

Electronic Supplementary Information

## Initiation and propagation of a single pit on stainless steel using local probe technique

Stéphane Heurtault<sup>a,b</sup>, Raphaël Robin<sup>a</sup>, Fabien Rouillard<sup>a,\*</sup> and Vincent Vivier<sup>b,\*\*</sup>

### Dependence of the current density with time for a diffusion-limited process

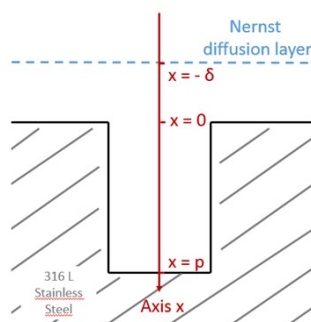


Fig. 15: Cylindrical pit with definition of axis X

For a cylindrical or disc shaped pit geometry sketched in Fig. 15, the second Fick law is used to represent the diffusion of a specie  $i$  out of the pit:

$$\frac{\partial C_i(x,t)}{\partial t} = D_i \frac{\partial^2 C_i(x,t)}{\partial x^2} \quad (8)$$

Where  $x$  the geometric coordinate normal to the pit propagation direction as defined in Fig. 15,  $C_i(x,t)$  the concentration of specie  $i$  at the point of coordinate  $x$  at time  $t$ ,  $D_i$  its diffusion coefficient.

The boundary conditions for the diffusive system are:

- On  $x = p$ , at the pit bottom, the concentration of specie  $i$  is assumed to be constant with time. It is the case for metallic cations and chloride ions when a salt film is present at the bottom of the pit.
- For  $x < -\delta$  with  $\delta$  the thickness of the Nernst diffusion layer, beyond the Nernst diffusion layer, the concentration of specie  $i$  is constant.
- At time  $t = 0$ , the concentration of specie  $i$  is constant in the diffusion domain, for  $-\delta < x < p$ :

$$\left(\frac{\partial C_i}{\partial x}\right)_t = 0, \quad -\delta < x < p = 0 \quad (9)$$

For this differential problem, Vetter proposed an analytical solution [46]:

$$\frac{C_i(x,t) - C_i(x < -\delta,t)}{C_i(p,t) - C_i(x < -\delta,t)} = \frac{\Delta C_i(x,t)}{\Delta C_i(p,t)} = \frac{2}{\sqrt{\pi}} \int_{\frac{x-p}{2\sqrt{D_i*t}}}^{\infty} \exp(-u^2) du \quad (10)$$

From relation (10), the derivative of the concentration is obtained as:

$$\frac{\partial C_i}{\partial x} = -\frac{\Delta C_i(p,t)}{\sqrt{\pi * D_i * t}} * \exp\left(-\frac{(x-p)^2}{4 * D_i * t}\right) \quad (11)$$

According to Fick first law, the current density is proportional to the concentration gradient at the active surface ( $x = p$ ).

$$J = -nFD_i \left( \frac{\partial C_i}{\partial x} \right)_{x=p} \quad (12)$$

Using equations (11) and (12):

$$J = nFD_i * \frac{\Delta C_i(p,t)}{\sqrt{\pi * D_i * t}} \quad (13)$$

Finally an expression the current density as a function of time is given by:

$$J = nF\Delta C_i(p,t) * \sqrt{\frac{D_i}{\pi * t}} \quad (14)$$

In this expression  $\Delta C_i(p,t)$  is the concentration difference of specie i between the bottom of the pit (coordinate  $x = p$ ) and the bulk electrolyte (coordinate  $x < -\delta$ ). If the diffusion is the rate determining step of the dissolution, the current density is proportional to  $1/\sqrt{t}$  according to relation (14).