1	Supplementary Information for:
2	Chain elongation with reactor microbiomes: upgrading dilute ethanol to
3	medium-chain carboxylates
4 5	Matthew T. Agler <sup>1</sup> , Catherine M. Spirito <sup>1</sup> , Joseph G. Usack <sup>1</sup> , Jeffrey J. Werner <sup>1,2</sup> , and Largus T. Angenent <sup>1</sup> *
6	<sup>1</sup> Department of Biological and Environmental Engineering, 214 Riley-Robb Hall, Cornell
7	University, Ithaca NY 14853, USA.
8	<sup>2</sup> Chemistry Department, SUNY Cortland, Bowers Hall, PO Box 2000, Cortland, NY 13045,
9	USA.
10	*Correspondence to: <u>la249@cornell.edu</u>
11	
12	Supplementary Information:
13	Results and Discussion
14	Materials and Methods
15	Figures S1-S5
16	Tables S1-S3
17	
18	Results and Discussion: Linking the 16S rRNA gene and shotgun metagenomic sequencing
19	surveys. Our analysis of the 16S rRNA gene sequencing effort found five abundant OTUs that
20	were significantly correlated (r > 0.8 and p < 0.05) with increasing <i>n</i> -caproic acid production
21	rates (Figure 2A and Table S1). The OTUs were of various taxonomies, indicating that a range
22	of bacteria played important roles in conversion of yeast-fermentation beer to <i>n</i> -caproic acid. To
23	more specifically determine the roles of the OTUs, and to provide more certainty as to which
24	bacteria were responsible for chain elongation, we performed a shotgun metagenomic
25	sequencing analysis of bioreactor samples. Taxonomic analysis of the seven genes most
26	significantly correlated with production rates of n-caproic acid (Figure S4) suggested the
27	importance of some of the same taxonomic groups as the 16S rRNA gene sequencing analysis

(genus *Clostridium* and family Ruminococcaceae). Seven genera made up most of the reads
assigned to the seven genes, and four of those (*Ethanoligenens* [family Ruminococcaceae],

30 Desulfitobacterium, Clostridium, and Propionibacterium) increased as n-caproic acid production 31 rates increased. To determine the probable roles of the 7 important genera, we looked at the 32 taxonomic breakdown of genes catalyzing what are likely to be the most important carbon 33 metabolism pathways in the bioreactor (Figure S3). Compared to the taxonomic breakdown of 34 all reads, *Ethanoligenens* and *Bifidobacterium* were relatively abundant in starch hydrolysis and 35 xylan metabolism, respectively, indicating that they may have been important in retrieving 36 carbon from complex substrate molecules. Clostridium spp. strongly dominated the chain-37 elongation gene pool, reflecting their important role in the terminal process for *n*-caproic acid 38 formation. Even though a chain-elongating bacterium, such as C. kluyveri, can oxidize ethanol 39 on its own, *Desulfitobacterium* was apparently a catalyst for this important step. We have not 40 clarified if they provided: i. reducing equivalents from ethanol to some chain-elongating 41 bacterium in a mutualistic relationship; ii. hydrogen to hydrogenotrophic methanogens (although 42 their large abundance and the relatively small flux of carbon to methane would indicate that it 43 should have had some other role as well); or iii. a drain of reducing equivalents from our system 44 to another electron acceptor, such as organic material or sulfate (we did not find H<sub>2</sub>S in biogas 45 analysis, though). The first option seems the most likely participation and more research is 46 necessary to substantiate.

47

48 Materials and Methods: Bioreactor Setup and Operation. We operated a 5-L glass bioreactor 49 for over a year to convert yeast fermentation beer to *n*-caproic acid (Figure 1 and Figure S1). 50 The yeast fermentation beer was received in one shipment from Western New York Energy in 51 Medina, NY. The raw, undiluted beer had a total and volatile solids content of  $125.73 \pm 0.14$  g  $L^{-1}$  (n = 6) and 117.19 ± 0.15 g  $L^{-1}$  (n = 6), respectively, a chemical oxygen demand (COD) of 52  $450.50 \pm 51.12$  g L<sup>-1</sup> (n = 6), and the ethanol content was  $152.7 \pm 3.4$  g L<sup>-1</sup> (~15%) (n = 4). We 53 54 diluted the beer 6.6 times before feeding to the bioreactor; in a real industrial setup, recycled 55 liquor would have been used instead of make-up water. The bioreactor included a heated water 56 jacket connected to a water heater to maintain a temperature of 30°C, an hourly automatic mixing 57 system that worked by recirculating biogas with a peristaltic pump, and an automated pH control 58 system, which pumped 5M NaOH or HCl during mixing to maintain a pH of 5.5 (range 5.4-5.6). 59 To prevent under pressure in the bioreactor during effluent withdrawal and feeding, the 60 headspace was connected to a device that equalized pressure with the room while preventing air

61 intrusion. We fed the bioreactor semi-continuously on a 48-hour schedule: substrate was first 62 fed into the bioreactor (time 0), followed by a react period with pH control, hourly mixing, and 63 continuous *n*-caproic acid extraction (hours 0-47), followed by a 1-h biomass settling period 64 (hour 47), and rapid effluent removal of a volume equal to substrate volume with a peristaltic 65 pump (time 0). We maintained a hydraulic retention time (HRT) of 15 days (666 mL of substrate fed per cycle to the 5-L bioreactor) and a substrate organic loading rate of 4.5 g COD 66  $L^{-1} d^{-1}$  (ethanol loading rate: 66.6 mmol C  $L^{-1} d^{-1}$ ) through day 120. By day 120, chain-67 68 elongation reactions consumed nearly all available ethanol in the substrate (Figure S5), and 69 therefore we decreased the HRT to 12 days (833 mL of substrate per cycle for the 5-L bioreactor). resulting in a higher substrate loading rate of 5.7 g COD  $L^{-1} d^{-1}$  (ethanol loading rate: 70 83.3 mmol C  $L^{-1} d^{-1}$ ) for the remainder of the operating period. The bioreactor was inoculated 71 72 from previously operating bioreactors optimized for *n*-butyric acid production from dilute-acid 73 pretreated corn fiber. Originally the *n*-butyric acid-producing bioreactor was started with a 74 natural microbiome from sheep rumen and a thermophilic anaerobic digester from the city of 75 Duluth, Minnesota (Western Lake Superior Sanitary District, Duluth, MN). For the first 30 days 76 of the current study, the bioreactor was fed dilute-acid pretreated corn fiber, which was supplemented with ethanol at an HRT of 15 days and a loading rate of 1.7 g COD  $L^{-1} d^{-1}$  (ethanol 77 loading rate: 32.6 mmol C L<sup>-1</sup> d<sup>-1</sup>). 78

79

80 In-line Liquid/Liquid n-Caproic Acid Extraction. To prevent product inhibition and to recover 81 the product, we continuously extracted *n*-caproic acid using a membrane-based liquid/liquid 82 extraction system (Figure 1). The extraction system consisted of hollow-fiber hydrophobic 83 membrane contactors that allowed a high surface area for contact between the aqueous and 84 solvent phases. We used eight commercially available hydrophobic membranes with a contact area of 2.32  $m^2$  for both the bioreactor/solvent and solvent/stripping interfaces (four on each 85 86 side) (1.5x5.5 MiniModule X50, Liqui-Cel, Membrana, Wuppertal, Germany). On day 300, we 87 increased the membrane contact area for both the bioreactor/solvent and solvent/stripping interfaces to 8.1 m<sup>2</sup> to avoid limitations due to rate of product extraction (4x13 316L SS X50, 88 89 Liqui-Cel, Membrana). Indeed, until the end of the study the substrate-feeding rate was limiting 90 the production rate and not the extraction rate. The driving force for the extraction was two-fold: 91 1. We used a reactive solvent (3% tri-*n*-octylphosphineoxide in mineral oil, Sigma-Aldrich, St.

Louis, MO), which is more selective for hydrophobic molecules, such as *n*-caproic acid, 92 compared to shorter-chain molecules, such as acetic acid<sup>1</sup>; and 2. We maintained a pH gradient 93 to take advantage of the dissociation constant for *n*-carboxylic acids ( $pK_a = 4.8-4.9$ ) to 94 95 selectively extract undissociated acids from the bioreactor at pH 5.5 and recover them in the 96 dissociated form in a pH 9 aqueous solution. First, the bioreactor supernatant was pumped into 97 the lumen side (inside the fibers) of the hollow-fiber membrane units at 10 mL/min after being 98 filtered to remove remaining large particles (as much of the particles as possible were returned to 99 the bioreactor on a weekly basis). The solvent, which wet the hydrophobic membranes, was 100 pumped at the same rate on the shell side (outside the fibers) of the membrane, counter-flow to 101 the bioreactor liquid. The solvent was constantly recirculated between contact with the 102 bioreactor liquid and the shell side of a second membrane unit, where it contacted an aqueous 103 phase buffered with a 0.5 M borate solution at pH 9. The pH 9 solution was continuously 104 recirculated from a 5-L reservoir where a pH controller maintained the pH by automatic addition 105 of 5M NaOH.

106

107 Methanogenic Activity Test. We operated 35-mL batch fermentation vessels in 93-h 108 fermentations to test whether bioreactor microbiomes produced methane from acetic acid or only 109 from carbon dioxide with hydrogen or ethanol as the source of reducing equivalents (electrons). 110 All batch reactions were carried out in triplicate. Four triplicate sets of batch bottles were 111 prepared (no source of electrons for methanogens). In short, in an anaerobic hood, we added 0.75 mL basal medium (described in Agler et al. <sup>2</sup>), ~8 mmol  $g^{-1}$  VS acetic acid, ~4 mmol  $g^{-1}$  VS 112 113 *n*-butyric acid, and 100 mM 2-(*N*-morpholino)ethanesulfonic acid (MES) buffer to a total 114 volume of 7.25 mL, added 0.25-mL inoculum and 0.1-mL sodium sulfide, corrected to pH 5.5 at 115 30°C with NaOH (total volume ~10 mL), capped the bottles with butyl rubber stoppers and 116 crimp caps, and flushed each bottle with nitrogen for 10 min (set A). To set B, we also added ~10 mmol g<sup>-1</sup> VS carbon dioxide and hydrogen; to set C, we added ~6 mmol g<sup>-1</sup> VS ethanol; and 117 to set **D**, we added ~ 10 mmol  $g^{-1}$  VS carbon dioxide and hydrogen and ~6 mmol  $g^{-1}$  VS ethanol. 118 119 The inoculum was collected from the well-mixed bioreactor before the substrate was changed 120 from dilute-acid pretreated corn fiber to yeast fermentation beer on day 30. We periodically 121 measured the headspace pressure in the batch bottles and analyzed headspace gas for methane, 122 carbon dioxide, and hydrogen. We measured the liquid substrates and the products ethanol,

123 acetic acid, and *n*-butyric acid at the time of inoculation and at the end of 93 h. At the end of the 124 run, we measured the volatile solids (VS) concentration in each bottle to normalize the 125 measurements for the amount of biomass in each batch bottle.

126

127 Chemical Analysis. We performed all chemical analyses on a regular schedule. At the end of 128 each 48-h feeding cycle we measured the biogas production and recorded the temperature and 129 pressure to standardize the measurements. Biogas composition was measured weekly. For 130 hydrogen composition, we used a Gow-Mac Series 580 GC (Gow-Mac Instrument Co, 131 Bethlehem, PA) with a 5' x 1/4" stainless column packed with 60/80 Carboxen 1000 packing 132 material (Supelco, Sigma-Aldrich, St. Louis, MO). The temperature of the column, injector, and 133 detector were 100°C, 110°C, and 105°C, respectively, and the current to the TCD detector was 70 134 mA. Carbon dioxide and methane were measured with an SRI 8610C GC with a 1m x 1/4" Rt-135 XLSulfur column (Restek, Corp, Bellefonte, PA). The temperature of the column, injector, and 136 detector were 40°C, 25°C, and 101°C, respectively, and the current was 167 mA. We determined 137 the composition of the effluent and the stripping solution by measuring the individual carboxylic 138 acids and ethanol concentration after every feeding cycle. Individual carboxylic acids were 139 measured with an HP 5890 Series II GC (Hewlett-Packard, Palo Alto, CA) equipped with an 140 autosampler with a 15m x 0.53mm Nukol column. Ethanol was measured with the same GC setup and a Supelco 6' 1/4" x 2mm glass column packed with 10% CW-20M (treated with 0.01% 141 142 H3PO4) on 80/100 Chromasorb WAW support.

143

144 Genomic DNA (gDNA) extraction. We collected biomass by first mixing the bioreactors well 145 for 5 min and sampling ~50 mL. We rapidly transferred three aliquots of sample to 2-mL vials 146 and centrifuged at 10,000 rpm for 10 min, disposed of the supernatant, then froze them 147 immediately at -80°C until further analysis. We extracted genomic DNA (gDNA) from ~200 mg 148 of biomass using the MoBio PowerSoil 96-well gDNA isolation kit (MoBio Labs, Inc, Carlsbad, 149 CA), according to the MoBio protocol, except that cell lysis was performed by beadbeating.

150

151 *16S rRNA Gene Sequencing and Data Analysis.* To amplify 16S rRNA genes, PCR was
152 carried out in triplicate for each sample and for water blanks. The PCR mastermix included 2.5
153 U Agilent Easy-A High Fidelity PCR Cloning Enzyme, 5 µl of 10X Easy-A reaction buffer

154 (Agilent Technologies, Inc., Santa Clara, CA), and 1µL each of 10 µM forward and reverse 155 primers and 1 µL of 10mM dNTP. The forward primer combined the 454 primer 'B' and the 156 universal bacterial primer 8F: 5'-157 GCCTTGCCAGCCCGCTCAGTCAGAGTTTGATCCTGGCTCAG-3'. The reverse primer 158 was a concatenation of the 454 primer 'A', followed by a barcode, unique for each sample, 159 followed 5'by the universal bacterial primer 338R: 160 GCCTCCCTCGCGCCATCAGXXXXXXXXXXXXXCATGCTGCCTCCCGTAGGAGT-3'. On 161 each 96-well PCR plate we included negatives composed of randomly selected reverse primers 162 and no template. Triplicates were pooled with the Mag-Bind EZ Pure magnetic purification kit 163 (Omega Bio-Tek, Norcross, GA), and were eluted into 40 ul TE buffer according to the 164 manufacturer's instructions. Pooled triplicates were run on a 1% agarose gel to verify the 165 product. All negatives had no visible band and were not analyzed further. The concentration of 166 dsDNA in each pooled triplicate was measured via fluourometric analysis with the PicoGreen 167 dsDNA quantitation kit (Invitrogen Corp, Carlsbad, CA). The samples were pooled in equimolar amounts into a single sample with a final concentration 8.88 ng  $\mu$ l<sup>-1</sup> dsDNA. Sequencing was 168 169 performed on the Roche 454 pyrosequencing platform using Titanium chemistry and beginning 170 sequencing at 454 adaptor A (Engencore, Columbia, SC).

We used the QIIME 1.4.0 pipeline  $^{3}$  for sequence denoising, quality filtering, processing, 171 172 and data analysis. Our efforts resulted in on average 5,875 high-quality 16S rRNA gene 173 sequences per sample from which we picked and assigned taxonomy to 839 operational 174 taxonomic units (OTUs; 97% ID). We determined OTUs whose relative abundance (i.e. the 175 fraction of all sequence reads assigned to a specific OTU) was correlated to the *n*-caproic acid 176 production rate with a correlation coefficient (r) of at least 0.8 and significance of correlation (p-177 value) < 0.05 (Table S1). We plotted the relative abundance vs. time for five of these OTUs that 178 had a relative abundance by day 90 of at least 0.05 (Figure 2A). To determine how diverse the 179 microbiome OTUs were, we calculated the phylogenetic diversity and the Gini coefficient and 180 plotted both vs. time (Figure 2B). Phylogenetic diversity is a measure of the OTU diversity 181 where higher numbers represent a more diverse sample. It uses the whole-sample phylogenetic 182 tree to take into consideration the phylogenetic relatedness of OTUs. The Gini coefficient is a 183 measure of microbiome evenness, where for a Gini coefficient of 0 (perfectly even) sequences 184 are perfectly distributed between all OTUs, and 1 (perfectly uneven) would indicate that all

185 sequences are concentrated in one OTU. The measures were calculated with error bars by 186 randomly subsampling 500 sequences from each sample, calculating both measures, repeating 187 this process 100 times, and calculating standard deviation from the 100 replicate measurements. 188 To measure changes in the overall sample microbiome structure, we calculated between-sample 189 unweighted UniFrac distances, which takes into account not only changes in OTU 190 presence/absence, but also in OTU phylogenetic relatedness. To visualize changes to the 191 microbiome structure, we plotted the samples on the first two principal coordinates of the 192 UniFrac distances, directly showing 49.8% of the total microbiome variation (Figure 2C).

193

194 Shotgun metagenome sequencing and data analysis. We quantified gDNA extracted from 10 195 bioreactor samples via fluourometric analysis with the PicoGreen dsDNA quantitation kit 196 (Invitrogen Corp, Carlsbad, CA). The samples were then sequenced on an Illumina HiSeq 2000 197 system on two lanes (Columbia NextGen Genome Center, Columbia University, New York, 198 NY). Quality filtering was performed on the reads using a trimming threshold of two 199 consecutive low-quality bases, no unknown bases, and a final minimum length of 75 bp, and removal of identical sequences, using the QIIME 1.4.0 pipeline  $^{3}$ . We uploaded the reads to 200 MG-RAST<sup>4</sup> for further analysis. After all quality control, each sample contained an average of 201 202 24,286,497 reads with an average length of 98 bp (~2.4 billion bp per sample). Using MG-203 RAST we created a functional (gene) annotation table by applying a maximum e-value cutoff of  $1e^{-2}$  and a minimum percent identity of 50% to annotations based on the KEGG Orthology (KO) 204 205 database. We used the metagenomic functional annotations as a way to supplement our findings 206 in the 16S rRNA gene sequencing analysis of the communities. Specifically, we looked at the 207 taxonomic breakdown of genes involved in conversion of yeast-fermentation beer to *n*-caproic 208 acid.

We used two methods to determine the genes for which taxonomic identification can provide information about the role of bacteria in the bioreactor. First, we looked at genes significantly correlated with rates of *n*-caproic acid production (Figure S4). To do so, we converted the functional annotation table from MG-RAST into a table compatible with QIIME 1.4.0. We used QIIME to determine the genes whose relative abundance across the 10 samples was correlated with *n*-caproic acid production, limiting the analysis to genes that appeared in at least 5 of 10 samples. This produced 10 genes correlated at  $R^2 > 0.9$  and with at least 1000 reads

## Electronic Supplementary Material (ESI) for Energy & Environmental Science This journal is © The Royal Society of Chemistry 2012

216 per sample by day 126 (Table S3). Second, we looked at genes catalyzing the major steps 217 leading to conversion of yeast-fermentation beer components to *n*-caproic acid (Figure S3). 218 Specifically, we considered genes involved in: 1. Complex molecule hydrolysis (starch, 219 xylan/xylose, and cellulose/cellobiose), 2. Glycolysis (we assume this was the central primary 220 carbon metabolism pathway), 3. Ethanol oxidation, and 4. Chain elongation. Some of the 221 enzymes could theoretically be used for other processes; for example, chain elongation genes 222 could be involved in  $\beta$ -oxidation, but we labeled Figure S3 based on the most likely role of the 223 gene in *n*-caproic acid production. We did not include any genes with less than 1000 assigned 224 reads (Table S2). To simplify Figure S3, we also combined several steps for the processes: xylan 225 hydrolysis, cellulose and cellobiose hydrolysis, ethanol oxidation, and glycolysis (Table S2). To 226 determine the taxonomy distribution of genes, we used MG-RAST's "best hit" implementation to annotate read taxonomy at the level of genus by applying a maximum e-value cutoff of 1e<sup>-4</sup> 227 228 and a minimum percent identity of 50% to annotations based on the M5NR database. We used 229 relatively strict cutoffs, because the best-hit method of gene annotation may produce faulty 230 annotations, especially when two potential annotations have a close quality hit in the 231 implemented BLAST search. Since our goal here is only to indicate potential roles of taxonomic 232 groups, the annotations at these cutoff values should be sufficient.

233

## 234 **References:**

- 235
- E. Alkaya, S. Kaptan, L. Ozkan, S. Uludag-Demirer and G. k. N. Demirer, *Chemosphere*, 2009, **77**, 1137-1142.
- M. T. Agler, Z. Aydinkaya, T. A. Cummings, A. R. Beers and L. T. Angenent, *Bioresour*.
   *Technol.*, 2010, **101**, 5842-5851.
- J. G. Caporaso, J. Kuczynski, J. Stombaugh, K. Bittinger, F. D. Bushman, E. K. Costello,
  N. Fierer, A. G. Pena, J. K. Goodrich, J. I. Gordon, G. A. Huttley, S. T. Kelley, D.
- 242 Knights, J. E. Koenig, R. E. Ley, C. A. Lozupone, D. McDonald, B. D. Muegge, M.
- 243 Pirrung, J. Reeder, J. R. Sevinsky, P. J. Turnbaugh, W. A. Walters, J. Widmann, T.
- 244 Yatsunenko, J. Zaneveld and R. Knight, *Nat. Methods*, 2010, **7**, 335-336.
- F. Meyer, D. Paarmann, M. D'Souza, R. Olson, E. Glass, M. Kubal, T. Paczian, A.
   Rodriguez, R. Stevens, A. Wilke, J. Wilkening and R. Edwards, *BMC Bioinformatics*, 2008, 9, 386.
- 248



A-C. Carboxylates Produced

251 Fig. S1. Performance of the *n*-caproic acid producing bioreactor on days 120-180 and 350-374, 252 including the effects of an extraction module failure on day 157, and the maximum n-caproic 253 acid production rate on day 364 after extraction rates were increased on day 300 due to 254 increasing the extraction membrane surface area 3.5 times. Days 120-130 correspond to the 255 same days in Figure 1: A. Production rate of C2-C8 carboxylic acids on days 120-180 and 350-256 374; B. Extraction efficiency of C2-C8 carboxylic acids as the percentage of produced acid that was extracted in-line; and C. Extraction rate of C2-C8 carboxylic acids is the rate of in-line 257 recovery of each acid. The vertical line in A-C represents the failure of an extraction module on 258 259 day 157. Performance data between days 180 and 350 was omitted to only focus on one 260 membrane failure and the sustained production of *n*-caproic acid after installation of a new and larger extraction system on day 300. In the interim, problems arose from cracking membrane 261 262 housing, and these problems disappeared after switching to stainless steel housing. 263



266 Fig. S2. A 93-h methanogenic activity test at pH 5.5 and 30°C demonstrates that microbiomes 267 did not produce methane from acetic acid but produced it from CO<sub>2</sub> with H<sub>2</sub> or ethanol as 268 sources of reducing equivalents: A. Control set demonstrates that methane is not produced by 269 microbiomes in the presence of acetic acid; B. The microbiome produces methane from  $CO_2$  and 270 H<sub>2</sub> but acetic acid is not consumed; C. By consuming ethanol, the microbiome elongates some of the acetic acid to *n*-butyric acid (*n*-caproic acid was not detected); and D. When CO<sub>2</sub> and ethanol 271 272 are added, microbiomes consume most of the ethanol because acetic acid is elongated to n-Despite acetic acid elongation, acetic acid 273 butyric acid and  $CO_2$  is reduced to  $CH_4$ . 274 concentrations increase because ethanol is oxidized to acetic acid either by methanogens or by 275 other microbes, which transfer H<sub>2</sub> to methanogens.



**Fig. S3.** Results of the shotgun metagenomic sequencing analysis. Taxonomic breakdown of gene pools involved in specific steps of carbon metabolism, indicate bacterial taxa that could be involved in specific steps of carbon metabolism. The figure is only a subset of all potential

281 metabolic genes, but includes those that we expect to be important in conversion of yeast-

- fermentation beer to *n*-caproic acid. All data is from a sample taken on day 126 when
- conversion occurred at high rates. Extracellular molecules are highlighted in white. For
   simplicity, some enzymatic steps have been combined and genes with only a small number of
- assigned metagenomic reads (<1000) have been left out. For comparison, the taxonomic
- breakdown of all taxonomically-assigned reads is shown. The genera shown are the same as
- those shown in Figure S4A.
- 288
- 289



**Fig. S4.** Results of our shotgun metagenomic sequencing analysis. Genera important to *n*caproic acid formation determined by the taxonomic breakdown of the seven genes most

correlated to the production rate of *n*-caproic acid ( $\mathbb{R}^2 > 0.9$ ): A. Taxonomy key and phylogenetic

relatedness of the bacterial genera; and B. Total relative abundance and breakdown of taxonomy

for genes associated with production rate of *n*-caproic acid. The production rate of *n*-caproic

- acid (green line) is shown for reference.
- 297

298



300 301 Fig. S5. Ethanol concentration in effluent of the *n*-caproic acid producing bioreactor. Ethanol in

the effluent occurred when it was not oxidized during chain elongation. The black lines 302

303 represent: 1. The switch to yeast fermentation beer substrate; 2. The HRT decrease from 15 days

304 to 12 days, and 3. The failure of the extraction modules.

**Table S1:** Correlation coefficient (with significance) for OTUs whose relative abundance was positively correlated to the *n*-caproic acid production rate (with 16S rRNA gene sequencing analysis). <sup>1</sup>OTUs with r > 0.80 and p-value < 0.05 and whose relative abundance reached at least 0.05 by day 90 (Figure 2). <sup>2</sup>OTUs without taxonomic information could only be identified as belonging to the domain bacteria.

	Ci	Correlation						
0711	Significance	Coefficient	Dhula	<b>C</b> 1	Ouder	From the	6	Constant
010	(p-value)	(r)	Phyla	Class	Order	Family	Genera	Species
1466	0.002	0.000	n Firmieutes	a Clastridia	a Clastridialas	f Clastridialas Family VI Incentos Cadia	a Charanaarahaatar	. Charanaanahaatan aaatiganaa
400 1722	0.002	0.960	pFirmicutes	cclostridia	oClostridiales	f	gsporanaerobacter	ssporanaerobacter_acetigenes
733	0.008	0.926	2 primicules	CClostridia	0Clostridiales	IRuminococcaceae		
740	0.008	0.926	. Flowstandar			6 Duralization		
260	0.010	0.917	pFirmicutes	cClostridia	oClostridiales	fRuminococcaceae	a Clastridium	a Clastridium klunuari
12	0.011	0.912	2 pFirmicules	cclostridia	0Clostridiales	IClostridiaceae	gclostrialum	sclostnaium_kiuyven
107	0.015	0.899	2					
1225	0.015	0.897	n Firmieutes	a Clastridia	a Clastridialas	f Clastridianaa	a Clastridium	a Clastridium klunuari
225	0.016	0.895	pFirmicutes	cclostridia	0Clostridiales	fClostridiaceae	gClostridium	sclostrialum_kluyveri
702	0.027	0.804	pFirmicutes	cclostridia	oClostridiales	fRuminococcaceae	gclostrialum	0lu_2118
/92	0.035	0.849	pFirmicutes	cclostridia	0Clostridiales	IRuminococcaceae		
6/4	0.041	0.830	pFirmicutes	a Clastridia	a Clastridialas	f Duminananan	a Ossillaspira	atu: 2126
221	0.052	0.808	pFirmicutes	cclostridia	0Clostridiales	fRuminococcaceae	gOscillospira	0lu_2128
123	0.070	0.776	pFirmicutes	cClostridia	oClostridiales	fRuminococcaceae	a Clastridium	a Clastridium klunuari
509	0.080	0.749	pFirmicutes	cclostridia	0Clostridiales	fClostridiaceae	gclostrialum	sclostnaium_kiuyven
13	0.097	0.734	pFirmicutes	cClostridia	oClostridiales	fRuminococcaceae	a Clastridium	
200	0.098	0.732	pFirmicutes	cclostridia	0Clostridiales	fClasteldiases	gClostridium	
289	0.099	0.731	pFirmicutes	cClostridia	oClostridiales	fClostridiaceae	gClostridium	
251	0.099	0.731	pFirmicutes	cclostridia	0Clostridiales	fClostridiaceae	gclostrialum	
26	0.106	0.721	pFirmicutes	cClostridia	oclostridiales	fRuminococcaceae		
406	0.112	0.712	2 pbacteroidetes	CDacterolola	0Bacteroidales	IPorphyromonadaceae		
462	0.134	0.084	n Firmieutes	a Clastridia	a Clastridialas	f Duminananan		
405	0.135	0.005	pFirmicutes	cclostridia	oClostridiales	fRuminococcaceae		
50	0.140	0.677	pFirmicutes	cclostridia	oClostridiales	fRuminococcaceae	a Clastridium	
3/8	0.152	0.002	pFirmicutes	cclostridia	oClostridiales	fRuminococcaceae	gclostrialum	
415	0.247	0.561	pFirmicutes	cclostridia	oClostridiales	fRuminococcaceae		
207	0.255	0.555	pFirmicutes	cclostridia	oClostridiales	fRuminococcaceae		
250	0.254	0.554	pFirmicutes	cclostridia	oClostridiales	fRuminococcaceae	a Clastridium	atu 2116
235	0.207	0.525	pFirmicutes	cclostridia	0Clostridiales	f Duminococcaceae	gclosti lului	otu_2110
201	0.303	0.307	2	cclostitula	0Clostitulales	IRummococcaceae	gOscillospila	010_2128
204	0.332	0.465	n Eirmicutor	c Clostridia	o Clostridialos	f Burningsossasaa	a Clostridium	otu 2116
274	0.370	0.430	p	c_Clostridia	o_Clostridiales	f Buminococcaceae	gclostituluiti	010_2110
120	0.378	0.444	pFirmicutes	cclostitula	0Clostitulales	IRummococcaceae		
100	0.380	0.442	p	c Clostridia	o Clostridialos	f Burningsossasaa	a Clostridium	
286	0.380	0.442	pFirmicutes	c_Clostridia	o_Clostridiales	f Ruminococcaceae	gClostridium	
200	0.415	0.410	pn	cClostridia	o Clostridiales	f Buminococcaceae	gclostituluiti	
144	0.422	0.400	p	c_Clostridia	o Clostridiales	f Ruminococcaceae	g Clostridium	otu 2116
497	0.434	0.398	pFirmicutes	c_Clostridia	o Clostridiales	f Buminococcaceae	sclostituluiti	044_2110
637	0.434	0.336	p	cClostridia	o Clostridiales	f Buminococcaceae	g Clostridium	otu 2116
620	0.528	0.326	pFirmicutes	c Clostridia	o Clostridiales	f Buminococcaceae	s_clostituluiti	010_2110
490	0.520	0.324	pFirmicutes	c_Clostridia	o Clostridiales	f_Clostridiaceae	g Clostridium	s Clostridium acetobutylicum
278	0.531	0.324	pFirmicutes	c Clostridia	o Clostridiales	f Buminococcaceae	g_Clostridium	otu 2116
402	0.582	0.286	pFirmicutes	c Clostridia	o Clostridiales	f_Clostridiaceae	gClostridium	s Clostridium kluweri
689	0.625	0.255	pFirmicutes	c Clostridia	o Clostridiales	f Clostridiaceae	g Clostridium	5005011010011_110()*011
719	0.646	0.233	n Firmicutes	c_Clostridia	o Clostridiales	f Buminococcaceae	8elostilatani	
282	0.649	0.239	pFirmicutes	c Clostridia	o Clostridiales	f Buminococcaceae	g Clostridium	otu 2116
176	0.678	0.218	2		00.00011414169	·	<u></u>	
369	0.685	0.214	p Firmicutes	c Clostridia	o Clostridiales	f Ruminococcaceae		
550	0.695	0.206	p Firmicutes	c Clostridia	o Clostridiales	f Ruminococcaceae		
457	0.723	0.187	p Firmicutes	c Clostridia	o Clostridiales	f Ruminococcaceae		
1	0.761	0.161	p Firmicutes	c Clostridia	o Clostridiales	f Ruminococcaceae		
742	0 771	0.154	n Firmicutes	c Clostridia	o Clostridiales	f Ruminococcaceae		

	Significance	Correlation Coefficient							
ΟΤΟ	(p-value)	(r)	Phyla	Class	Order	Family	Genera	Species	
440	0.802	0.133	pFirmicutes	cClostridia	oClostridiales	f_Lachnospiraceae			
428	0.860	0.094	pBacteroidetes	cBacteroidia	oBacteroidales			otu_973	
119	0.919	0.054	pFirmicutes	cClostridia	oClostridiales	fRuminococcaceae			
439	0.967	0.022	pFirmicutes	cClostridia	oClostridiales	fRuminococcaceae		otu_2109	
803	0.975	0.017	pFirmicutes	cClostridia	oClostridiales	fRuminococcaceae	gClostridium	otu_2116	

**Table S2:** Genes included in the analysis for Figure S3 (with shotgun metagenomic sequencing analysis). Only those genes with >1000 assigned reads are included in the figure. <sup>1</sup>The transketolase involved in conversion of xylulose to a glycolysis intermediate is separated from other xylan degradation genes because the taxonomy distribution of the gene was very different.

Pathway Involvement EC Number		Name	>1000 Reads
Starch to Glycolysis	rch to Glycolysis 2.4.1.1 Phosphorylase		Yes
	3.2.1.37	Xylan 1,4-β-Xylosidase	Yes
Valor /Valoro to	1.1.1.21	Aldehyde Reductase	No
Aylan/Aylose to	1.1.1.9	D-Xylulose Reductase	Yes
Aylulose	5.3.1.5	Xylose Isomerase	Yes
	2.7.1.17	Xylulokinase	No
<sup>1</sup> Xylulose to Glycolysis	2.2.1.1 Transketolase		Yes
	3.2.1.4	Cellulase	No
	3.2.1.91	Cellulose 1,4-β-cellobiosidase	No
	3.2.1.21	β-glucosidase	Yes
Calledon to Classic	2.7.1.1	Hexokinase	No
Cellulose to Glycolysis	2.7.1.2	Glucokinase	No
	2.7.1.63	Polyphosphate-glucose phosphotransferase	No
	5.1.3.15	Glucose-6-phosphate 1-epimerase	No
	5.1.3.3	Aldose 1-epimerase	No
	5.4.2.2	Phosphoglucomutase	Yes
	5.3.1.9	Glucose 6-phosphate isomerase	Yes
	2.7.1.11	6-Phosphofructokinase	Yes
	2.7.1.146	ADP-specific phosphofructokinase	No
	4.1.2.13	Fructose-bisphosphate aldolase	Yes
	1.2.1.12	Glyceraldehyde 3-phosphate dehydrogenase	Yes
	1.2.1.59	Glyceraldehyde 3-phosphate dehydrogenase (NADP)	No
Glycolysis to Pyruvate	5.3.1.1	Triose-phosphate isomerase	Yes
	2.7.2.3	Phosphoglycerate kinase	Yes
	5.4.2.4	Bisphosphoglycerate mutase	No
	3.1.3.13	Bisphosphoglycerate phosphatase	No
	5.4.2.1	Phosphoglycerate mutase	Yes
	4.2.1.11	<b>Phosphopyruvate hydratase</b>	Yes
	2.7.1.40	Pvruvate kinase	No
Pyruvate to Acetyl- CoA	2.3.1.54	Formate C-acetyltransferase (Pvruvate-formate lvase)	Yes

## Electronic Supplementary Material (ESI) for Energy & Environmental Science This journal is C The Royal Society of Chemistry 2012

Pathway Involvement	EC Number	C Number Name	
	1.1.1.1	Alcohol dehydrogenase	Yes
Ethonol to Apotyl CoA	1.1.1.2	Alcohol dehydrogenase (NADP)	No
Ethanoi to Acetyi-CoA	1.2.1.3	Aldehyde dehydrogenase (NAD)	No
	1.2.1.5	Aldehyde dehydrogenase (NADP)	No
	2.3.1.9	Acetyl-CoA C-acetyltransferase	Yes
	1.1.1.36	Acetoacetyl-CoA reductase	No
	1.1.1.35	3-Hydroxylacyl-CoA dehydrogenase	No
Chain Elengation	1.1.1.157	3-Hydroxybutyryl-CoA dehydrogenase	Yes
Cham Elongation	4.2.1.55	3-Hydroxybutyryl-CoA dehydratase	Yes
	4.2.1.17	Enoyl-CoA hydratase	No
	1.3.8.1	Butyryl-CoA dehydrogenase	Yes
	2.8.3.6	3-Oxoadipate CoA transferase	No

**Table S3:** Coefficient of correlation to *n*-caproic acid production rate for genes included in the analysis for Figure S4 (with shotgun metagenomic sequencing analysis). Only those genes with >1000 assigned reads are included in the figure.

EC Number	Name	Correlation Coefficient [r   r <sup>2</sup> ]	>1000 Reads
2.4.1.7	Sucrose phosphorylase	0.98   0.95	Yes
2.4.2.2	Pyrimidine-nucleoside	0.97   0.94	Yes
	phosphorylase		
1.17.4.2	<b>Ribonucleoside-triphosphate</b>	0.96   0.94	Yes
	reductase		
5.4.2.7	Phosphopentomutase	0.96   0.92	Yes
4.2.3.3	Methylglyoxal synthase	0.96   0.92	Yes
5.4.2.8	Phosphomannomutase	0.95   0.91	Yes
5.4.3.3	β-lysine 5,6 aminomutase	0.95   0.91	No
2.2.1.1	Transketolase	0.95   0.90	Yes