

## Supporting Information

### **A Perfluorinated Covalent Triazine-based Framework for Highly Selective and Water-tolerant CO<sub>2</sub> Capture**

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<sup>§</sup> These authors contribute equally to this work.

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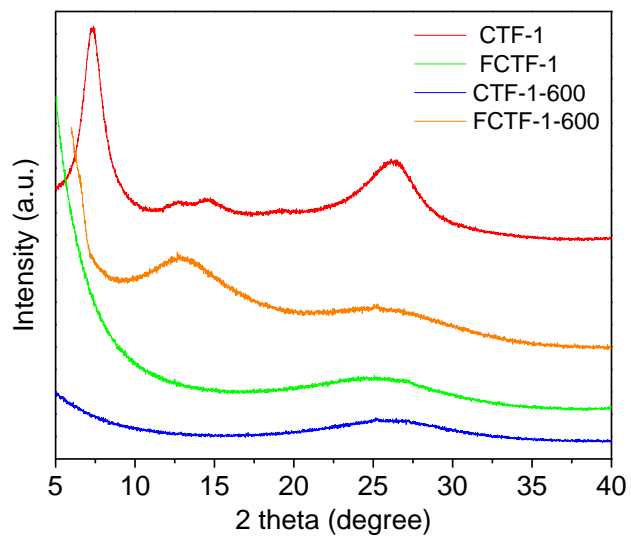
**Figure S1.** X-ray diffraction patterns of various sorbents.

**Figure S2.** Pore size distribution curve of CTF-1-600 in the mesopore range.

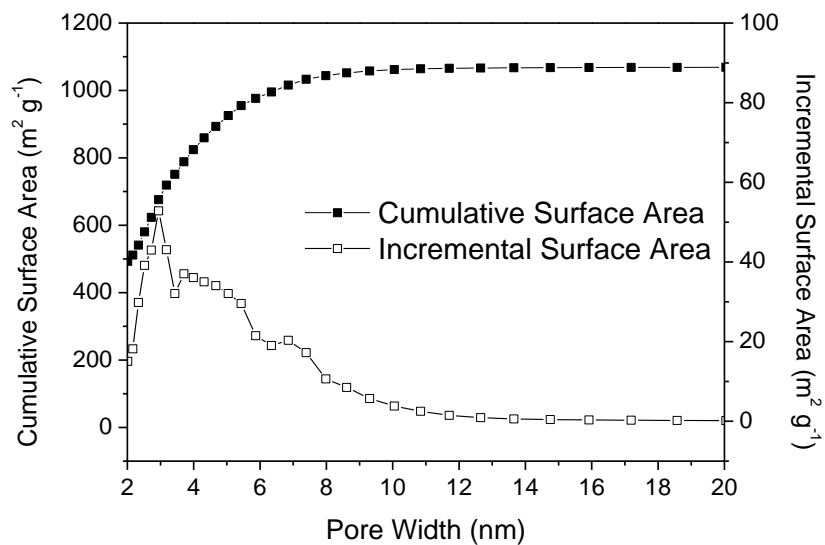
**Figure S3.** C1s and N1s XPS spectra of (a) CTF-1, (b) CTF-1-600, and (c) FCTF-1-600.

**Figure S4.** N<sub>2</sub> adsorption isotherms at 298 K of various sorbents.

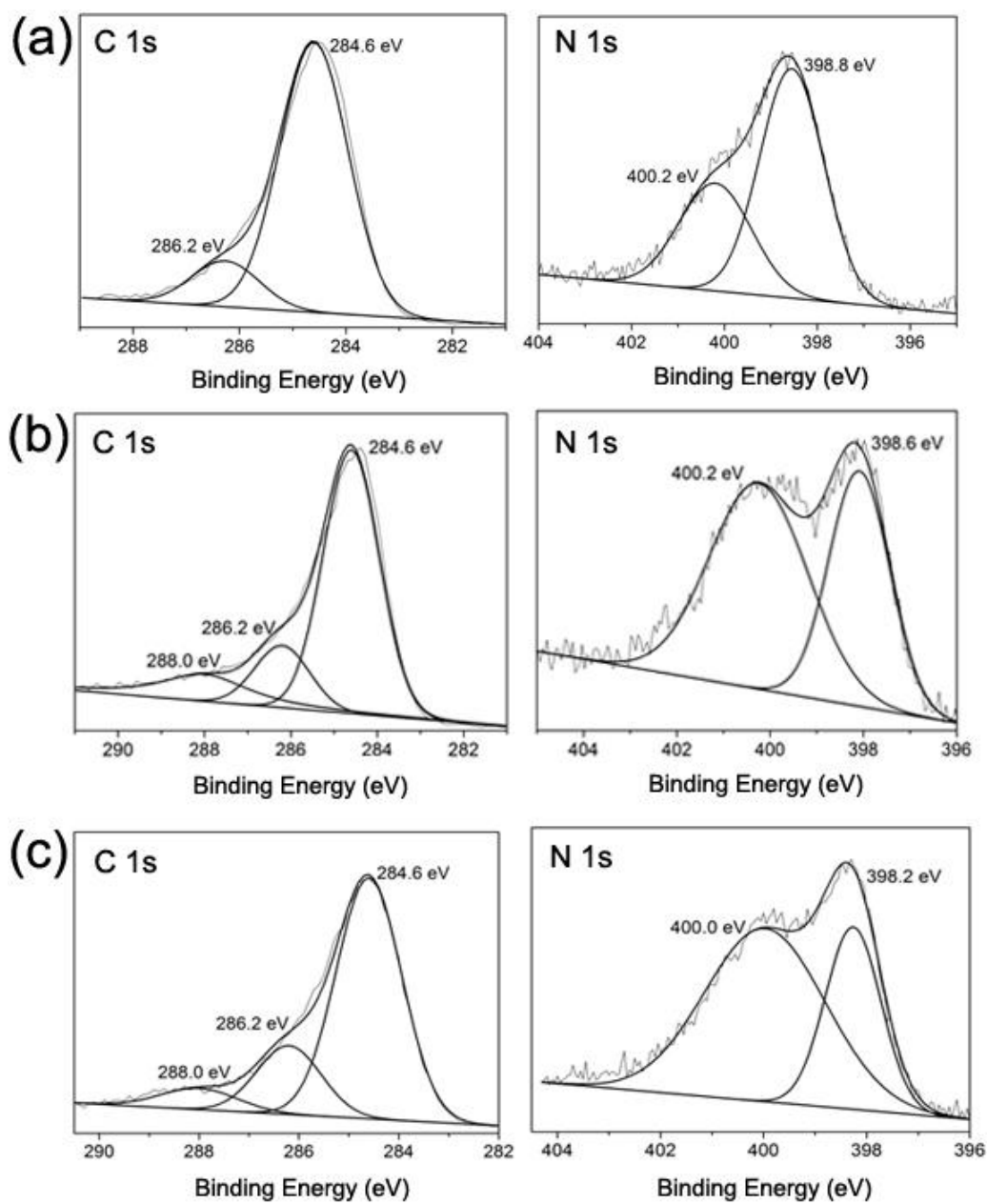
**CO<sub>2</sub>/N<sub>2</sub> selectivity calculation by the ideal adsorption solution theory (IAST)**



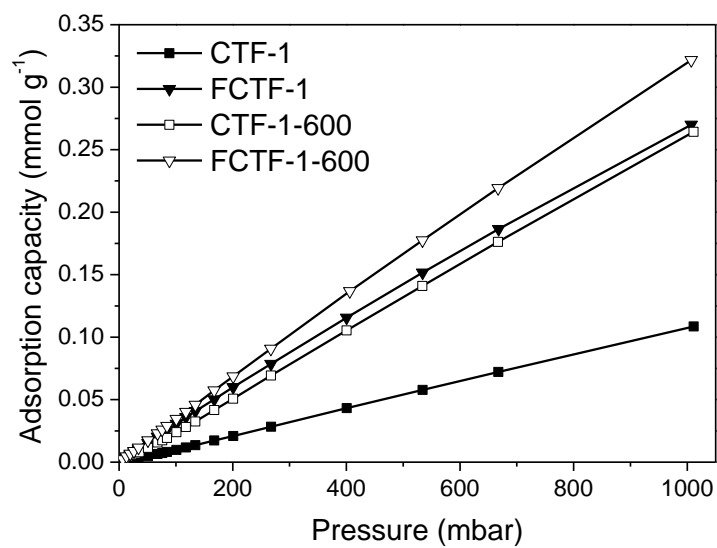
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## CO<sub>2</sub>/N<sub>2</sub> selectivity calculation by the ideal adsorption solution theory (IAST)

The experimental adsorption isotherms were firstly fitted using the single-site Langmuir model:

$$q_i = q_{i,sat} \frac{b_i p_i}{1 + b_i p_i}$$

where

$b_i$  = Langmuir constant, Pa<sup>-1</sup>

$p_i$  = bulk gas phase pressure of species  $i$ , Pa

$q_i$  = molar loading of species  $i$ , mmol g<sup>-1</sup>

$q_{i,sat}$  = saturation capacity of species  $i$ , mmol g<sup>-1</sup>

According to the ideal adsorption solution theory (IAST) proposed by Myers and Prausnitz,<sup>1</sup> the adsorption selectivity,  $S_{ads}$ , for binary mixtures of **1** and **2**, is defined as

$$S_{ads} = \frac{q_1/q_2}{p_1/p_2}$$

In this study, selectivity calculations were carried out for CO<sub>2</sub>/N<sub>2</sub> binary mixtures with N<sub>2</sub> molar fraction ranging from 70% to 100%, which is typical composition range of flue gases.