

Supplementary Information

Compressed-air flow control system

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1. Channel geometries

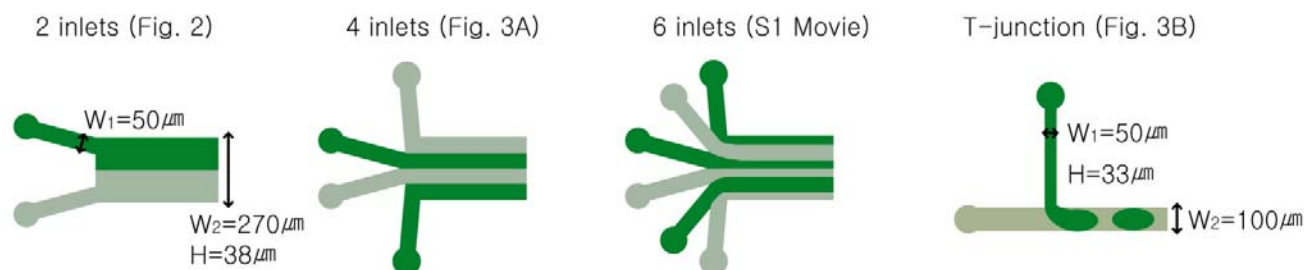


Figure S1. Schematic depicting the four types of channels used in this article. For the three channels generating laminar coflows, the dimensions were all identical; only the number of inlets differed.

2. Estimation of maximum fluid velocity

The following assumptions were made in the estimation:

1. Newtonian, incompressible, fully developed, and laminar flows
2. Negligible surface tension between solutions
3. Viscosity μ is the same (65 cP) in all inlet flow streams.
4. Pressure drop occurs in narrow inlet channels.
5. Negligible PDMS channel deformation for W (channel width) \sim H (channel height)¹

Basic Equations

For laminar flow in a pipe, the volumetric flow rate Q is given by the following equation²,

$$Q = \frac{AD_h^3}{32\mu L} (P_{\text{loss}}) \quad (1)$$

Hydraulic diameter of rectangular tubes is also given by the following equation².

$$D_h = \frac{2ab}{a+b} \quad (2) \quad \text{where } a = \text{width of a pipe and } b = \text{height of a pipe.}$$

Table S1. Inlet geometry for the channel used in Fig. 2.

Width, W_1	Area, A_1	Hydraulic Diameter, $D_{h,1}$	Length, L_1
50 μm	1900 μm^2	43 μm	4000 μm

Equation Setup

$$2Q_{\text{inlet}} = \frac{A_2 D_{h,2}^2}{16\mu L_2} (P) = Q_t \quad (3)$$

$$U_{\text{max}} = 1.5 U_{\text{avg}} = 1.5(Q_t/A_2) = 858 \times P \text{ (}\mu\text{m/s)} \quad (4)$$

3. Bead Tracking

A 0.02 % solution of 1.6 μm polystyrene beads in PEG-DA 700 was used to measure maximum fluid velocity (U_{max}). The bead velocity was maximum in the center of the channel, and midway between the two walls. After a given pressure was applied, beads in the center of the channel were followed with a 20X microscope objective (Zeiss) with an optivar setting of 2.5X leading to effective magnifications of 50X. Movies of translating beads were taken by a CCD camera that captured images at the rate of 30 fps using an exposure time of 1/500 s. From the frame-to-frame position of beads, bead velocities were calculated using the central difference approximation.

Table S2. Comparison between measured and estimated U_{max} .

P (Psi)	Measured U_{max} ($\mu\text{m/s}$) (From bead tracking)	Estimated U_{max} ($\mu\text{m/s}$) (From equation (4))	% Deviation from the estimation
0.5	591	429	37.8 %
1.0	954	858	11.1 %
1.5	1344	1288	4.4 %
2.0	1801	1717	4.9 %
2.5	2374	2146	10.6 %
3.0	2696	2575	4.7 %
3.5	3252	3005	8.2 %
4.0	3642	3434	6.0 %

4. Automation of pulsed-flow operation

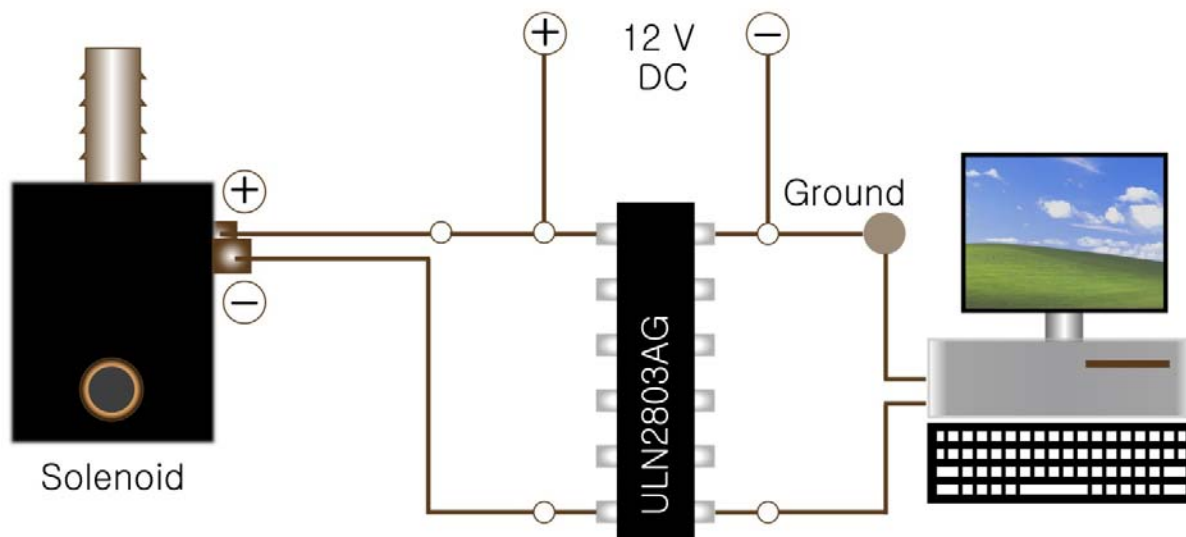


Figure S2. Schematic description of the electrical circuit used for automated control of the three-way solenoid valve via the parallel port connection. A simple GUI was constructed using Python to allow the user to cycle this process automatically through the specification of a flow duration and a stoppage duration.

5. A python script for the automation

A sample code for the GUI used to control the solenoid valve is provided as a separate pdf file.

6. Syringe Setup

In order to compare the response time of our system with that of a syringe setup, we performed additional bead tracking experiments with a two-inlet PDMS microchannel. For the syringe measurements, two Hamilton Gastight Syringes (Model 1701, 10 μ L volume) were driven on the same Harvard Apparatus PHD programmable syringe pump, with polyethylene feed tubing

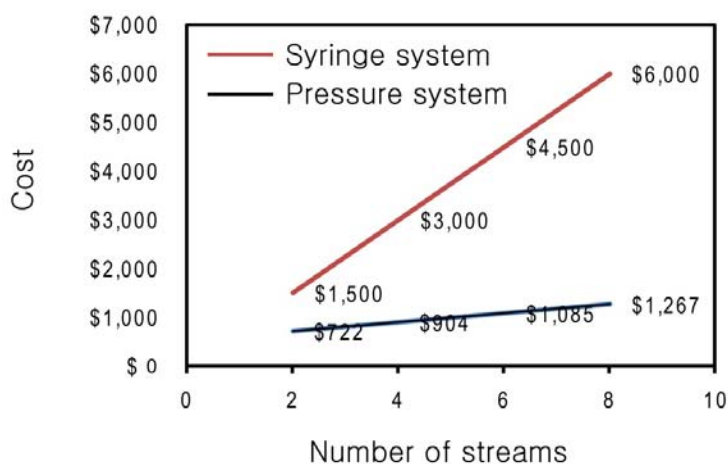
(1/16" I.D. and 1/8" O.D.) connected to the device via plastic adapter units. For the data collected in Fig. 4, the syringe pump was programmed so as to alternate between 1 s of flow at a prescribed flow rate and 1 s of stoppage. For the data collected in Table 1, the syringe pump was driven at a prescribed flow rate for 10 min and then manually stopped; the time required for suspended fluorescent beads to come to a stop was measured.

7. Cost Estimation

Table S3. Cost estimation for the compressed-air flow control system. Estimates are given for versions of the system capable of controlling 2, 4, 6, or 8 streams. Marginal cost of adding an additional stream is ~\$90.

Number of Streams	2	4	6	8
Swagelok Needle Valves	\$ 60.00	\$ 120.00	\$ 180.00	\$ 240.00
Solenoid Valve	\$ 50.00	\$ 50.00	\$ 50.00	\$ 50.00
High-P Pressure Regulator	\$ 100.00	\$ 100.00	\$ 100.00	\$ 100.00
Low-P Pressure Regulator	\$ 50.00	\$ 50.00	\$ 50.00	\$ 50.00
Digital Pressure Gauge	\$ 260.00	\$ 260.00	\$ 260.00	\$ 260.00
PTFE Tape	\$ 5.00	\$ 5.00	\$ 5.00	\$ 5.00
PVC Tubing	\$ 20.00	\$ 20.00	\$ 20.00	\$ 20.00
Tygon Tubing	\$ 10.00	\$ 10.00	\$ 10.00	\$ 10.00
Luer Stubs	\$ 7.20	\$ 12.00	\$ 16.80	\$ 21.60
Pipette Tips	\$ 9.00	\$ 18.00	\$ 27.00	\$ 36.00
Plastic Syringes	\$ 3.00	\$ 5.00	\$ 7.00	\$ 9.00
Circuit Components	\$ 20.00	\$ 20.00	\$ 20.00	\$ 20.00
In-Line Pressure Gauges	\$ 100.00	\$ 200.00	\$ 300.00	\$ 400.00
Plastic Connectors	\$ 7.50	\$ 13.50	\$ 19.50	\$ 25.50
Threaded Male Connectors	\$ 20.00	\$ 20.00	\$ 20.00	\$ 20.00
TOTAL	\$ 722	\$ 904	\$ 1,085	\$ 1,267

Figure S3. Cost comparison between syringe-based and pressure-based systems. The economic advantage of the pressure-based system is particularly evident in applications that require the control of a large number of streams.



8. Supplementary Video 1

Real-time video showing the manipulation of six coflowing laminar streams. Channel is 38 μm tall and 270 μm wide. Dark streams: 30% PEG-DA, 70% food coloring. Light streams: 30% PEG-DA, 70% water.

9. Supplementary Video 2

Video (0.5X real-time) showing the generation of droplets of different sizes. Droplet size is modulated in a continuous fashion by the gradual closing of the relief valve connected to the dispersed-phase sample arm. Channel is 33 μm tall and 100 μm wide. Dispersed phase: food coloring. Continuous phase: mineral oil.

10. Supplementary Video 3

Real-time video showing pulsed flow operation in a compressed-air flow control system followed by pulsed flow operation with a syringe pump system. Channel is 38 μm tall and 270 μm wide. Stream: 0.02 % solution of 1.6 μm polystyrene beads in PEG-DA.

11. References

- [1] Gervais, T., El-Ali, J., Günther, A., Jensen, K.F., *Lab Chip*. **2006**, 6, 500-507.
- [2] M. M. Denn, *Process Fluid Mechanics*, Prentice Hall, New Jersey, 1st edn., **1980**.