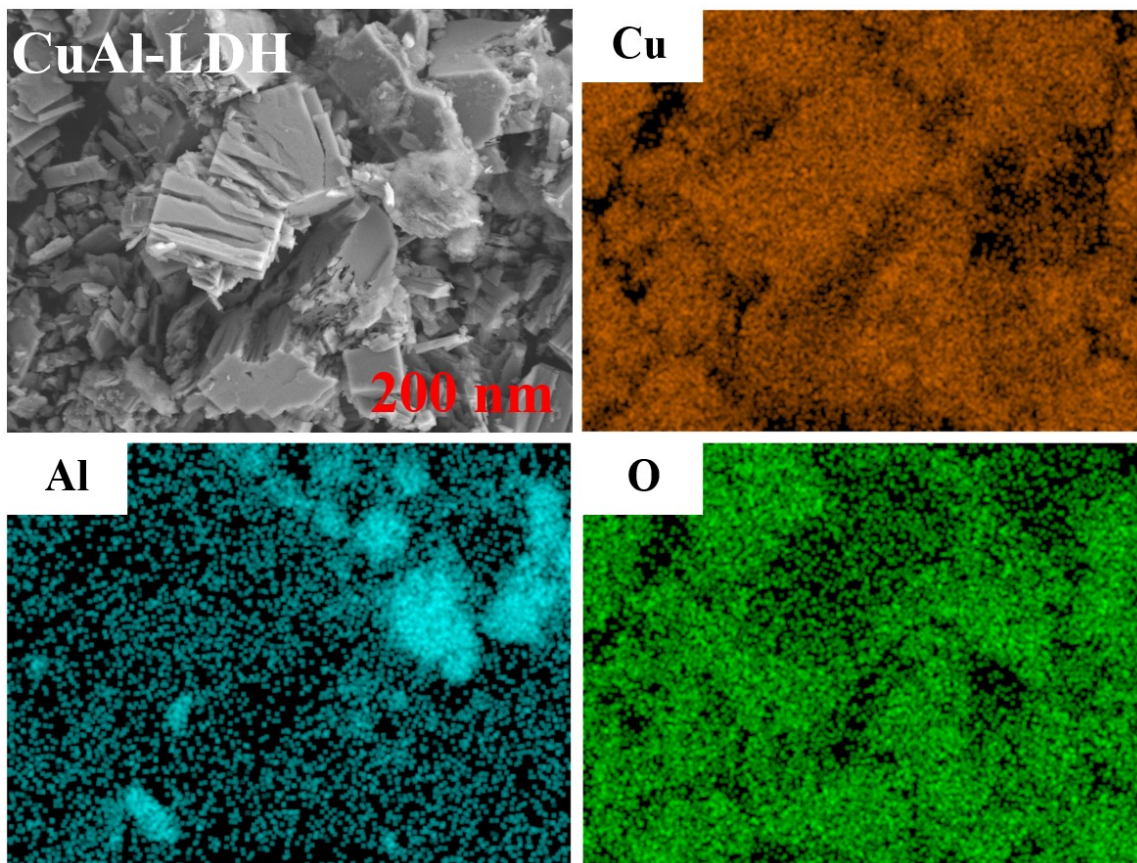
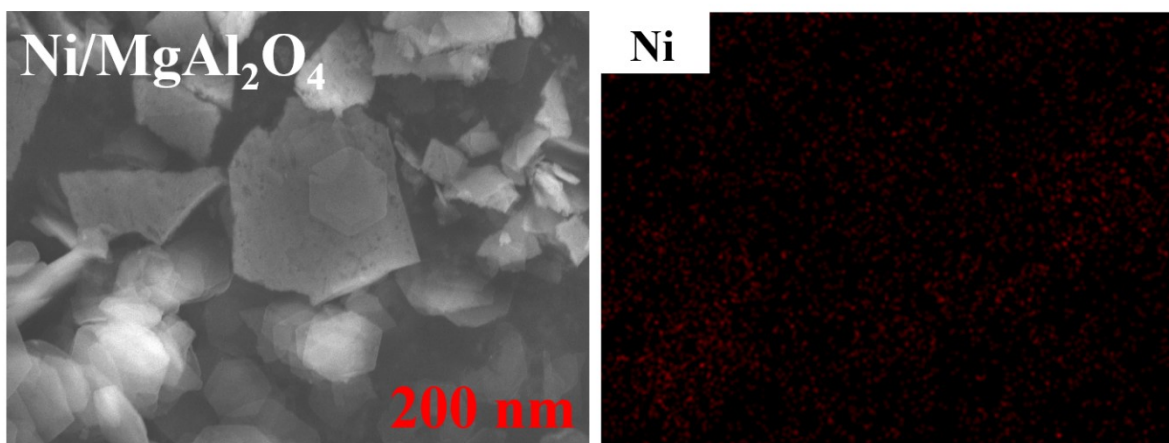


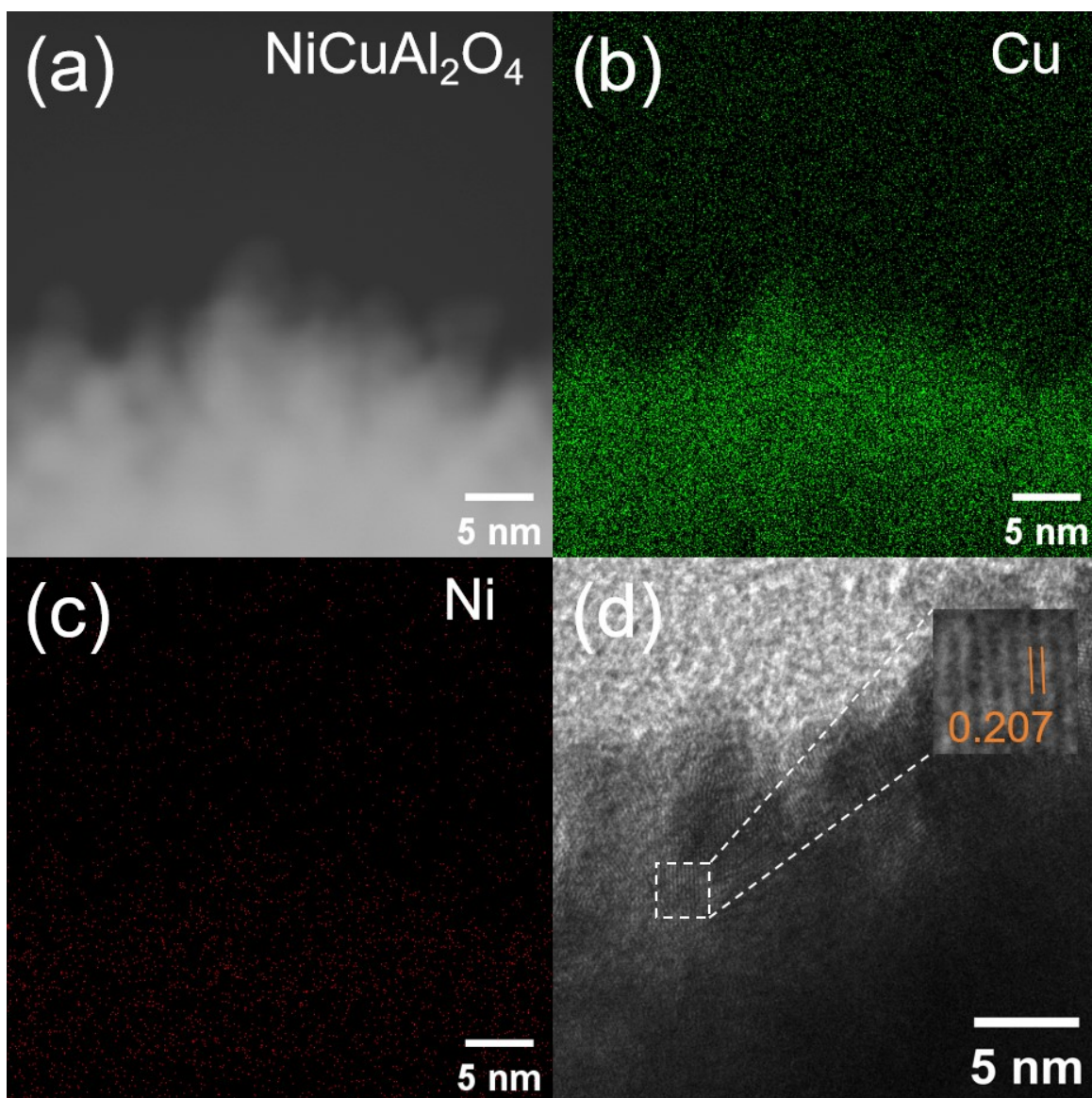
Figure S3. EDS image of CuAl-LDH.

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**Figure S4.** EDS image of Ni/MgAl<sub>2</sub>O<sub>4</sub>.

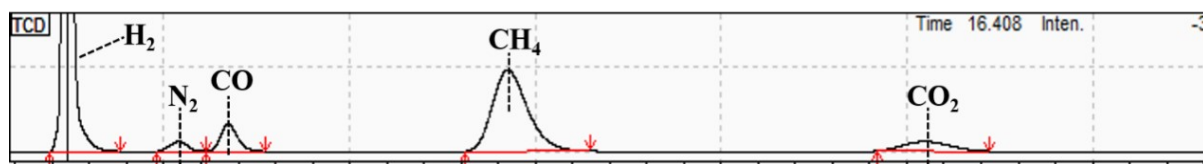


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49 **Figure S5.** TEM characterization of the Ni/CuAl<sub>2</sub>O<sub>4</sub> catalyst: (a) structural morphology; (b) EDS

50 elemental mapping of Cu; (c) EDS elemental mapping of Ni; (d) lattice fringe spacing.

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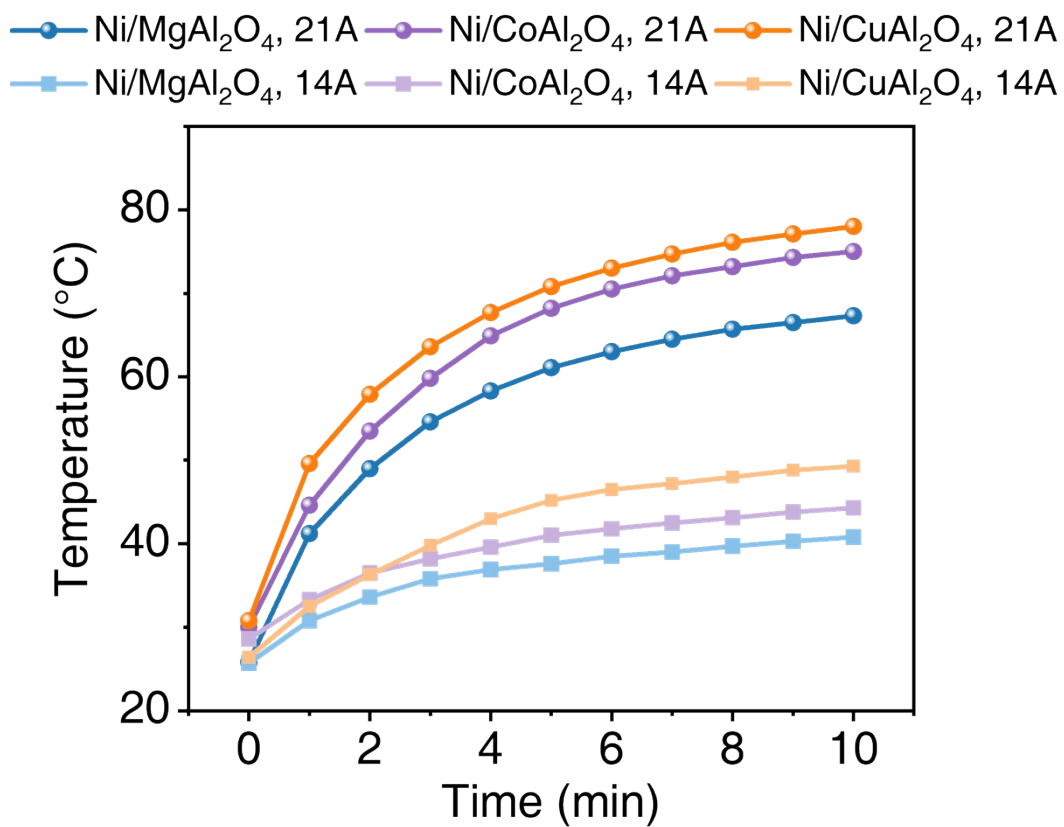


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**Figure S6.** Gas chromatography sample diagram of the reaction product.



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56 **Figure S7.** Effect of xenon lamp current on the temperature of Ni/MgAl<sub>2</sub>O<sub>4</sub>, Ni/CoAl<sub>2</sub>O<sub>4</sub>, and

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Ni/CuAl<sub>2</sub>O<sub>4</sub> (Reaction conditions: 600 °C, GHSV = 12000 mL·g<sup>-1</sup>·h<sup>-1</sup>).

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**Table S1.** Mass fraction of Ni in the catalyst.

<b>Catalyst</b>	<b>Actual loading amount of Ni</b>
	<b>wt%</b>
Ni/MgAl <sub>2</sub> O <sub>4</sub>	2.93
Ni/CoAl <sub>2</sub> O <sub>4</sub>	2.94
Ni/CuAl <sub>2</sub> O <sub>4</sub>	2.91

61 **Table S2.** The specific surface area, pore volume, and average pore diameter of Ni/MgAl<sub>2</sub>O<sub>4</sub>,  
62 Ni/CoAl<sub>2</sub>O<sub>4</sub>, and Ni/CuAl<sub>2</sub>O<sub>4</sub>.

Catalyst	Specific surface area	Pore volume	Average pore diameter
	(m <sup>2</sup> ·g <sup>-1</sup> )	(cm <sup>3</sup> ·g <sup>-1</sup> )	(nm)
Ni/MgAl <sub>2</sub> O <sub>4</sub>	181.29	0.16	13.37
Ni/CoAl <sub>2</sub> O <sub>4</sub>	52.8	0.22	17.58
Ni/CuAl <sub>2</sub> O <sub>4</sub>	44.81	0.12	7.45

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64 **Table S3.** Relative amounts of oxygen vacancies in Ni/MgAl<sub>2</sub>O<sub>4</sub>, Ni/CoAl<sub>2</sub>O<sub>4</sub>, and Ni/CuAl<sub>2</sub>O<sub>4</sub>  
65 calculated from XPS results.

Catalyst	Oxygen vacancy content
	$O_V / (O_L + O_V + O_C)$
Ni/MgAl <sub>2</sub> O <sub>4</sub>	32.06%
Ni/CoAl <sub>2</sub> O <sub>4</sub>	59.29%
Ni/CuAl <sub>2</sub> O <sub>4</sub>	58.26%

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67 **Table S4.** Reaction rates of Ni/CuAl<sub>2</sub>O<sub>4</sub>, Ni/CoAl<sub>2</sub>O<sub>4</sub>, and Ni/MgAl<sub>2</sub>O<sub>4</sub> catalysts in the TC-  
68 DRM and PTSC-DRM reactions (Reaction conditions: 600 °C, the light intensity is 2.91 W·cm<sup>-2</sup>,  
69 GHSV = 12000 mL·g<sup>-1</sup>·h<sup>-1</sup>).

Catalyst	Reaction rates (mL·g <sup>-1</sup> ·h <sup>-1</sup> )			
	PTSC-CH <sub>4</sub>	TC-CH <sub>4</sub>	PTSC-CO <sub>2</sub>	TC-CO <sub>2</sub>
Ni/CuAl <sub>2</sub> O <sub>4</sub>	1299.72	758.58	1587	1122.25
Ni/CoAl <sub>2</sub> O <sub>4</sub>	5489.2	3878.58	5545.8	3962.58
Ni/MgAl <sub>2</sub> O <sub>4</sub>	4618.54	2438.58	5055.16	3027.78

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71 **Table S5.** Selectivity of Ni/CuAl<sub>2</sub>O<sub>4</sub>, Ni/CoAl<sub>2</sub>O<sub>4</sub>, and Ni/MgAl<sub>2</sub>O<sub>4</sub> catalysts in TC/PTSC-DRM  
72 reactions (Reaction conditions: 600 °C, the light intensity is 2.91 W·cm<sup>-2</sup>, GHSV = 12000 mL·g<sup>-1</sup>·h<sup>-1</sup>).  
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Catalyst	H <sub>2</sub> /CO	
	PTSC	TC
Ni/CuAl <sub>2</sub> O <sub>4</sub>	0.77	0.62
Ni/CoAl <sub>2</sub> O <sub>4</sub>	0.99	0.97
Ni/MgAl <sub>2</sub> O <sub>4</sub>	0.96	0.87

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75 **Table S6.** Carbon deposition of Ni/MgAl<sub>2</sub>O<sub>4</sub> and Ni/CoAl<sub>2</sub>O<sub>4</sub> after TC and PTSC reactions.

Catalyst	Reaction	Detection	Weight	Carbon deposit	Carbon deposition
	time	quality	loss	amount	rate
	(h)	(mg)	(%)	(mg)	(mg·h <sup>-1</sup> )
Ni/MgAl <sub>2</sub> O <sub>4</sub> -PTSC	68.25	4.864	68.41	3.33	0.049
Ni/MgAl <sub>2</sub> O <sub>4</sub> -TC	19.5	4.532	63.39	2.87	0.15
Ni/CoAl <sub>2</sub> O <sub>4</sub> -PTSC	9.75	4.116	60.17	2.48	0.25
Ni/CoAl <sub>2</sub> O <sub>4</sub> -TC	6.5	4.837	67.2	3.25	0.5

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