

Supporting Information For

Amorphous Fe²⁺-rich FeO_x loaded in mesoporous silica as a highly efficient heterogeneous Fenton catalyst

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Table S1.Pore structural parameters and Fe content of the prepared FeO_x/SBA -15 catalysts.

Samples	S _{BET} (m ² ·g ⁻¹)	d _{BJH} (nm)	Pore volume (cm ³ ·g ⁻¹)	Fe%
SBA-15	704.3	6.78	0.98	0
FeO _x /SBA-9h-450	472.5	6.19	0.82	8.344
FeO _x /SBA-17h-450	313.9	4.90	0.43	13.832
FeO _x /SBA-27h-450	296.9	4.43	0.36	14.217
FeO _x /SBA-36h-450	260.7	3.84	0.19	16.387
FeO _x /SBA-48h-450	240.6	3.79	0.16	16.938
FeO _x /SBA-17h-400	290.5	4.40	0.38	12.089
FeO _x /SBA-17h-500	418.7	5.87	0.63	13.762
FeO _x /SBA-17h-550	394.4	5.48	0.54	12.663
FeO _x /SBA-17h-600	349.9	4.99	0.48	15.484

Table S2.XPS of Fe 2p in FeO_x/SBA -15 catalysts

Samples	FeO _x /SBA-17h-400	FeO _x /SBA-17h-450	FeO _x /SBA-17h-500	FeO _x /SBA-17h-550	FeO _x /SBA-17h-600
Fe ²⁺ %	57.88	57.99	53.24	54.12	54.37
Fe ³⁺ %	42.1	42.01	46.76	45.88	45.64

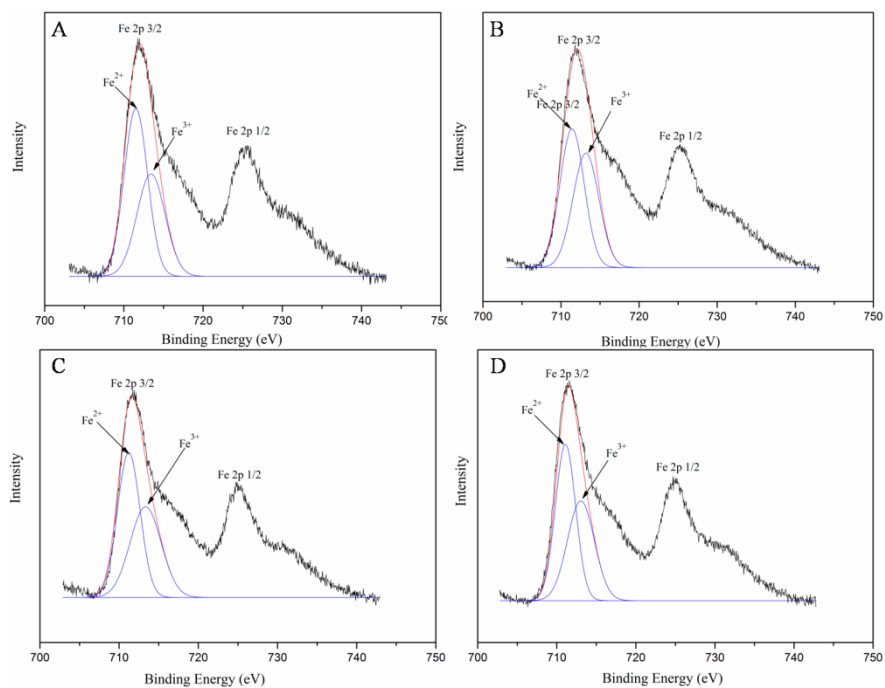


Fig. S1 XPS spectra of Fe 2p of FeO_x/SBA-17h-400 (A), FeO_x/SBA-17h-500 (B), FeO_x/SBA-17h-550 (C), FeO_x/SBA-17h-600 (D).

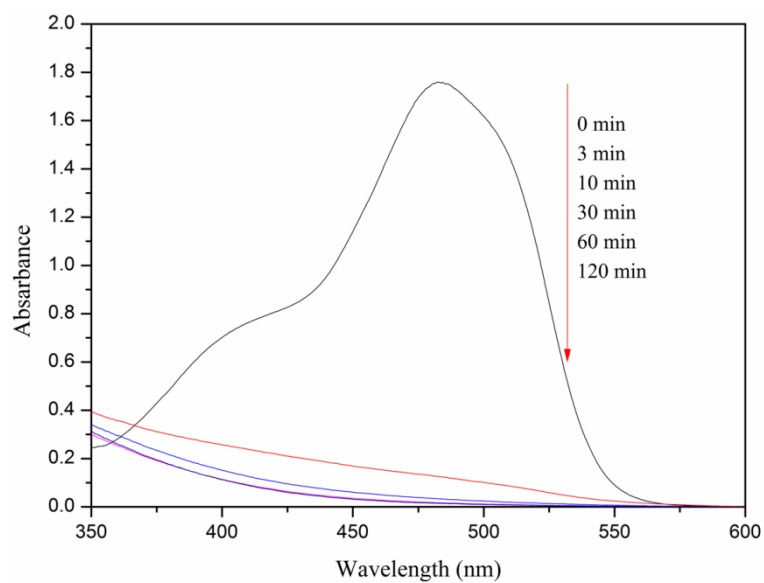


Fig. S2 UV-vis spectra changes of AO7 solution with reaction time ($\text{pH}_0 = 3$, $[\text{H}_2\text{O}_2] = 15 \text{ mM}$, and $[\text{FeO}_x/\text{SBA-17h-450}] = 0.6 \text{ g}\cdot\text{L}^{-1}$, $C_0 = 100 \text{ mg}\cdot\text{L}^{-1}$).

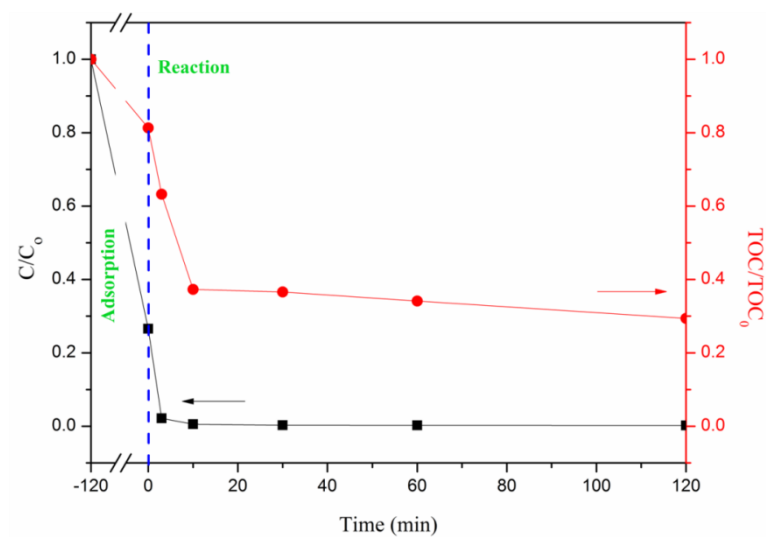


Fig. S3 Degradation efficiency and TOC removal of AO7 ($pH_0 = 3$, $[H_2O_2] = 15$ mM, $[FeO_x/SBA-17h-450] = 0.6$ g·L⁻¹, $C_0 = 100$ mg·L⁻¹).

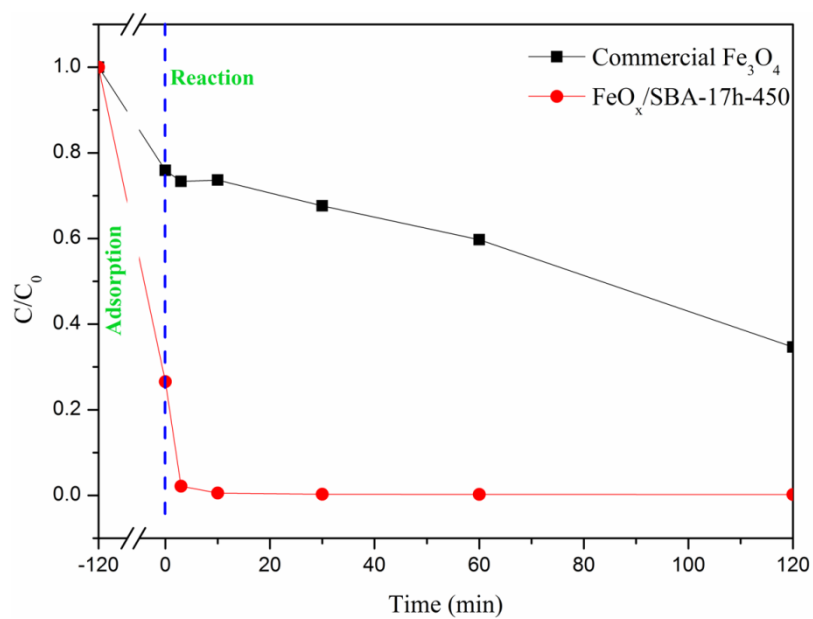


Fig. S4 Degradation efficiency of AO7 ($\text{pH}_0 = 3$, $[\text{H}_2\text{O}_2] = 15 \text{ mM}$, $[\text{FeO}_x/\text{SBA-17h-450}] = 0.6 \text{ g}\cdot\text{L}^{-1}$, $C_0 = 100 \text{ mg}\cdot\text{L}^{-1}$).

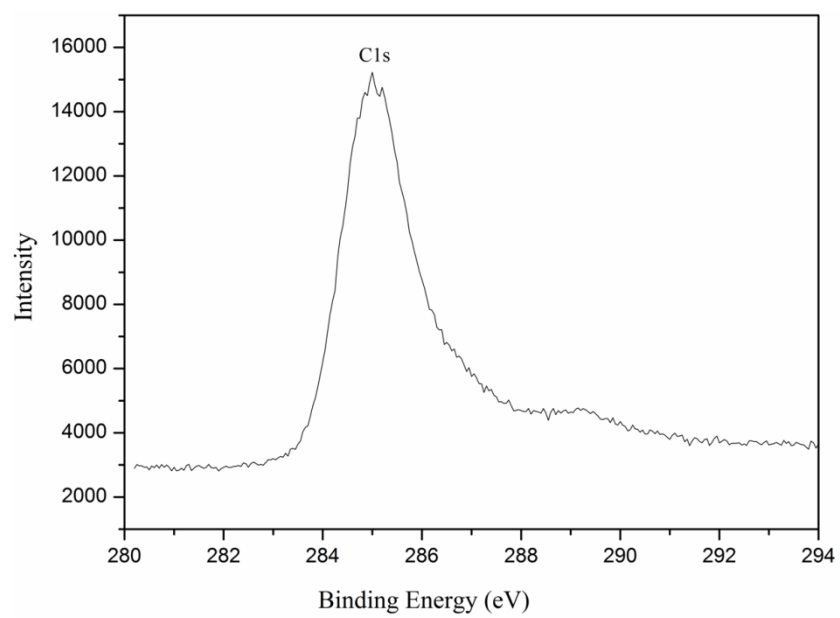


Fig. S5 XPS spectra of C1s of FeO_x/SBA-17h-450.

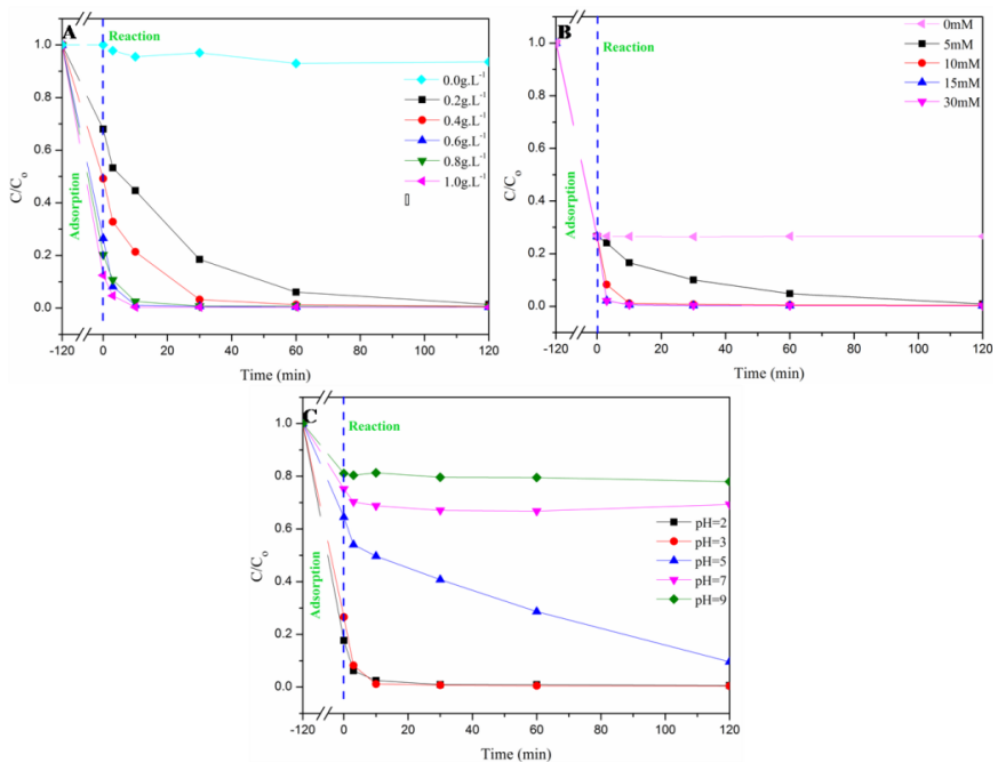


Fig. S6 A: Influence of catalyst dosage on the catalytic activity of sample FeO_x/SBA-17h-450 ([H₂O₂] = 10 mM, pH₀ = 3, C₀ = 100 mg·L⁻¹). B: Influence of H₂O₂ dosage on the catalytic activity of FeO_x/SBA-17h-450 ([FeO_x/SBA-15] = 0.6 g·L⁻¹, pH₀ = 3, C₀ = 100 mg·L⁻¹). C: Influence of initial pH value on the catalytic activity of FeO_x/SBA-15 (PVI duration time = 17 h, calcination temperature = 450 °C, [FeO_x/SBA-15] = 0.6 g·L⁻¹, [H₂O₂] = 10 mM, C₀ = 100 mg·L⁻¹).

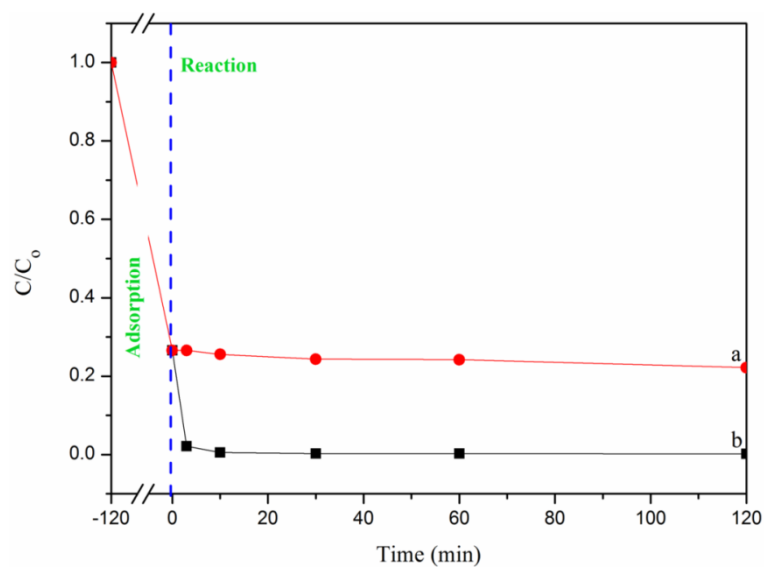


Fig. S7 Effect of HO• scavenger 2-propanol on the catalytic activity of FeOx/SBA-17h-450 ($[\text{FeO}_x/\text{SBA-17h-450}] = 0.6 \text{ g}\cdot\text{L}^{-1}$, $[\text{H}_2\text{O}_2] = 15 \text{ mM}$, $\text{pH}_0 = 3$, $C_0 = 100 \text{ mg}\cdot\text{L}^{-1}$, a: $C_{2\text{-propanol}}/C_{\text{AO7}}$ molar ratio = 400:1, b: $C_{2\text{-propanol}}/C_{\text{AO7}}$ molar ratio = 0).