

Supporting Information

Electronic Engineering of Ni₃S₂ via Mo/Cl Co-doping for Upcycling Polyethylene Terephthalate into Formate with Concurrent Hydrogen Evolution

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S1. Techno-economic assessment

The calculation process as follows:

(1) Input chemicals costs:

The costs associated with the required input chemicals are calculated as follows: 1 ton PET (390 \$/t)¹, 1.13 tons KOH (1126 \$/t)², 10 tons water (0.22 \$/t)³ and 0.53 tons formic acid (400 \$/t)⁴.

Thus, the input chemicals is:

$$\text{Costs} = (1 \times 390) + (1.13 \times 1126) + (10 \times 0.22) + (0.53 \times 400) = 1876.6 \$$$

(2) Electricity costs:

The total charge required for electrochemical PET upgrading per ton is determined by:

$$Q = \frac{N \times F \times n}{FE} = \frac{4770 \times 96485 \times 6}{0.82} = 3.36 \times 10^9 \text{ C}$$

Where Q is the total charge, N is the moles of EG per ton of PET, F is the Faraday constant (96485 C mol⁻¹), n is the number of electron transfer (6), and FE is the Faradaic efficiency of formate production.

The power consumption is then calculated as:

$$P = \frac{U \times Q}{3600 \times f} = \frac{1.61 \times 3.36 \times 10^9}{3600 \times 0.8} = 1878.3 \text{ kWh}$$

Where U is the cell potential (1.61 V), f is a capacity factor (0.8). Assuming an electricity price of 0.07 \$/kWh, the electricity cost amounts to:

$$\text{Electricity costs} = 1878.3 \times 0.07 = 131.4 \$$$

(3) Separation and purification costs

Separation and purification costs, estimated as 20% of the electricity costs, are given by:

$$\text{Separation and purification cost} = 131.4 \times 0.2 = 26.3 \$$$

(4) Miscellaneous costs

Miscellaneous costs, covering capital costs, Installation costs, balance of plant, operational costs, and maintenance costs, are estimated at 10% of the total costs

incurred thus far:

$$\text{Miscellaneous cost} = (1876.6 + 131.4 + 26.3) \times 0.1 = 203.4 \text{ \$}$$

(5) Total cost of PET upcycling:

$$\text{Total cost} = 1876.6 + 131.4 + 26.3 + 203.4 = 2237.7 \text{ \$}$$

(6) After electrolysis, 1 ton of PET feedstock finally yields 1.67 tons of HCOOK (852 \$/t)⁵, 0.84 tons of TPA (1260 \$/t)⁶ and 0.037 tons of H₂ (4800 \$/t)⁵.

The corresponding product value is:

$$\text{Product value} = (1.67 \times 852) + (0.84 \times 1260) + (0.037 \times 4800) = 2658.8 \text{ \$}$$

The net profit from electrolysis per ton of PET is calculated as:

$$\text{Total profit} = \text{Product value} - \text{Total Cost} = 2658.8 - 2237.7 = 421.1 \text{ \$}$$

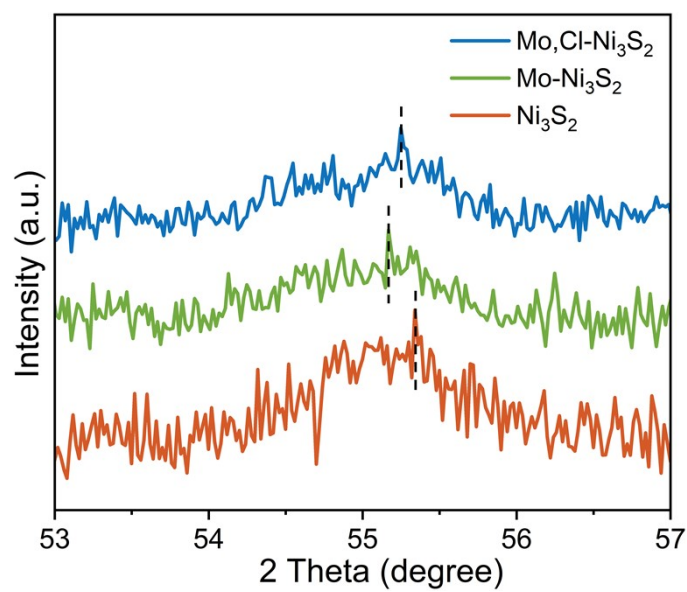


Fig. S1 XRD patterns of Mo,Cl-Ni₃S₂, Mo-Ni₃S₂ and Ni₃S₂.

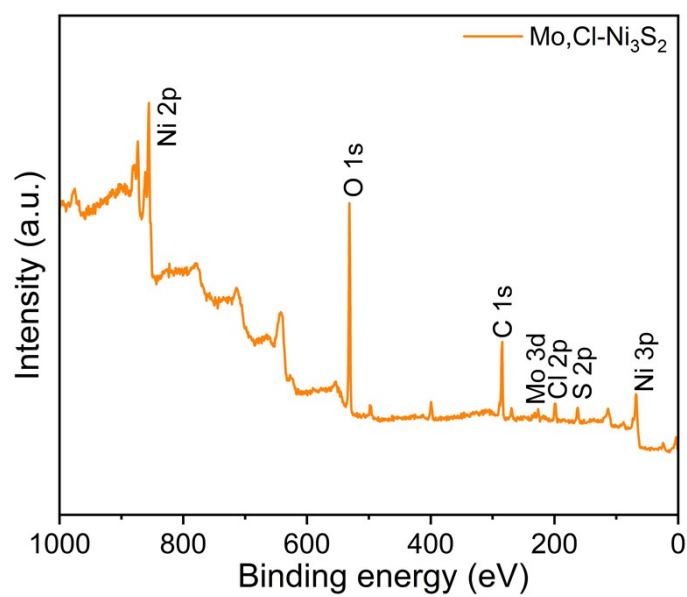


Fig. S2 XPS survey spectrum of Mo,Cl-Ni₃S₂.

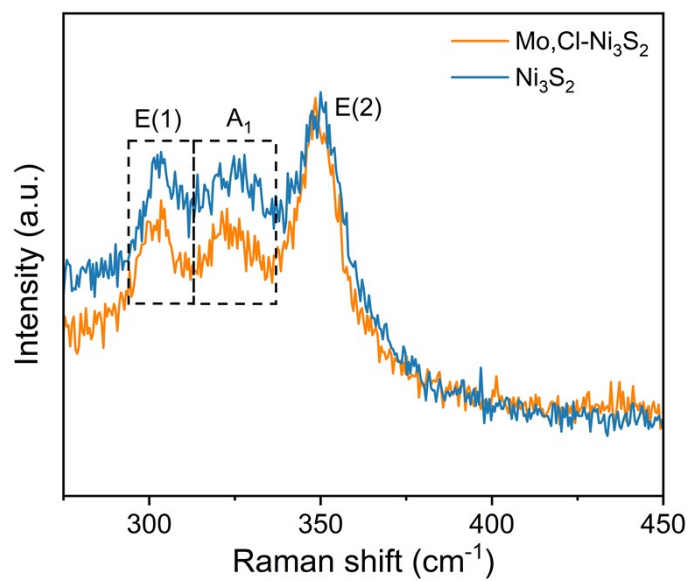


Fig. S3 Raman spectra of Mo,Cl-Ni₃S₂ and Ni₃S₂.

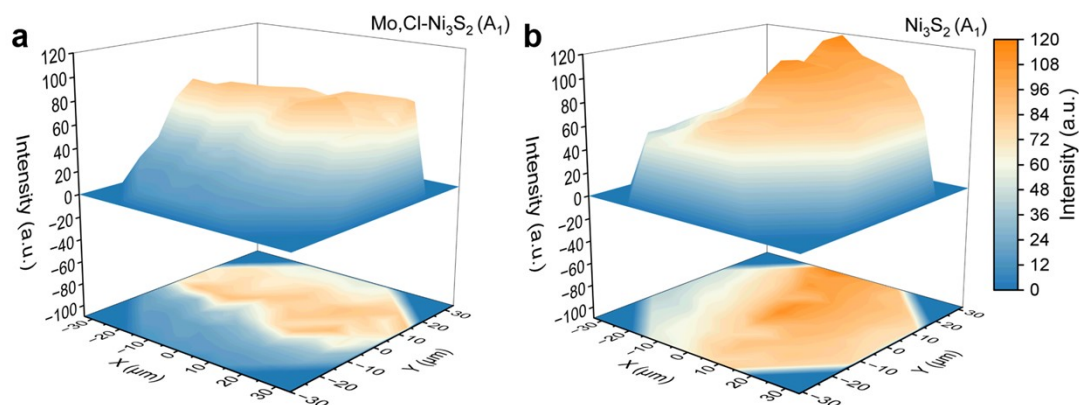


Fig. S4 Raman spectra heatmap of the A₁ vibrational mode of (a) Mo,Cl-Ni₃S₂ and (b) Ni₃S₂.

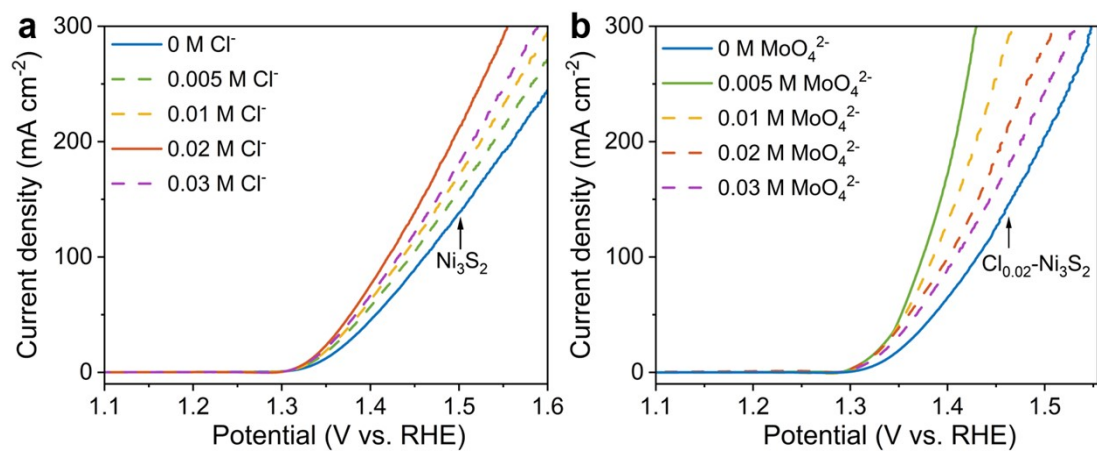


Fig. S5 (a) Effect of Cl⁻ doping level on the catalytic performance of Ni₃S₂. (b) Effect of MoO₄²⁻ doping level on the catalytic performance of Cl_{0.01}-Ni₃S₂ (Cl_{0.01} means the dosage of Cl⁻ precursor is 0.01 M).

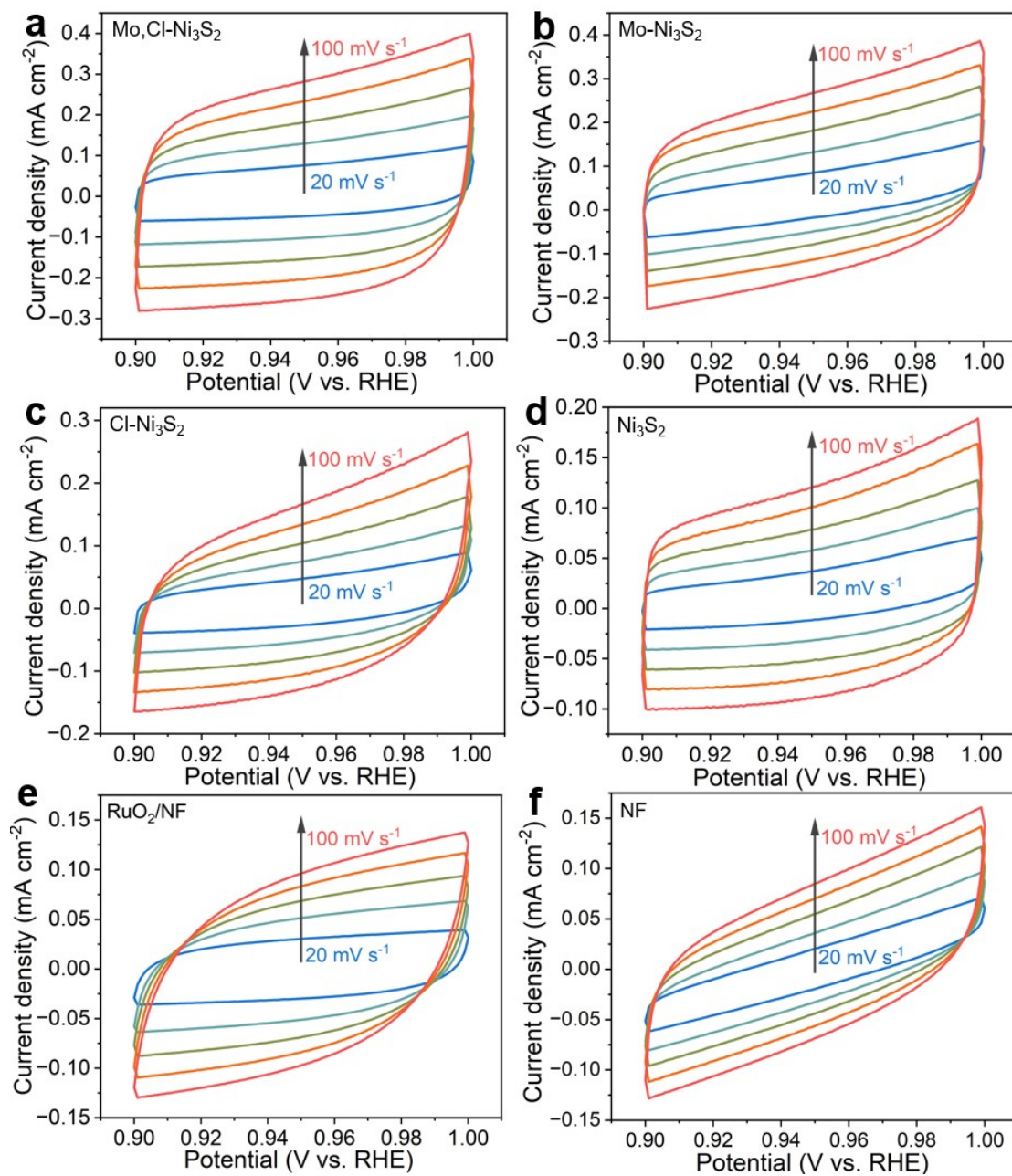


Fig. S6 CV of (a) Mo,Cl-Ni₃S₂, (b) Mo-Ni₃S₂, (c) Cl-Ni₃S₂, (d) Ni₃S₂ (e) RuO₂/NF and (f) NF at different scan rates (from 20 to 100 mV s⁻¹ with an increment of 20 mV s⁻¹).

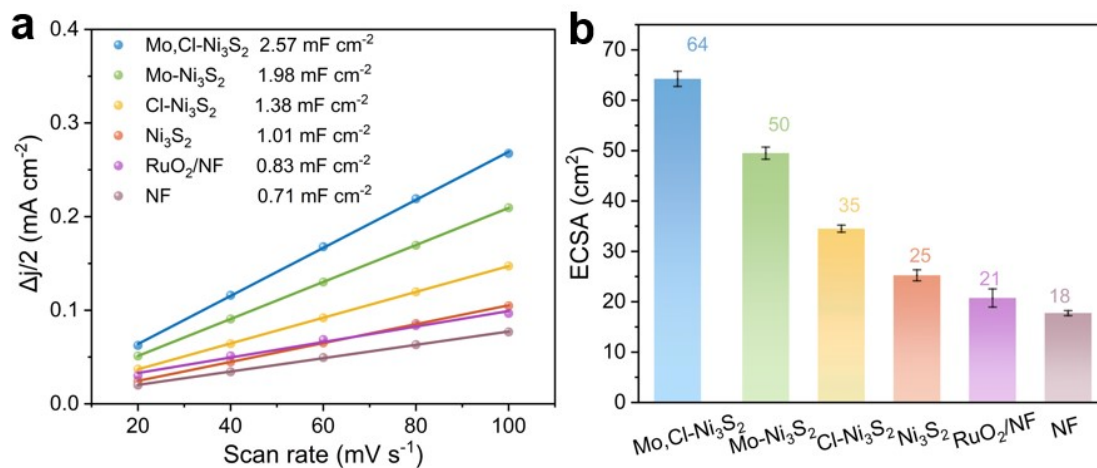


Fig. S7 (a) The difference in current density ($\Delta j = (j_a - j_c)/2$) plots against the scan rate of Mo,Cl-Ni₃S₂, Mo-Ni₃S₂, Cl-Ni₃S₂, Ni₃S₂, RuO₂/NF and NF. (b) ECSA values of catalysts.

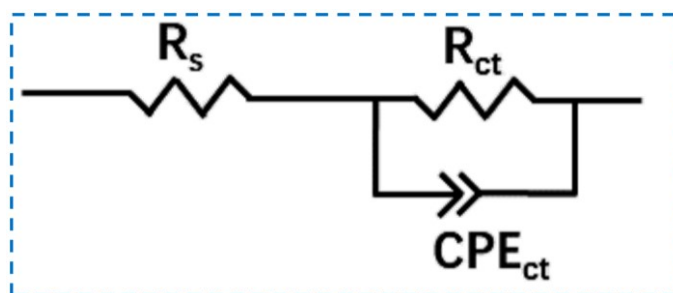


Fig. S8 Equivalent circuit model for EIS data fitting.

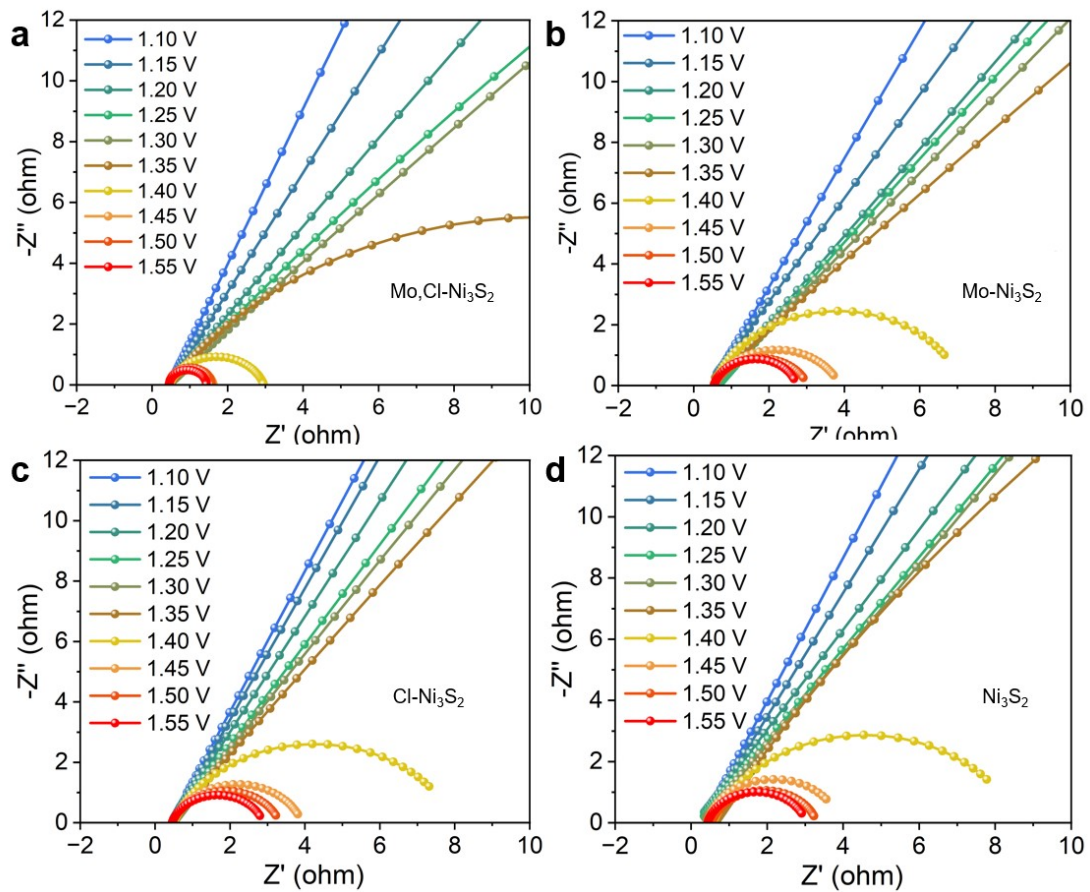


Fig. S9 Nyquist plots of (a) $\text{Mo,Cl-Ni}_3\text{S}_2$, (b) $\text{Mo-Ni}_3\text{S}_2$, (c) $\text{Cl-Ni}_3\text{S}_2$, and (d) Ni_3S_2 .

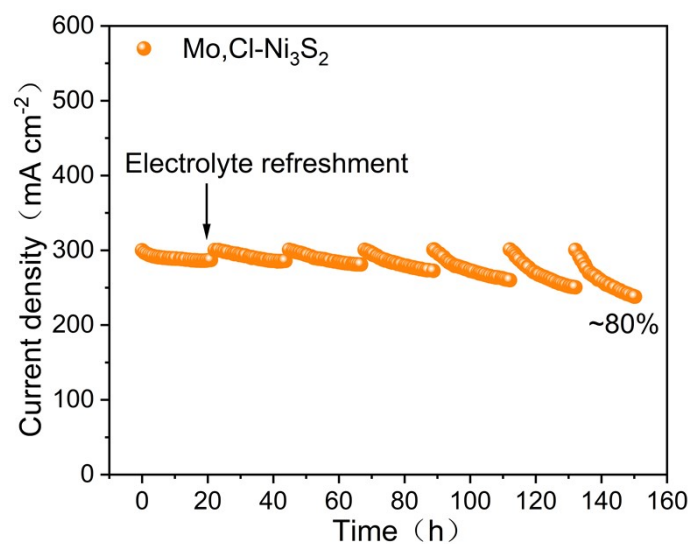


Fig. S10 The chronoamperometric curves of $\text{Mo,Cl-Ni}_3\text{S}_2$ for the 150 h EGOR test.

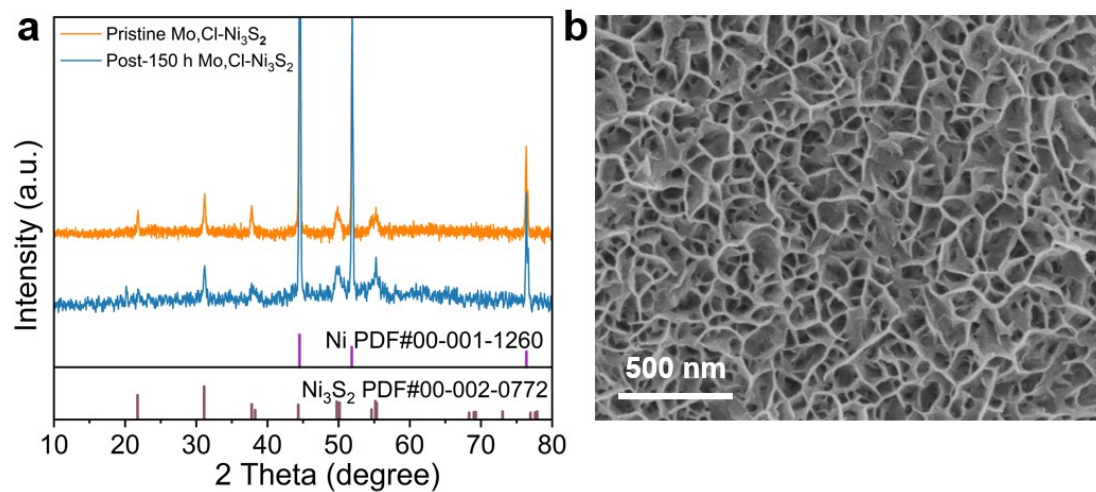


Fig. S11 (a) XRD and (b) SEM images of Mo,Cl-Ni₃S₂ after 150 h stability test.

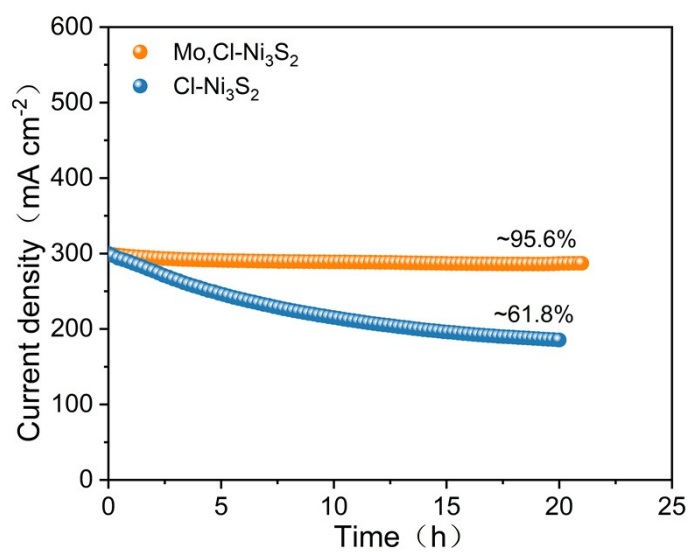


Fig. S12 Comparison of the long-term stability between Mo,Cl-Ni₃S₂ and Cl-Ni₃S₂.

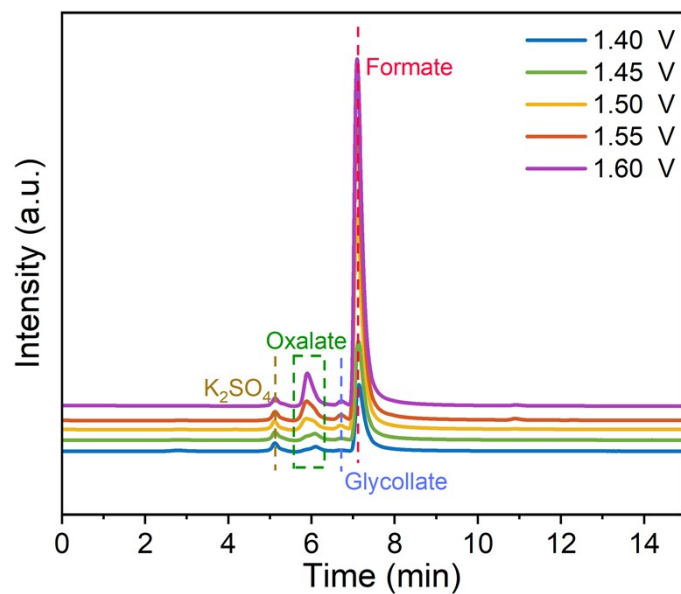


Fig. S13 HPLC products of EGOR at different potentials.

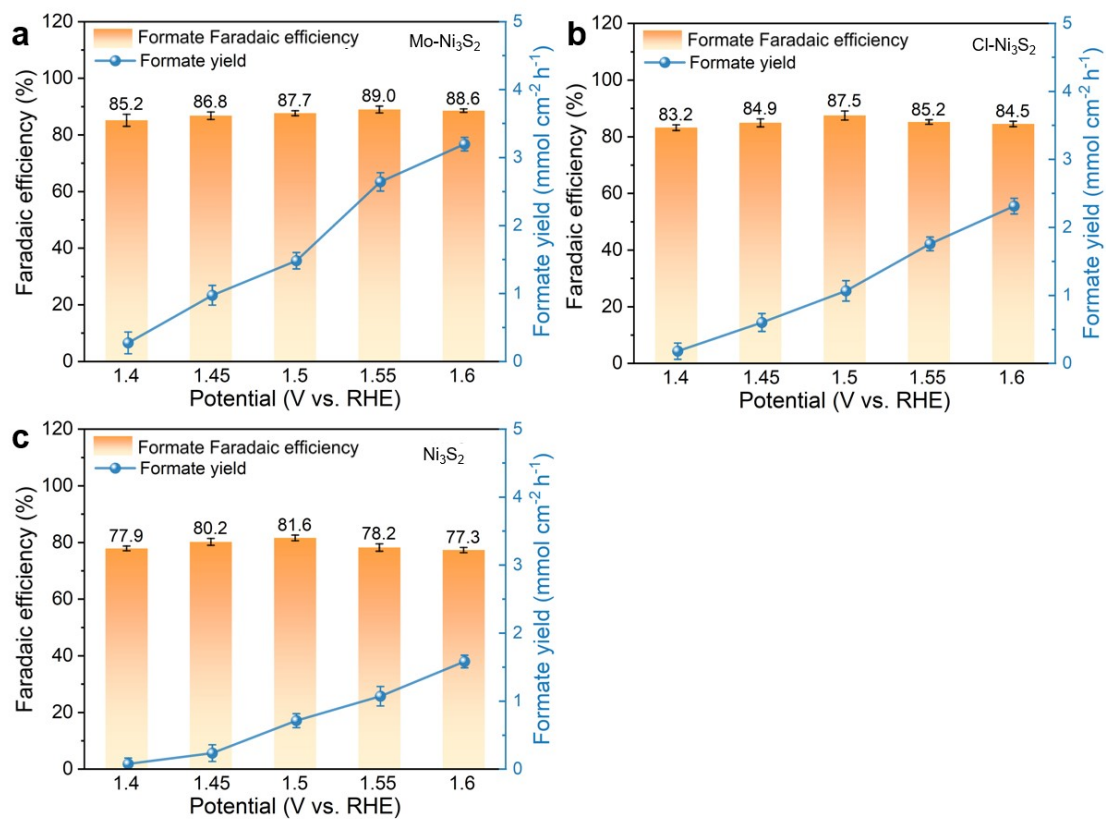


Fig. S14 Faradaic efficiency and yield for formate production of (a) Mo-Ni₃S₂, (b) Cl-Ni₃S₂, and (c) Ni₃S₂ at different potentials.

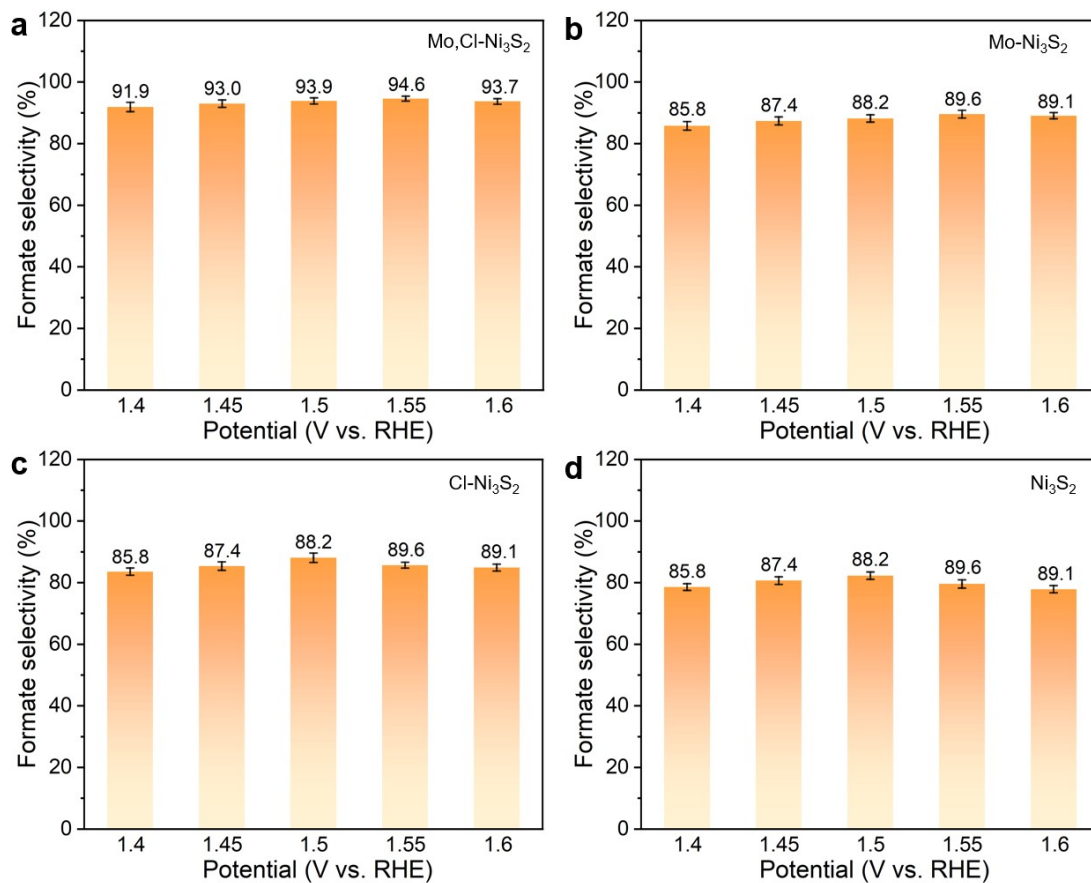


Fig. S15 Formate selectivity of (a) Mo,Cl-Ni₃S₂, (b) Mo-Ni₃S₂, (c) Cl-Ni₃S₂, and (d) Ni₃S₂ at varied applied voltages.

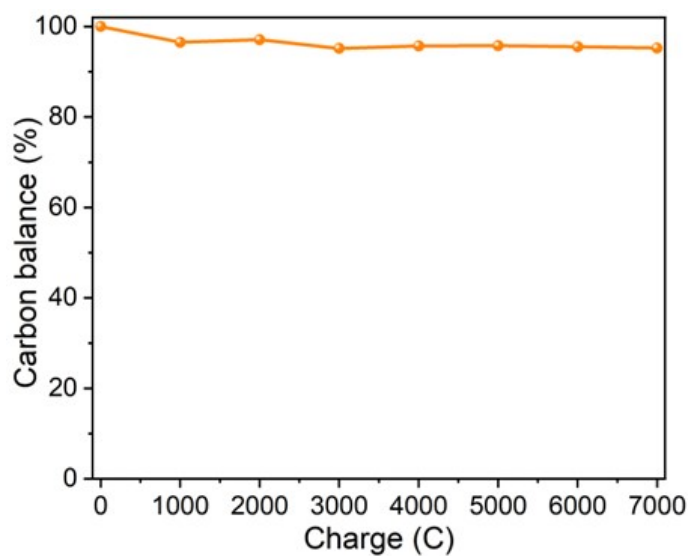


Fig. S16 Carbon balance of EGOR at different input charges.

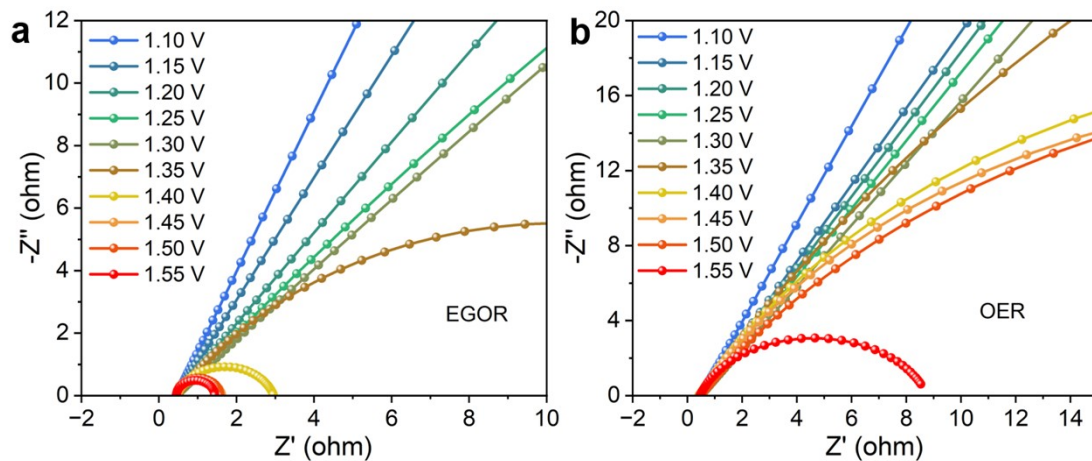


Fig. S17 Nyquist plots of Mo₂Cl-Ni₃S₂ for (a) OER and (b) EGOR.

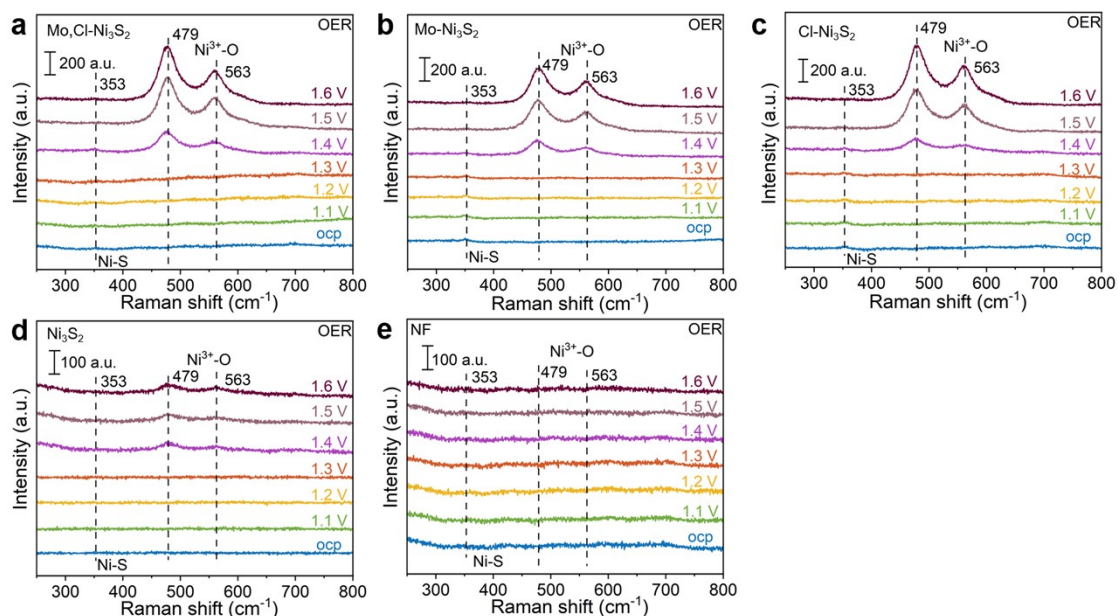


Fig. S18 *In situ* Raman spectra of (a) Mo₂Cl-Ni₃S₂, (b) Mo-Ni₃S₂, (c) Cl-Ni₃S₂, (d) Ni₃S₂, and (e) Ni₃S₂.

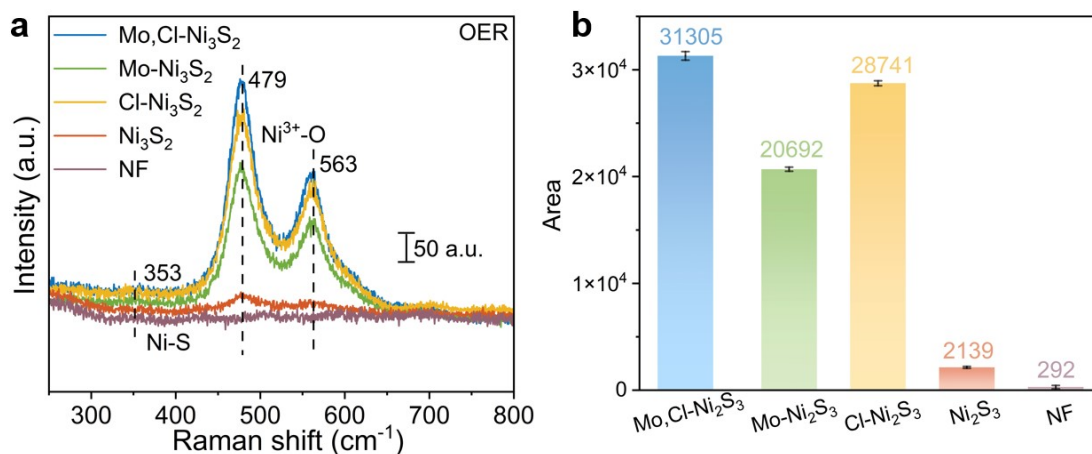


Fig. 19 (a) Comparison of *in situ* Raman peaks at 1.5 V vs. RHE. (b) The corresponding Raman peak area of NiOOH at 1.5 V vs. RHE.

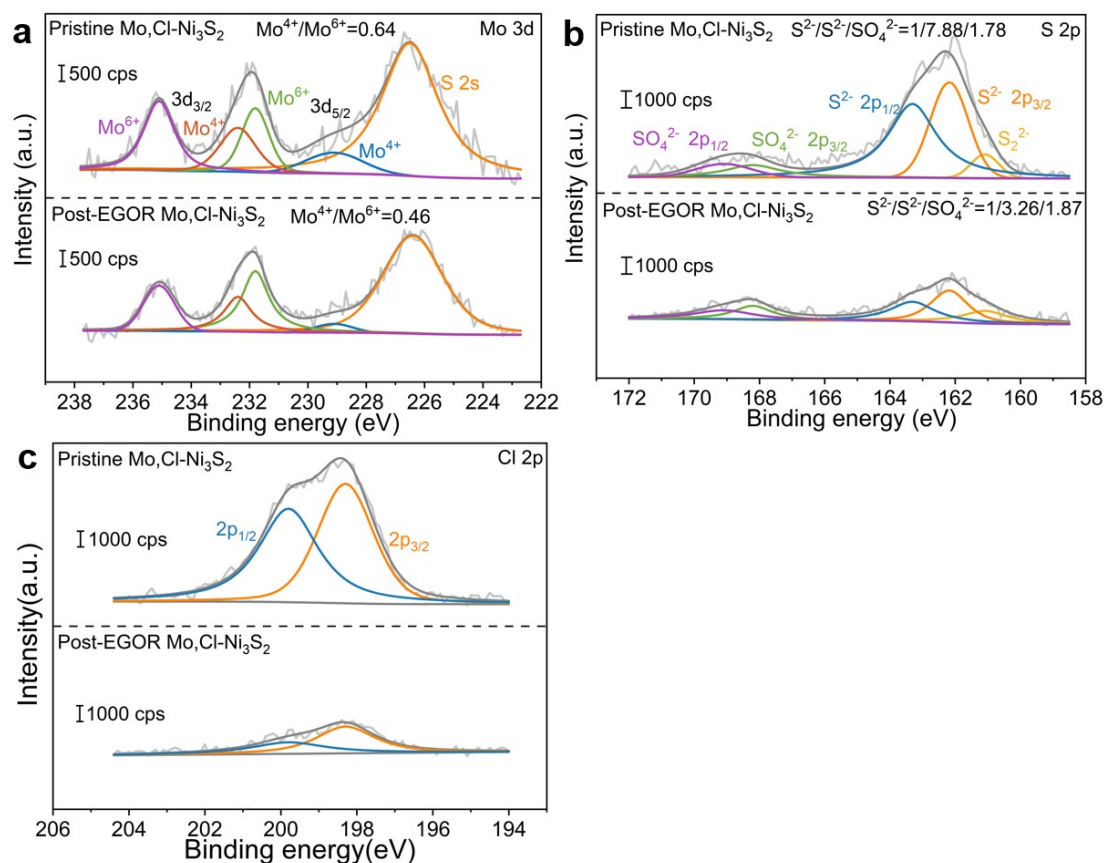


Fig. S20 (a) Mo 3d, (b) S 2p and (c) Cl 2p XPS spectra of Mo,Cl-Ni₃S₂ before and after EGOR process.

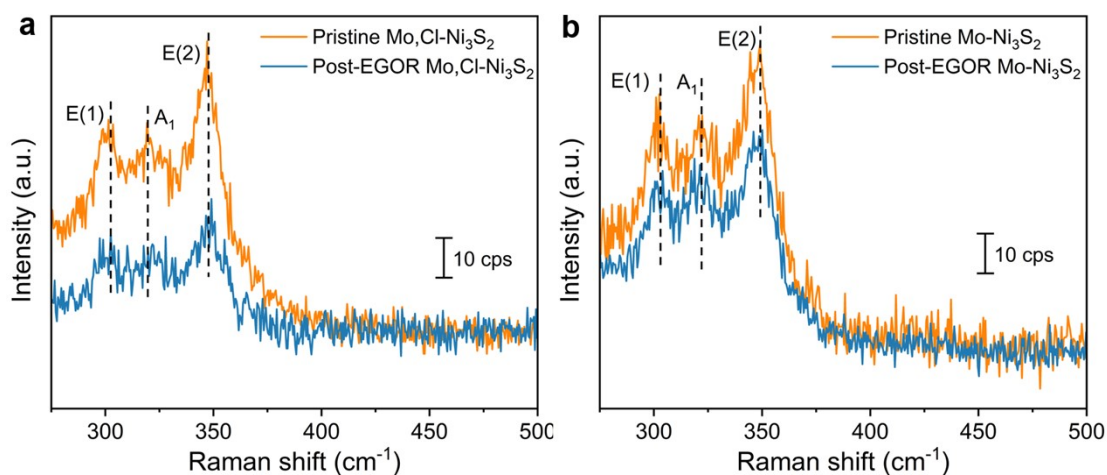


Fig. S21 Raman spectra of (a) Mo,Cl-Ni₃S₂ and (b) Mo-Ni₃S₂ before and after EGOR process.

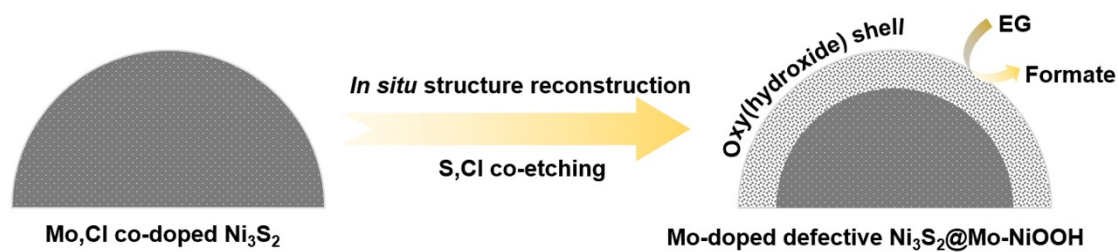


Fig. S22 Illustration of the self-reconstruction process of Mo,Cl-Ni₃S₂.

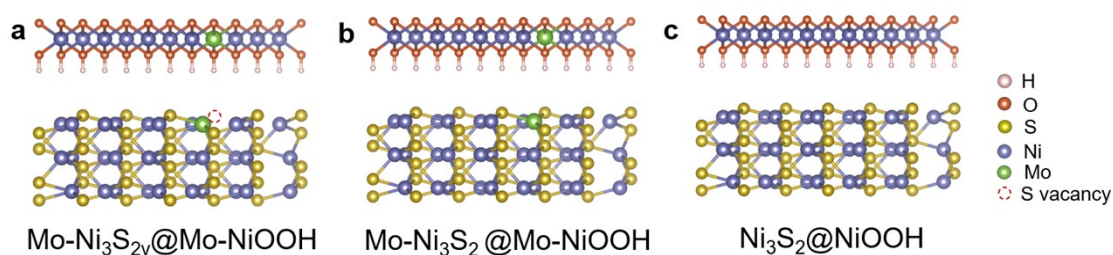


Fig. S23 Constructed (a) Mo-Ni₃S_{2v}@Mo-NiOOH, (b) Mo-Ni₃S₂@Mo-NiOOH, and (c) Ni₃S₂@NiOOH models for DFT calculations. Since Cl is a dopant and replace some S sites in the Ni₃S₂ crystal structure, the electrochemical etching of Cl will thus lead to S vacancy.

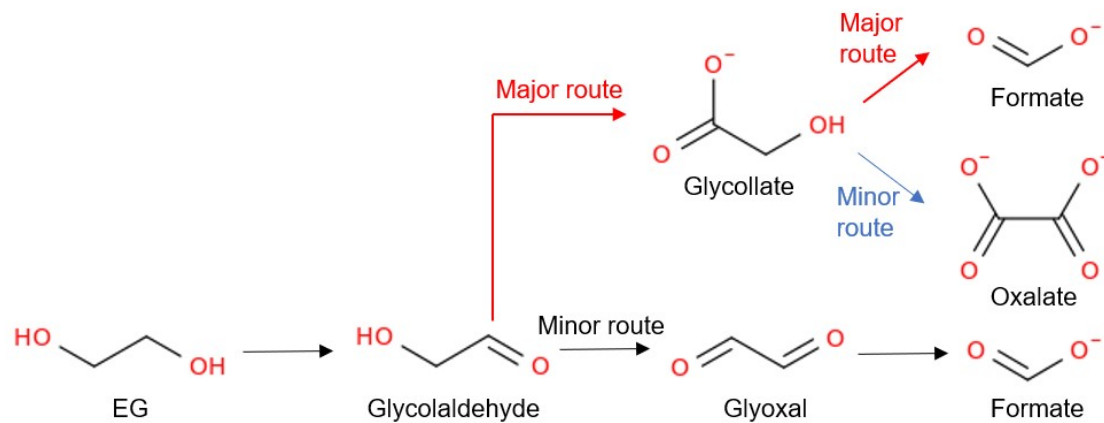


Fig. S24 Proposed reaction pathway for the electrocatalytic glycol conversion.

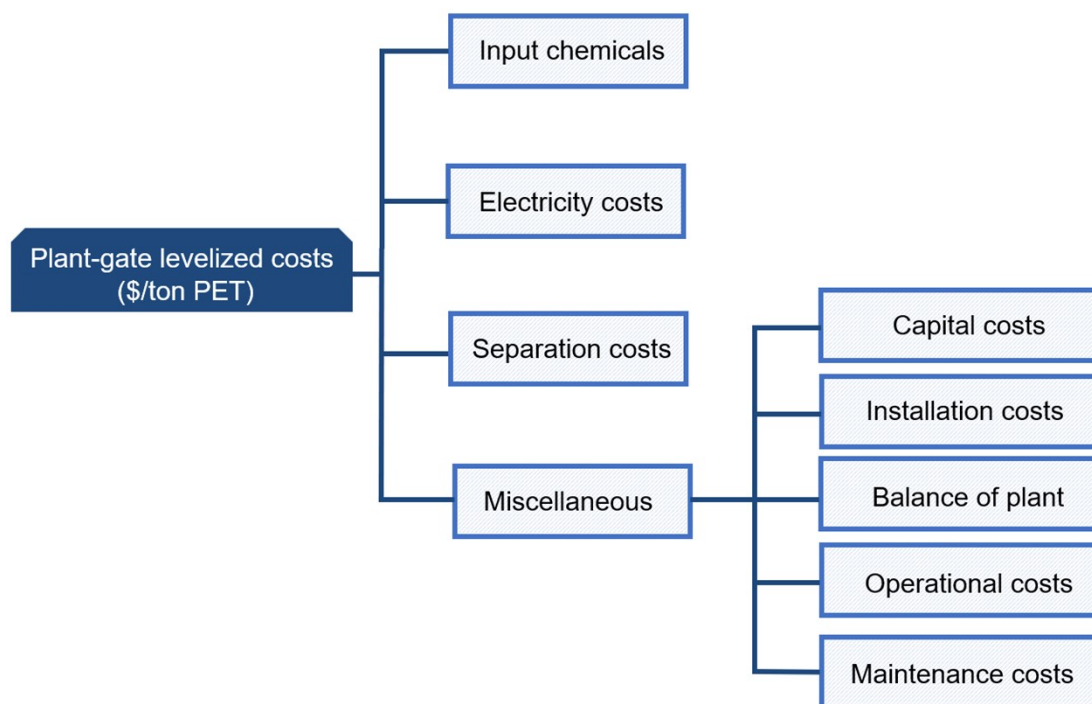


Fig. S25 The costs for calculating techno-economic analysis of electrolytic PET wastes conversion.

Table S1 A summary of OER properties of Mo,Cl-Ni₃S₂ and state-of-the-art TM-based catalysts in 1 M KOH.

Catalyst	η_{10} (mV)	References
CoMnOOH	256	<i>Angew. Chem. Int. Ed.</i> , 2024, 63, e202408005.
MEC-2	258	<i>Nat. Commun.</i> , 2025, 16:4389.
FeCoS _x -PBA	266	<i>J. Mater. Chem. A</i> , 2022, 10, 19757-19768.
CoNiS _x /NF	306	<i>ACS Appl. Nano Mater.</i> , 2024, 7, 9062-9067.
CeO ₂ (Co ₃ O ₄ /CeO ₂)	297	<i>Dalton Trans.</i> , 2024, 53, 5484-5494.
CoFeBTC-MOF	261	<i>Colloids Surf., A</i> 2022, 651, 129766.
Ni _{2.5} Co ₅ C ₂ O ₄	330	<i>Nanoscale Adv.</i> , 2021, 3, 3770-3779.
Ni _{0.8} Fe _{0.2}	264	<i>Langmuir</i> , 2025, 41, 23621-23631.
Co _{0.6} Fe _{0.4} C ₂ O ₄	292	<i>ACS Appl. Mater. Interfaces</i> , 2025, 17, 46874-46886.
RuO _x /γ-MnO ₂	255	<i>Adv. Funct. Mater.</i> , 2025, e17063.
H ⁺ -LSE _x O	270	<i>J. Power Sources</i> , 2025, 644, 237084.
MoO ₃ @NF	288	<i>Int. J. Hydrogen Energy</i> , 2025, 127, 137-146.
Ni ₃ Fe-CNT	301	<i>Molecules</i> , 2025, 30, 208.
FeCoNiCuYP/C	259	<i>Adv. Mater.</i> , 2025, 37, 2410295.
Co ₂ P/FeP	257	<i>J. Mater. Chem. A</i> , 2024, 12, 31518-31525.
(Ni ₈₇ Fe ₄ Cr ₉) ₇₈ Si ₈ B ₁₄	295	<i>Int. J. Hydrogen Energy</i> , 2024, 92, 174-185.
CCO5	337	<i>J. Electroanal. Chem.</i> , 2024, 973, 118677.
NiBDC-A	293	<i>Small</i> , 2024, 20, 2407328.
P-CoMoO ₄ -Co ₃ O ₄	279	<i>Nanoscale</i> , 2024, 16, 18076-18085.
NiCo-LDH/CN/AgPO	289	<i>J. Alloys Compd.</i> , 2024, 1004, 175860.
Mo,Cl-Ni₃S₂	254	This study

Table S2 A summary of EGOR properties of Mo,Cl-Ni₃S₂ and state-of-the-art TM-based catalysts.

Catalyst	Current density (mA cm ⁻²)	Potential (V vs. RHE)	Electrolyte	References
Cu _{0.5} Co _{0.5} SnO _{3.17}	10	1.46	1 M KOH + 0.3 M EG	<i>J. Colloid Interface Sci.</i> , 2025, 698, 138018.
PdFe/N-CNTs	10	1.43	1 M KOH + 0.3 M EG	<i>J. Mater. Chem. A</i> , 2024, 12, 15984.
A-CoFeNi	10	1.36	1 M KOH + 0.3 M EG	<i>Chem. Eng. J.</i> , 2024, 498, 155472.
Mo-Ni ₂ P/NF	50	1.37	1 M KOH + 0.3 M EG	<i>Appl. Catal. B: Environ.</i> , 2026, 386, 126372.
NiCu _{60s} /NF	100	1.52	1 M KOH + 0.3 M EG	<i>ACS Catal.</i> , 2024, 14, 5314–5325.
NiCu/NF	100	1.45	1 M KOH + 0.3 M EG	<i>ACS Catal.</i> , 2024, 14, 5314.
Ni-Fe ₃ Se ₄ /NF	100	1.37	1 M KOH + 0.3 M EG	<i>J. Mater. Chem. A</i> , 2026, 14, 1923.
NiCe@NiTe	100	1.38	1 M KOH + 0.3 M EG	<i>J. Mater. Chem. A</i> , 2026, 14, 3591–3604.
MoS ₂ - (Ni,Fe)S ₂ @WC	100	1.41	1 M KOH + 0.3 M EG	<i>Chem. Eng. J.</i> , 534 (2026) 175122.
Ni/Ni ₃ N _{1-x}	100	1.38	1 M KOH + 0.3 M EG	<i>J. Mater. Chem. A</i> , 2024, 12, 15772–15780.
2D-CoNi-PET	100	1.41	1 M KOH + 0.3 M EG	<i>Small</i> , 2026, 22, e12758.
Mo,Cl-Ni₃S₂	10	1.32		
	50	1.35	1 M KOH + 0.3 M EG	<i>This study</i>
	100	1.37		

Table S3 Calculated charge transfer resistance (R_{ct}) and solution resistance (R_s) of catalysts obtained from the Nyquist plot during the EIS experiments.

Catalyst	R_s (Ω)	R_{ct} (Ω)
Mo,Cl-Ni ₃ S ₂	0.70	3.6
Mo-Ni ₃ S ₂	0.76	6.2
Cl-Ni ₃ S ₂	0.79	8.3
Ni ₃ S ₂	0.82	29.4
NF	0.85	82.4

Table S4 The charge transfer resistance (R_{ct}) of Mo,Cl-Ni₂S₃ calculated from operando EIS data.

Potential (V vs. RHE)	EGOR (Ω)	OER (Ω)
1.10	1168.15	2243.74
1.15	717.82	1079.41
1.20	353.46	723.82
1.25	155.41	506.66
1.30	92.63	421.64
1.35	19.86	148.26
1.40	2.51	57.65
1.45	1.17	55.81
1.50	1.12	50.21
1.55	0.99	8.31

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