

Supplementary Information for:

Streamlining the Conversion of Biomass to Polyesters: Bicyclic Monomers with Continuous Flow

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Figure S19 Correlation between the glass transition temperature and the reaction time for the polymerization of glycerol with anhydride **2** ($[\text{glycerol}]/[\text{anhydride } \mathbf{2}] = 1$).

Table S1: Solubility studies for cyclohexadiene, maleic anhydride, and monomer **1**.^a

	Acetone	Ethanol	Ethyl acetate	Hexanes	Methanol	Toluene	DI water	Tetrahydrofuran
Maleic anhydride	2.317	0.246	0.595	insoluble	0.979	semi- soluble	0.579	1.392
1,3-CHD	soluble	soluble	soluble	soluble	soluble	soluble	insoluble	soluble
Monomer 1	soluble	0.0338	0.196	insoluble	0.0396	0.104	insoluble	0.422

^aSolubility studies were conducted at ambient temperature with stirred solutions.

Solubility values are given in grams solute/gram solvent.

Table S2. Influence of time and temperature on the alkene isomerization reaction.^a

Entry	Reaction ^b	Temp (° C)	Time (min)	Flow rate (mL/min)	Residence time (sec)	[1,3-CHD]/ [1,4-CHD] ^c	Benzene (%) ^c	Abs ₃₀₃₆ / Abs ₃₀₉₁ ^d
1	Continuous	25	-	1.5±1	13±1	1.9	68	1.96
2	Continuous	11	-	1.3±1	15±1	1.8	13	5.2
3	Continuous	0	-	1.5±1	13±1	1.1	7	6.7
4	Batch	5	5	-	-	1.7	3	-
5	Batch	5	15	-	-	1.8	6	-
6	Batch	5	45	-	-	1.8	10	-
7	Batch	5	140	-	-	1.8	14	-
9	Batch	5	260	-	-	1.8	14	-

^aAll reactions were conducted with neat 1,4-CHD derived from soybean oil that contained ~20 % dodecene isomers which result from monounsaturated triglycerides. ^bContinuous flow reactions flushed 2 mL of 1,4-CHD through a catalyst tube (ID 2.1 mm x 100 mm) with 100 mg of Na₂O/Na/Al₂O₃ catalyst. Batch reactions used 2 mL of 1,4-CHD and 17 mg of Na₂O/Na/Al₂O₃ catalyst in a vial under nitrogen. ^cBased on GC analysis of product mixtures indicating lower temperature and shorter reactions times are beneficial. ^dFTIR data for ratio of 1,3-CHD absorbance at 3036cm⁻¹ and benzene absorbance at 3091 cm⁻¹.

Table S3. Yield data as a function of temperature for neat Diels-Alder reaction between 1,3-CHD and maleic anhydride.

Entry	T (°C)	Time (h)	% Yield based on MA
1	25	12	6.5
2	25	24	9.1
3	30	12	11.8
4	30	24	13.6
5	30	24	12.2
6	40	24	85.0
7	40	24	84.5
8	50	24	88.2
9	50	24	82.7
10	60	24	88.0

[MA] = 12.6 mmol

[CHD] = 19.3 mmol

Table S4: Comparison of polymerization of anhydride **2** with glycerol and 1,4-BDO.^a

Entry	Monomers	M _w (g/mol) ^b	M _w /M _n ^b	[η] ^b (mL/g)	Abs ₁₇₂₆ /Abs ₁₇₇₆ ^c	T _g ^d (°C)	T _d ^e (°C)	X _n ^f
1	1,4-BDO	8730	1.4	6.8	1.9	13	185	25
2	glycerol	9350	2.2	6.7	10	57	286	17

^aPolymerizations were conducted at 120°C for 24 h under dynamic vacuum (150 mbar) with [glycerol or 1,4-BDO]/[**2**] = 1. ^bMeasured by GPC in THF at 35°C using light scattering and viscometer detectors. ^cAbsorbance ratios of ester (1726 cm⁻¹) and anhydride (1776 cm⁻¹) peaks determined by FTIR spectroscopy. ^dMeasured by DSC (20 °C/min) under nitrogen. ^eDecomposition temperature reflects 5 % weight loss as measured by TGA (20 °C/min) under nitrogen. ^fNumber-average degree of polymerization calculated from GPC data.

Table S5: Influence of catalyst choice on polymerization of **2** and glycerol.^a

Entry	Catalyst	M _w (g/mol) ^b	M _w /M _n ^b	[η] ^b (mL/g)	Abs ₁₇₂₆ /Abs ₁₇₇₆ ^c	T _g ^d (°C)	T _d ^e (°C)	X _n ^f
1	none	2560	2.6	3.0	1.4	-nd-	137	4
2	Zn(OAc) ₂	4960	5.0	3.1	1.3	-9	154	4
3	Ti(OBu) ₄	5040	4.9	3.2	1.6	-10	162	4
4	PTSA	9350	2.2	6.7	10	57	286	17

^aPolymerizations conducted with catalyst (0.2 mol %) at 120°C for 24 h under dynamic vacuum (150 mbar) with [glycerol]/[**2**] = 1. ^bMeasured by GPC in THF at 35°C using light scattering and viscometer detectors. ^cAbsorbance ratios of ester (1726 cm⁻¹) and anhydride (1776 cm⁻¹) peaks determined by FTIR spectroscopy. ^dDetermined by DSC (20 °C/min). ^eT_d values reflect 5 % weight loss as measured by TGA (20 °C/min) under nitrogen. ^fNumber-average degree of polymerization calculated from GPC data.

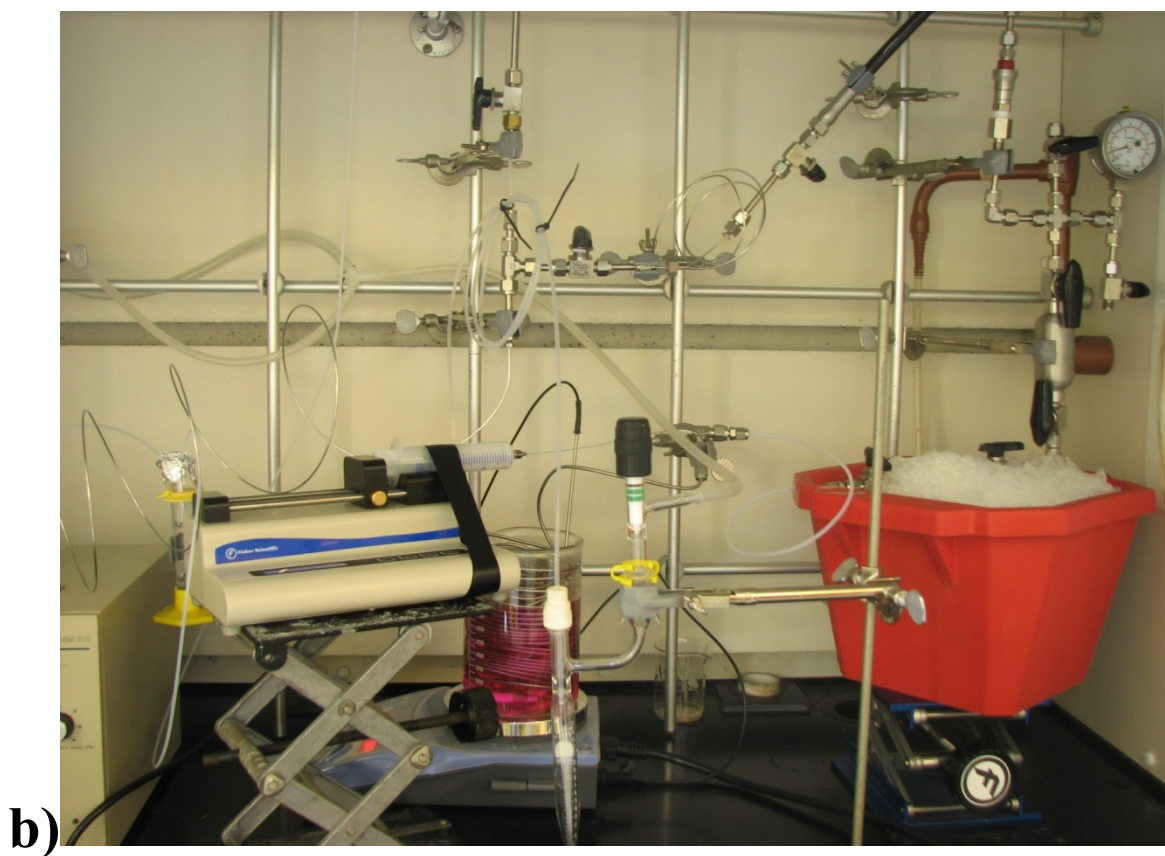
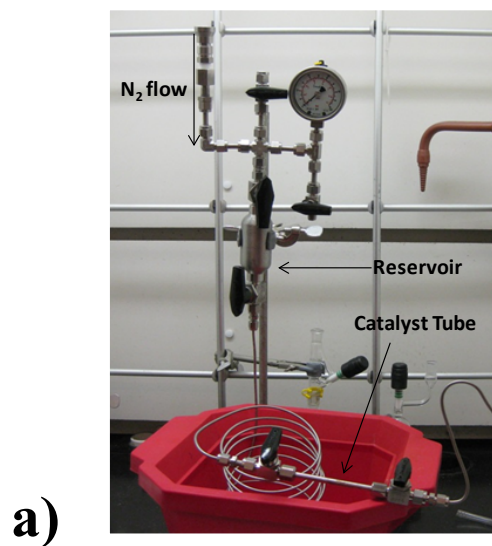


Figure S1. Continuous flow setup showing close-up of alkene isomerization reactor (top picture). The bottom picture shows the three step synthesis involving alkene isomerization

reactor (on right), syringe pump for MA solution (on left), heating bath for Diels-Alder reaction, and vertical hydrogenation tube (on top) with hydrogen inlet.

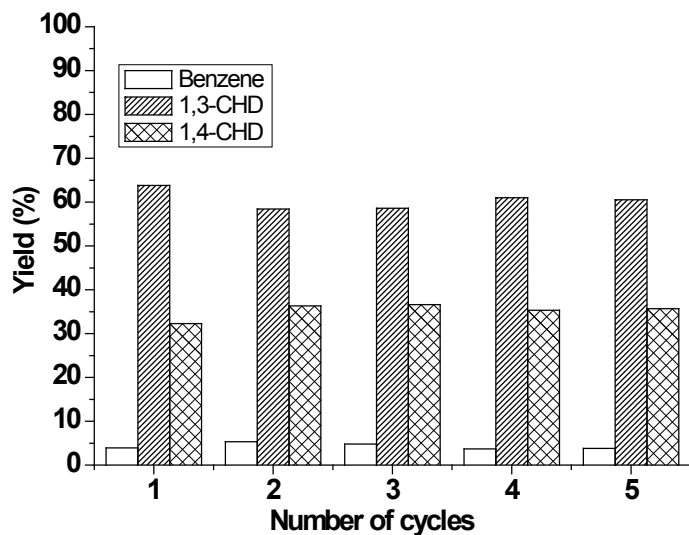


Figure S2. Recycling of catalyst (Na/Na₂O) for the isomerization of 1,4-CHD to 1,3-CHD. The catalyst (100 mg) was subjected to sequential injections of 1,4-CHD (2 mL). The 1,3-CHD:1,4-CHD ratio reflects the thermodynamic stability of the isomers at 0°C.

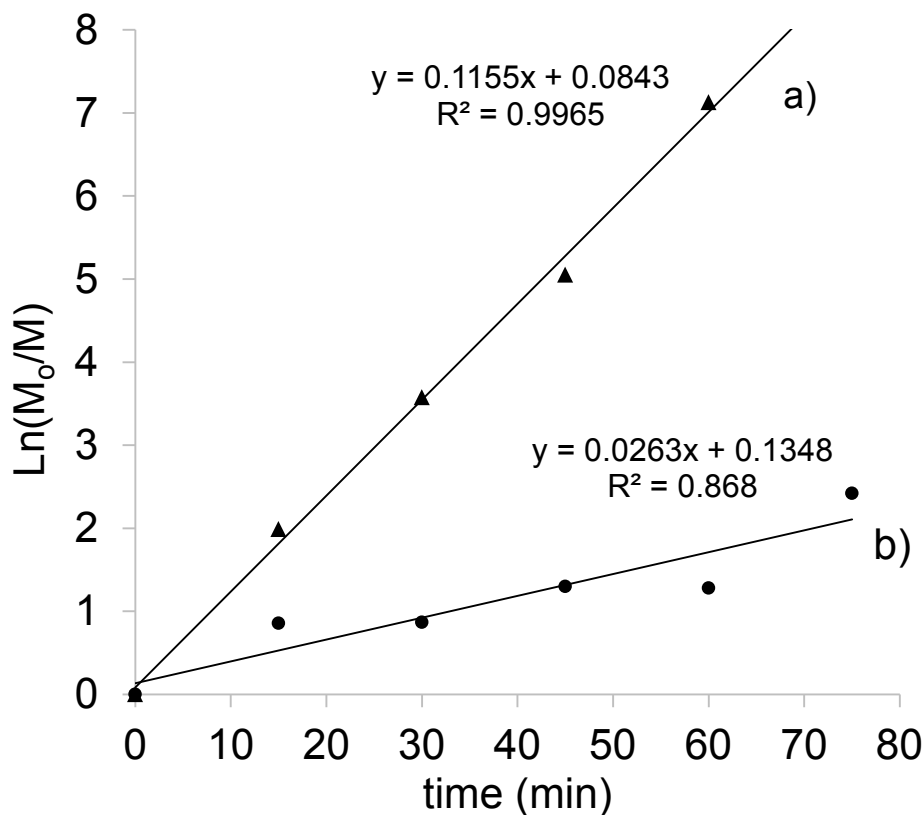


Figure S3. Comparison of Diels Alder reaction of maleic anhydride and 1,3-cyclohexadiene at a) 75 °C and b) 50 °C. The reaction was conducted with MA (1.66 g) in ethyl acetate (12 mL) with 1,3-CHD (4 mL). Data collected by examining the disappearance of the alkene C-H absorbance for maleic anhydride with FTIR spectroscopy.

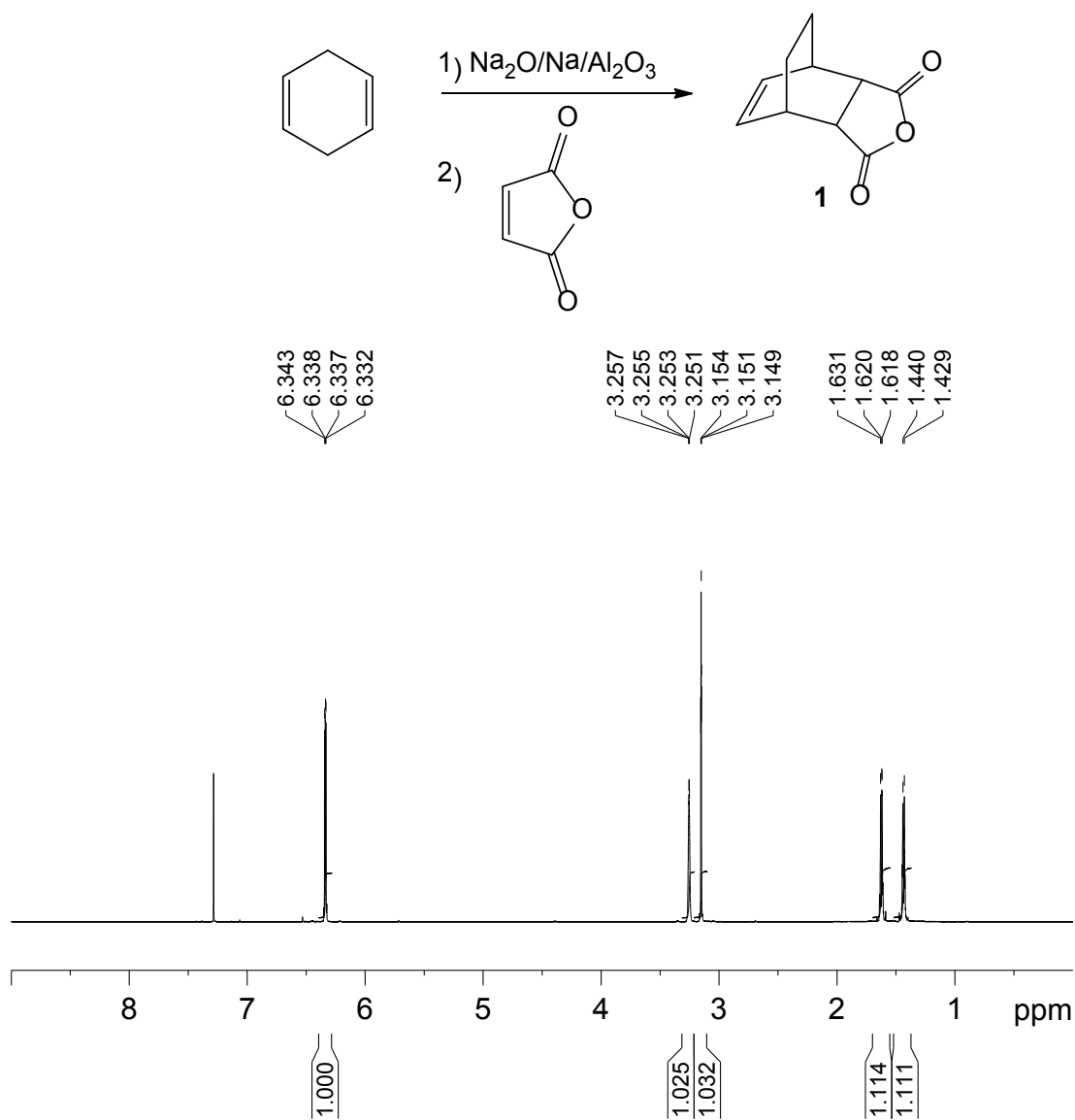


Figure S4. ¹H NMR spectrum (700 MHz, CDCl₃) for the Diels Alder product (**1**) of maleic anhydride and 1,3-cyclohexadiene. Initially, the 1,4-cyclohexadiene was isomerized at 0°C before adding to the maleic anhydride. The Diels Alder reaction was conducted without additional solvent at 60°C for 3 h before recovering the product in 88 % yield.

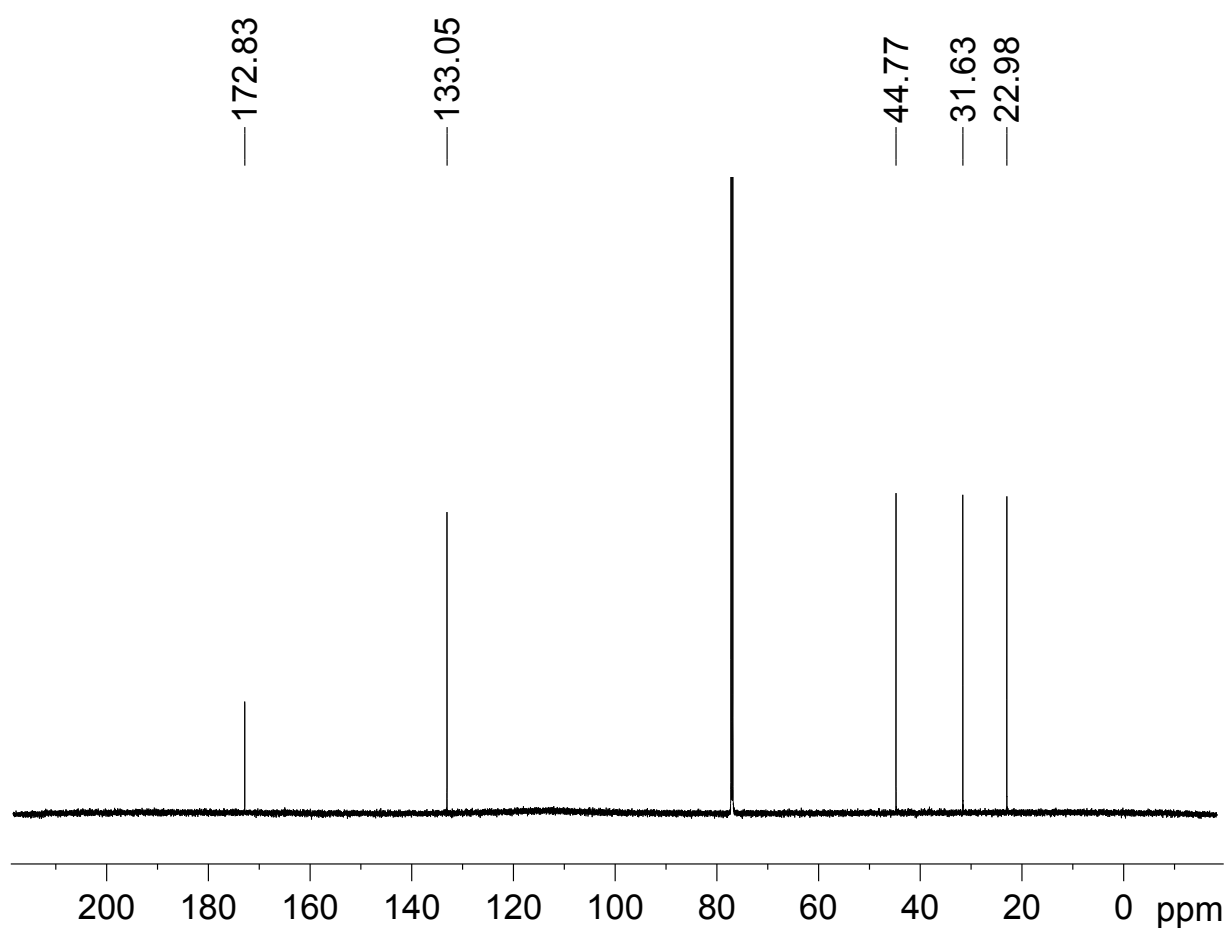
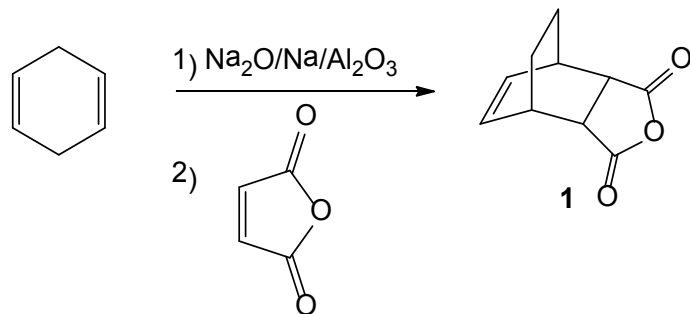


Figure S5. ^{13}C NMR spectrum (700 MHz, CDCl_3) for the Diels Alder product (**1**) of maleic anhydride and 1,3-cyclohexadiene.

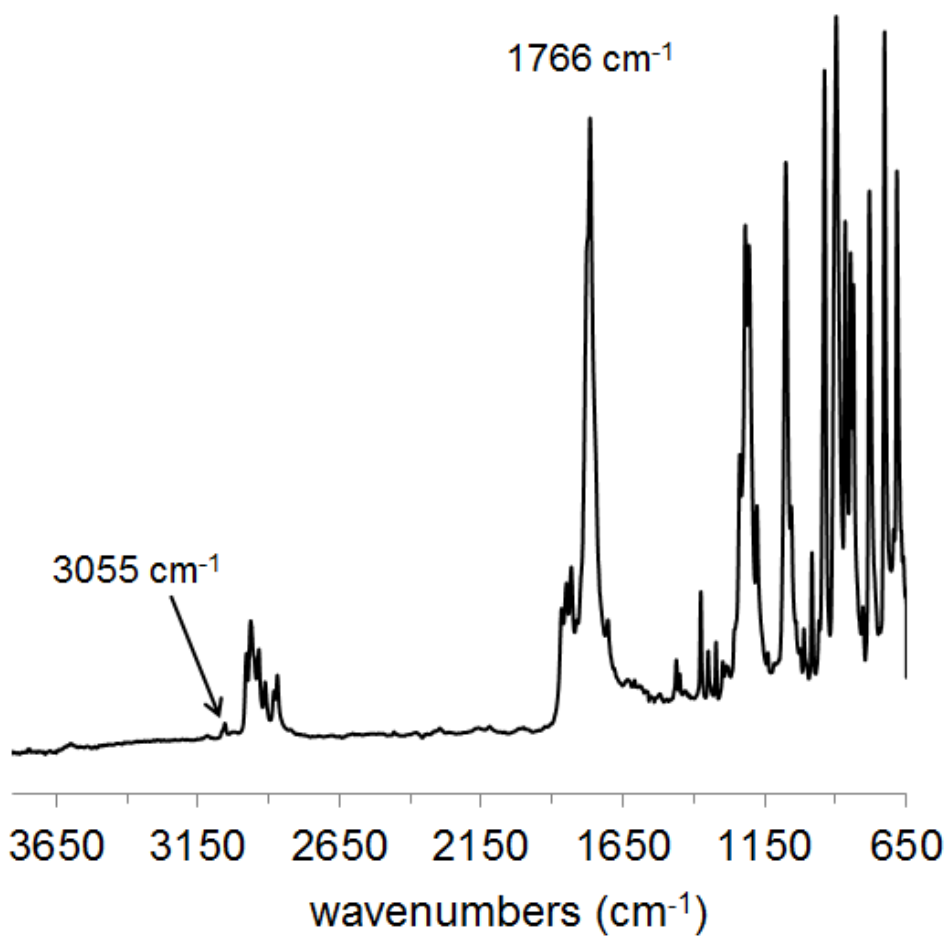
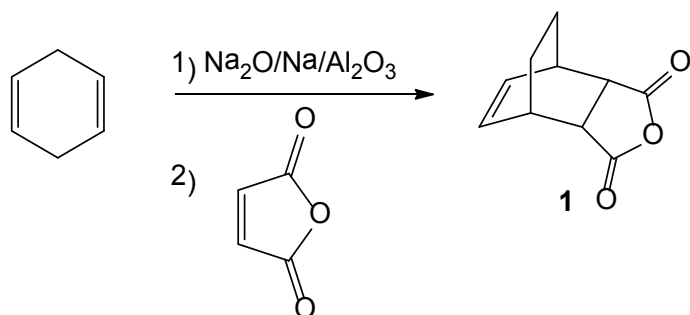
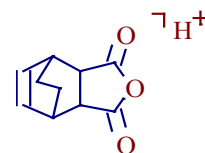
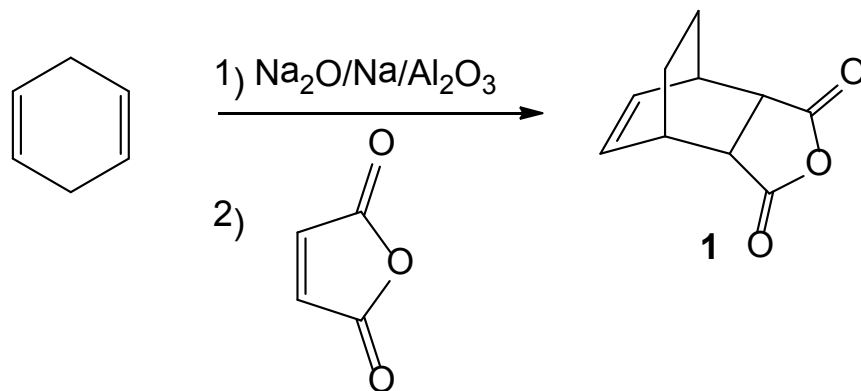


Figure S6. FTIR data for the Diels Alder product (**1**) of maleic anhydride and 1,3-cyclohexadiene. The Diels Alder reaction was conducted under neat conditions at 60°C for 3 h before recovering the product in 88 % yield. The alkene C-H absorbance was detected at 3055 cm^{-1} .



Theo 179.07027
Actual 179.07023
-0.227 ppm difference

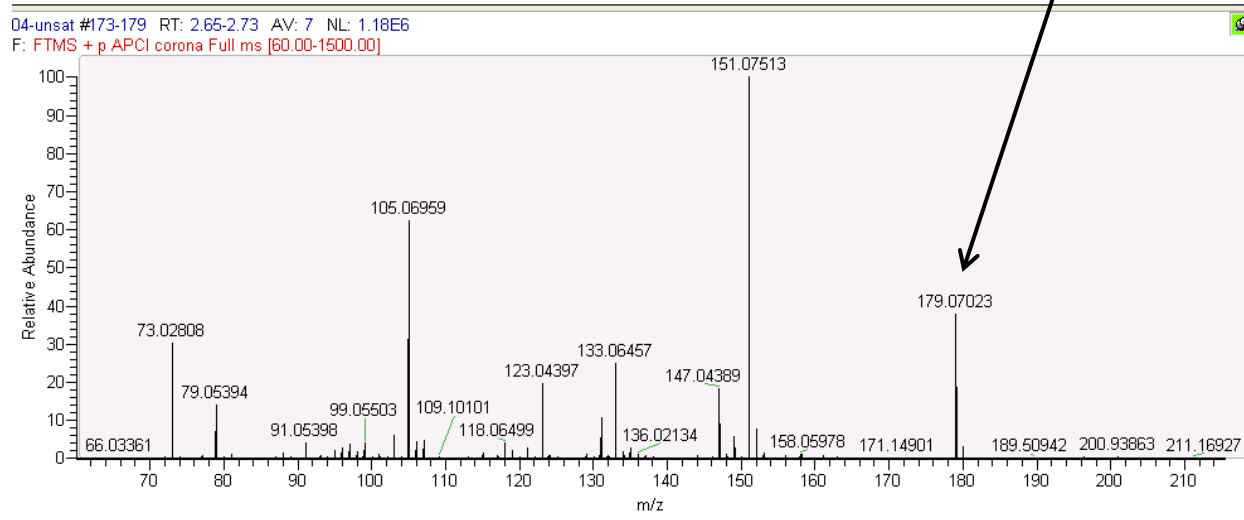


Figure S7. LC/MS data for the Diels Alder adduct (**1**) of maleic anhydride and 1,3-cyclohexadiene.

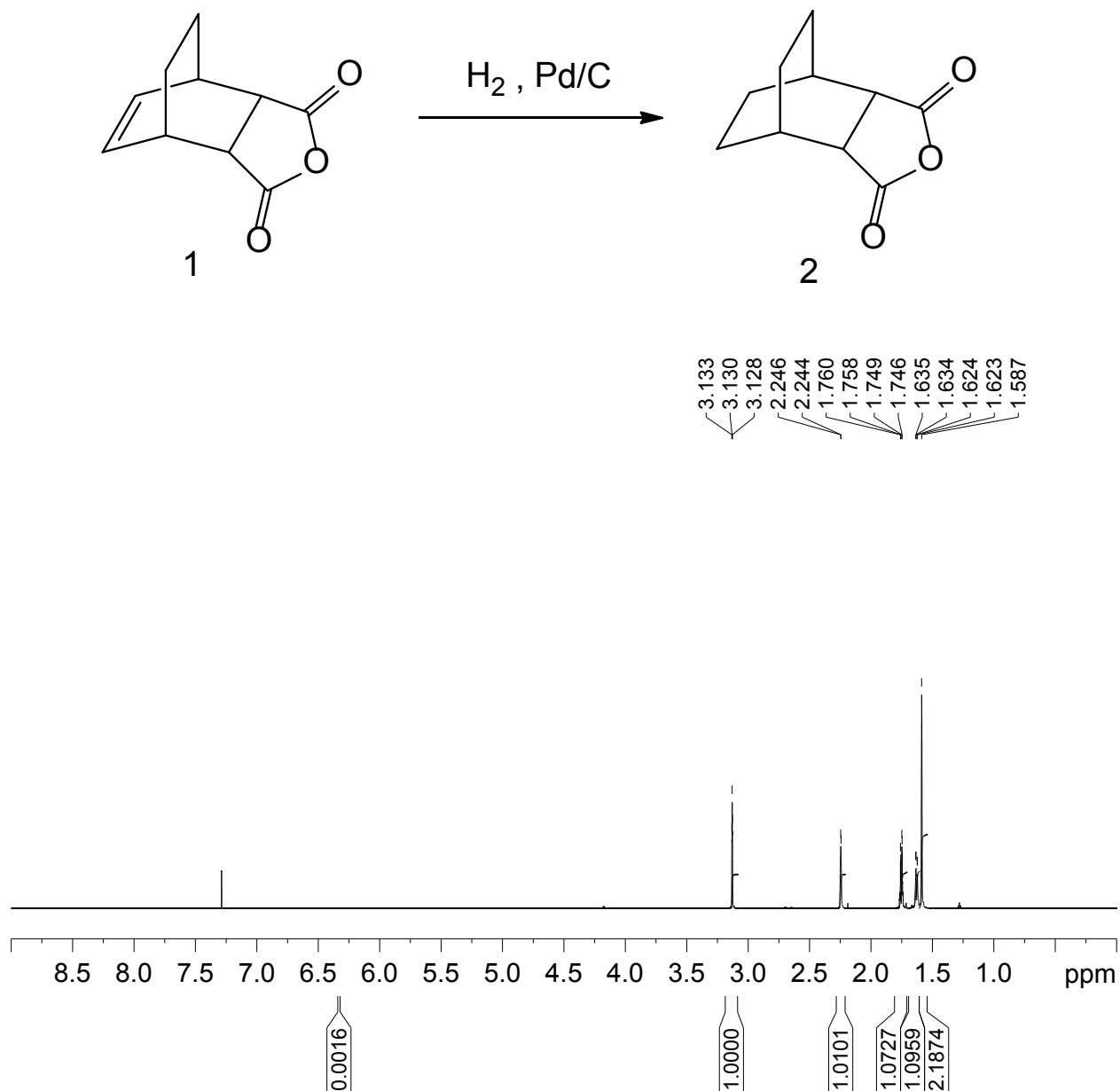


Figure S8. ¹H NMR spectrum (700 MHz, CDCl₃) for the product (2) resulting from the hydrogenation of the Diels Alder adduct (1) in ethyl acetate using Pd/C and hydrogen (20 psi). The reaction was conducted at ambient temperature for 1 day before recovering the product in 95% yield. Based on the disappearance of the alkene integration at δ 6.3 ppm, the hydrogenation was > 99.8 %.

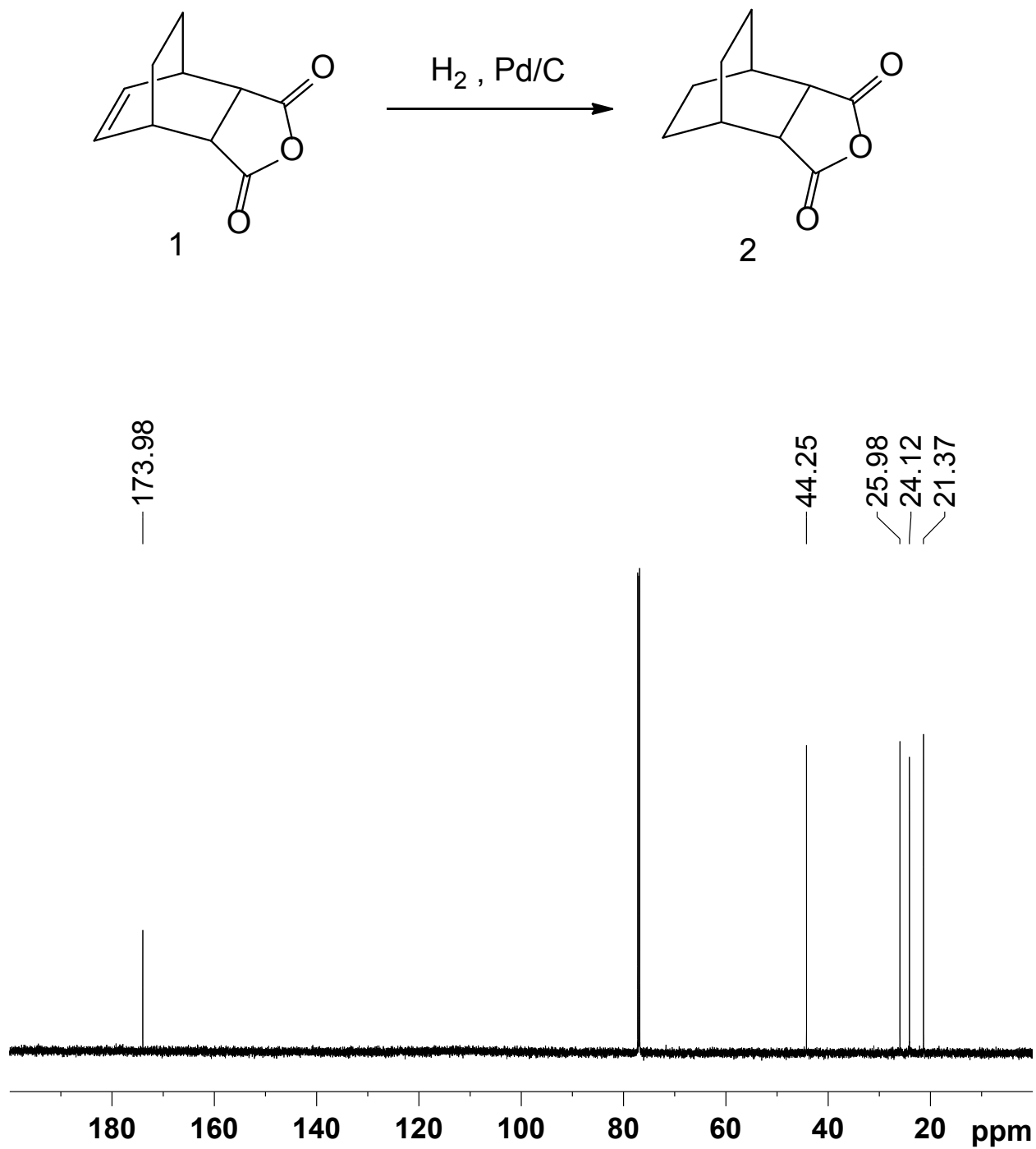


Figure S9. ¹³C NMR spectrum (700 MHz, CDCl₃) for the product (2) resulting from the hydrogenation of the Diels Alder adduct (1) in ethyl acetate using Pd/C and hydrogen (20 psi).

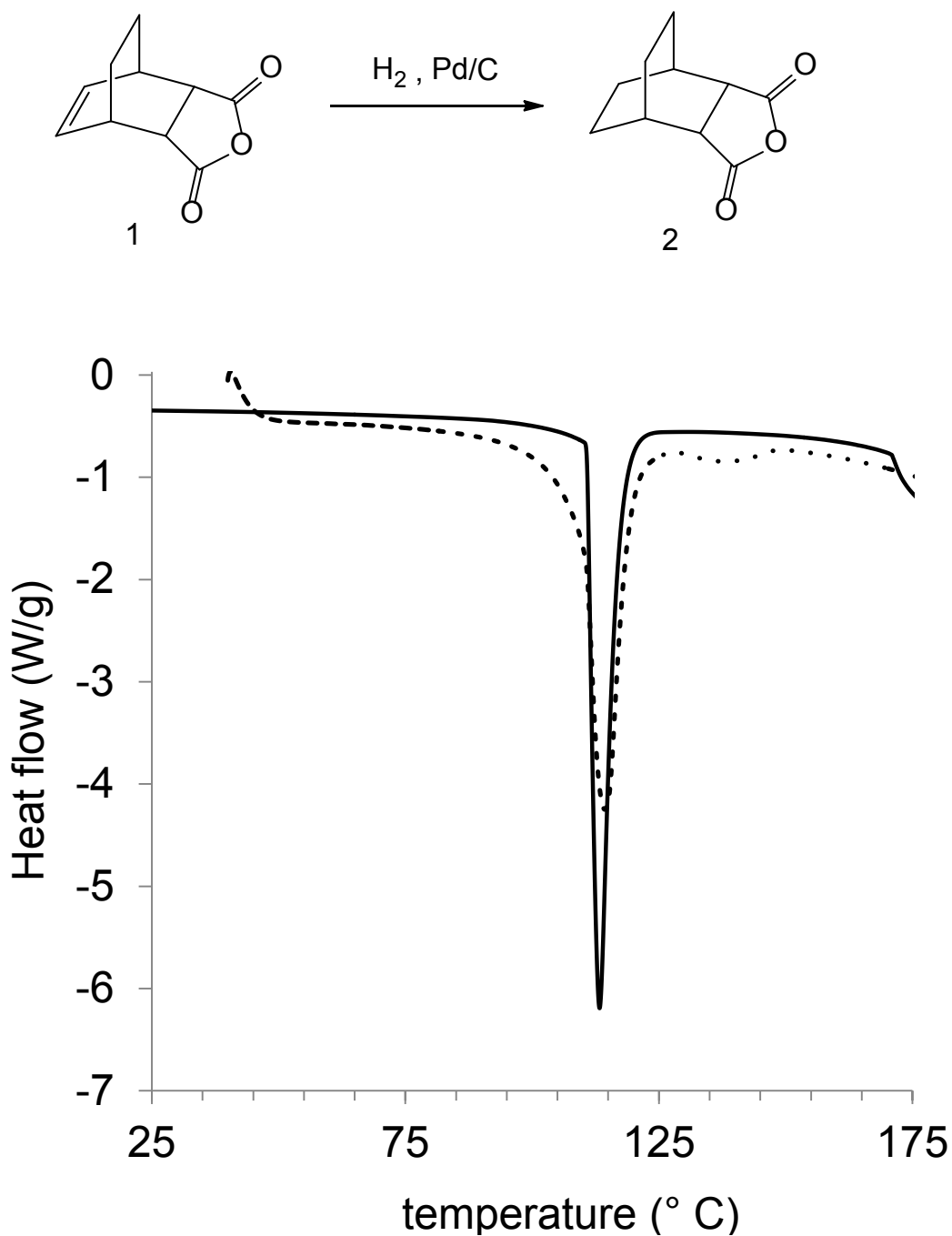


Figure S10. Differential scanning calorimetry (DSC) data (20 $^{\circ}C/min$) for the product (solid line, 2) resulting from the hydrogenation of the Diels Alder adduct (dashed line, 1) in ethyl acetate using Pd/C and hydrogen (20 psi). The reaction was conducted at ambient temperature for 1 day before filtering the Pd/C and recovering the product in 95% yield.

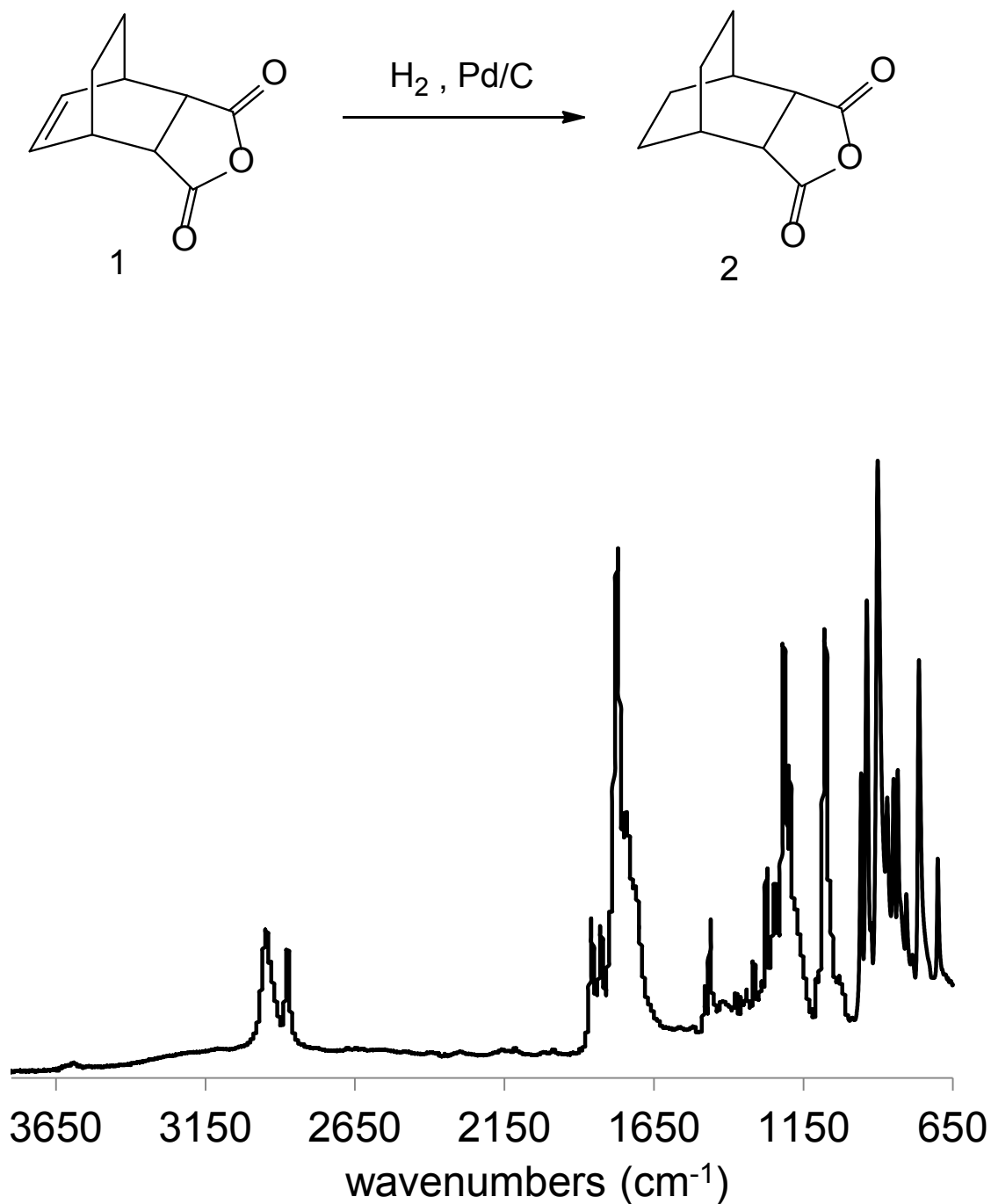


Figure S11. FTIR data for the product (2) resulting from the hydrogenation of the Diels Alder adduct (1) in ethyl acetate using Pd/C and hydrogen (20 psi). The reaction was conducted at ambient temperature for 2 days before filtering the Pd/C and recovering the product in 95% yield.

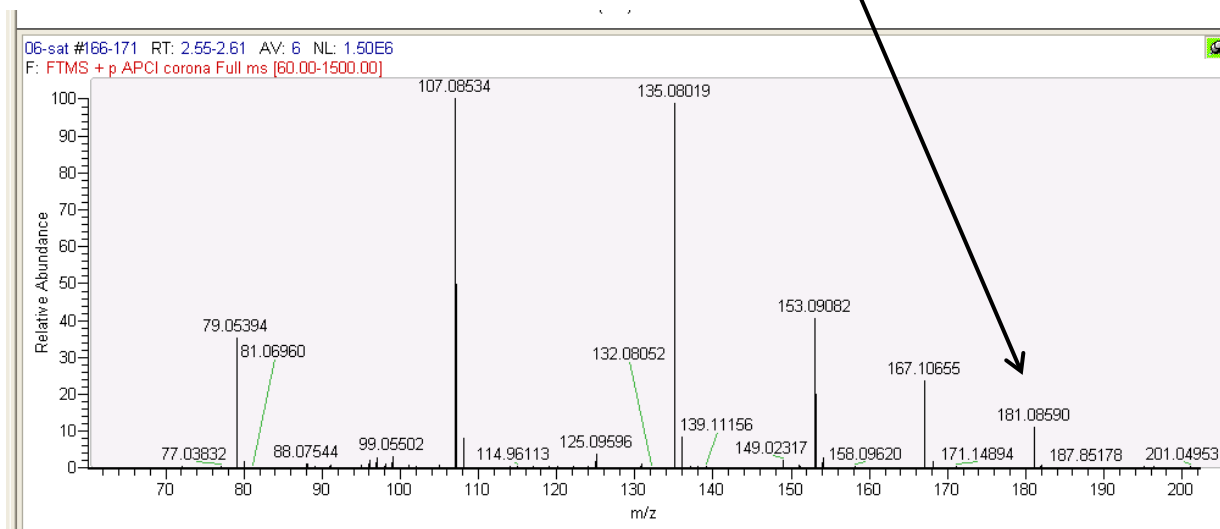
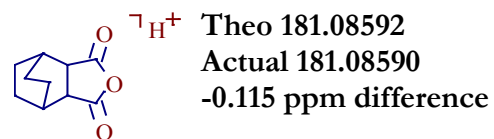
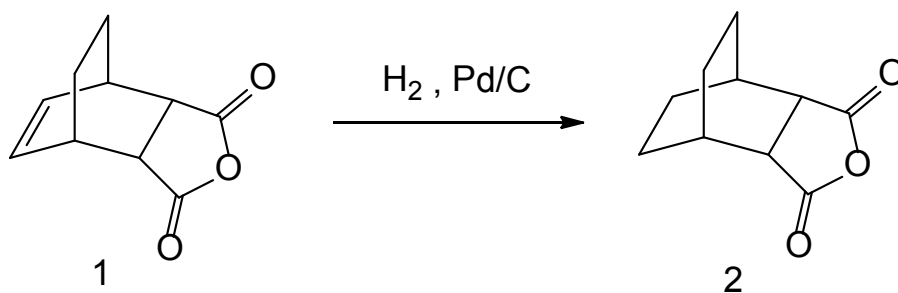


Figure S12. LC/MS data for the product resulting from the hydrogenation of the Diels Alder adduct in ethyl acetate using Pd/C and hydrogen (20 psi).

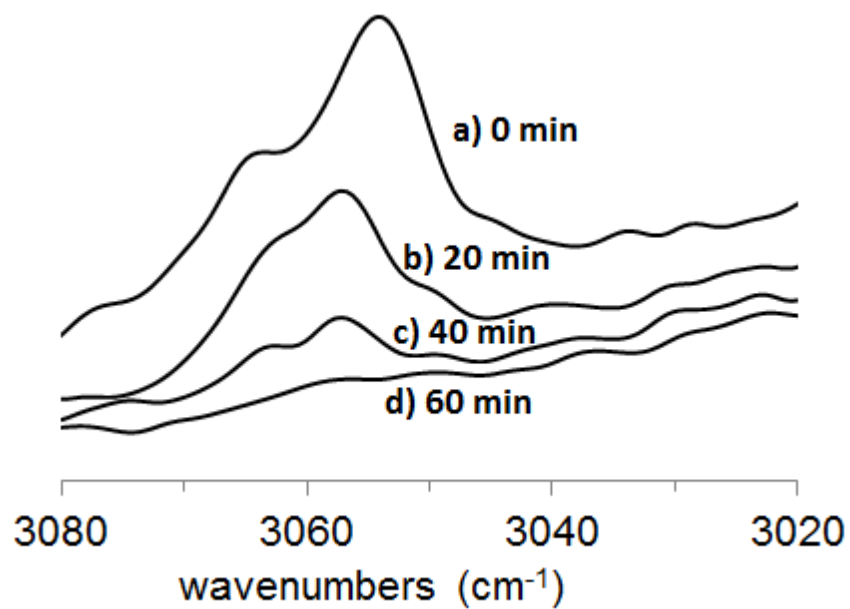


Figure S13. Overlay of FTIR spectra showing the disappearance of the alkene C-H absorbance (3055 cm^{-1}) at different time intervals during the hydrogenation of Diels Alder product (**1**). The data was used in Figure S14b.

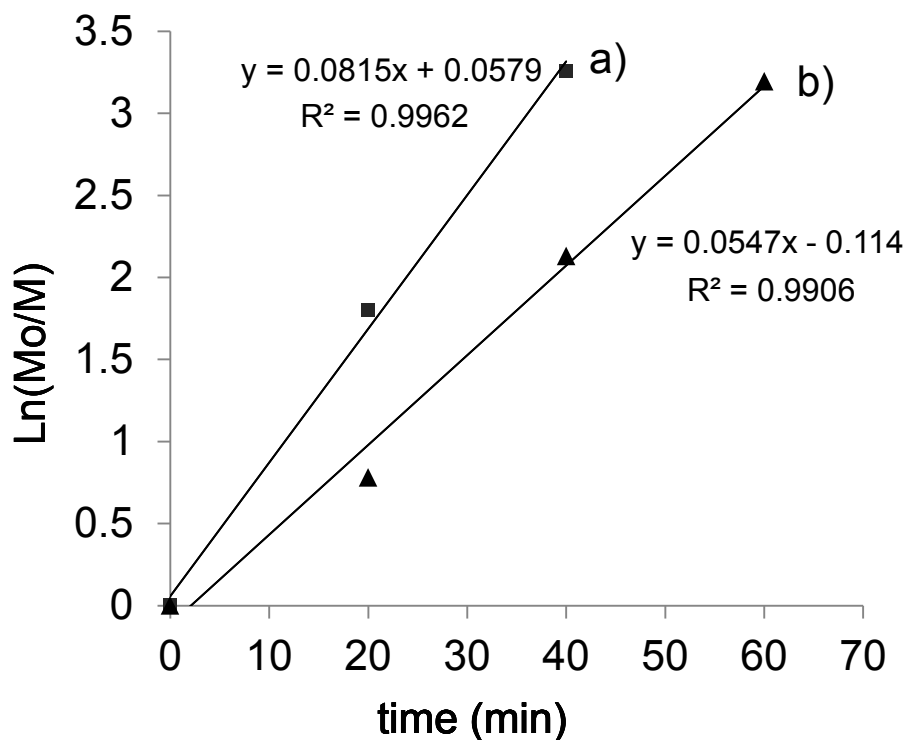


Figure S14. Comparison of continuous flow hydrogenation data for the hydrogenation of a) cyclooctene with b) Diels Alder product (monomer **1**). Both reactions were conducted in ethyl acetate at a concentration of 0.06 g/mL. The comparison of monomer **1** and cyclooctene used a continuous flow setup (1.8 mL/min) at ambient temperature with 0.50 g Pd/C and 125 psi hydrogen. Data for hydrogenation was collected and analyzed with GC (cyclooctene) and FTIR (monomer **1**).

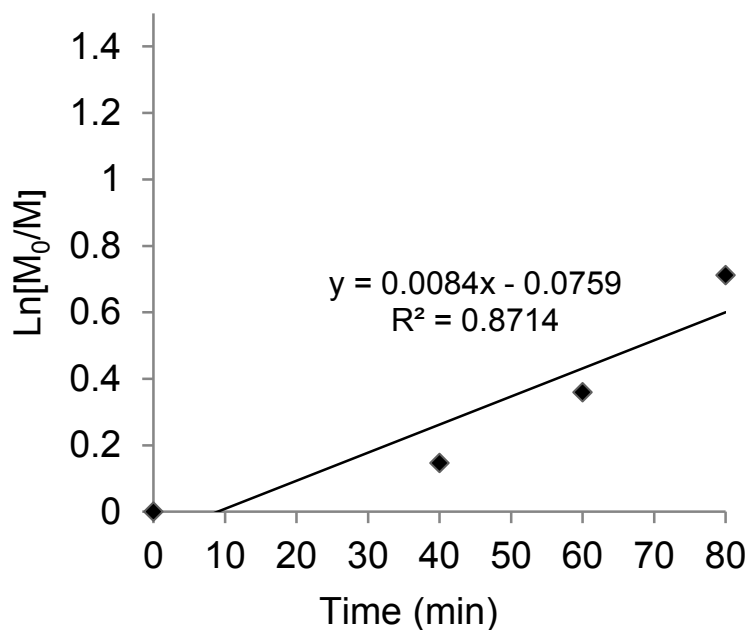


Figure S15. Continuous flow hydrogenation of Diels Alder product (monomer **1**) with less Pd/C than Figure S14. The reaction was conducted in ethyl acetate at a concentration of 0.06 g/mL and flow rate of 1.8 mL/min at ambient temperature with 0.30 g Pd/C and 125 psi hydrogen. The decrease in catalyst loading in Figure S15 gave a slower hydrogenation rate ($k_{\text{rel}} = 1$) compared to Figure S14b ($k_{\text{rel}} = 6.5$).

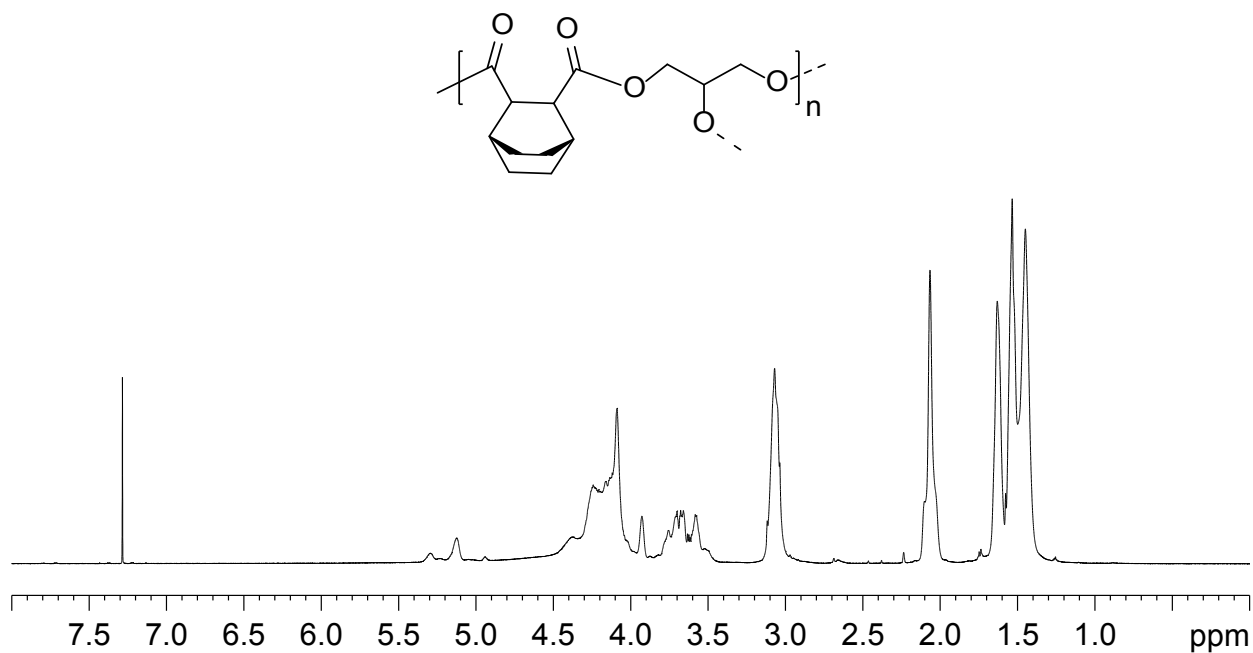


Figure S16. ¹H NMR spectrum (700 MHz, CDCl₃) of polyester synthesized from bicyclic anhydride **2** and glycerol after 24 h at 120 °C under dynamic vacuum (150 mbar).

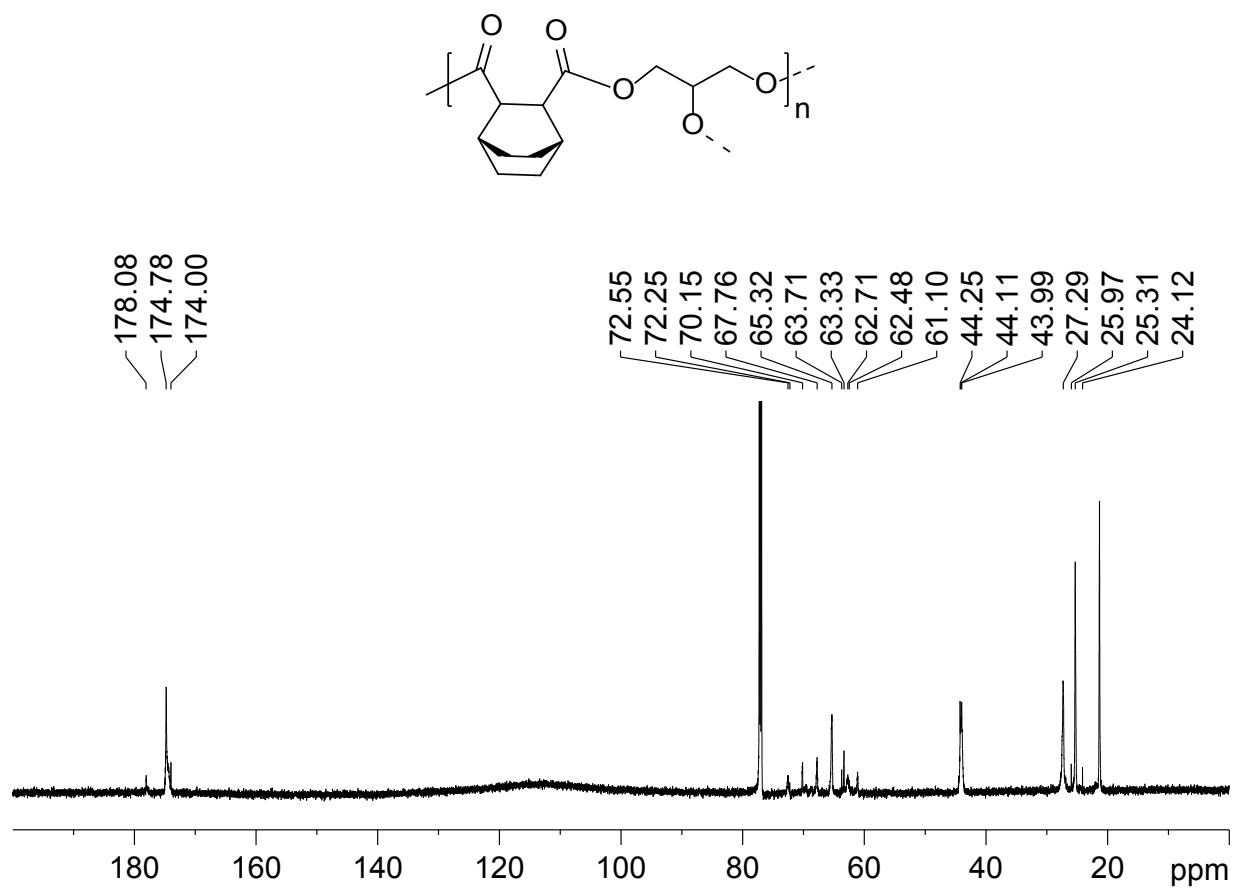


Figure S17. ^{13}C NMR spectrum (700 MHz, CDCl_3) of polyester synthesized from bicyclic anhydride **2** and glycerol after 24 h at 120 °C under dynamic vacuum (150 mbar).

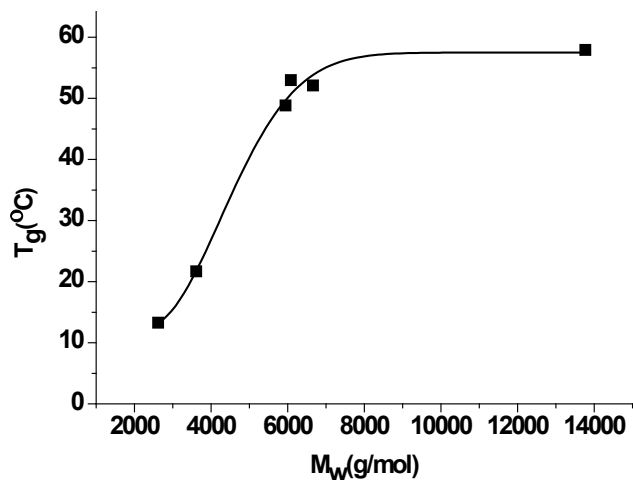


Figure S18. Dependence of glass transition temperature on M_w for the polymerization of glycerol with anhydride **2** ($[\text{glycerol}]/[\text{anhydride } \mathbf{2}] = 1$).

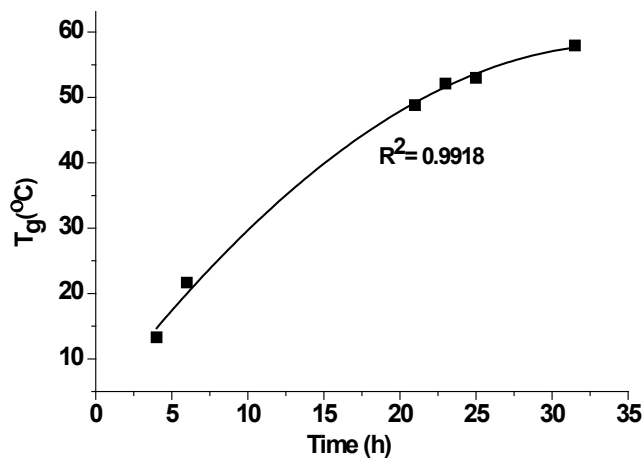


Figure S19. Correlation between the glass transition temperature and the reaction time for the polymerization of glycerol with anhydride **2** ($[\text{glycerol}]/[\text{anhydride } \mathbf{2}] = 1$).