

## Synthesis and characterization of three amino-functionalized metal-organic frameworks based on 2-Aminoterephthalic ligand

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### **SUPPORTING INFORMATION**

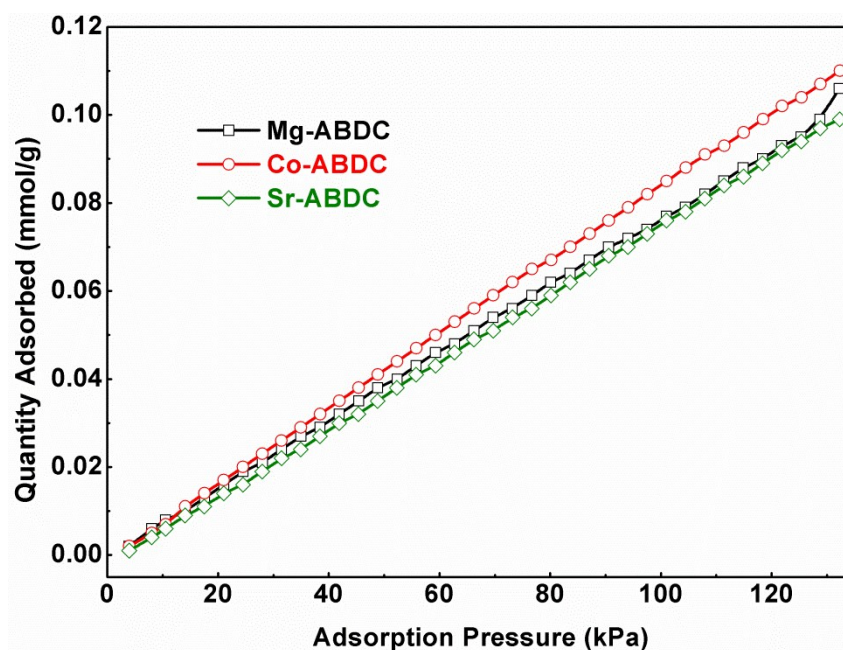


Fig. S1 N<sub>2</sub> adsorption at 25 °C on M-ABDC (M = Mg, Co, Sr)

Table S1 Langmuir constants of CO<sub>2</sub> and N<sub>2</sub> adsorption at 0 °C and selectivity of CO<sub>2</sub>/N<sub>2</sub> on M-ABDC<sup>a</sup>

Samples	CO <sub>2</sub>		N <sub>2</sub>		Selectivity of CO <sub>2</sub> /N <sub>2</sub>
	$q_{m1}$ (mmol/g)	$b_1$ (kPa <sup>-1</sup> )	$q_{m2}$ (mmol/g)	$b_1$ (kPa <sup>-1</sup> )	
Mg-ABDC	2.022	0.0151	17.24	4.47E-06	396
Co-ABDC	1.536	0.0179	13.14	6.41E-06	326
Sr-ABDC	285.53	4.66E-06	51.84	1.44E-06	18

<sup>a</sup> Langmuir equation:  $q = \frac{q_m b p}{1 + b p}$ ; The adsorption equilibrium selectivity:

$$S_{CO_2/N_2} = \frac{x_1}{x_2} \times \frac{y_1}{y_2} \approx \frac{q_{m1} b_1}{q_{m2} b_2}$$

## CO<sub>2</sub>/N<sub>2</sub> selectivity prediction via IAST

This method was following the procedures in the reporting references.<sup>1,2</sup> The experimental adsorption data for pure CO<sub>2</sub> and N<sub>2</sub> (measured at 0 °C) were fitted using a Langmuir-Freundlich (L-F) model:

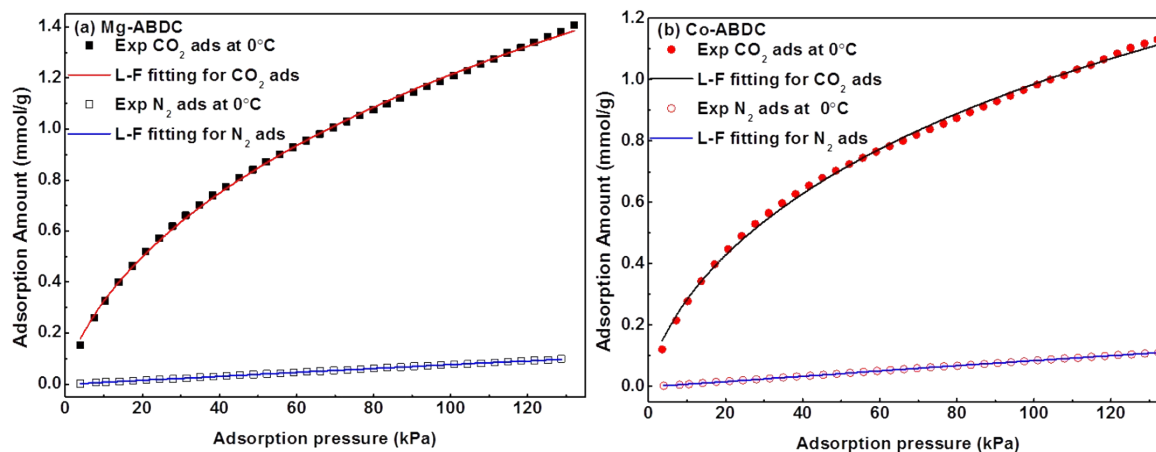
$$q_i = \frac{a \times b \times p_i^{1/n}}{1 + b \times p_i^{1/n}}$$

Where  $q_i$  adsorbed amounts at pressure and  $p_i$ .

The adsorption selectivities for binary mixtures of CO<sub>2</sub>/N<sub>2</sub> were calculated using the Ideal Adsorption Solution Theory (IAST), which was reported by Myers and Prausnitz.<sup>1</sup> And the selectivity was defined by:

$$S_{i/j} = \frac{x_i \times y_j}{x_j \times y_i}$$

Where  $x_i$  is the mole fraction of component i in the adsorbed phase and  $y_i$  is the mole fraction of component i in the bulk.

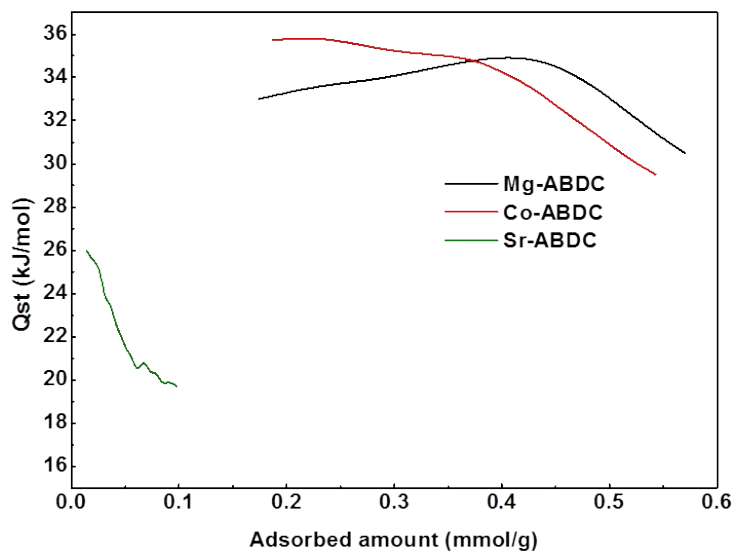


**Fig. S2** CO<sub>2</sub> and N<sub>2</sub> adsorption isotherms at 0 °C and fitting by L-F model

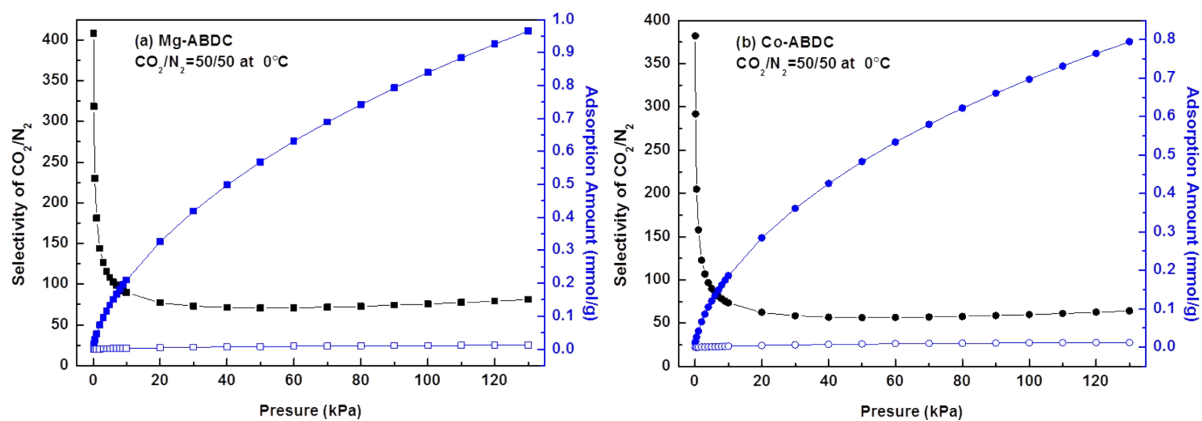
**Table S2** Fitting parameter of CO<sub>2</sub> and N<sub>2</sub> adsorption data by L-F model

L-F model fitting parameter		a	b	n	Chi <sup>2</sup>	R <sup>2</sup>
Mg-ABDC	CO <sub>2</sub> ads	4.33649	0.01709	1.47436	0.0001	0.99919
	N <sub>2</sub> ads	0.84485	0.00073	0.93764	2.0336E-7	0.99977
Co-ABDC	CO <sub>2</sub> ads	3.04922	0.02229	1.50271	0.00016	0.99795

N <sub>2</sub> ads	0.68623	0.00087	0.90620	1.3745E-7	0.99988
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**Fig. S3** Isothermic heats of CO<sub>2</sub> adsorption calculated by Clausius-Clapeyron equation based on adsorption isotherms at 0 °C and 25 °C



**Fig. S4** IAST adsorption isotherms of CO<sub>2</sub>+N<sub>2</sub> mixture at 50/50 and selectivities of Mg-ABDC and Co-ABDC



**Table S3** Comparison of the adsorption capacity and selectivity with some reported MOFs containing LBSs or/and OMSs

Material	Features	BET surface area (cm <sup>2</sup> /g)	CO <sub>2</sub> adsorbed amount (mmol/g)	Adsorption conditions	Selectivity of CO <sub>2</sub> /N <sub>2</sub>	References
Mg-ABDC	LBSs and OMSs	63	1.4	1.0 bar&298 K	>70 <sup>a</sup>	This work
Co-ABDC	LBSs and OMSs	71	1.1	1.0 bar&298 K	>55 <sup>a</sup>	This work
IRMOF-3	LBSs	2160	1.2	1.1 bar&298 K		<u>3</u>
Uio-66(Zr)-NH <sub>2</sub>	LBSs	1112	1.8	1.0 bar&303 K		<u>4</u>
[CuL <sub>4</sub> ]	LBSs	810	4.95	1.0 bar&298 K		<u>5</u>
NH <sub>2</sub> -MIL-53(Al)	LBSs and breathing		7.2	24 bar&283 K	12 <sup>c</sup>	<u>6</u>
CAU-1	LBSs	1268	7.2	1 bar&273 K	101 <sup>b</sup>	<u>7</u>
Cu-BTC	OMSs	1571	12.7	15 bar&298 K	5.1 <sup>b</sup>	<u>8</u>
Cu-BTC (hydrated 4 wt%)	OMSs	1492(Langmuir)	11.36	4.8 bar&298 K	28 <sup>a</sup>	<u>9</u>
Cu-TDPAT	LBSs and OMSs	1938	5.89	1.0 bar&298 K	~79 <sup>a</sup>	<u>10</u>
CuBTTri	OMSs	345	1.27	1.0 bar&298 K	25 <sup>c</sup>	<u>11</u>
mmen-CuBTTri	LBS	870	2.38	1.0 bar&298 K	327 <sup>a</sup>	<u>12</u>
Cu <sub>3</sub> (bte)[PCN-61]	OMSs	3350	21.4	20 bar&298 K	20 <sup>a</sup>	<u>13</u>
Cu <sub>3</sub> (tpbtm)	OMSs	3160	23.5	20 bar&298 K	33 <sup>a</sup>	<u>13</u>
Ni <sub>2</sub> (dhtp)	OMSs	1218	1.1	1.0 bar&298 K	7 <sup>c</sup>	<u>14</u>
ZTF-1	LBS	355.3	5.6	1.0 bar&273 K	10 <sup>c</sup>	<u>15</u>
Cd-ANIC-1	LBS	329.3	4.72	1.0 bar&273 K		<u>16</u>
Co-ANIC-1	LBS	274.0	4.22	1.0 bar&273 K		<u>16</u>

Selectivity calculation: a, from IAST; b, from slopes of adsorption isotherms at low pressure; c,  $S=q_1/q_2$  (where component 1 is more adsorbed).

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