# Selective oxidation of dimethyl ether to methyl formate over trifunctional MoO<sub>3</sub>-SnO<sub>2</sub> catalyst under mild conditions

Guangbo Liu,<sup>*a b*</sup> Qingde Zhang,<sup>*a*</sup> Yizhuo Han,<sup>*a*</sup> Noritatsu Tsubaki<sup>*a c*</sup> and Yisheng Tan<sup>*a*</sup>\*

<sup>a</sup> State Key Laboratory of Coal Conversion, Institute of Coal Chemistry, Chinese Academy of Sciences, 27 South Taoyuan Road Taiyuan 030001, Shanxi, P. R. China Tel: +86 351 4044287; fax: +86 351 4044287. E-mail address: tan@sxicc.ac.cn (Y. Tan).

<sup>b</sup>University of Chinese Academy of Sciences, Beijing 100049, P. R. China

<sup>c</sup> Department of Applied Chemistry, School of Engineering, University of Toyama, Gofuku 3190, Toyama 930-8555, Japan.

#### Experimental

#### **Catalyst Preparation**

The MoO<sub>3</sub>-SnO<sub>2</sub> catalysts were prepared as follows: the obtained catalysts were referred to their Sn salt precursors: MoO<sub>3</sub>-SnO<sub>2</sub> (SnCl<sub>4</sub>), MoO<sub>3</sub>-SnO<sub>2</sub> (Na<sub>2</sub>SnO<sub>3</sub>) and MoO<sub>3</sub>-SnO<sub>2</sub> (SnCl<sub>2</sub>).

The  $MoO_3$ -SnO<sub>2</sub> (SnCl<sub>4</sub>) catalyst was prepared as follows: co-precipitating Tin chloride (SnCl<sub>4</sub>·5H<sub>2</sub>O) aqueous solution and aqueous ammonia in drops at pH=8 at 333K. The obtained suspension was filtered and washed with deionized water until pH=7. Then the cake-like hydroxide was added to the required ammonium molybdate solution. After evaporation of the solvent in a rotary evaporator at 353K, the solid obtained was dried at 393K for 10h and annealed at 573K for 5h and then at 773K for 8h.

The MoO<sub>3</sub>-SnO<sub>2</sub> (SnCl<sub>2</sub>) catalyst was also prepared as above, but using SnCl<sub>2</sub> instead of SnCl<sub>4</sub>.

The  $MoO_3$ -SnO<sub>2</sub> (Na<sub>2</sub>SnO<sub>3</sub>) catalysts were prepared as follows: co-precipitating sodium stannate aqueous solution (Na<sub>2</sub>SnO<sub>3</sub>.3H<sub>2</sub>O) and hydrochloric acid (HCl) in drops at pH=8. The obtained suspension was filtered and washed with deionized water until pH=7, and there was no precipitation when the AgNO<sub>3</sub> was added into the mother liquid. Then the cake-like hydroxide was added to the required ammonium molybdate solution. After evaporation of the solvent in a rotary evaporator at 353K, the solid obtained was dried at 393K for 10h and annealed at 573K for 5h and then at 773K for 8h.

#### **Catalytic Activity Tests**

The reactions were carried out in a continuous flow type fixed-bed reactor containing catalyst (5ml, 20-40mesh) diluted with ground quartz. The catalyst was treated in a flow of  $O_2$  (25ml/min) for 2h at 523K before reaction. The reactant mixture consisted of DME and  $O_2$  with molar ratio of 1:1. The outlet stream line from the reactor to the gas chromatograph was heated at 423K. The hydrocarbon of reaction products were analyzed by gas chromatograph GC-9A (Shimadzu Co.) equipped with flame ionization detector (30m x 0.32mm, PEG-20M), and GC-4000A (Beijing Dongxi Co.) with thermal conductivity detector (Porapak T column). The GC-4000 (Beijing Dongxi Co.) equipped with thermal conductivity detector (TDX-01 column) was used to analyze  $H_2$ , CO, CO<sub>2</sub> and CH<sub>4</sub>.

## Surface texture

The surface area and the particle size of the samples were measured by BET nitrogen adsorption isotherms at 77K using a Tristar 3000 machine.

## **Temperature Programmed Desorption (TPD)**

The NH<sub>3</sub>-TPD spectra were recorded in a fixed-bed reactor system equipped with a thermal

conductivity detector (TCD). The catalyst (100mg) was pretreated at 873K under Ar flow (40ml/min) for 2h and then cooled down to 373K under Ar flow. Then  $NH_3$  was introduced into the flow system. After purging the residual  $NH_3$  for 4h, the TPD spectra were recorded at a temperature rising rate of 5K/min from 373K to 873K.

The CO<sub>2</sub>-TPD spectra were recorded using the same instrument as the NH<sub>3</sub>-TPD. The catalyst (100mg) was pretreated at 873K under Ar flow (40ml/min) for 2h and then cooled down to 303K under Ar flow. Then CO<sub>2</sub> was introduced into the flow system. After purging the residual CO<sub>2</sub> for 4h, the TPD spectra were recorded at a temperature rising rate of 5K/min from 303K to 873K.

#### NH<sub>3</sub> adsorption IR spectra

Diffuse reflectance infrared spectra were measured by a Bruker Tensor 27 with a MCT detector (64 scans, 4 cm<sup>-1</sup>). The catalyst was placed in an in-situ IR cell equipped with KBr windows (Harrick). After heating at 673 K for 2 h and evacuating at  $10^{-4}$  bar, the cell was cooled down to room temperature and the spectrum was recorded. Next, the NH<sub>3</sub> gas was introduced into the cell, and after the equilibrium the sample was degassed. Finally, the spectra were recorded at 373K and the pressure of the cell was evacuated at  $10^{-3}$  bar.

## **Temperature Programmed Reduction (TPR)**

 $H_2$ -TPR was conducted in a fixed-bed reactor system equipped with a thermal conductivity detector. The sample (100mg) was pretreated in Ar at 973K for 2h and then cooled down to 303K. After that, a 10%  $H_2$ /Ar mixture gas was switched on and the temperature was increased linearly at a rate of 5K/min from 303K to 973K.

## **Raman Spectra**

Raman spectra were recorded on a Jobin-Yvon Labram-HR Confocal Laser Micro Raman spectrometer with an argon-ion laser at the excitation wavelength of 514.5nm and the resolution of 1cm<sup>-1</sup>. The Raman spectra were obtained in the range of 100-1100cm<sup>-1</sup> under ambient conditions.