Electronic Supplementary Information (ESI)

The discharge rate capability of rechargeable Li-O₂ batteries

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1. Rate capability - specific capacity normalized by discharged electrode weight

The discharged electrode weight (carbon + catalyst + binder + **discharge products**) was used to normalize the discharge capacity of all Li-O₂ cells **assuming that all the charge is associated** with Li_2O_2 formation. The mass of Li_2O_2 formed for each cell was obtained by converting the discharge capacity (C) to the weight of Li_2O_2 via the following equation

weight of
$$\text{Li}_2\text{O}_2$$
 (g) = $\frac{\text{M.W.}_{\text{Li}2\text{O}2} \text{ (g/mol)} \cdot \text{discharge capacity (C)}}{\text{n} \cdot \text{F}(\text{C/mol})}$

, where M.W.Li₂O₂ is the molecular weight of Li₂O₂ (45.882 g/mol), n is the numbers of electron transferred of discharge reaction assuming final product as Li₂O₂ (n = 2), F is Faraday constant (96485 C/mol).



Fig. S1 Discharge profiles of Li-O₂ single cells of pure Vulcan (a)-(e) and Au/C. The discharge rate is 100 mA/g_{carbon} for (a) and (f), 250 mA/g_{carbon} for (b) and (g), 500 mA/g_{carbon} for (c) and (h), 1000 mA/g_{carbon} for (d) and (i), and 2000 mA/g_{carbon} for (e) and (j).

2. Transport properties estimation in selected electrolytes

Symbols:
D: Diffusion coefficient
t: Transference number
η: viscosity of solvent
T: temperature
Co: solubility of oxygen
α: Bunsen coefficient of Oxygen in the electrolyte

Stokes-Einstein diffusion equation

 $D = \frac{k_B T}{6\pi\eta a}$ where the hydrodynamic radius a = 121 pm for oxygen

Ionic diffusion equation

$$D_{Li^+} = \frac{\sigma_{Li^+} RT}{z^2 F^2 [Li^+]} t_{Li^+}$$
 where z = 1 for lithium cations

For the binary ionic salts used in lithium-based electrolytes, lithium ion transference number is calculated as follows:

$$t_{Li^+} = \frac{D_{Li^+}}{D_{Li^+} + D_-}$$

- 1) Species transport in 0.1 M Li⁺ in pure DME
 - Oxygen diffusion coefficient^{1, 2}
 - $\eta = 4.5 \cdot 10^{-4} Pa / s \Longrightarrow D_{O_2} \approx 4.0 \cdot 10^{-5} cm^2 s^{-1}$
 - Solubility of Oxygen³ $\alpha_{DME} = 0.2143L_{O_2} / L_{DME} \Longrightarrow C_o = 0.00876M$
 - Lithium transference number⁴ In 0.1 M LiCF₃SO₃/DME, $D_{Li^+} \approx D_{CF_3SO_3^-} \approx 13.3 \cdot 10^{-6} cm^2 s^{-1} \Longrightarrow t_{Li^+} \approx 0.5$

This calculated value of transference number agrees well with the value of 0.43 reported in 0.01 M LiClO4 in PC/DME by Makoto et al.⁵

- Lithium diffusion^{4, 2} In 0.1 M LiCF₃SO₃/DME, $D_{Li^+} \approx 13.3 \cdot 10^{-6} cm^2 s^{-1}$ $D_{Ii^+} \approx 7.3 \cdot 10^{-6} cm^2 s^{-1}$ in ~0.5 M LiTFSI/DME at 30°C
- 2) Species transport in 1 M in PC/DME (1:2)
 - Oxygen diffusion coefficient $\eta = 1.98 \cdot 10^{-3} Pa / s \Longrightarrow D_{O_2} \approx 9 \cdot 10^{-6} cm^2 s^{-1}$

- Solubility of Oxygen³ $\alpha_{PC/DME} = 0.0998L_{O_2} / L_{PC/DME} \Longrightarrow C_o = 0.0041M$
- Lithium transference number²

A mixture of PC and DME (1:2) by volume corresponds to a molar ratio of ~40% PC in DME. This value is used to read needed data in fig. 2 of the work of Hayamizu et al.

In ~0.5 M LiTFSI/DME, $D_{Li^+} \approx 5 \cdot 10^{-6} cm^2 s^{-1}$, $D_{TFSI} \approx 6.5 \cdot 10^{-6} cm^2 s^{-1} \Rightarrow t_{Li^+} \approx 0.43$ As a first order approximation, the lithium transference number is assumed to vary very little from 0.5 M to 1 M Li⁺ in PC/DME.

• Lithium diffusion⁶

By approximating the transference number of lithium in PC/DME to 0.4, the diffusion coefficient of lithium is calculated from data provided by Yoshio et al.⁶

In 1 M LiBF4 in PC/DME (1:2), $\sigma \approx 7.2 \cdot 10^{-3} S \cdot cm^{-1} \Longrightarrow D_{L^+} \approx 7.7 \cdot 10^{-7} cm^2 s^{-1}$

- 3) Species Transport in 1 M in pure PC
 - Oxygen diffusion coefficient³ $\eta = 8.06 \cdot 10^{-3} Pa / s \Longrightarrow D_{o_s} \approx 2.2 \cdot 10^{-6} cm^2 s^{-1}$
 - Solubility of Oxygen³ $\alpha_{PC} = 0.0516L_{Q_2} / L_{PC} \Longrightarrow C_q = 0.0021M$
 - Lithium transference number²

In ~0.5 M LiTFSI/PC, $D_{Li^+} \approx 1.6 \cdot 10^{-6} cm^2 s^{-1}$, $D_{TFSI} \approx 2.8 \cdot 10^{-6} cm^2 s^{-1} \Rightarrow t_{Li^+} \approx 0.35$ As a first order approximation, the lithium transference number is assumed to be fixed from 0.5 M to 1 M Li⁺ in PC.

• Lithium diffusion⁶

By approximating the transference number of lithium in pure PC to 0.35, the diffusion coefficient of lithium is calculated from data provided by Yoshio et al.

In 1 M liBF₄/PC, $\sigma \approx 2.8 \cdot 10^{-3} S \cdot cm^{-1} \Longrightarrow D_{U^+} \approx 3 \cdot 10^{-7} cm^2 s^{-1}$

3. Transport characteristics in the O₂ electrodes used in our experiments

3-a. Limiting fluxes of O₂ and Li⁺ within the porous cathode in 0.1 M Li⁺ DME electrolyte

Symbols:

J: Flux of the species D = Diffusion coefficient of the species $C(x), C_0$: Concentration and soluble concentration of species in the media n: Number of Electron transferred j: Electrode-area normalized current density D_{eff} : Effective diffusion coefficient in the flooded-porous electrode β_{O2} : Bruggeman constant of oxygen in the porous cathode

$$J_{\text{lim}} = D \cdot \varepsilon^{\beta - 1} \cdot \frac{C_o}{t}$$
 where β is equal to 3 for oxygen and 2.5 for Li⁺.⁷

$$J_{\lim_{O_2}} = (4 \cdot 10^{-5} \, cm^2 \, / \, s) \cdot (0.73)^{3-1} \cdot \frac{0.00876 \cdot 10^{-3} \, mol_{O_2} \, / \, cm^3}{20 \cdot 10^{-4} \, cm} \approx 9 \cdot 10^{-8} \, mol \cdot cm^{-2} \cdot s^{-1}$$

$$J_{\lim_{L^{+}}} = (10 \cdot 10^{-6} \, cm^2 \, / \, s) \cdot (0.73)^{2.5-1} \cdot \frac{0.1 \cdot 10^{-3} \, mol_{O_2} \, / \, cm^3}{20 \cdot 10^{-4} \, cm} \approx 3 \cdot 10^{-7} \, mol \cdot cm^{-2} \cdot s^{-1}$$

In the calculation of limiting flux of Li^+ , an average value of the reported diffusion coefficients is used. The diffusion coefficient values vary from $7*10^{-6} \text{ cm}^2 \text{.s}^{-1}$ to $13*10^{-6} \text{ cm}^2 \text{.s}^{-1}$ depending on the lithium salt in the electrolyte as exemplified in ESI section 2.

3-b. Concentration of O₂ in the flooded electrode: simplified model



The arrow indicates the distance into the electrode

The Bruggeman relation applied to the diffusion of oxygen in the porous, flooded oxygen electrode states⁷,

$$D_{eff} = D \cdot \varepsilon^{\beta_{O_2} - 1}$$
 with $\beta_{O_2} = 3$

A combination of Fick's diffusion law and electrochemical conversion of oxygen yields the following equation for the O_2 -concentration from the entrance of the porous electrode (x=0) to the electrode/separator interface (x = L).

$$C(x) = C_o \exp\left(-x\sqrt{\frac{k}{D_{eff}}}\right)$$

$$J = -D\frac{\partial C(x)}{\partial x} \Longrightarrow J(x=0) = C_o \sqrt{kD_{eff}}$$

$$J = \frac{j}{nF}$$

$$k = \frac{j^2}{n^2 F^2 C_o^2 D_{eff}}$$

$$\frac{C(x)}{C_o} = \exp\left(-x\frac{j}{nFC_o D_{eff}}\right)$$

$$2Li^+ + 2e^- + O_2 \rightleftharpoons Li_2 O_2 \Longrightarrow n = 2$$

3-c. Oxygen consumption at the O₂ electrode

$$2Li^{+} + 2e^{-} + O_{2} \rightleftharpoons Li_{2}O_{2} \Longrightarrow n = 2$$

$$M_{O_{2}} = 32g_{O_{2}} / mol_{O_{2}}$$

$$C(mol_{O_{2}} / mAh) = \frac{1}{2(\frac{mol_{e^{-}}}{mol_{O_{2}}})F(\frac{C}{mol_{e^{-}}})} (3.6 C/mAh) = 1.9 \cdot 10^{-5} mol_{O_{2}} / mAh$$

Assuming Oxygen is an ideal gas at 1atm and 25°C during the cell testing,

$$\overline{V_{O_2}}(L/mol_{O_2}) = 22.465L/mol_{O_2}$$

Henceforth,

$$\overline{C}(mL_{O_{\gamma}} / mAh) = 0.419mL_{O_{\gamma}} / mAh$$

The maximum capacities achieved for the cells in the present publication is \sim 3500 mAh/g_{carbon} for an average carbon content of 0.5 mg in all electrodes. This corresponds to a maximum total

discharge of 1.75 mAh and 0.73 mL of oxygen consumed. Consequently, all cells tested contained at least 340 times more oxygen than required (250 mL oxygen tank); the pressure drop from oxygen consumption by the cell was negligible.



4. Li-K edge X-ray absorption near edge structure spectra of reference compounds

Fig S2 Li K edge XANES spectra of reference compounds: Li-Nafion, Li₂CO₃, LiOH, and LiClO₄.

Reference:

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