

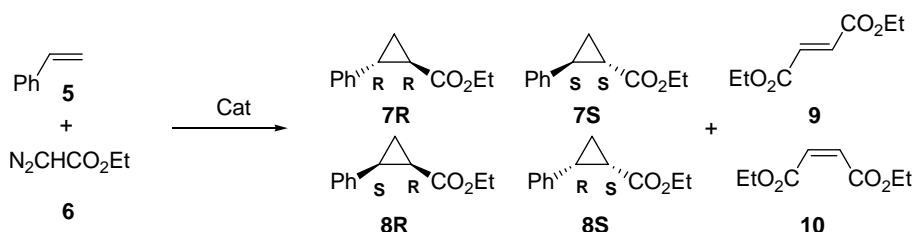
## Bisoxazoline-Functionalised Enantioselective Monolithic Mimi-Flow-reactors: Development of Efficient Processes from batch to Flow Conditions

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### Kinetic calculation BOX

Continuous cyclopropanation reaction between **5** (EDA) and **6** (STR) in CH<sub>2</sub>Cl<sub>2</sub>.  
The main reagents and products involved in the reaction path are:

- % 1.Styrene: STR
- % 2.Ethyl diazotate : EDA
- % 3.Fumarate: FMT
- % 4.Maleate: MLT
- % 5.Trans-cyclopropane\_a: CPTa 7R
- % 6.Trans-cyclopropane\_b: CPTb 7S
- % 7.Cis-cyclopropane\_a: CPCa 8R
- % 8.Cis-cyclopropane\_b: CPCb 8S



The sequence of reactions used was:

$$r_1 = k_1 \cdot c_2^{2.2} \quad (1)$$

$$r_2 = k_2 \cdot c_2^{1.6} \quad (2)$$

$$r_3 = k_3 \cdot c_1 \cdot c_2^{1.6} \quad (3)$$

$$r_4 = k_4 \cdot c_1 \cdot c_2^{4.0} \quad (4)$$

$$r_5 = k_5 \cdot c_1 \cdot c_2^{1.5} \quad (5)$$

$$r_6 = k_6 \cdot c_1 \cdot c_2^{1.5} \quad (6)$$

The different mass balance equations for a fixed bed catalytic reactor are:

$$\frac{dc_1}{d\tau} = -r_3 - r_4 - r_5 - r_6 \quad (7)$$

$$\frac{dc_2}{d\tau} = -2 \cdot r_1 - 2 \cdot r_2 - r_3 - r_4 - r_5 - r_6 \quad (8)$$

$$\frac{dc_3}{d\tau} = +r_1 \quad (9)$$

$$\frac{dc_3}{d\tau} = +r_1 \quad (10)$$

$$\frac{dc_4}{d\tau} = +r_2 \quad (11)$$

$$\frac{dc_5}{d\tau} = +r_3 \quad (12)$$

$$\frac{dc_6}{d\tau} = +r_4 \quad (13)$$

$$\frac{dc_7}{d\tau} = +r_5 \quad (14)$$

$$\frac{dc_8}{d\tau} = +r_6 \quad (15)$$

Final values of the parameters were:

$$k_1 = 0.117 \text{ L}^{1.2} \cdot \text{mol}^{-1.2} \cdot \text{min}^{-1}$$

$$k_2 = 0.0475 \text{ L}^{0.6} \cdot \text{mol}^{-0.6} \cdot \text{min}^{-1}$$

$$k_3 = 0.0350 \text{ L}^{0.6} \cdot \text{mol}^{-0.6} \cdot \text{min}^{-1}$$

$$k_4 = 0.120 \text{ L}^3 \cdot \text{mol}^{-3} \cdot \text{min}^{-1}$$

$$k_5 = 0.0232 \text{ L}^{0.5} \cdot \text{mol}^{-0.5} \cdot \text{min}^{-1}$$

$$k_6 = 0.0070 \text{ L}^{0.5} \cdot \text{mol}^{-0.5} \cdot \text{min}^{-1}$$

