

Supplementary Information

Unveiling Wavelength-Dependent Light Roles on Dynamic Structures for Photothermal Toluene Oxidation over Atomically Dispersed Pd/TiO₂

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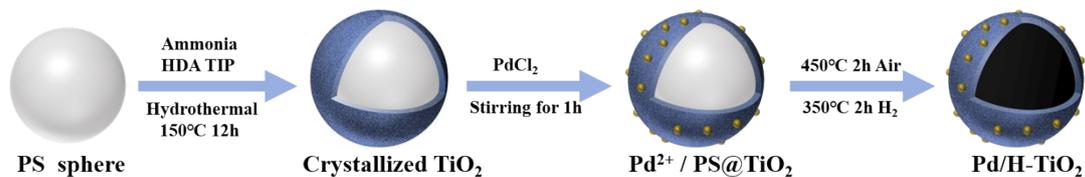


Figure S1. Schematic preparation of Pd/H- TiO_2 .

Pd/H- TiO_2 were synthesized by *in situ* growth of TiO_2 on the surface of PS spheres, followed by the introduction of varying amounts of Pd and subsequent template removal through calcination. The as-obtained samples were denoted as X% Pd/H- TiO_2 (X = 1, 1.5 and 2) and the actual content of Pd in these samples was 1.07, 1.51 and 1.88 % determined by atomic absorption spectrometry (AAS).

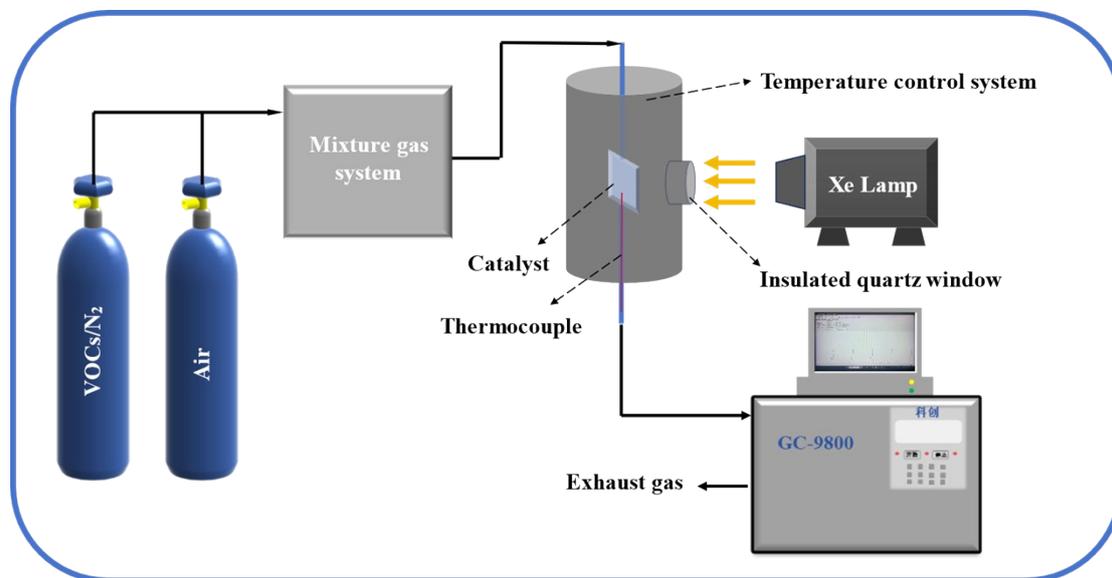


Figure S2. Diagram of photothermal synergistic catalytic oxidation device.

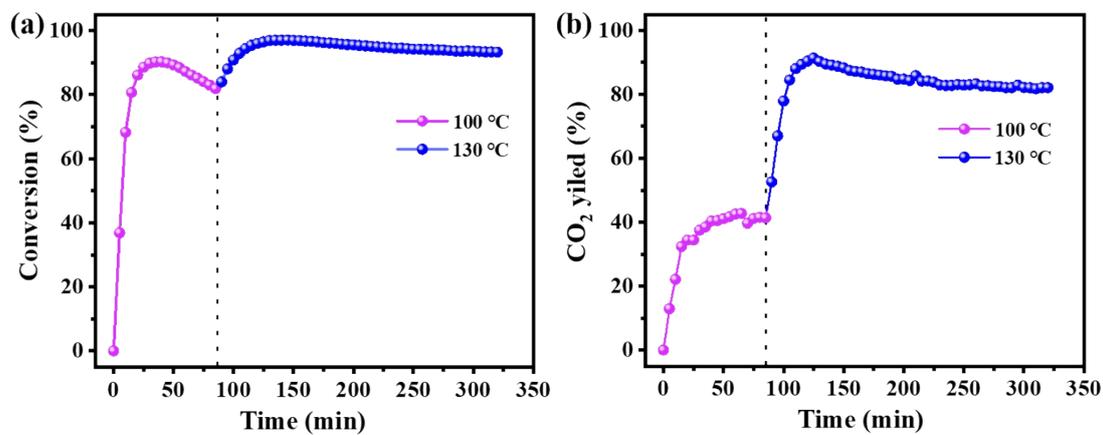


Figure S3. (a) Toluene conversion and (b) CO₂ yield over 1.5% Pd/H-TiO₂ under UV-Vis light at 100 and 130 °C.

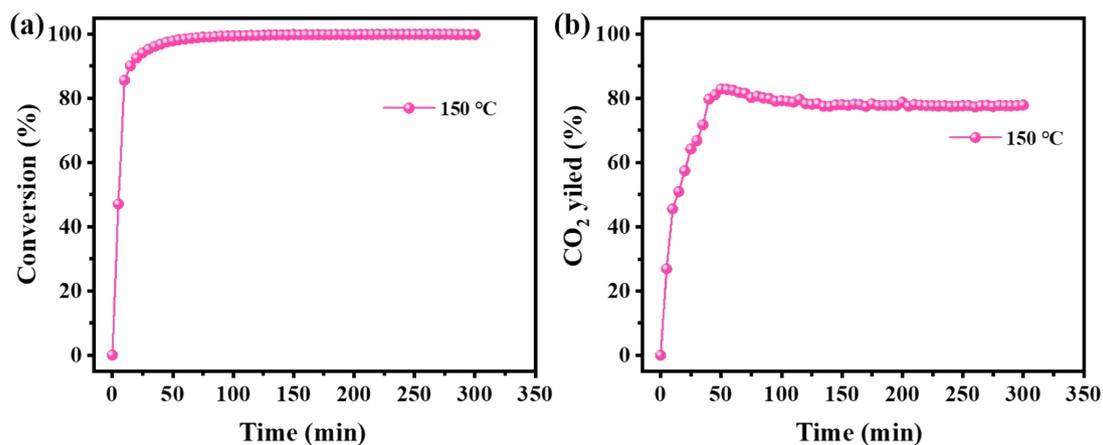


Figure S4. (a) Toluene conversion and (b) CO₂ yield over 1.5% Pd/H-TiO₂ under UV-Vis light at 150 °C.

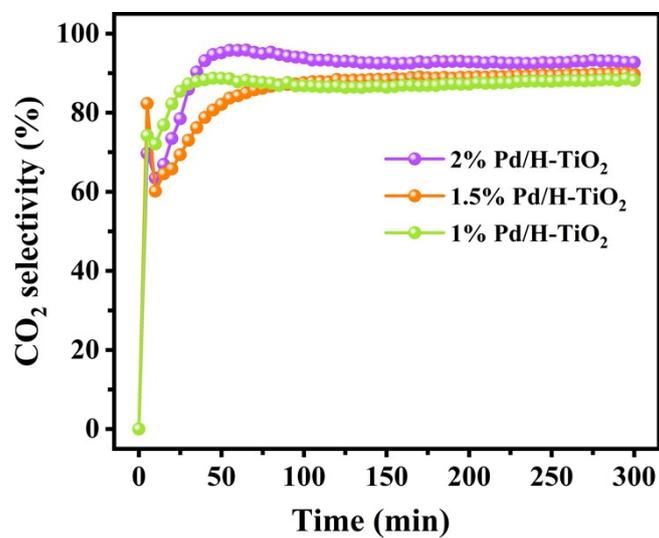


Figure S5. CO₂ selectivity of Pd/H-TiO₂ under UV-Vis light at 130 °C.

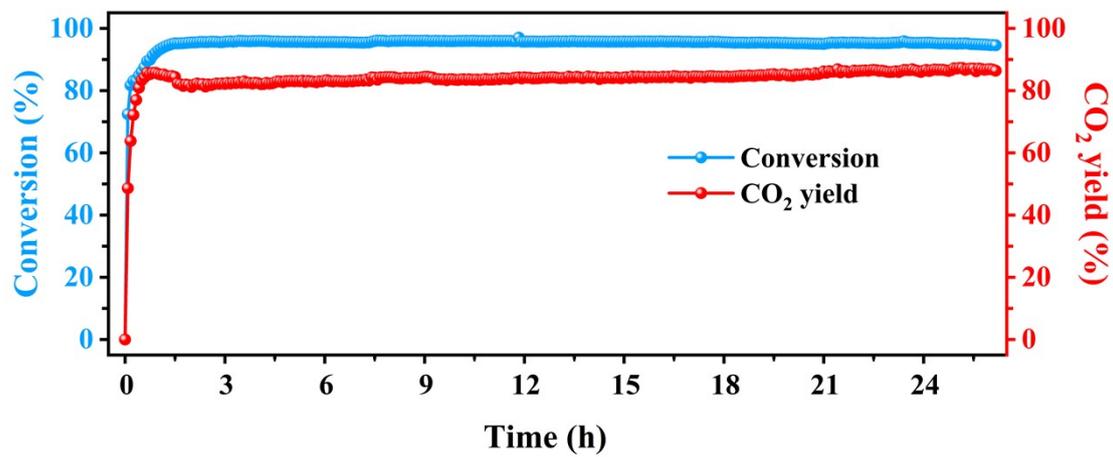


Figure S6. Photothermal catalytic stability test over Pd/H-TiO₂ under UV-Vis light at 130 °C.

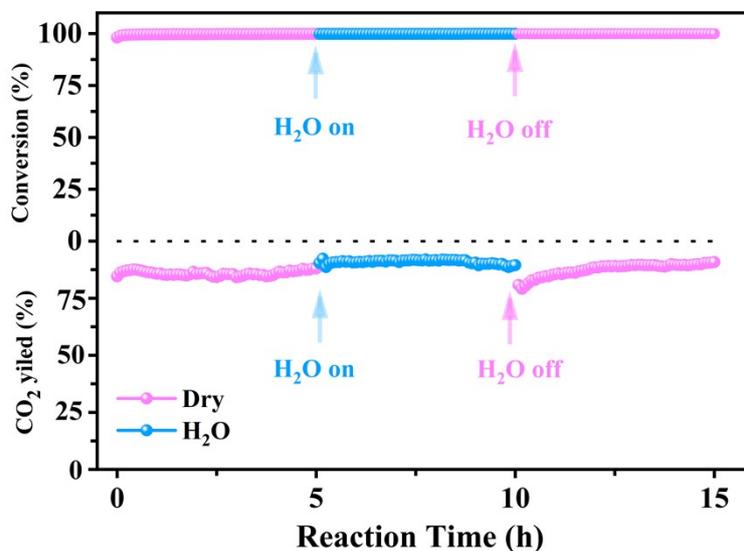


Figure S7. Photothermal catalytic activity for toluene oxidation over Pd/H-TiO₂ under humidity under UV-Vis light at 130 °C.

It is highly desirable for a catalyst to exhibit excellent stability and water resistance to ensure its suitability for practical applications. The stability of the Pd/H-TiO₂ catalyst was evaluated under UV-Vis light at 130 °C. As shown in Figure S6, the Pd/H-TiO₂ demonstrated remarkable stability during 25 h of toluene oxidation (dry conditions), maintaining a toluene conversion of 94.5% and a CO₂ yield of 86.3%. In practical industrial applications, water vapor is often present. To evaluate the catalyst's water resistance, 10 vol% water vapor was introduced after 5 hours of catalytic reaction. As shown in Figure S7, following the introduction of water vapor, the toluene conversion remained stable. Surprisingly, the CO₂ yield increased from an average of 85.9% to 90.9%. After the water vapor was removed, the CO₂ yield stabilized at 90.7%.

According to previous study, the oxygen in the water would exchange with the adsorbed oxygen or lattice oxygen of the catalyst, generating new OOH species, which could be decomposed into $\bullet\text{OH}$.¹ The $\bullet\text{OH}$ could further react with the adsorbed oxygen, generating more active oxygen species ($\bullet\text{O}_2^-$ and $\bullet\text{O}$).² Therefore, the improved catalytic activity after the introduction of water was reasonable. The above results indicate that Pd/H-TiO₂ exhibits excellent stability and water resistance, demonstrating its practical applicability in the photothermal degradation of toluene.

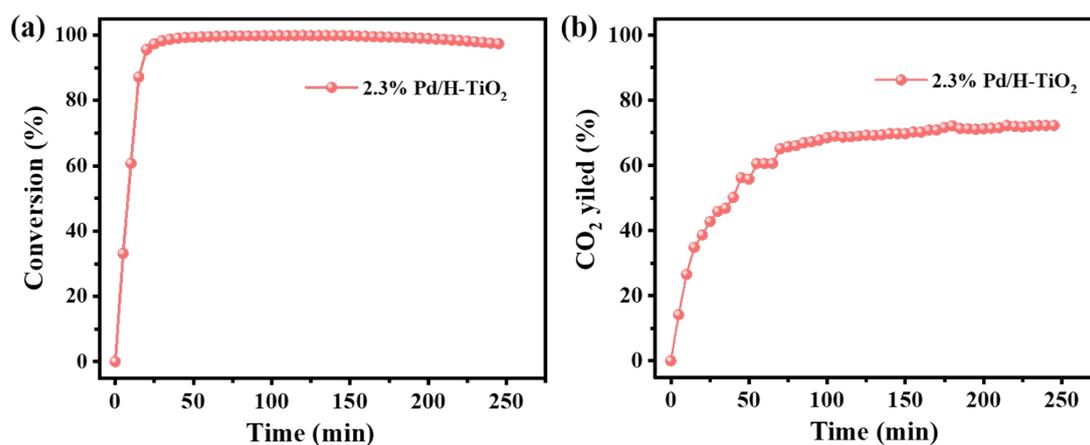


Figure S8. (a) Toluene conversion and (b) CO₂ yield over 2.3% Pd/H-TiO₂ under UV-Vis light at 130 °C.

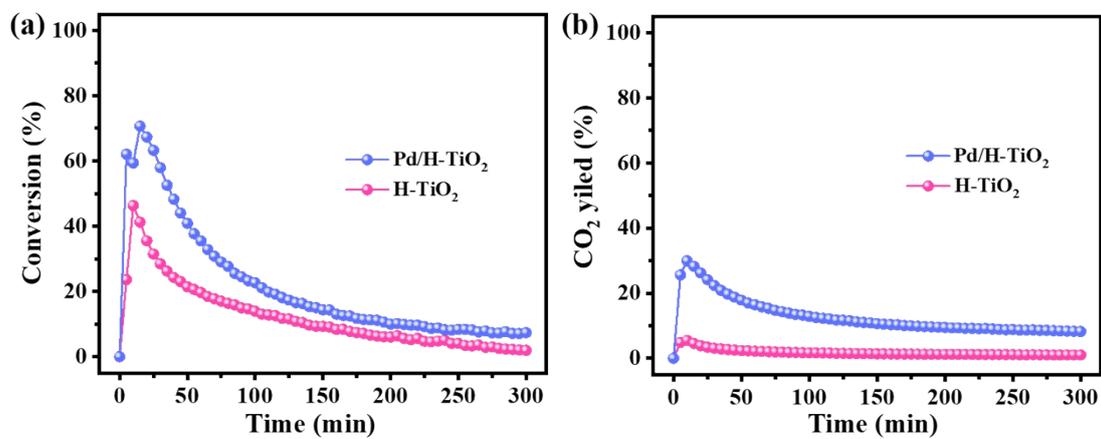


Figure S9. (a) Toluene conversion and (b) CO₂ yield over H-TiO₂ and Pd/H-TiO₂ under UV-Vis light at 30 °C.

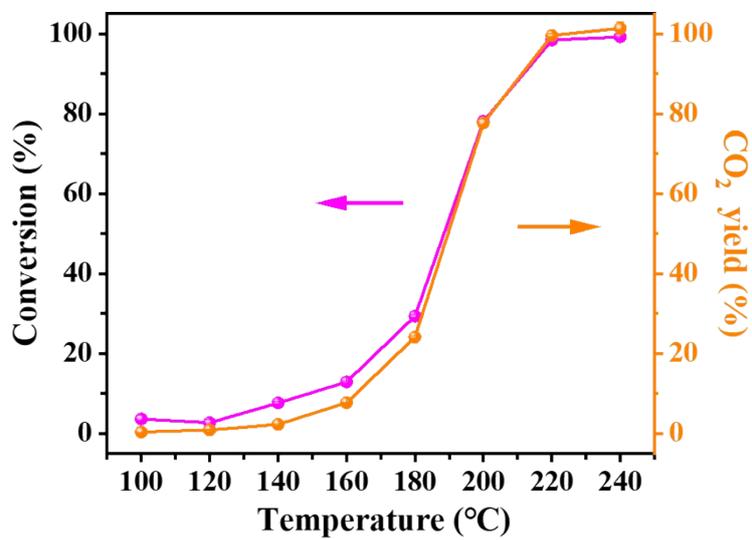


Figure S10. Toluene conversion and CO₂ yield over Pd/H-TiO₂ under different reaction temperatures without light irradiation.

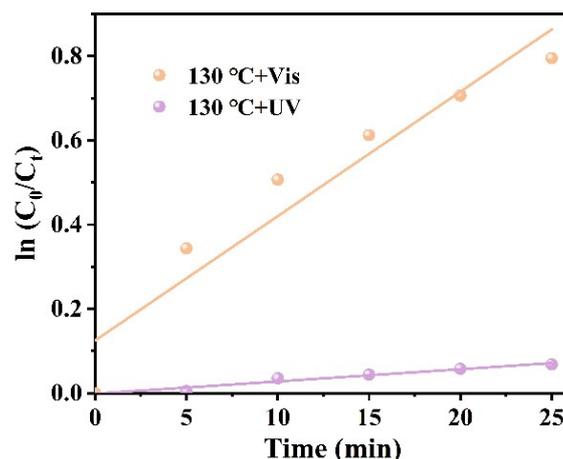


Figure S11. Pseudo first-order kinetic fitting curves of CO₂ yield

The CO₂ yield over Pd/H-TiO₂ under UV and visible light irradiation was also evaluated using a pseudo-first-order kinetic model. The apparent reaction rate constants (k) can be evaluated from the slope of $\ln(C_0/C_t)$ versus time curves (Figure 11). Based on this analysis, the k values under UV and visible photothermal catalytic conditions were determined to be 2.9×10^{-3} and $29.5 \times 10^{-3} \text{ min}^{-1}$, respectively (Table S2). Clearly, the k value under visible-light conditions is about ten times higher than that under UV irradiation, which provides quantitative support for the distinct reaction behaviors and pathways induced by different irradiation wavelengths.

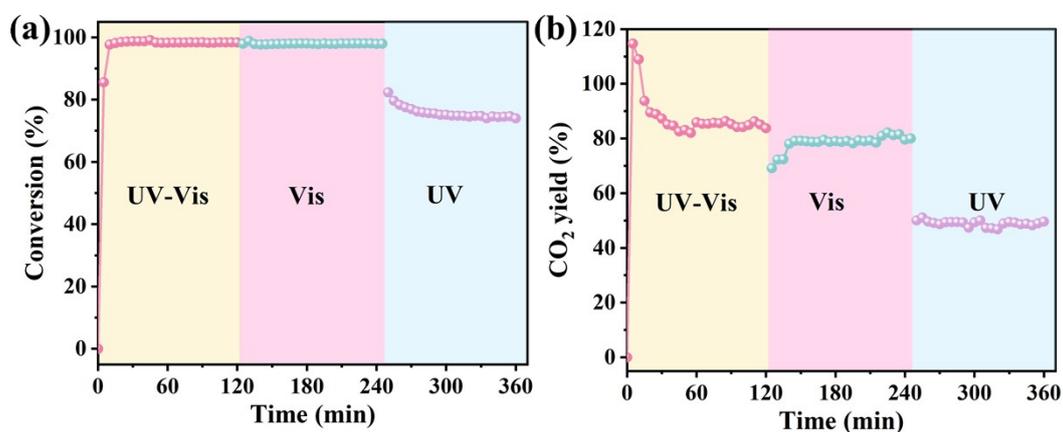


Figure S12. (a) DCM conversion and (d) CO₂ yield over Pd/H-TiO₂ under photothermal catalysis with different light irradiation.

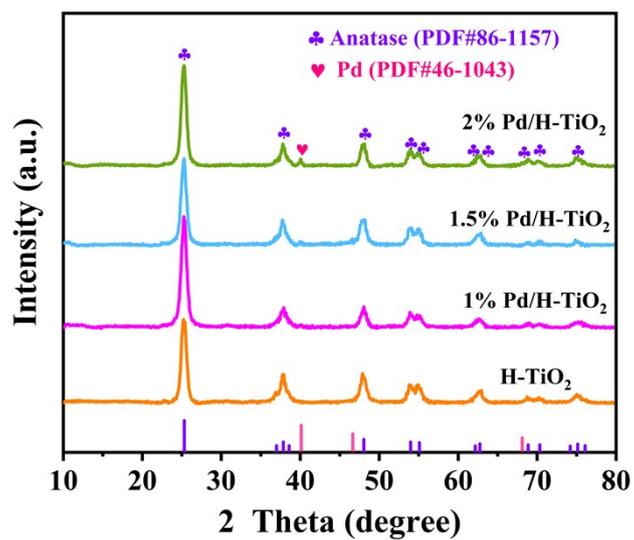


Figure S13. XRD patterns of the H-TiO₂ and Pd/H-TiO₂ samples.

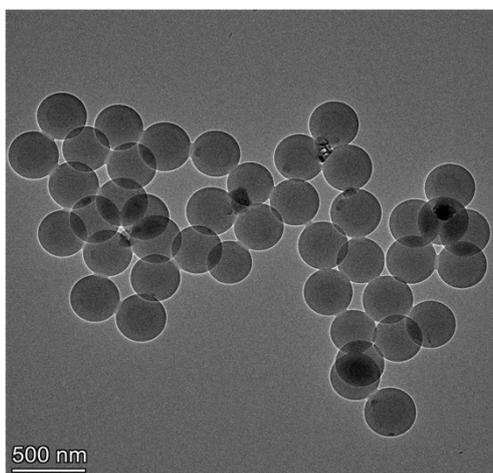


Figure S14. TEM images of polystyrene spheres.

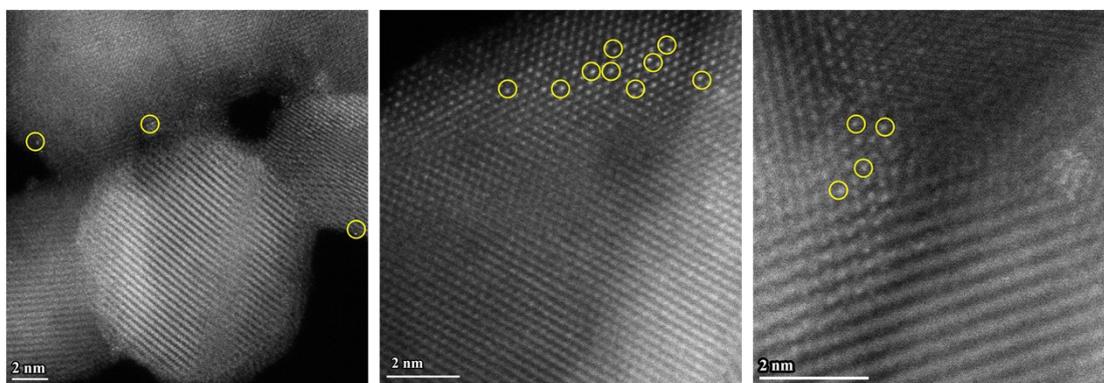


Figure S15. AC-HAADF-STEM images of the 2% Pd/H-TiO₂ catalyst.

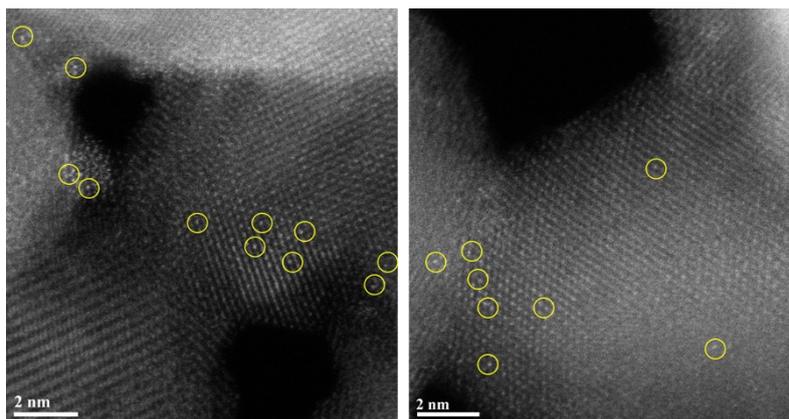


Figure S16. AC-HAADF-STEM images of the Pd/H-TiO₂ catalyst after the photothermal catalytic toluene.

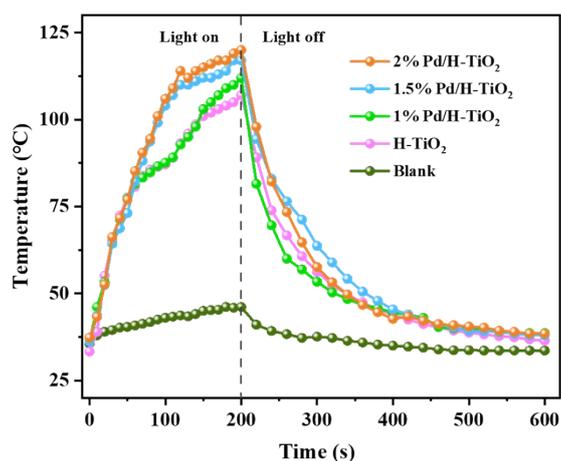


Figure S17. Surface temperature of the H-TiO₂ and Pd/H-TiO₂ samples under UV-Vis light irradiation measured by an infrared thermal imager.

The catalyst powder was loaded into a quartz reactor tube and irradiated by a 300 W xenon lamp at a lamp-to-sample distance of 10 cm. Then, the surface temperature was monitored using an infrared thermal imaging camera after turning on the xenon lamp.

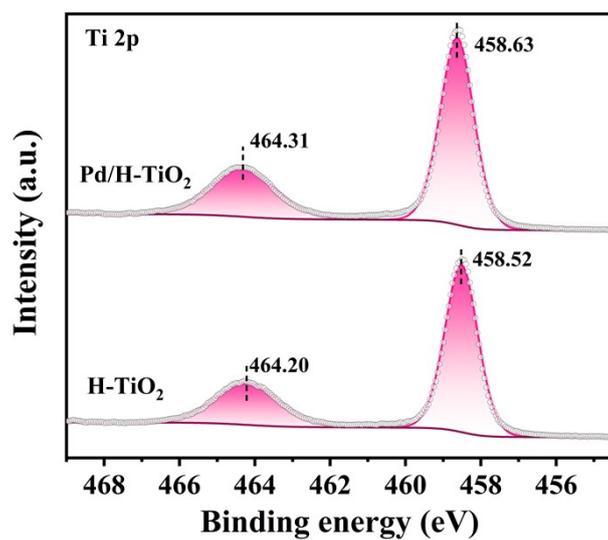


Figure S18. Ti 2p XPS spectra of H-TiO₂ and 2% Pd/H-TiO₂.

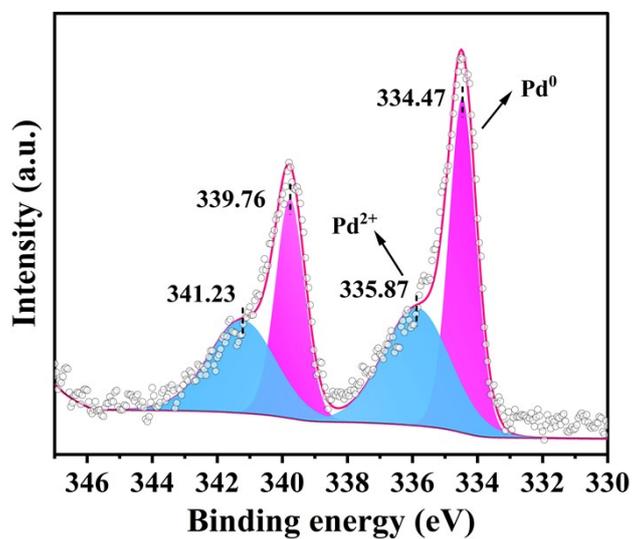


Figure S19. Pd 3d XPS spectra of 2% Pd/H-TiO₂.

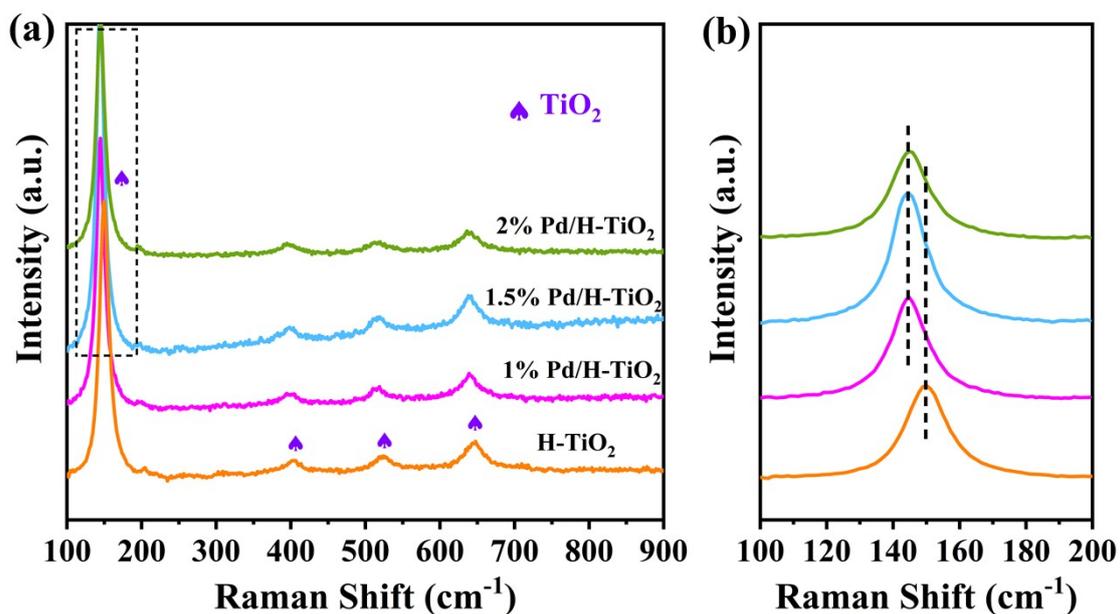


Figure S20. (a) Raman spectra of the H-TiO₂ and Pd/H-TiO₂ samples and (b) the enlarged spectra in the ranges of 100-200 cm⁻¹.

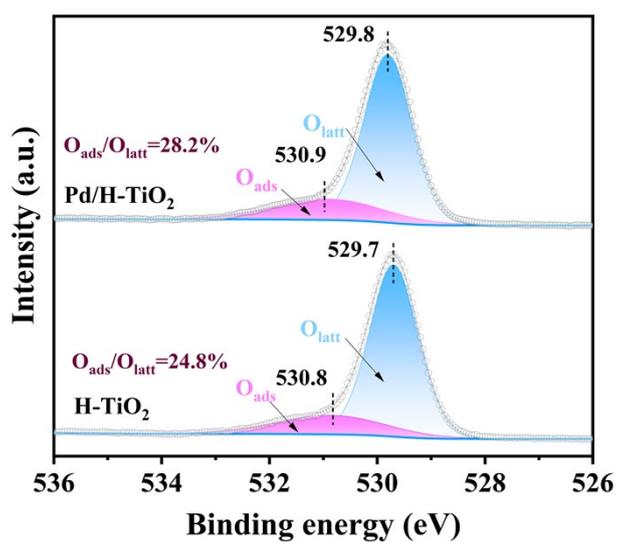


Figure S21. O 1s XPS spectra of the H-TiO₂ and Pd/H-TiO₂ catalysts.

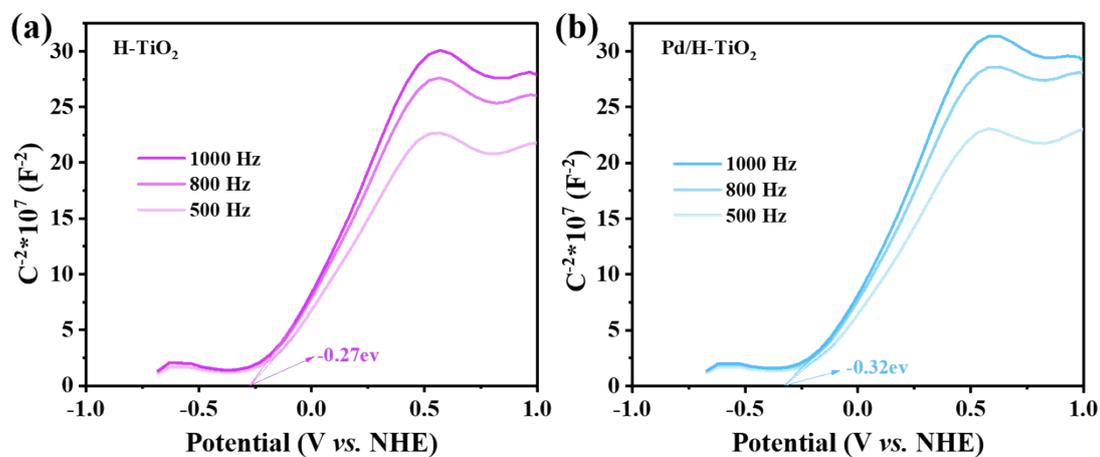


Figure S22. Mott-Schottky curves of (a) H-TiO₂ and (b) Pd/H-TiO₂ measured at 500, 800 and 1000 Hz.

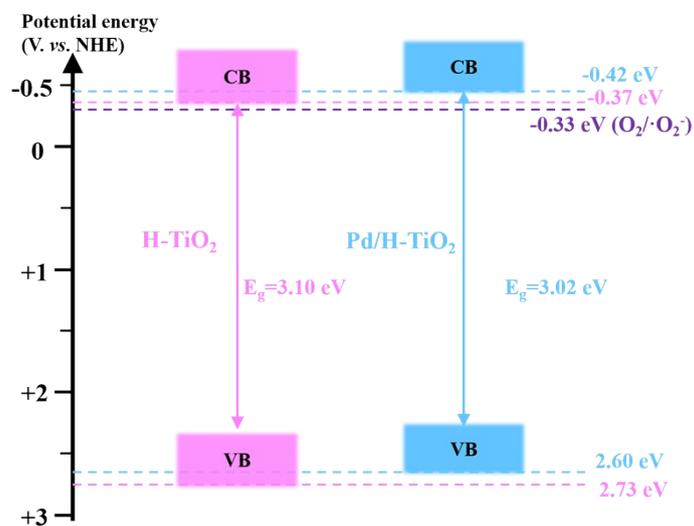


Figure S23. Band structure of H-TiO₂ and Pd/H-TiO₂.

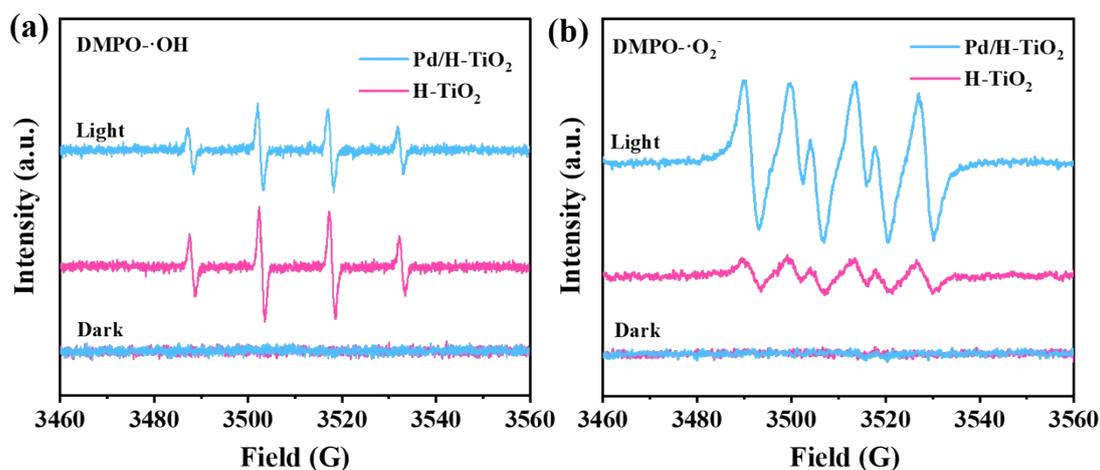


Figure S24. (a) DMPO-•OH and (b) DMPO-•O₂⁻ EPR spectra of H-TiO₂, Pd/H-TiO₂ in the dark and UV-Vis light irradiation.

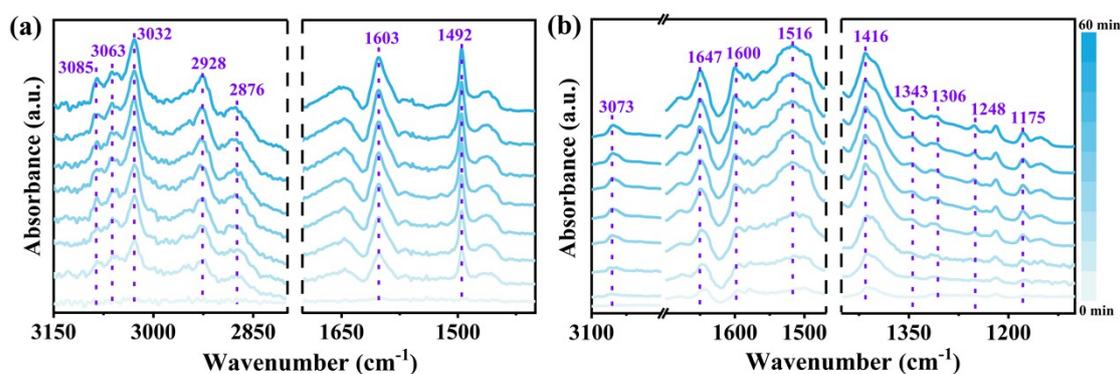


Figure S25. *In situ* DRIFT spectra of toluene adsorption (a) and oxidation (b) over Pd/H-TiO₂.

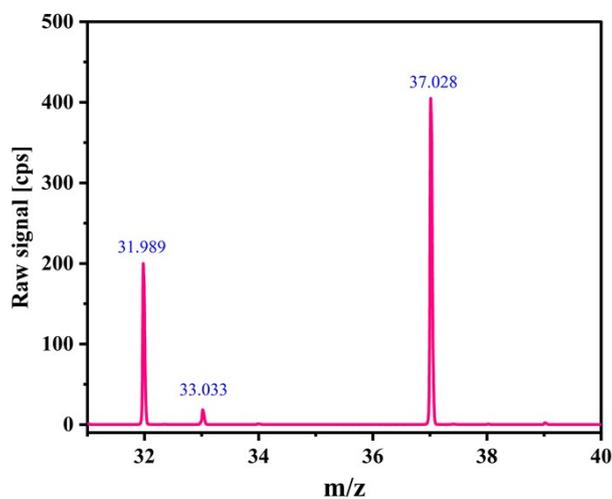


Figure S26. The possible intermediates during photothermal catalytic oxidation of toluene measured by PTR-ToF-MS.

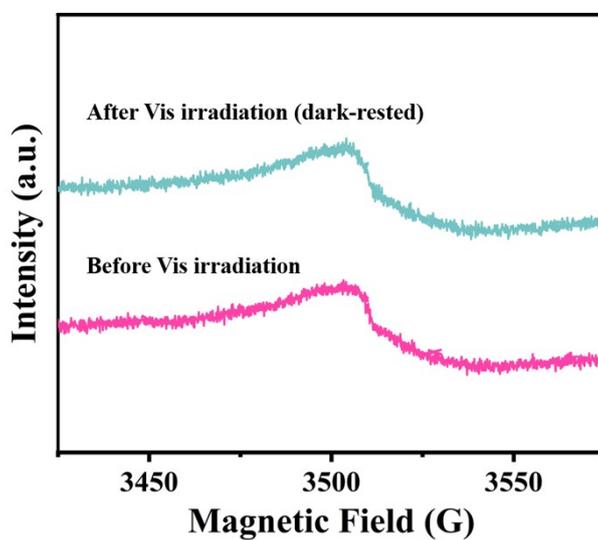


Figure S27. Solid-state EPR of Pd/H-TiO₂ before visible-light irradiation and after irradiation followed by resting in the dark for a certain period.

The reversibility of oxygen vacancies was examined by EPR spectra recorded for Pd/H-TiO₂ before visible-light irradiation and after irradiation followed by a period of

recovery in the dark (Figure S27). The results showed that the intensity of oxygen vacancies after vis light irradiation and subsequent dark storage recovered to its original level before irradiation, indicating the reversibility of the oxygen vacancies induced by vis light irradiation.

Table S1. Catalytic performance for toluene oxidation over various catalysts.

Catalyst	Toluene concentration (ppm)	GHSV (mL/g/h)	Temperature (°C)	Conversion	References
Pt/MO	200	30000	142	90%	3
0.7wt%Pd/0.4wt%Fe-TiO ₂	200	30000	165	90%	4
0.5wt%Pt/Fe ₂ O ₃	200	20000	190	90%	5
CoTi	200	30000	200	90%	6
Pt ₁ /CuO-CeO ₂	200	20000	186	90%	7
0.65Pt/Mn- TiO ₂	200	56250	197	90.4%	8
Pt-rGO-TiO ₂	930	31080	176	98%	9
ZMO-H	200	30000	158	93%	10
CeO ₂ /LaMnO ₃	200	31320	275	89%	11
La _{0.9} Fe _{0.1} MnO ₃	500	30000	183	86.7%	12
Pd/H-TiO ₂	200	32730	130	97%	This work

Table S2. Regressed reaction rate constants (k) and R^2 values for CO_2 mineralization over Pd/H-TiO₂ under UV and visible photothermal catalytic conditions.

Pd/H-TiO ₂	UV	Vis
K (10^{-3} min^{-1})	2.9	29.5
R^2	0.96	0.92

Table S3. Fitted parameters for time-resolved photoluminescence tests of H-TiO₂ and Pd/H-TiO₂.

Sample		Value/ps	A		Value/ μs	Rel%	Average value/ps
H-TiO ₂	τ_1	126.09	8.49	B ₁	25.06	17.95	215.09
	τ_2	11.33		B ₂	701.10	82.05	
Pd/H-TiO ₂	τ_1	151.43	10.14	B ₁	22.62	18.02	240.85
	τ_2	11.19		B ₂	621.56	81.98	

Reference

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