

Supplementary Figures

Modular Microfluidic Probe for Addressable Fluidic Landscapes

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Supplementary Figures

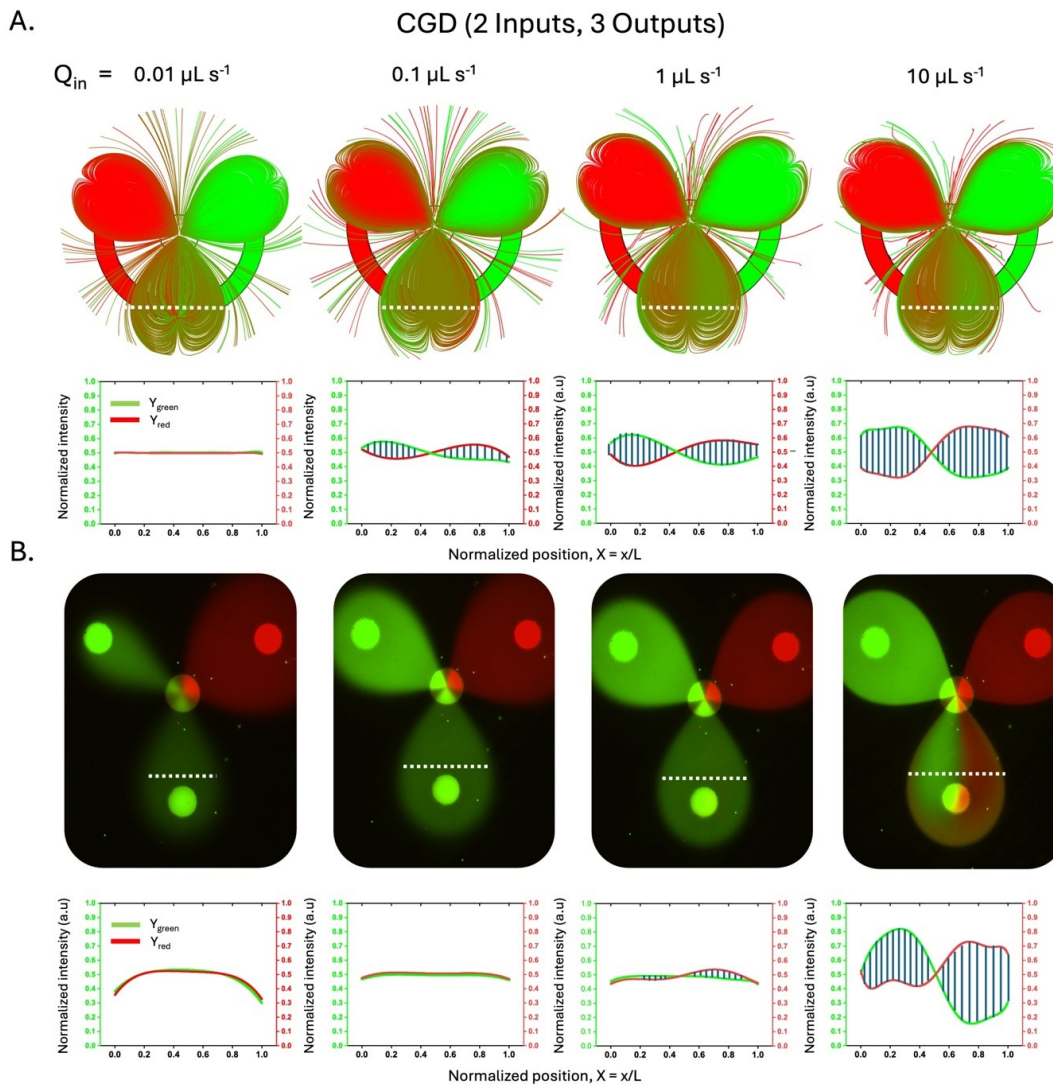


Fig. S1 Quantitative evaluation of mixing within a representative CGD output node. **(A)** Numerical simulations of the CGD (2 inputs, 3 outputs) configuration at increasing injection flow rates of $Q_{in} = 0.01 \mu\text{L s}^{-1}$, $0.1 \mu\text{L s}^{-1}$, $1 \mu\text{L s}^{-1}$, and $10 \mu\text{L s}^{-1}$ with a constant aspiration-to-injection flow-rate ratio of $\alpha = 2$. The dashed white line marks the cross-section used for profile extraction. The corresponding normalized red and green intensity profiles are shown below each panel, illustrating the transition from near-complete mixing at low flow rate to increasingly separated concentration fields at higher flow rates. **(B)** Experimental fluorescence images of the same CGD (2 inputs, 3 outputs) configuration under the corresponding flow conditions, using green and red fluorescent dyes to visualize the confined output node patterns. Dashed white lines indicate the extracted cross-sections, and the corresponding normalized intensity profiles are shown below each image. The overall agreement between (A) and (B) confirms that the numerical model captures the main flow-dependent mixing behavior observed experimentally within the representative output node.

Supplementary Figures

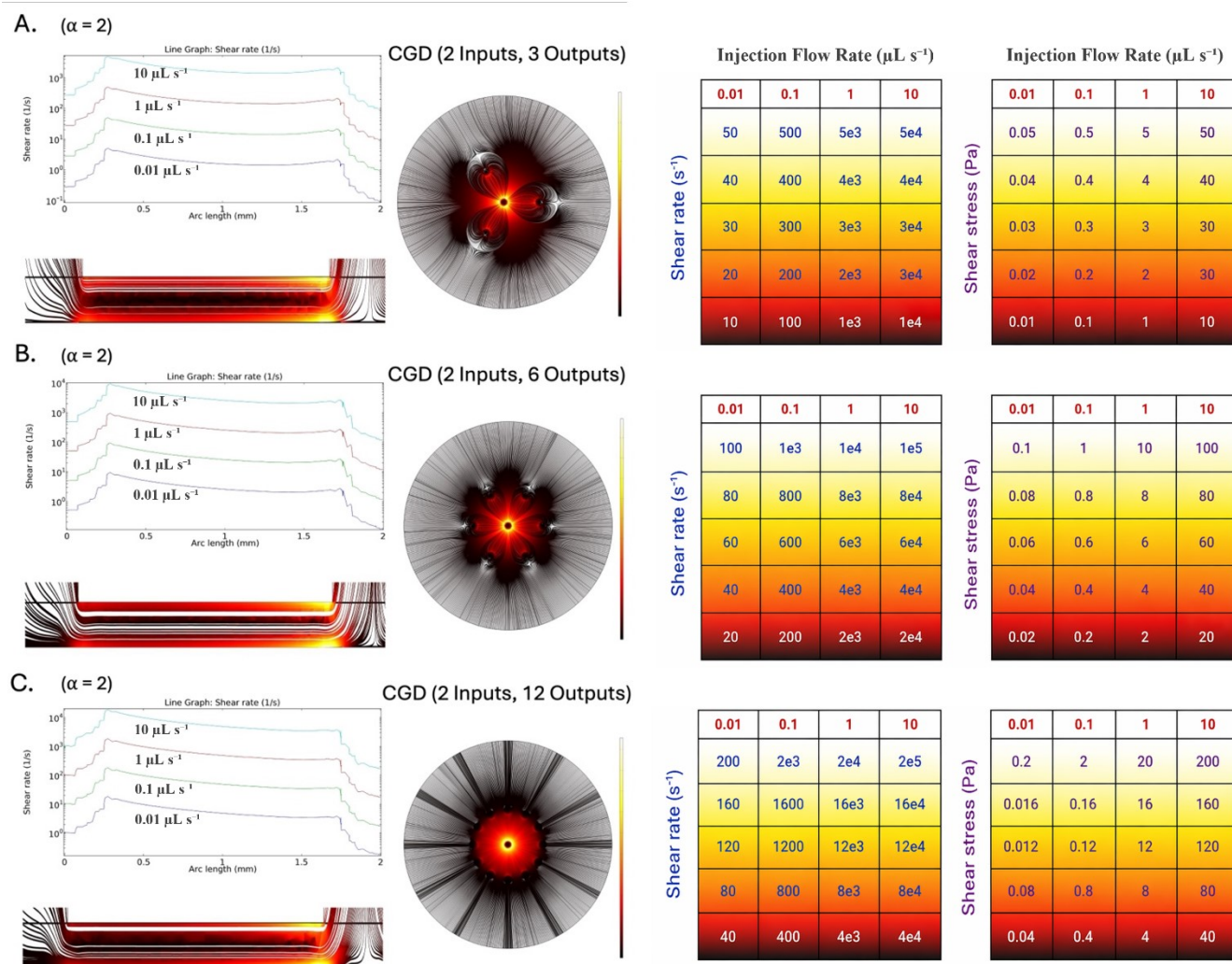


Fig. S2 Numerical characterization of shear conditions across CGD architectures. (A–C) Shear-rate and shear-stress distributions calculated for CGD (2 inputs, 3 outputs), CGD (2 inputs, 6 outputs), and CGD (2 inputs, 12 outputs) configurations, respectively, at a constant aspiration-to-injection flow-rate ratio of $\alpha = 2$ and a probe-to-substrate separation distance of $100 \mu\text{m}$. For each configuration, the left panels show the shear-rate profile extracted along the arc length of the HFC footprint (top) and a side-view cross-section of the confined region (bottom), while the center panels show the corresponding top-view streamline and shear-rate distribution within the HFC. The right panels summarize the calculated shear rate (s^{-1}) and corresponding shear stress (Pa) for injection flow rates of $Q_{\text{in}} = 0.01, 0.1, 1, \text{ and } 10 \mu\text{L s}^{-1}$, assuming water-like viscosities. Across all configurations, the highest shear occurs near the aspiration apertures, whereas most of the confined processing area remains within substantially lower shear ranges.

Supplementary Figures

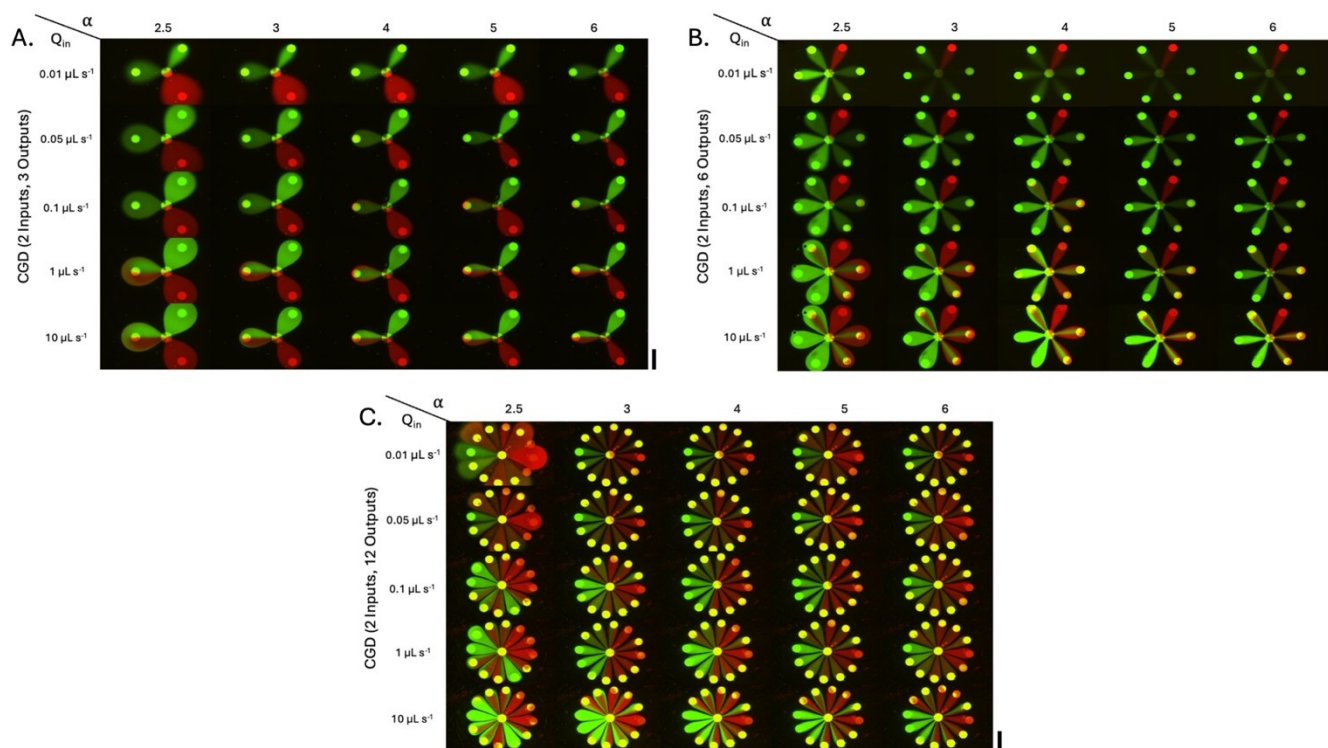


Fig. S3 Parametric characterization of CGD output patterns across flow rate and aspiration-to-injection flow-rate ratio. Representative fluorescence images showing the effect of the aspiration-to-injection flow-rate ratio ($\alpha = 2.5, 3, 4, 5,$ and 6) and injection flow rate ($Q_{in} = 0.01, 0.05, 0.1, 1,$ and $10 \mu\text{L s}^{-1}$) on the output node patterns of **(A)** CGD (2 inputs, 3 outputs), **(B)** CGD (2 inputs, 6 outputs), and **(C)** CGD (2 inputs, 12 outputs). The explored parameter space defines the practical operating envelope used to assess hydrodynamic flow confinement, mixing behavior, and discretization across the different architectures. Lower flow rates favor more mixed or near-homogeneous output states, whereas higher flow rates promote increasingly discretized and spatially separated output nodes. The figure also includes boundary cases to illustrate the limits of operation, including incomplete mixing at high flow and reduced confinement sharpness at very low flow. Simpler configurations achieve clear discretization over a broader operating range, while the 2 inputs, 12 outputs design requires higher flow and shows greater sensitivity to operating conditions. Scale bars: 1 mm.

Supplementary Figures

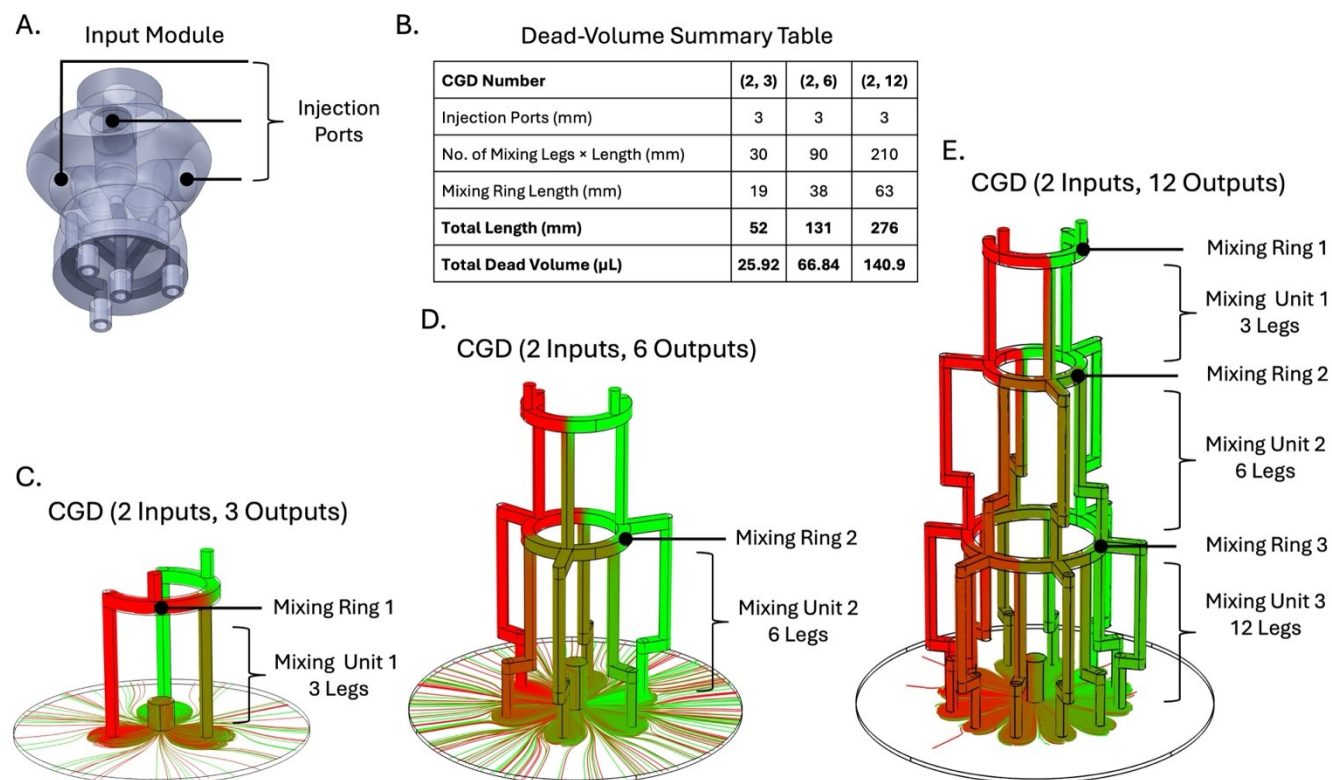


Fig. S4 Architecture-dependent channel length and dead-volume scaling in CGD configurations. **(A)** Schematic of the Input module, highlighting the three injection ports that feed the downstream CGD architectures. **(B)** Dead-volume summary table for the CGD (2 inputs, 3 outputs), CGD (2 inputs, 6 outputs), and CGD (2 inputs, 12 outputs) designs, listing the number and length of mixing legs, mixing-ring length, total channel length, and estimated total dead volume. **(C–E)** Representative schematics of the CGD (2 inputs, 3 outputs), CGD (2 inputs, 6 outputs), and CGD (2 inputs, 12 outputs) architectures, respectively, illustrating how increasing configuration complexity is accompanied by additional mixing rings, longer mixing paths, and a larger internal fluidic volume. As the number of outputs increases, the total upstream path length and dead volume increase substantially, which contributes to greater sensitivity to hydraulic resistance mismatch and to the need for higher flow rates to achieve clear discretization. These estimates also indicate that reagent consumption can be reduced in practice through shorter operating times, reduced dead volume, shorter upstream flow paths, or the use of simpler configurations when maximum concentration resolution is not required.