Supplementary Data and Information - Oxidative Methylation of Aromatics over Zeolite Catalysts
Table SD1 - Data for calculating AE, CE, RME, EMY, MI and MP

| Reaction | Catalyst/Amount of catalyst (g) | Reagent | Mol. weight of Reagent ( $\mathrm{g} / \mathrm{mol}$ ) | Moles of <br> Reagent converted | Amount of Reagent converted (g) | Mol. weight of <br> Toluene product ( $\mathrm{g} / \mathrm{mol}$ ) | Amount of Toluene product (g) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Equation 14 | HZSM-5/0.2 | Benzene | 78.11 | $9.378 \times 10^{-4}$ | 0.07327 | 92.14 | 0.1018 |
|  |  | Methanol | 32.04 | $1.579 \times 10^{-3}$ | 0.05061 |  |  |
|  | CoZSM-5/0.2 | Benzene | 78.11 | $9.823 \times 10^{-4}$ | 0.07674 | 92.14 | 0.1015 |
|  |  | Methanol | 32.04 | $1.609 \times 10^{-3}$ | 0.05156 |  |  |
|  | CuZSM-5/0.2 | Benzene | 78.11 | $9.844 \times 10^{-4}$ | 0.07691 | 92.14 | 0.1044 |
|  |  | Methanol | 32.04 | $1.607 \times 10^{-3}$ | 0.05149 |  |  |
| Equation 15 | HZSM-5/0.055 | Benzene | 78.11 | $2.181 \times 10^{-4}$ | 0.01704 | 92.14 | 0.01869 |
|  | $0.31 \% \mathrm{O}_{2}$ used | Methane | 16.043 | $2.181 \times 10^{-4}$ | 0.003499 |  |  |
|  |  | Oxygen | 32.0 | $1.090 \times 10^{-4}$ | 0.003489 |  |  |
|  | $1.42 \% \mathrm{O}_{2}$ used | Benzene | 78.11 | $5.282 \times 10^{-4}$ | 0.04126 | 92.14 | 0.04118 |
|  |  | Methane | 16.043 | $5.282 \times 10^{-4}$ | 0.008474 |  |  |
|  |  | Oxygen | 32.0 | $2.641 \times 10^{-4}$ | 0.008452 |  |  |

Table SD2 - Data for calculating RMC

| Reaction | Catalyst | Reagent | Mol. weight of Reagent (g/mol) | Liquid Density $(\mathrm{g} / \mathrm{ml})$ or Gas Specific Vol. ( $\mathrm{m}^{3} / \mathrm{kg}$ ) | Reagent cost* (\$AUS/kg) | Toluene yield (\%) | Mol. weight ( $\mathrm{g} / \mathrm{mol}$ )/Mass of Toluene produced (g) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Equation 14 | HZSM-5 | Benzene | 78.11 | 0.874 | 33.75 | 22.12 | 92.14/0.1018 |
|  |  | Methanol | 32.04 | 0.791 | 8.38 |  |  |
|  | CoZSM-5 | Benzene | 78.11 | 0.874 | 33.75 | 24.13 | 92.14/0.1015 |
|  |  | Methanol | 32.04 | 0.791 | 8.38 |  |  |
|  | CuZSM-5 | Benzene | 78.11 | 0.874 | 33.75 | 24.88 | 92.14/0.1044 |
|  |  | Methanol | 32.04 | 0.791 | 8.38 |  |  |
| Equation 15 | HZSM-5 | Benzene | 78.11 | 0.874 | 33.75 | 3.88 | 92.14/0.01869 |
|  | $0.31 \% \mathrm{O}_{2}$ used | Methane | 16.043 | 1.48 | 357.41 |  |  |
|  |  | Oxygen | 32.0 | 0.755 | 66.09 |  |  |
|  |  | Benzene | 78.11 | 0.874 | 33.75 | 8.54 | 92.14/0.04118 |
|  | $1.42 \% \mathrm{O}_{2}$ used | Methane | 16.043 | 1.48 | 357.41 |  |  |
|  |  | Oxygen | 32.0 | 0.755 | 66.09 |  |  |

*The costs of the largest quantities listed in the catalogue of Sigma-Aldrich was used for ACS reagent grade benzene ( $\geq 99$ \%, thiophene-free) and methanol $\left((\geq 99.8 \%)\right.$, which are $\$$ AUS590/20 L and $\$ 1325 / 200 \mathrm{~L}$, respectively. For methane, the cost of $\$ 1982.65$ of Size G (= $\left.8.21 \mathrm{~m}^{3}\right)$ of BOC Ultra Pure Grade Part No 149200 was used while for oxygen the cost of \$AUS597.29 of Size G $\left(=6.21 \mathrm{~m}^{3}\right)$ of BOC Ultra High Purity Grade Part No 226200 was used.

## Sample Calculations for Metric listed in Table 7 of Article

## Atom Economy, AE (Reaction 15, Experiment 1):

$\left(\frac{M W_{\text {product }}}{\sum M W_{\text {reagents }}}\right) \times 100 \%=\left(\frac{M W_{\text {toluene }}}{M W_{\text {benzene }}+M W_{\text {methane }}+1 / 2 M W_{\text {oxygen }}}\right) \times 100 \%=\left(\frac{92.14 \times 100}{78.11+16.043+1 / 2(32.0)}\right)=83.6 \%$

## Carbon Efficiency, CE (Reaction 15, Experiment 1):

$\left(\frac{\text { no.of moles of product x no. of carbons in product x } 100}{\Sigma \text { moles of reagents x no. of carbons in reagent }}\right) \%=\left(\frac{\text { moles of toluene x } 7 \times 100}{(\text { moles of benzene } \times 6)+(\text { moles of methane } \times 1)}\right) \%$ $=\left(\frac{(0.01869 / 92.14) \times 700}{\left(2.181 \times 10^{-4} \times 6\right)+\left(2.181 \times 10^{-4} \times 1\right)}\right)=93.0 \%$

## Reaction Mass Efficiency, RME (Reaction 15, Experiment 1):

$\left(\frac{\text { mass of product }}{\sum \text { mass of reagents }}\right) \times 100 \%=\left(\frac{\text { mass of toluene }}{(\text { mass of benzene }+ \text { mass of methane }+ \text { mass of oxygen })}\right) \times 100 \%=\left(\frac{0.01869 \times 100}{(0.01704+0.003499+0.003489)}\right)=77.8 \%$

## Effective Mass Yield, EMY (Reaction 15, Experiment 1):

$\left(\frac{\text { mass of product }}{\sum \text { mass of non }- \text { benign reagents } *}\right) \times 100 \%=\left(\frac{\text { mass of toluene }}{(\text { mass of benzene }+ \text { mass of oxygen })}\right) \times 100 \%=\left(\frac{0.01869 \times 100}{(0.01704+0.003489)}\right)=91.1 \%$
*Non-benign reagents are those that are classified as hazardous substances in the MSDS according to the criteria of National Occupational Health and Safety Commission (NOHSC) of Australia, namely benzene and oxygen. In the case of the reaction 14, the methylation of benzene with methanol, methanol is also classified as hazardous substance.

Mass Intensity, MI (Reaction 15, Experiment 1):

$$
\begin{aligned}
& \left(\frac{\text { Total mass used in a process or process step }(\mathrm{kg})}{\text { mass of product }(\mathrm{kg})}\right)=\left(\frac{(\text { mass of benzene }+ \text { mass of methane }+ \text { mass of oxygen }+ \text { mass of catalyst })(\mathrm{kg})}{\text { mass of toluene }(\mathrm{kg})}\right) \\
& =\left(\frac{(0.01704+0.003499+0.003489+0.055)}{0.01869}\right)=4.23 \mathrm{~g} / \mathrm{g} \equiv 4.23 \mathrm{~kg} / \mathrm{kg}
\end{aligned}
$$

Mass Productivity, MP (Reaction 15, Experiment 1):
$\left(\frac{1}{\mathrm{MI}} \times 100 \%\right)=\left(\frac{\text { mass of product } \mathrm{x} 100}{\text { Total mass used in process or process step }}\right)=\left(\frac{\text { mass of toluene } \mathrm{x} 100}{(\text { mass of benzene }+ \text { mass of methane }+ \text { mass of oxygen }+ \text { mass of catalyst })}\right)$
$=\left(\frac{0.01869}{(0.01704+0.003499+0.003489+0.055)}\right)=23.6 \%$

## Raw Materials Cost, RMC (Reaction 15, Experiment 1):

$$
\begin{aligned}
& \left(\frac{\text { mass of target product } \times \Sigma\left(M W_{\text {reagents }} \times \text { Cost per } \mathrm{g} \text { of reagent }\right)}{M W_{\text {product }} \times \text { Product yield }}\right)=\left(\frac{\Sigma\left(M W_{\text {reagents }} \times \text { Cost per kg of reagent }\right)}{M W_{\text {product }} \times \text { Product yield }}\right)=\$ / \mathrm{kg} \text { product } \\
& =\left(\frac{\left[\left(M W_{\text {benzene }} \times \text { Benzene cost } / \mathrm{kg}\right)+\left(M W_{\text {methane }} \times \text { Methane cost } / \mathrm{kg}\right)+\left(M W_{\text {oxygen }} \times \text { Oxygen cost } / \mathrm{kg}\right)\right]}{\left(M W_{\text {toluene }} \times \text { Toluene yield }\right)}\right) \\
& =\left(\frac{[(78.11 \times 33.75)+(16.043 \times 357.41)+(32.0 \times 66.09)]}{(92.14 \times 3.88 / 100)}\right)=\$ 2934.34 / \mathrm{kg} \text { toluene }
\end{aligned}
$$

Raw Materials Cost at 100\% product yield, RMC $_{100}$ (Reaction 15, Experiment 1):
$\mathrm{RMC}_{100}=\mathrm{RMC} \times$ Product yield $=2934.34 \times(3.8781 / 100)=\$ 113.80$
$\Delta G$ Energy Intensity, $\Delta$ G-EI at 298 K (Reaction 15, Experiment 1):
$\left(\frac{\Delta \mathrm{G} \text { at } 298 \mathrm{~K}}{M W_{\text {product }}}\right)=\left(\frac{-185.8}{92.14}\right)=-2.02 \mathrm{~kJ} / \mathrm{g} \equiv-2.02 \mathrm{MJ} / \mathrm{kg}$
$\Delta H$ Energy Intensity, $\Delta H-E I$ at 298 K (Reaction 15, Experiment 1):
$\left(\frac{\Delta \mathrm{H} \text { at } 298 \mathrm{~K}}{M W_{\text {product }}}\right)=\left(\frac{-200.1}{92.14}\right)=-2.17 \mathrm{~kJ} / \mathrm{g} \equiv-2.17 \mathrm{MJ} / \mathrm{kg}$

