

Supporting Information

Revealing Transport Kinetics for Efficient Electrochemical Conversion of Captured CO₂ in Amine Solutions

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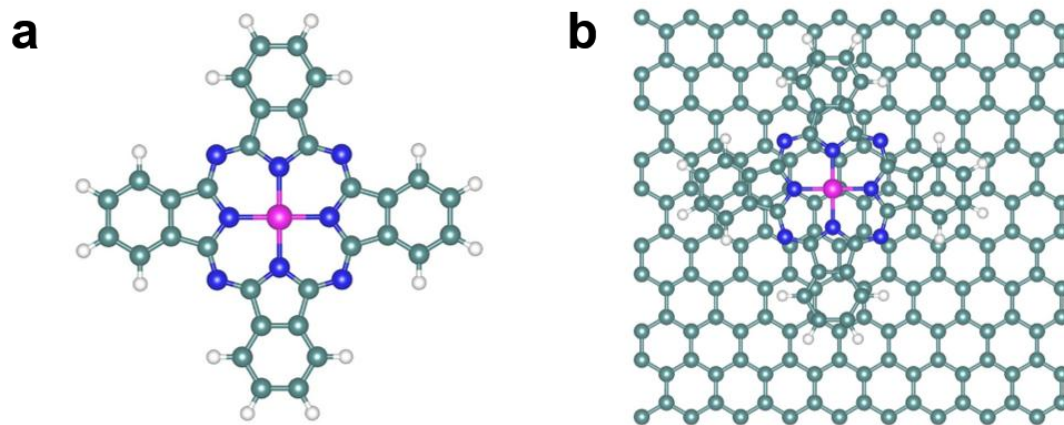


Figure S1. The structures of (a) CoPc and (b) CoPc/CB for DFT calculations. The green, blue, pink, and white balls denote C, N, Co, and H atoms, respectively.

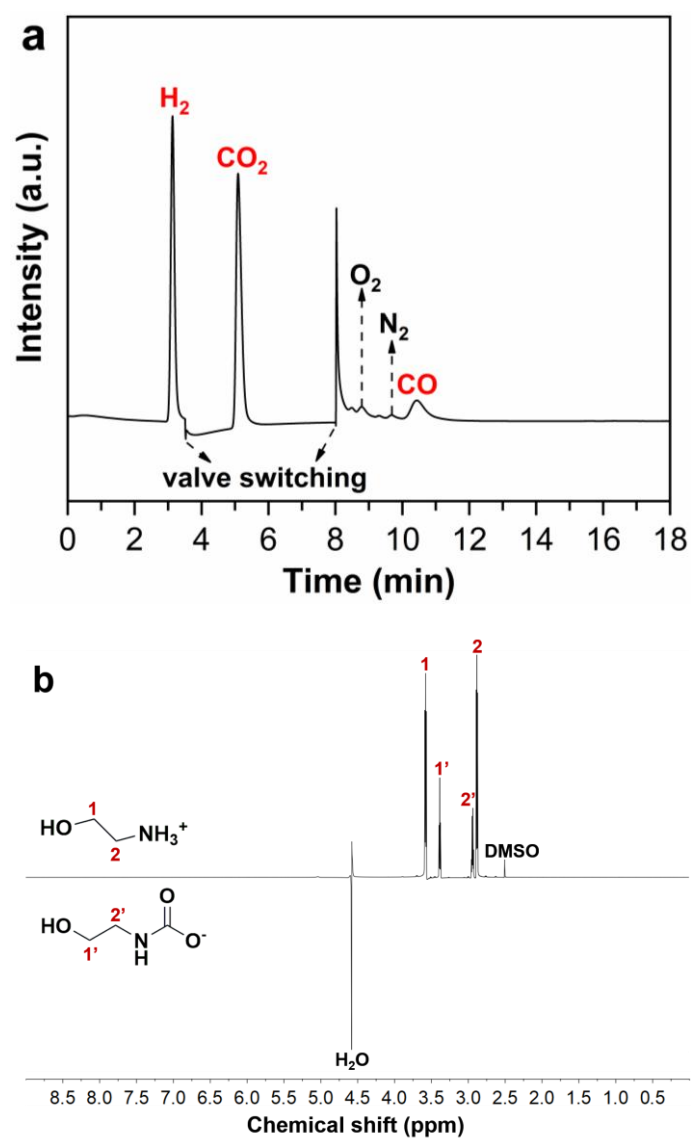


Figure S2. (a) Gas chromatogram of the gaseous products and (b) ^1H NMR spectrum of the electrolyte solution after electrolysis of CO_2 -loaded 2 M MEA at -0.85 V vs RHE for 15 min using CoPc/CB catalyst. Since the concentration of MEA-derived species is too high, the electrolyte is diluted with ultrapure water for 10 times before ^1H NMR measurement.

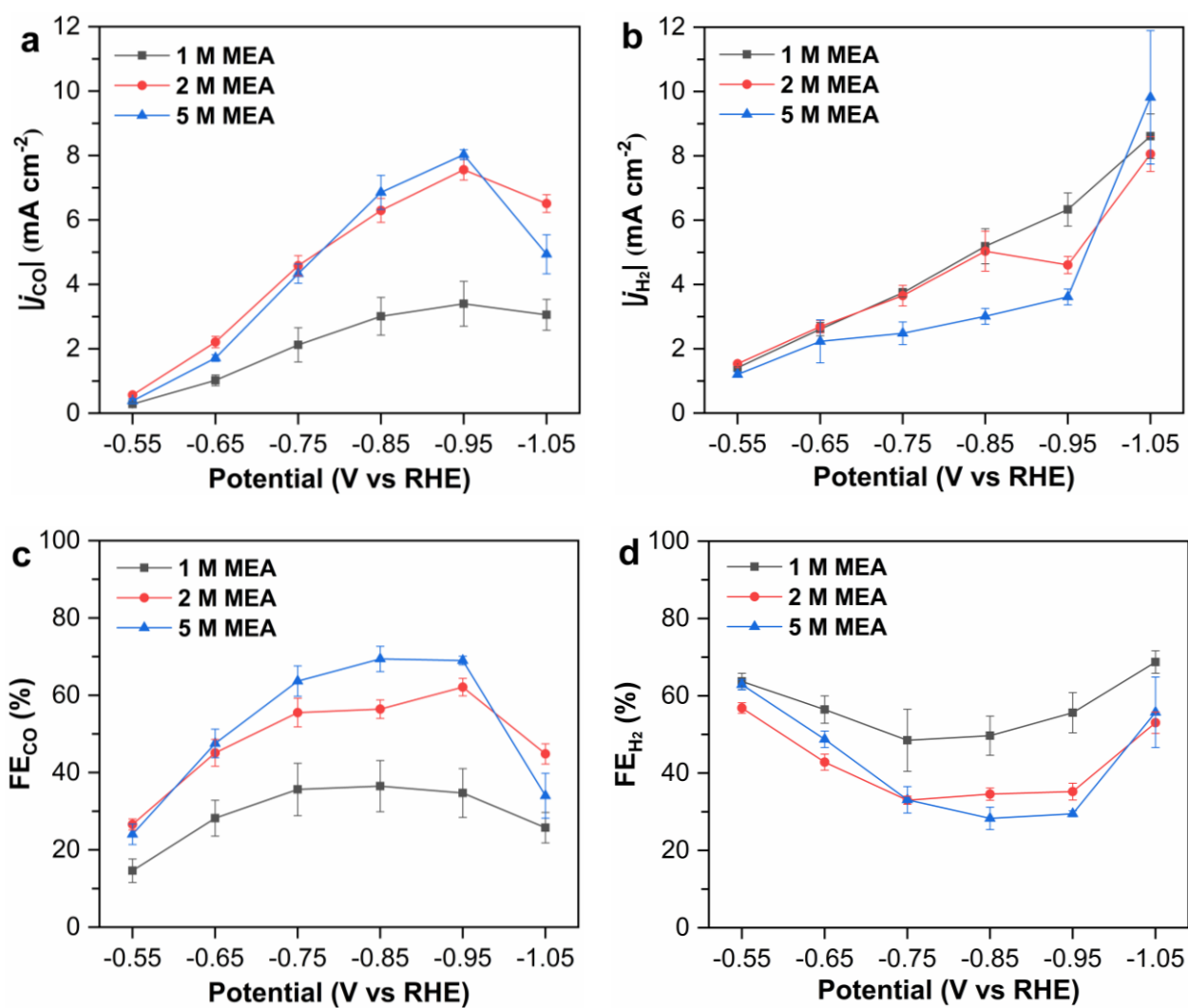


Figure S3. (a) $|j_{CO}|$, (b) $|j_{H_2}|$, (c) FE_{CO}, and (d) FE_{H₂} recorded for the electrolysis of captured CO₂ in MEA solutions of varying concentrations using CoPc/CB catalyst.

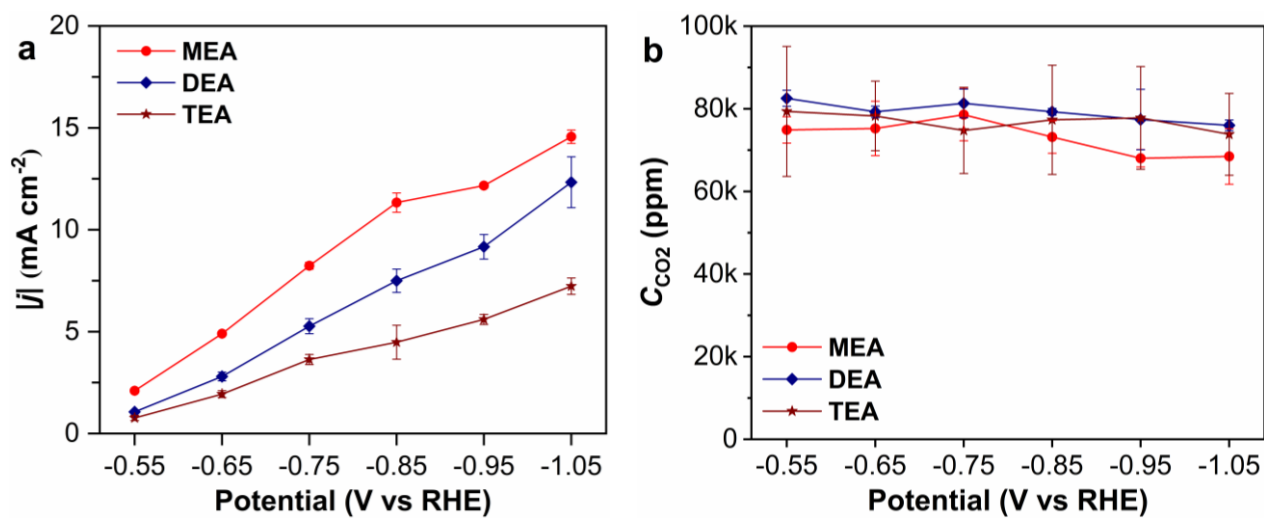


Figure S4. (a) $|j|$ and (b) concentrations of CO₂ in the headspace recorded for the electrolysis of CO₂-loaded 2 M MEA, DEA, and TEA solutions using CoPc/CB catalyst.

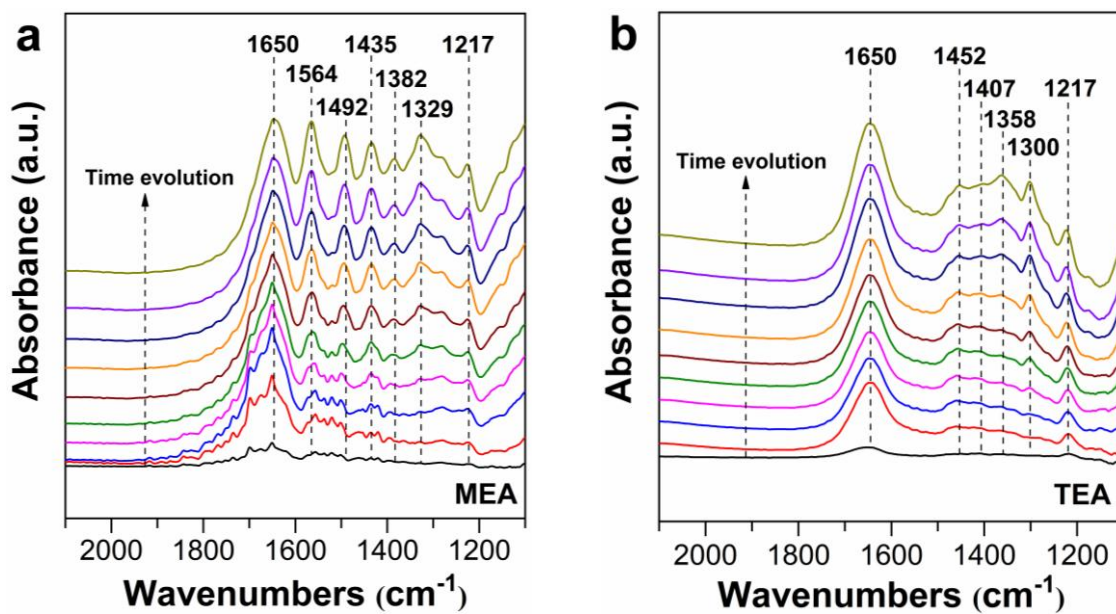


Figure S5. *In-situ* ATR-FTIR recorded during the process of CO₂ capture in 2 M (a) MEA and (b) TEA solutions for 30 min.

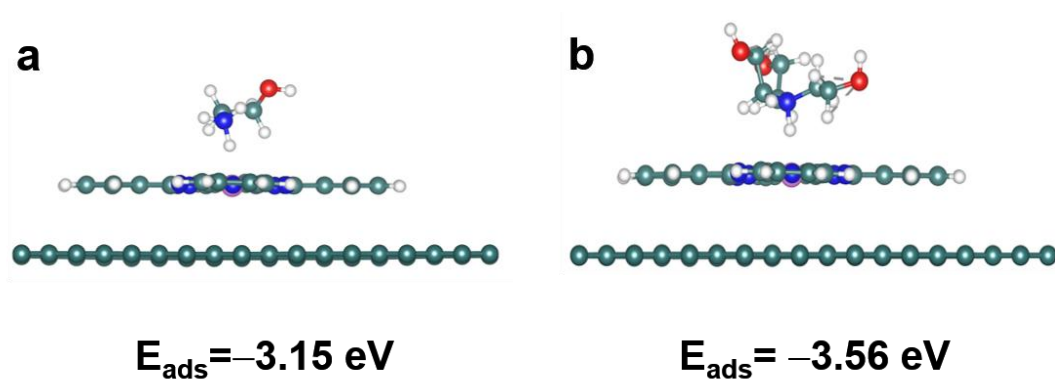


Figure S6. E_{ads} of (a) MEA- H^+ and (b) TEA- H^+ on the Co active site. The green, blue, red, and white balls denote C, N, O, and H atoms, respectively.

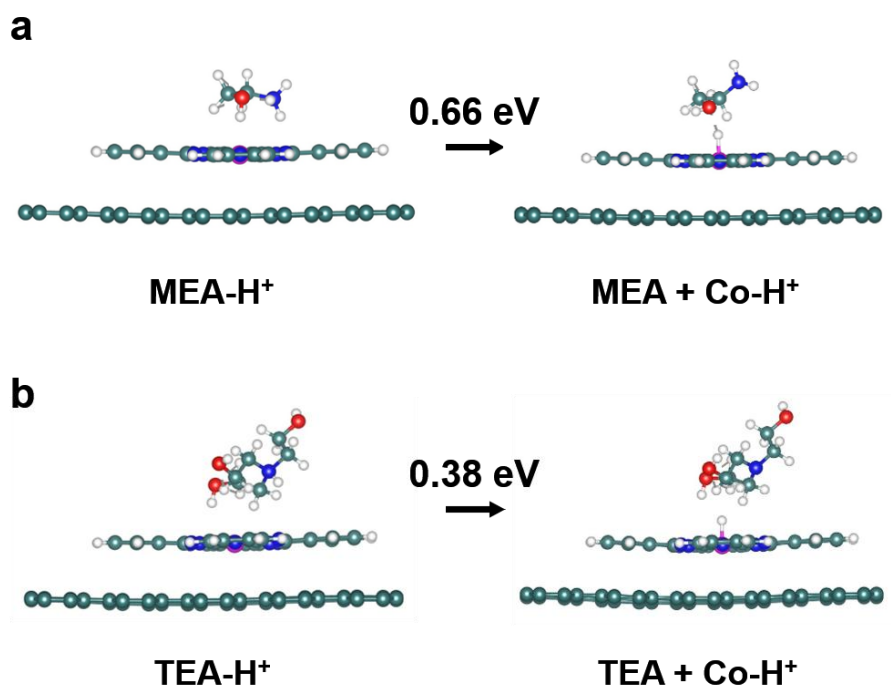


Figure S7. The energy required for H transferred from (a) MEA-H⁺ and (b) TEA-H⁺ to the Co active site. The green, blue, red, and white balls denote C, N, O, and H atoms, respectively.

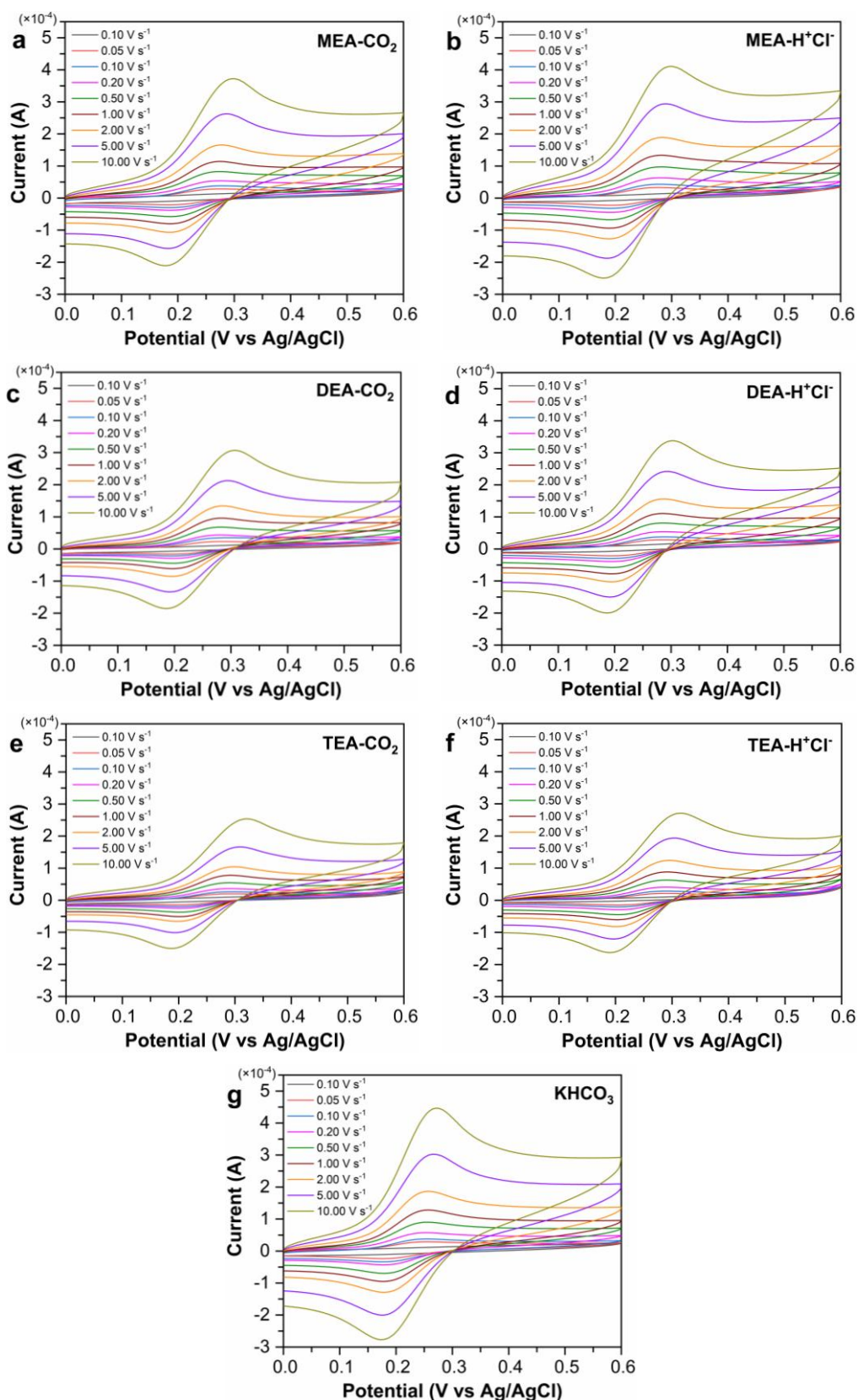


Figure S8. Cyclic voltammograms recorded in (a,c,e) CO₂-loaded 2 M amine solutions, (b,d,f) ammonium chloride solutions of the corresponding amines, and (g) 2 M KHCO₃ solution at different scan rates.

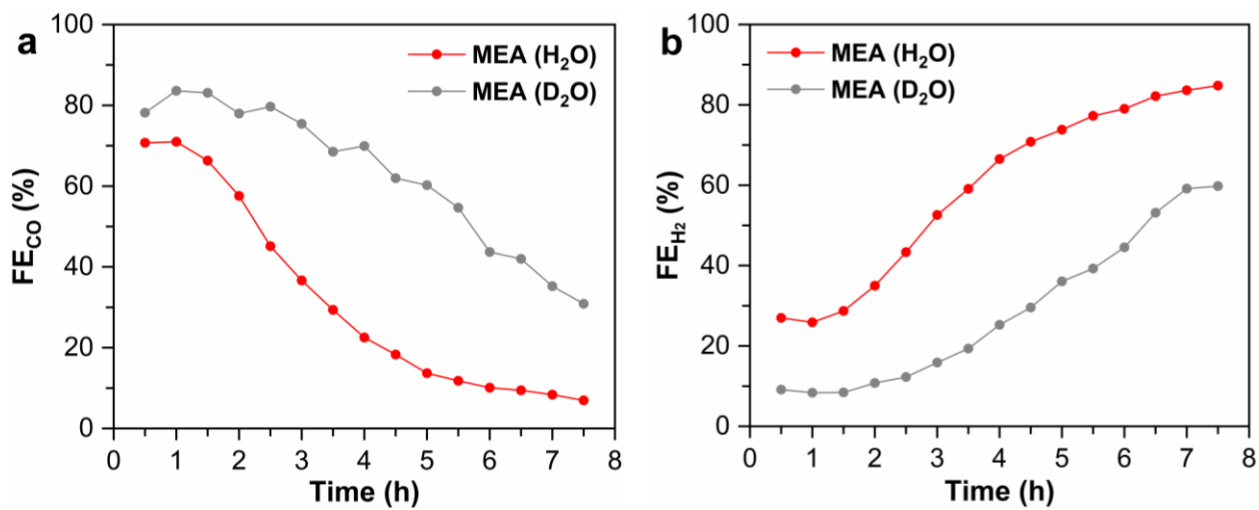


Figure S9. (a) FE_{CO} and (b) FE_{H₂} recorded for the prolonged electrolysis of captured CO₂ in 2 M MEA at -0.85 V vs RHE using CoPc/CB catalyst and H₂O or D₂O as solvent.

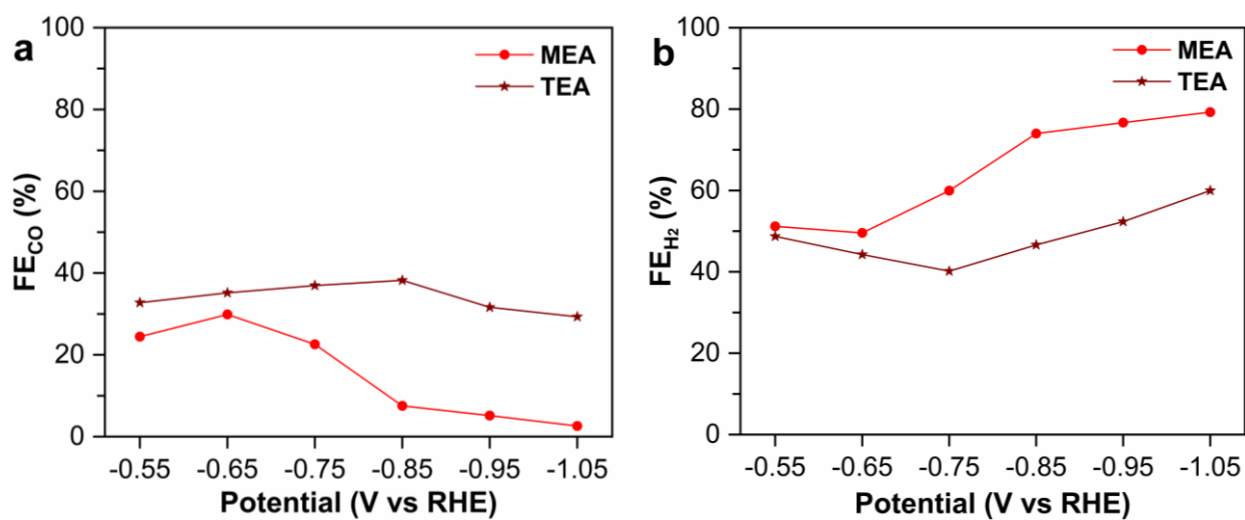


Figure S10. (a) FE_{CO} and (b) FE_{H₂} recorded for the electrolysis of captured CO₂ in 2 M MEA and TEA solutions using Ni-N-C catalyst.

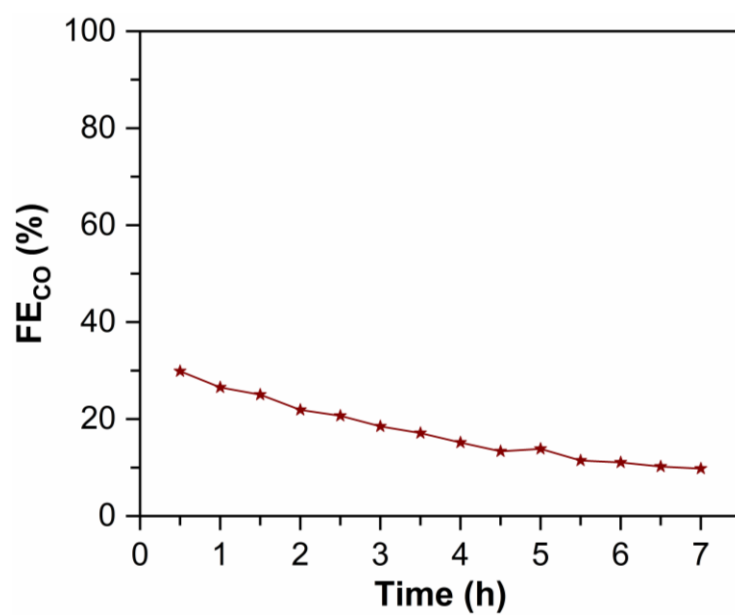


Figure S11. FE_{CO} recorded for the prolonged electrolysis of captured CO₂ in 2 M TEA solution at -0.85 V vs RHE using Ni-N-C catalyst.

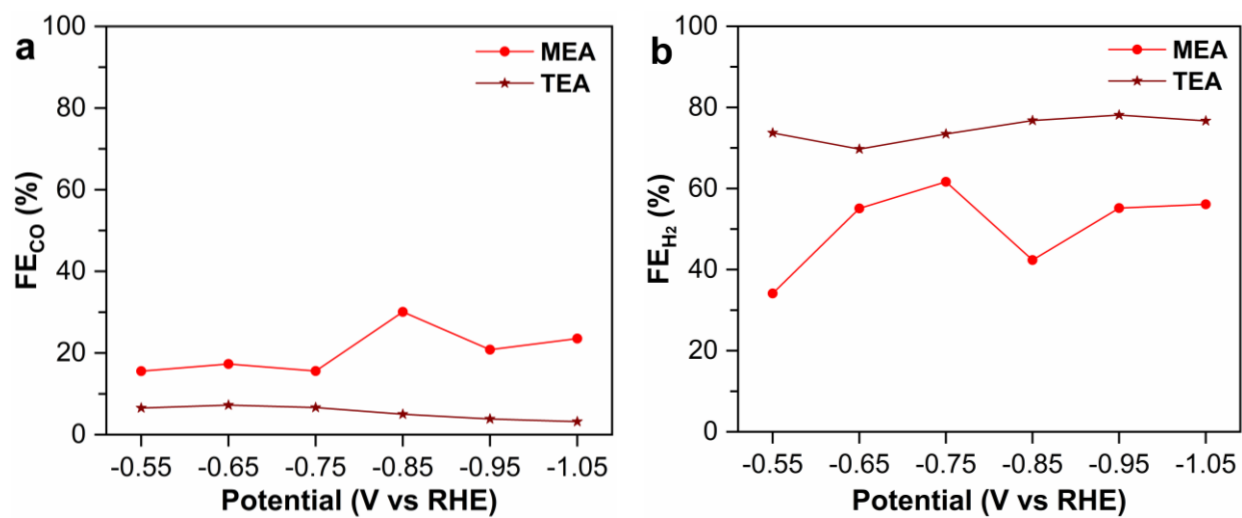


Figure S12. (a) FE_{CO} and (b) FE_{H2} recorded for the electrolysis of captured CO₂ in 2 M MEA and TEA solutions using Ag catalyst.

Table S1. The pH values of various amine solutions.

Amine solutions	pH
2 M MEA	12.04
CO ₂ -loaded 2 M MEA	7.45
Ar-purged CO ₂ -loaded 2 M MEA	7.64
2 M DEA	11.55
CO ₂ -loaded 2 M DEA	7.53
Ar-purged CO ₂ -loaded 2 M DEA	7.76
2 M TEA	10.93
CO ₂ -loaded 2 M TEA	7.53
Ar-purged CO ₂ -loaded 2 M TEA	7.71

Table S2. Performance comparison for electrochemical conversion of captured CO₂ in various amine solutions within an H-cell.

Catalyst	Electrolyte (pH)	FE _{CO} ^a (%)	j ^b (mA cm ⁻²)	Potential ^c	Ref.
CoPc/CB	Ar-purged CO ₂ -loaded 2 M MEA (7.64)	69	12.2	-0.95 V vs RHE	This work
	Ar-purged CO ₂ -loaded 2 M DEA (7.76)	76	7.5	-0.85 V vs RHE	
	Ar-purged CO ₂ -loaded 2 M TEA (7.71)	80	4.5	-0.85 V vs RHE	
Ag	N ₂ -purged CO ₂ -loaded 2 M MEA + 3 M KCl (8.3)	38	N. A.	-0.66 V vs RHE	S1
Ag	N ₂ -purged CO ₂ -loaded 2 M KCl + 2 M MEA (7.6)	19	30	-0.85 V vs RHE ^d	S2
Ni-N/C	Ar-purged CO ₂ -loaded 1 M MEA (pH not reported)	78	1.7 ^e	-0.58 V vs RHE	S3
	Ar-purged CO ₂ -loaded 1 M DEA (pH not reported)	65	1.5 ^e	-0.64 V vs RHE	
Ni(cyclam)Cl ₂	Ar-purged CO ₂ -loaded 0.1 M MEA + 0.05 M phosphate (7.9)	77	1.41	-0.74 V vs RHE ^d	S4
	Ar-purged CO ₂ -loaded 0.1 M DEA + 0.05 M phosphate (8.0)	41	1.42	-0.74 V vs RHE ^d	

^a Maximum FE_{CO} under reported conditions. ^b Current density achieved at the listed potential. ^c The electrolysis potential at which the maximum FE_{CO} achieved. ^d Potentials converted from reported potentials against SHE or Ag/AgCl according to the pH of electrolyte in the reference. ^e |j| calculated from the reported |j_{CO}| and FE_{CO} in the reference. N. A. denotes data not available.

Table S3. The coefficients of viscosity for different CO₂-loaded amine solutions.

Electrolyte	Coefficient of viscosity (mPa·s)
CO ₂ -loaded 1 M MEA	1.0
CO ₂ -loaded 2 M MEA	1.1
CO ₂ -loaded 5 M MEA	2.0
CO ₂ -loaded 2 M DEA	1.4
CO ₂ -loaded 2 M TEA	1.8

References

- S1. G. Lee, Y. C. Li, J.-Y. Kim, T. Peng, D.-H. Nam, A. Sedighian Rasouli, F. Li, M. Luo, A. H. Ip, Y.-C. Joo and E. H. Sargent, Electrochemical upgrade of CO₂ from amine capture solution, *Nat. Energy*, 2020, **6**, 46-53.
- S2. G. Leverick, E. M. Bernhardt, A. I. Ismail, J. H. Law, A. Arifutzzaman, M. K. Aroua and B. M. Gallant, Uncovering the active species in amine-mediated CO₂ reduction to CO on Ag, *ACS Catal.*, 2023, **13**, 12322-12337.
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- S4. A. Q. Mir, A. Banerjee, F. Ihiri, S. Chiu, A. N. Alexandrova, C. Morales-Guio and J. Y. Yang, Optimizing CO₂-Loaded Aqueous Amine Solutions for Higher Electrocatalytic CO₂ Reduction Activity, *J. Am. Chem. Soc.*, 2025, **147**, 39123-39133.