

# Construction Inverse NiCoCeAl-LDO/Ni Catalyst for Effective CO<sub>2</sub> Methanation in Low Temperature

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### **Synthesis of CoCeAl-LDO**

3.28 g  $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (11.2 mmol), 1.22 g  $\text{Ce}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$  (2.80 mmol) and 1.05 g  $\text{Al}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  (2.79 mmol) were dissolved in 50 mL deionized water to obtain solution C. 1.19 g  $\text{Na}_2\text{CO}_3$  (11.20 mmol) and 1.07 g  $\text{NaOH}$  (26.70 mmol) were dissolved in 50 mL deionized water to obtain solution D. Then solution C and solution D were simultaneously dropped into a three-necked flask using a peristaltic pump, maintaining a pH of 9-10 at 60 °C, followed by aging at 60 °C for 12 h. The mixed solution was cooled to room temperature, filtered, washed with deionized water and alcohol. Subsequently, dried at 60 °C for 24 h, denoted as CoCeAl-LDH. The CoCeAl-LDH were calcinated at 500 °C in a muffle furnace for 3 h, denoted as CoCeAl-LDO. The obtained sample was reduced in  $\text{H}_2$  at 400 °C for 3 h to obtain the final catalyst, denoted as CoCeAl-LDO-R

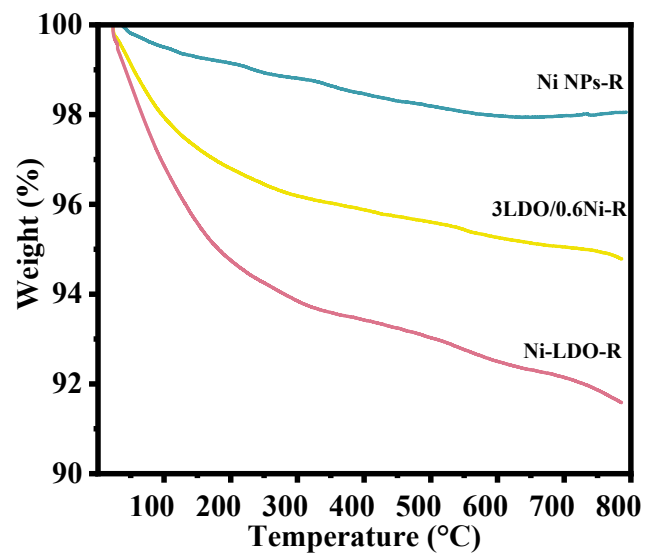
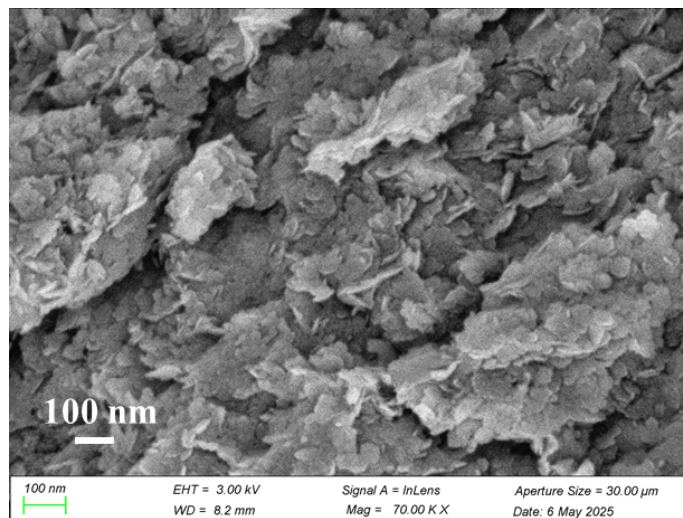


Fig. S1 TG profiles of the catalysts.



**Fig. S2.** SEM images of Ni(OH)<sub>2</sub>.

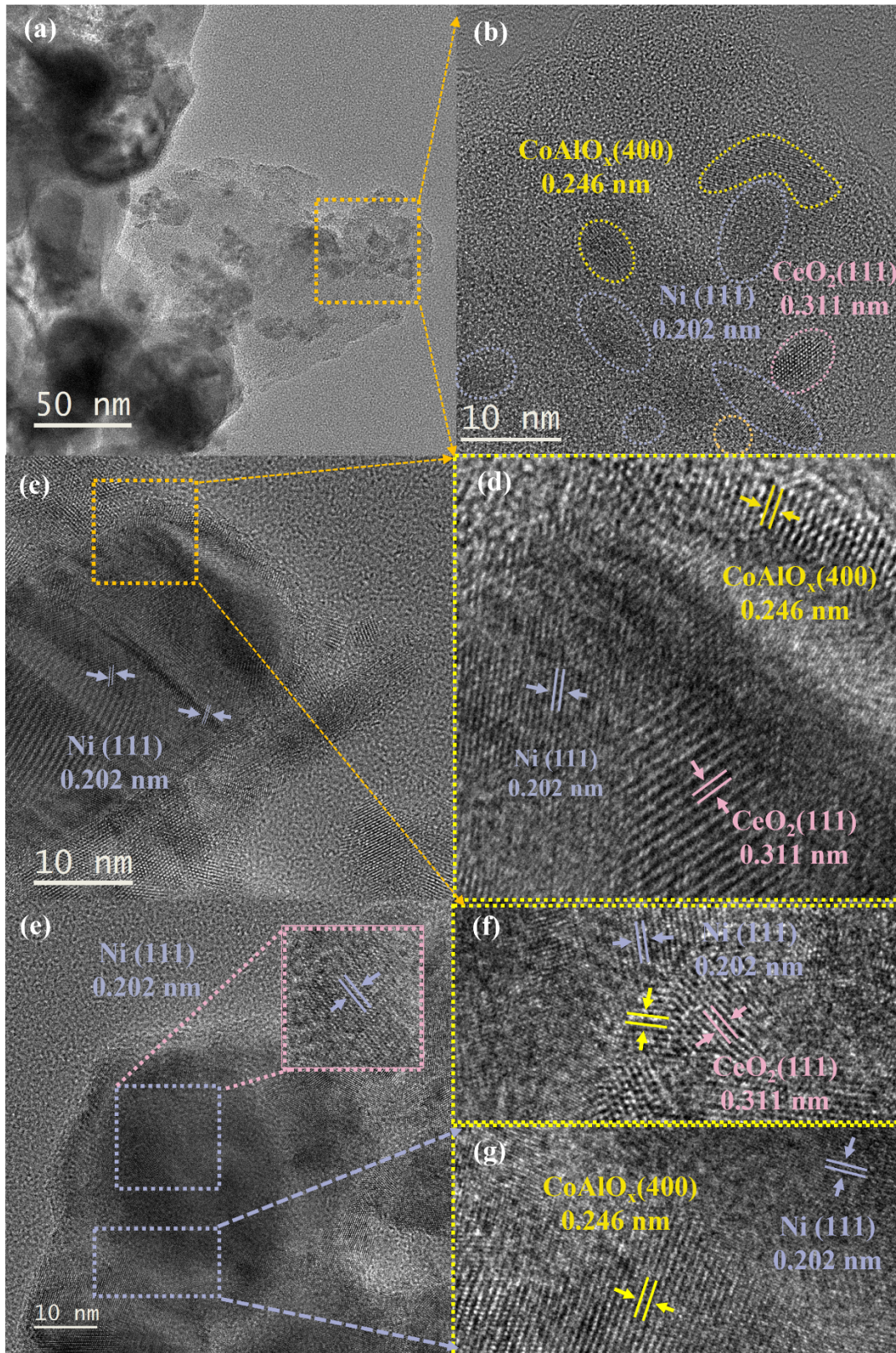


Fig. S3 (a-f) TEM and HRTEM images of 3LDO/0.6Ni-R.

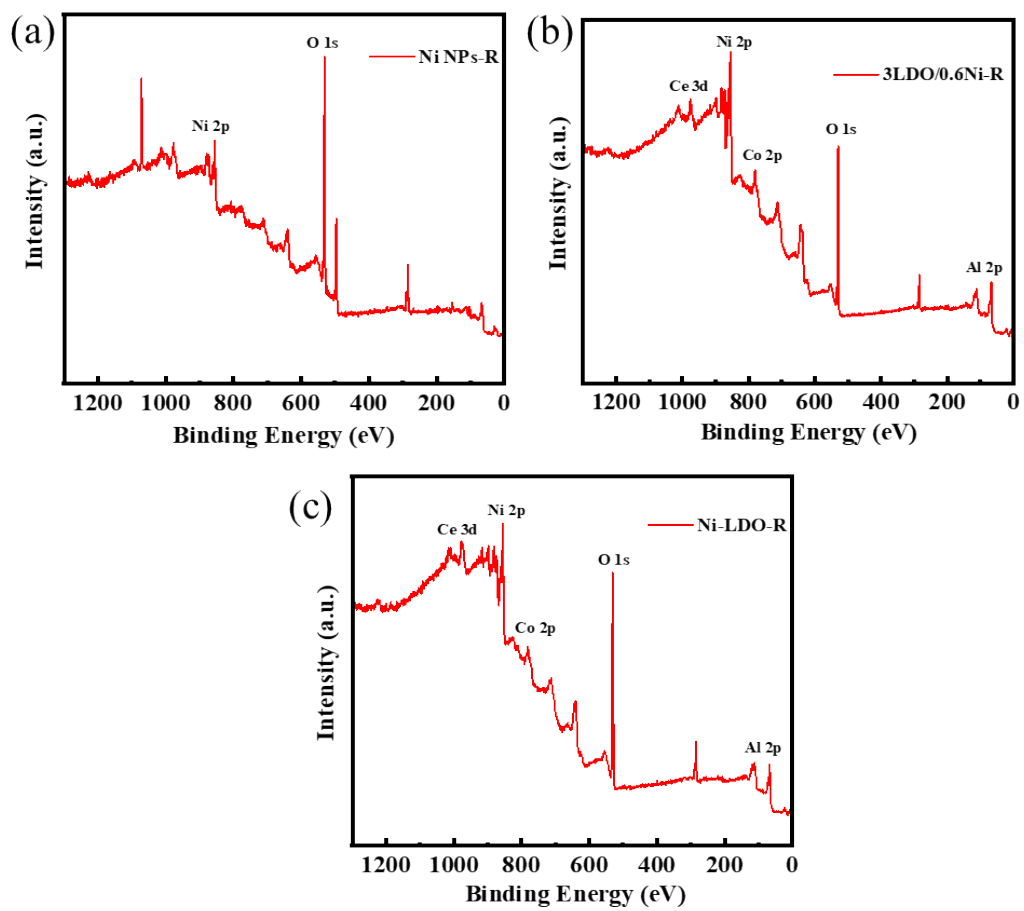


Fig. S4 XPS survey spectra of the catalysts.

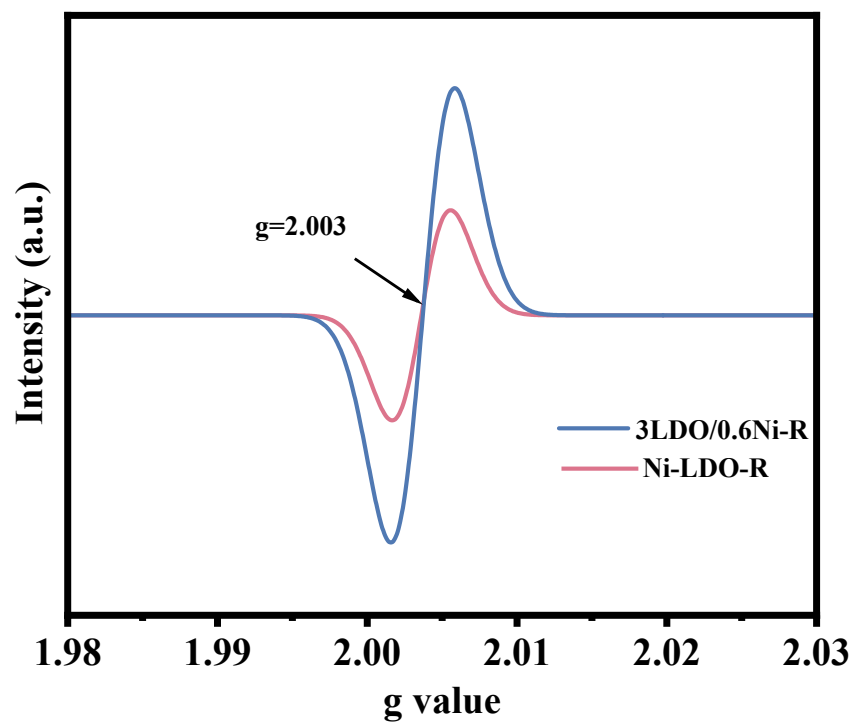
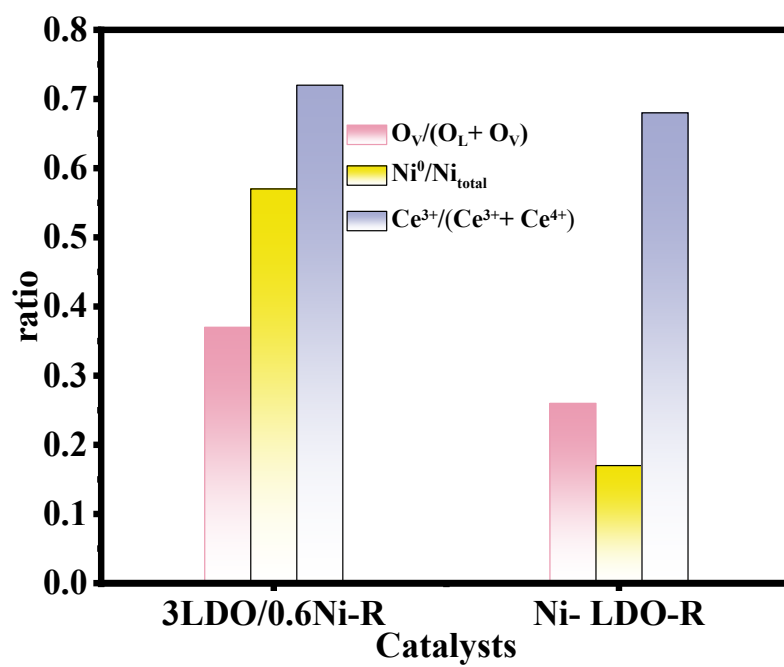


Fig. S5 EPR signals of LDO/0.6Ni-R and Ni-LDO-R samples.



**Fig. S6** The ratios of  $O_v/(O_L + O_v)$ ,  $Ni^0/Ni_{total}$ , and  $Ce^{3+}/(Ce^{3+} + Ce^{4+})$  for LDO/0.6Ni-R and Ni-LDO-R samples.

**Tab. S1** The compositions of the catalysts

Catalysts		Ni loading (wt %)	Co loading (wt %)	Ce loading (wt %)	Al loading (wt %)
3LDO/0.6Ni-R	Actual	58.55	4.53	11.11	2.15
	Theoretical	60.05	4.81	11.42	2.20
Ni- LDO-R	Actual	31.59	10.41	24.63	4.55
	Theoretical	34.12	11.46	26.24	5.24

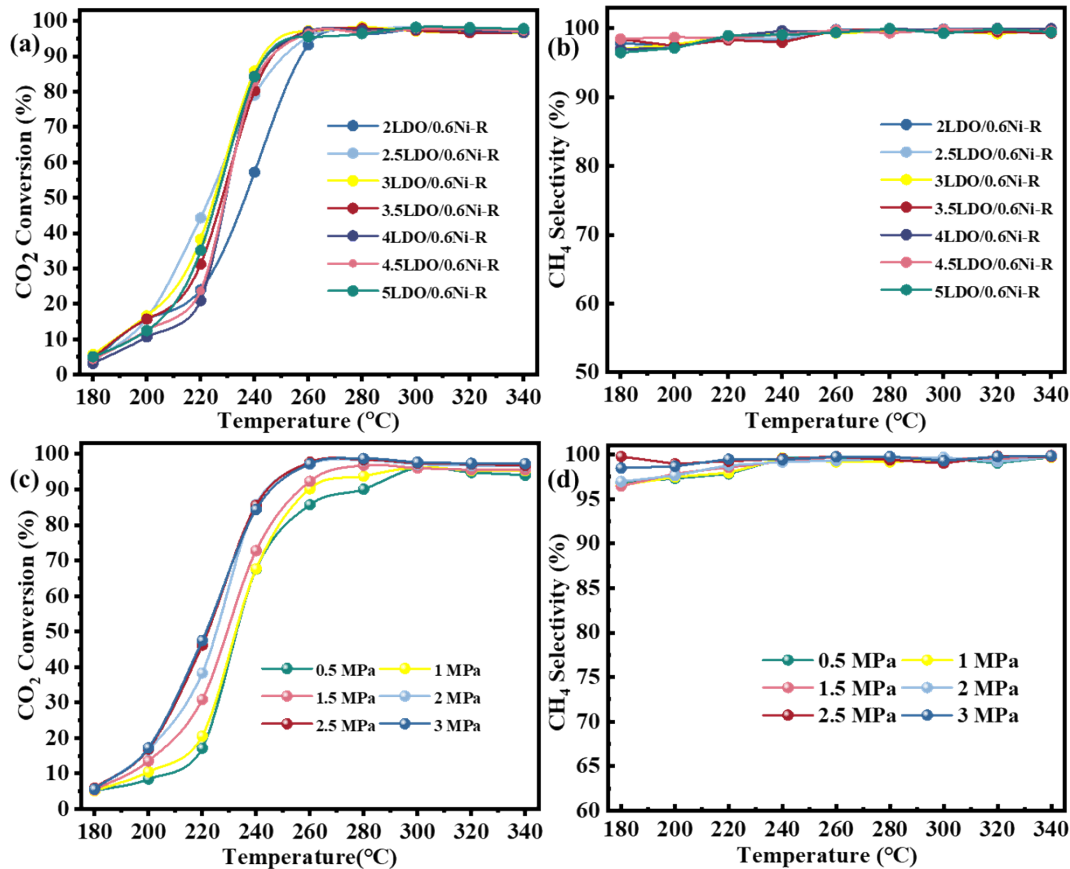
Obtained based on the ICP-OES results.

**Tab. S2** The carbon equilibrium data of the catalysts sample under the conditions of 260 °C, 2 MPa, and WHSV=15000 mL·g<sup>-1</sup>·h<sup>-1</sup>.

Catalysts	V <sub>CO<sub>2</sub>, in</sub> (mL·min <sup>-1</sup> )	V <sub>CO<sub>2</sub>, out</sub> (mL·min <sup>-1</sup> )	V <sub>CH<sub>4</sub>, out</sub> (mL·min <sup>-1</sup> )	Carbon balance coefficient
Ni NPs-R	27.00	25.52	1.12	0.98
3LDO/0.6Ni-R	27.00	0.77	26.05	0.99
Ni-LDO-R	27.00	6.52	20.45	0.99

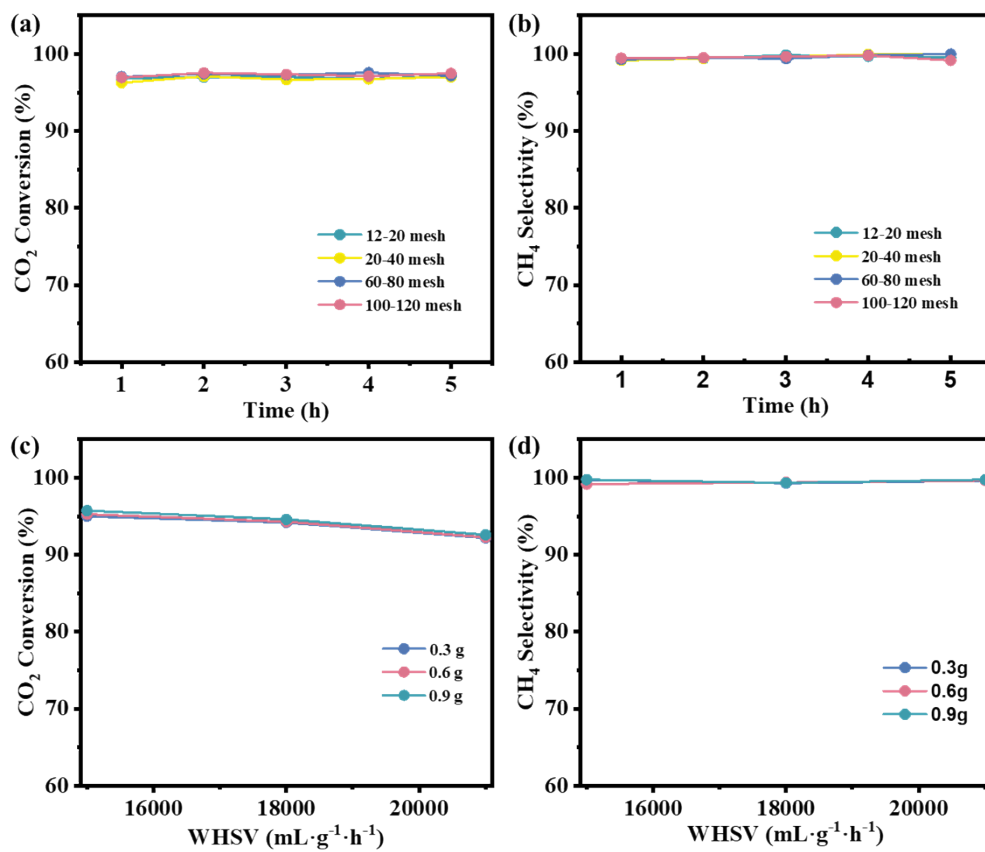
Note: V<sub>CO<sub>2</sub>, out</sub> and V<sub>CH<sub>4</sub>, out</sub> are calculated based on the exhaust gas flow rate at the outlet and the concentrations of each component in the GC.

$$\text{Carbon balance coefficient} = \frac{V_{CO_2, out} + V_{CH_4, out}}{V_{CO_2, in}}$$



**Fig. S7** The effect of different Ni:Co:Ce:Al mole ratio of LDO on (a) CO<sub>2</sub> conversion and (b) CH<sub>4</sub> selectivity; the effect of different pressure on (c) CO<sub>2</sub> conversion and (d) CH<sub>4</sub> selectivity over 3LDO/0.6Ni-R at various reaction temperature.

Note: y is the mole ratio of Ni:Co:Ce:Al = y:1:1:1 in LDO.



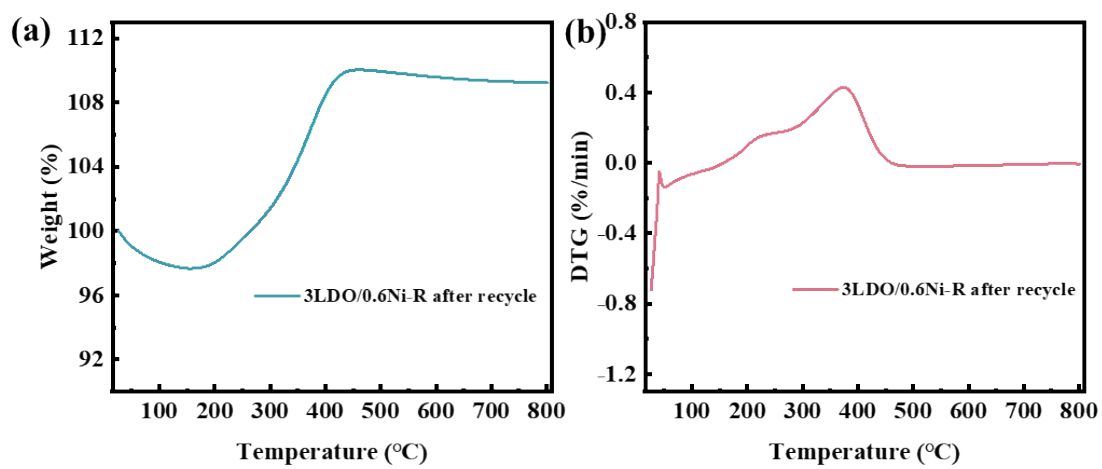
**Fig. S8** (a-b) CO<sub>2</sub> conversion and CH<sub>4</sub> selectivity over catalysts with different particle sizes. (2 MPa, 260 °C, H<sub>2</sub>/CO<sub>2</sub> mole ratio of 4:1, WHSV=15000 mL·g<sup>-1</sup>·h<sup>-1</sup>); (c-d) CO<sub>2</sub> conversion and CH<sub>4</sub> selectivity over catalysts with different catalyst quantity and different WHSV. (2 MPa, H<sub>2</sub>/CO<sub>2</sub> mole ratio of 4:1, 260 °C, 20-40 mesh)

**Tab. S3** Conversion and  $R_{CO_2}$  over various reaction temperature

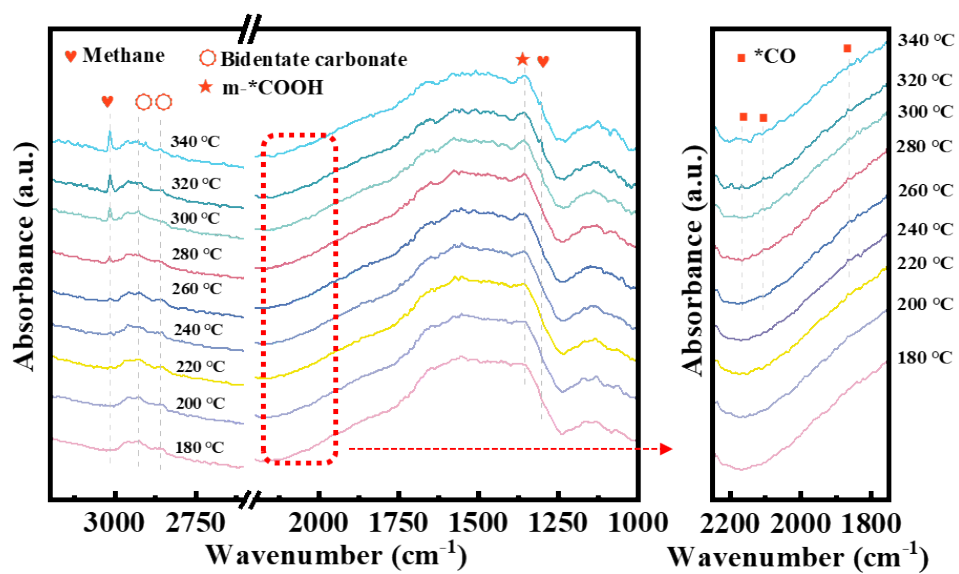
Temperature (°C)	Conversion (%)		$R_{CO_2}$ (mol/g·h)	
	3LDO/0.6Ni-R	Ni-LDO-R	3LDO/0.6Ni-R	Ni-LDO-R
220	38.27	22.93	0.047	0.027
230	60.55	40.14	0.074	0.048
240	82.51	54.18	0.099	0.068
250	94.75	67.96	0.114	0.082

**Tab. S4** Comparison of catalysts performance of CO<sub>2</sub> methanation over different catalysts in the literature.

Catalyst	H <sub>2</sub> /CO <sub>2</sub>	CO <sub>2</sub> Con. (%)	WSHV (mL·g <sub>cat</sub> <sup>-1</sup> ·h <sup>-1</sup> )	Temperature (°C)	Ref.
3LDO/0.6Ni-R	4:1	97.2	15000	260	This work
NiZrAl-LDH	4:1	93.3	15000	310	1
5Ni/NPs	4:1	85.0	12000	350	2
Co <sub>3</sub> O <sub>4</sub> -Al <sub>2</sub> O <sub>3</sub>	3:1	42.5	8000	250	3
Ru/CeO <sub>2</sub>	4:1	86.0	36000	300	4
Co (3)-N/CA2	4:1	83.1	18000	450	5
Ni15C10	4:1	62.1	21500	375	6
0.16Ni/0.15Co/CeO <sub>2</sub>	4:1	84.3	11000	300	7
3Mg10Ni5Co/MS	4:1	72.0	12000	400	8
NiCe EISA	4:1	68.5	15000	300	9
13Ni5MgO-BEA	4:1	78.0	7500	350	10



**Fig. S9** (a) TG and (b) DTG spectra of 3LDO/0.6Ni-R after recycle in air atmosphere



**Fig. S10** DRIFTS spectra recorded at different temperature in 72% H<sub>2</sub>/18% CO<sub>2</sub>/10% N<sub>2</sub> on 3LDO/0.6Ni.(1800-2200 cm<sup>-1</sup>)

**Tab. S5** Infrared band assignments of the surface species for CO<sub>2</sub> methanation.<sup>1,11-15</sup>

Wavenumber (cm <sup>-1</sup> )	Surface species
1511	monodentate carbonate
1584	bidentate carbonate
1370	monodentate formate
1548	bidentate formate
2850, 2923	methoxy
1306, 3012	methane
1733, 1740	formyl
1863, 2105, 2168	carbonyl

## Notes and references

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