

## SUPPLEMENTARY MATERIAL

### Aggregation in solution of neutral half-sandwich Ru(II) precatalysts for transfer hydrogenation

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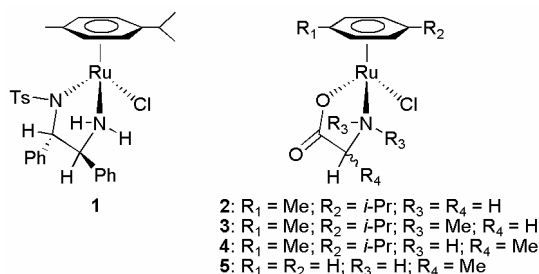
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Catalysts **1**,<sup>1</sup> **2-5**<sup>2</sup> (Scheme 1) and *trans*-[Ru(COMe)(CO){(pz<sub>2</sub>)BH<sub>2</sub>}(PMe<sub>3</sub>)<sub>2</sub>] (**6**)<sup>3</sup> were synthesized by the reaction of [Ru<sub>2</sub>(η<sup>6</sup>-arene)<sub>2</sub>Cl<sub>2</sub>(μ-Cl)<sub>2</sub>] with the appropriate N, X-ligand according to the literature. [Ru<sub>2</sub>(η<sup>6</sup>-arene)<sub>2</sub>Cl<sub>2</sub>(μ-Cl)<sub>2</sub>] were prepared as described by Benneth *et al.*<sup>4</sup> Deuterated solvents were purchased from Sigma and used without further purification.



Scheme 1

#### PGSE Measurements

All the PGSE NMR measurements were performed by using the standard stimulated echo pulse sequence<sup>5</sup> on a Bruker AVANCE DRX 400 spectrometer equipped with a GREAT 1/10 gradient unit and a QNP probe with a Z-gradient coil, at 296 K without spinning. The shape of the gradients was rectangular, their duration ( $\delta$ ) was 4-5 ms, and their strength (G) was varied during the experiments. All the spectra were acquired using 32K points, a spectral width of 5000 (<sup>1</sup>H), and processed with a line broadening of 1.0 Hz. After having checked

that the change of total relaxation time (from 5 to 15 s) does not affect the measurement results, standard experiments were carried out with a total recycle time of 5 s. The semi-logarithmic plots of  $\ln(I/I_0)$  vs  $G^2$  were fitted using a standard linear regression algorithm obtaining an  $R$  factor always better than 0.99. Different values of  $\Delta$ , “nt” (number of transients) and number of different gradient strengths ( $G$ ) were used for different samples. For example, for the measurements of solution of catalysts **1** in 2-propanol- $d_8$ , the “nt” was 48 ( $^1\text{H}$ ). The arene resonances (methyl and isopropyl for cymene) and methyl of Ts group for compound **1** were usually investigated.

The dependence of the resonance intensity ( $I$ ) on a constant waiting time and on a varied gradient strength ( $G$ ) is described by the equation 1:

$$\ln \frac{I}{I_0} = -(\gamma\delta)^2 D_t \left( \Delta - \frac{\delta}{3} \right) G^2 \quad (1)$$

where  $I$  = intensity of the observed spin echo,  $I_0$  = intensity of the spin echo without gradients,  $D$  = diffusion coefficient,  $\Delta$  = delay between the midpoints of the gradients,  $\delta$  = length of the gradient pulse, and  $\gamma$  = magnetogyric ratio. The diffusion coefficient  $D_t$  is directly proportional to the slope of the regression line ( $-m$ ) divided by  $\Delta - \delta/3$  and its value was estimated by measuring the  $-m/(\Delta - \delta/3)$  parameter for a sample of HDO (5%) in  $\text{D}_2\text{O}$  (known diffusion coefficient:  $1.902 \cdot 10^{-9} \text{ m}^2/\text{s}$  at 298 K)<sup>6</sup> under the same conditions as those for compounds.

According to the Stokes-Einstein equation 2,  $D_t$  is proportional to  $1/r_H$  (where  $r_H$  represents the hydrodynamic radius of the diffusing particle).

$$D_t = \frac{kT}{c\pi\eta r_H} \quad (2)$$

$k$  is the Boltzmann constant,  $T$  is the absolute temperature,  $c$  is a numerical factor that depends on the size and shape of the solute and the hydrodynamic behavior of the solute-solvent system<sup>7</sup>, and  $\eta$  is the viscosity of the pure solvent. By applying equations (2) to samples of catalyst containing TMSS as internal standard, the average hydrodynamic radii and  $c$  factors for the catalysts were estimated (Table 1).<sup>8</sup>

From the average hydrodynamic radii of the aggregates, assumed to be spherical, their volumes were obtained. The ratios of these volumes and the Van der Waals volumes of catalysts afforded the aggregation numbers  $N$  (Table 1). Van der Waals volumes of catalysts

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were computed from the crystal structures using the software package WebLab ViewerLite  
4.0.

The measurement uncertainty was estimated by determining the standard deviation of  $m$  by performing experiments with different  $\Delta$  values. Standard propagation of errors analysis yielded a standard deviation of approximately 8-9 % in the volume.

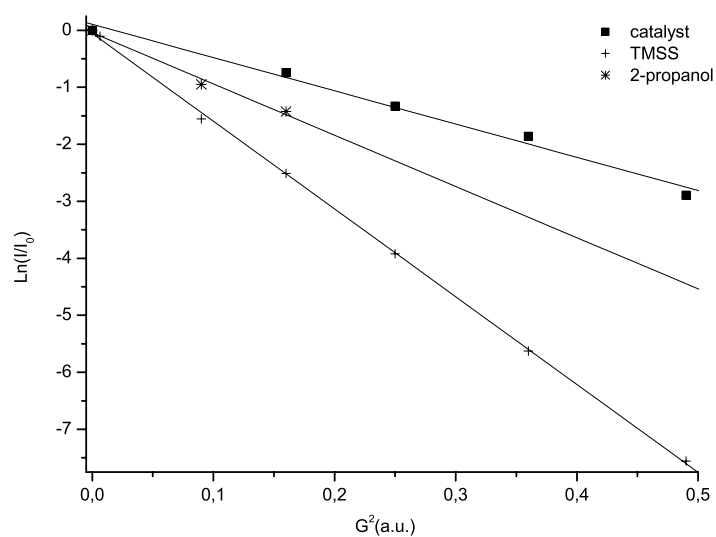
**Table 1S** Diffusion coefficients ( $10^{10}D_t$  m<sup>2</sup>s<sup>-1</sup>), hydrodynamic radii ( $r_H$ , Å),  $c$  factors, hydrodynamic volumes (Å<sup>3</sup>) and aggregation numbers (N) as a function of concentration (C, mM) in isopropanol-d<sub>8</sub>

Entry	Comp.	$D_t$	$r_H$	$c$	$V_H$	N	C
1	<b>1</b>	1.6	5.8	5.2	833	1.8	0.05
2	<b>1</b>	1.6	5.8	5.2	842	1.8	0.2
3	<b>1</b>	1.6	6.2	5.2	988	2.1	1.0
4	<b>1</b>	1.5	6.3	5.3	1051	2.3	4.0
5	<b>1</b>	1.4	6.7	5.4	1264	2.8	12.0
6	<b>1</b>	1.1	7.6	5.5	1823	4.0	42.0 <sup>a</sup>
7	<b>1<sup>b</sup></b>	6.1	6.4	5.5	1087	2.4	2.0
8	<b>1<sup>b</sup></b>	4.6	8.1	5.7	2242	4.9	12.0
9	<b>1<sup>c</sup></b>	11.4	5.8	5.3	815	1.8	2.0
10	<b>1<sup>d</sup></b>	6.3	5.8	5.5	834	1.8	2.0
11	<b>1<sup>e</sup></b>	1.6	6.6	5.5	1204	2.6	2.0
12	<b>2</b>	2.0	5.1	4.9	572	2.6	0.5
13	<b>2</b>	1.9	5.3	5.0	623	2.8	1.5
14	<b>2</b>	1.9	5.3	5.0	630	2.8	4.0 <sup>a</sup>
15	<b>3</b>	2.4	4.7	4.7	443	1.7	0.2
16	<b>3</b>	2.1	4.9	4.8	492	1.9	4.0
17	<b>3</b>	2.1	4.9	4.8	501	2.0	7.0 <sup>a</sup>
18	<b>3<sup>e</sup></b>	2.5	4.6	5.0	415	1.7	2.6
19	<b>4</b>	1.9	5.3	5.0	613	2.6	9.0
20	<b>4</b>	1.6	5.9	5.2	847	3.6	50.0
21	<b>5</b>	2.1	4.9	4.8	480	2.7	0.5 <sup>a</sup>
22	<b>5<sup>e</sup></b>	2.2	4.9	5.1	498	2.7	60.0
23	<b>6</b>	2.5	4.6	4.7	410	1.1	2.0
24	<b>6<sup>b</sup></b>	9.2	4.7	5.1	470	1.2	2.0
25	<b>6<sup>b</sup></b>	8.5	4.7	5.1	448	1.2	16.0
26	<b>6<sup>d</sup></b>	8.6	4.7	5.0	451	1.2	2.0
27	<b>6<sup>f</sup></b>	8.2	4.4	4.9	368	1.0	2.0

<sup>a</sup> Saturated solution. <sup>b</sup> In CDCl<sub>3</sub>. <sup>c</sup> In acetone-d<sub>6</sub>. <sup>d</sup> In methanol-d<sub>4</sub>. <sup>e</sup> In DMSO-d<sub>6</sub>. <sup>f</sup> In benzene-d<sub>6</sub>.

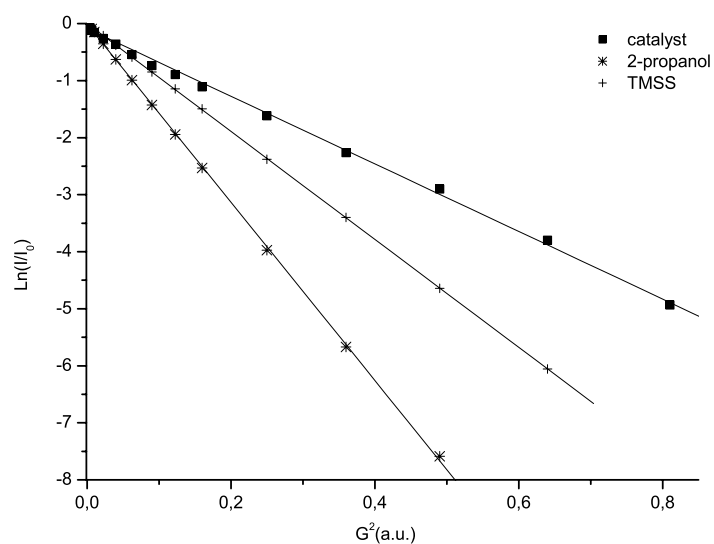
**Table 2S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **1** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 1)

$G^2$	0.05 $10^{-3}$ M. $\Delta = 90$ ms		
	catalyst	TMSS	2-propanol
1.00E-04	0	0	0
9.00E-02	-	-1.5563	-0.94655
0.49	-2.89137	-7.55481	-
0.36	-1.86033	-5.62525	-
0.25	-1.33026	-3.91975	-
0.16	-0.74297	-2.50939	-1.42582
0.0064	-	-0.10528	-



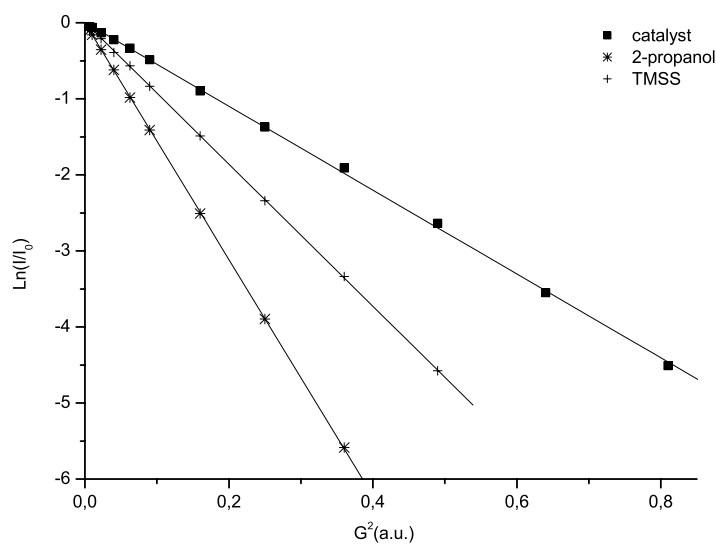
**Table 3S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **1** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 2).

$G^2$	$0.2 \cdot 10^{-3} \text{ M. } \Delta = 90 \text{ ms}$		
	catalyst	TMSS	2-propanol
1.00E-04	0	0	0
4.00E-04	-0.01229	-6.08E-05	-0.01471
0.0016	0.01043	-0.01725	-0.01622
0.0036	-0.00787	-0.04621	-0.03414
0.0064	-0.11504	-0.09501	-0.06277
0.01	-0.15879	-0.14922	-0.08562
0.0225	-0.26156	-0.35351	-0.21291
0.04	-0.35896	-0.62781	-0.38065
0.0625	-0.54226	-0.99347	-0.58992
0.09	-0.73631	-1.42655	-0.85006
0.1225	-0.89355	-1.94254	-1.14284
0.16	-1.10894	-2.534	-1.49377
0.25	-1.61733	-3.97364	-2.38153
0.36	-2.26242	-5.66799	-3.39704
0.49	-2.90008	-7.58887	-4.64136
0.64	-3.79639	-	-6.05554
0.81	-4.93338	-	-



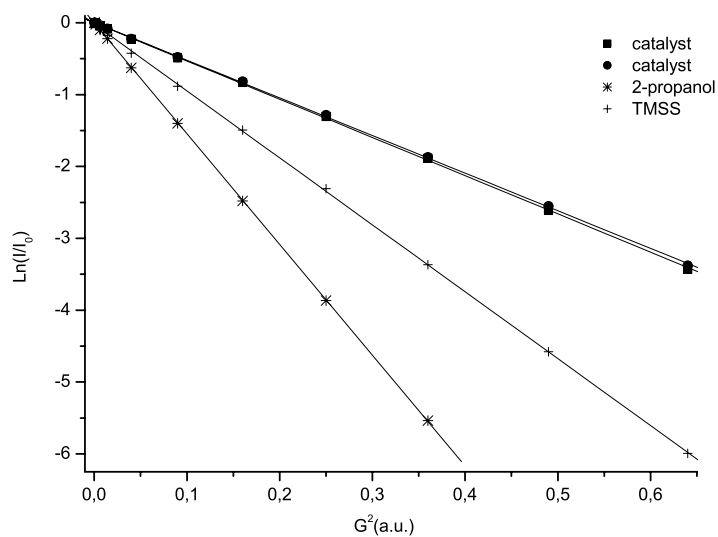
**Table 4S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **1** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 3)

$G^2$	$1 \cdot 10^{-3} \text{ M. } \Delta = 90 \text{ ms}$		
	catalyst	TMSS	2-propanol
1.00E-04	0	0	0
4.00E-04	-0.00484	-7.84E-03	-3.28E-05
0.0016	-9.03E-04	-0.0179	0.00859
0.0036	-0.01874	-0.05013	-0.02399
0.0064	-0.03587	-0.10063	-0.04405
0.01	-0.05994	-0.15706	-0.07661
0.0225	-0.13052	-0.35247	-0.20759
0.04	-0.22317	-0.62075	-0.39194
0.36	-1.90911	-5.58584	-3.33753
0.0625	-0.33356	-0.98187	-0.56539
0.09	-0.48626	-1.41017	-0.83493
0.16	-0.89468	-2.50991	-1.48727
0.25	-1.37198	-3.89411	-2.34043
0.49	-2.63794	-	-4.57413
0.64	-3.54932	-	-
0.81	-4.50717	-	-



**Table 5S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **1** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 4)

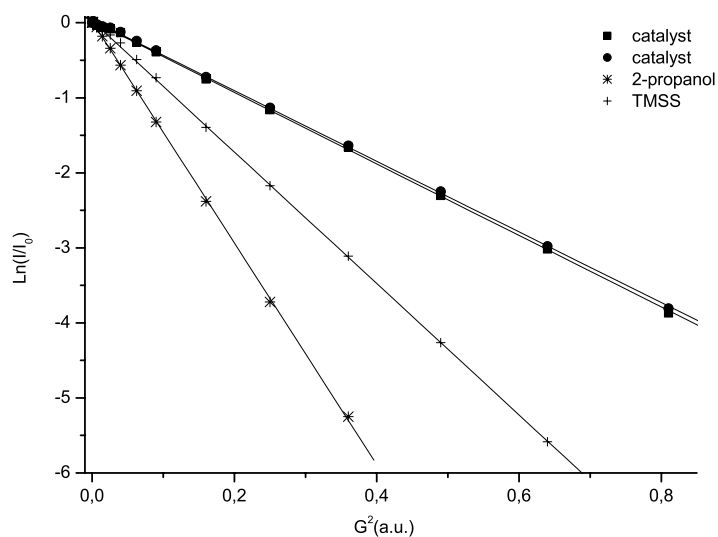
$G^2$	$4 \cdot 10^{-3} \text{ M. } \Delta = 90 \text{ ms}$			
	catalyst	catalyst	2-propanol	TMSS
1.00E-04	0	0	0	0
4.00E-04	5.12E-04	5.17E-03	1.09E-04	0.00934
0.0016	-9.98E-03	-0.00233	-0.0205	-0.01497
0.0064	-0.04077	-0.03645	-0.09804	-0.09289
0.0144	-0.08659	-0.08157	-0.22244	-0.17538
0.04	-0.22953	-0.22441	-0.62693	-0.42454
0.09	-0.48937	-0.47832	-1.40146	-0.88196
0.16	-0.83002	-0.81738	-2.47887	-1.49329
0.25	-1.30522	-1.28295	-3.8666	-2.30905
0.36	-1.88415	-1.86895	-5.53617	-3.36802
0.49	-2.61075	-2.5515	-	-4.58015
0.64	-3.43188	-3.37886	-	-5.99427





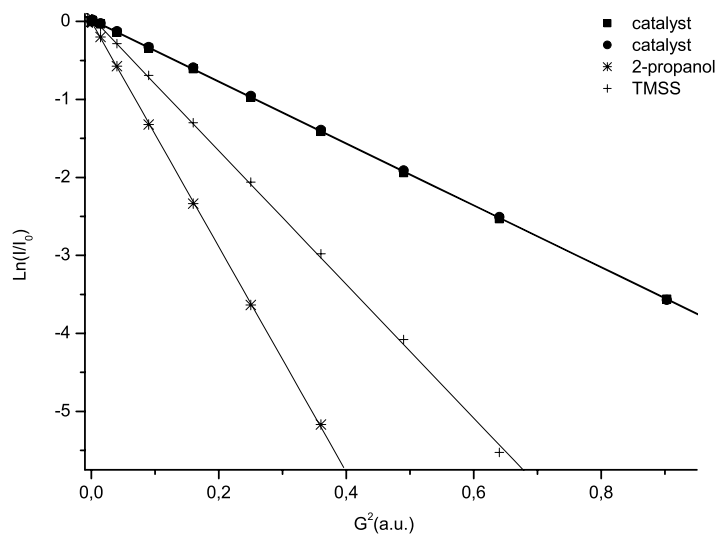
**Table 6S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **1** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 5)

$G^2$	$1.2 \cdot 10^{-2} \text{ M. } \Delta = 90 \text{ ms}$			
	catalyst	catalyst	2-propanol	TMSS
1.00E-04	0	0	0	0
4.00E-04	3.13E-03	1.05E-02	1.34E-02	0.00142
0.0016	1.26E-02	0.02392	0.00763	0.00429
0.0064	-0.03169	-0.0195	-0.05613	-0.06538
0.0144	-0.06016	-0.04586	-0.17767	-0.11294
0.0256	-0.082	-0.06451	-0.34046	-0.16375
0.04	-0.13206	-0.12052	-0.56578	-0.26776
0.0625	-0.26028	-0.24093	-0.90442	-0.49002
0.09	-0.38837	-0.3653	-1.32313	-0.73261
0.16	-0.74943	-0.7225	-2.37844	-1.3934
0.25	-1.15934	-1.13022	-3.71964	-2.17318
0.36	-1.65795	-1.63519	-5.24904	-3.11094
0.49	-2.29983	-2.24742	-	-4.26381
0.64	-3.01421	-2.97573	-	-5.58289
0.81	-3.86922	-3.80605	-	-



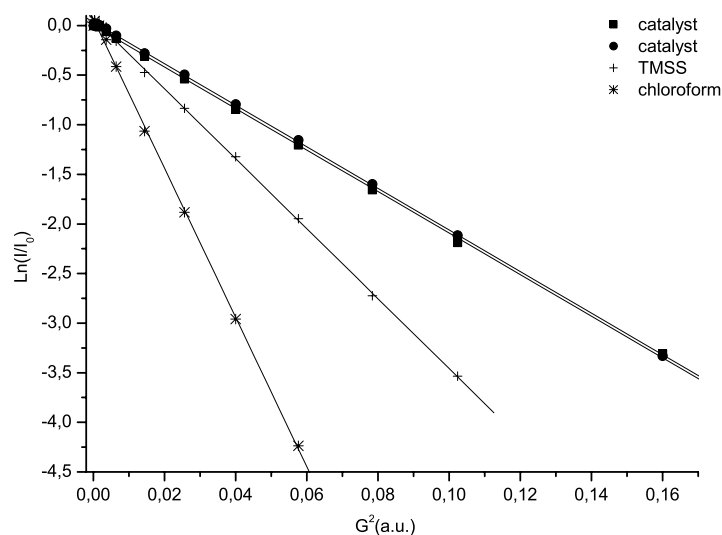
**Table 7S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **1** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 6)

$G^2$	$4.2 \cdot 10^{-2}$ M. $\Delta = 90$ ms			
	catalyst	catalyst	2-propanol	TMSS
1.00E-04	0	0	0	0
4.00E-04	7.72E-03	1.41E-02	-5.78E-03	0.03556
0.0016	1.34E-02	0.02438	-0.01365	0.02985
0.0144	-0.03249	-0.02023	-0.19795	-0.07138
0.04	-0.14044	-0.12186	-0.57282	-0.28323
0.09	-0.3411	-0.32817	-1.32018	-0.69037
0.16	-0.60734	-0.59012	-2.33458	-1.29722
0.25	-0.97369	-0.9533	-3.63555	-2.05986
0.36	-1.4093	-1.39011	-5.17014	-2.97907
0.49	-1.93844	-1.90885	-	-4.07833
0.64	-2.53055	-2.50646	-	-5.52773
0.9025	-3.55993	-3.5717	-	-



**Table 8S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **1** in chloroform-d at 296 K using TMSS as internal standard (entry 7)

$G^2$	$2.0 \cdot 10^{-3}$ M. $\Delta = 90$ ms			
	catalyst	catalyst	TMSS	chloroform
0,0001	0	0	0	0
0,0004	0,00306	0,02218	0,05798	0,04497
0,0016	-0,01405	0,00824	0,04095	-0,00133
0,0036	-0,06107	-0,02801	-0,01258	-0,14367
0,0064	-0,12869	-0,10137	-0,15732	-0,41475
0,0144	-0,30889	-0,27859	-0,47232	-1,06451
0,0256	-0,53672	-0,49337	-0,83387	-1,88316
0,04	-0,84552	-0,79244	-1,32201	-2,95868
0,0576	-1,20316	-1,15385	-1,94731	-4,23713
0,0784	-1,65603	-1,59942	-2,7244	-
0,1024	-2,18621	-2,11565	-3,53579	-
0,16	-3,311	-3,32981	-	-

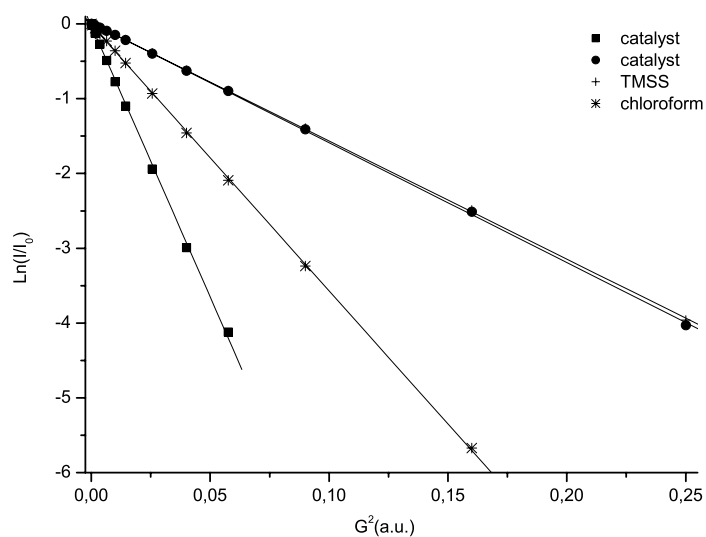


**Table 9S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **1** in chloroform-d at 296 K using TMSS as internal standard (entry 8)

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$G^2$	$1.2 \cdot 10^{-2}$ M. $\Delta = 90$ ms			
	catalyst	catalyst	TMSS	chloroform
1.00E-04	0	0	0	0
4.00E-04	-0.02124	-0.00622	0.00247	-0.01571
0.0016	-0.12196	-0.02093	-0.02221	-0.05842
0.0036	-0.26987	-0.05014	-0.04499	-0.13132
0.0064	-0.48903	-0.09015	-0.09193	-0.23027
0.01	-0.77268	-0.14712	-0.14793	-0.35845
0.0144	-1.09897	-0.21365	-0.20944	-0.52301
0.0256	-1.94019	-0.39586	-0.38606	-0.93076
0.04	-2.99177	-0.6249	-0.61829	-1.45762
0.0576	-4.1224	-0.8971	-0.8898	-2.09028
0.09	-	-1.40995	-1.39284	-3.23912
0.16	-	-2.513	-2.48622	-5.67286
0.25	-	-4.02691	-3.9586	-

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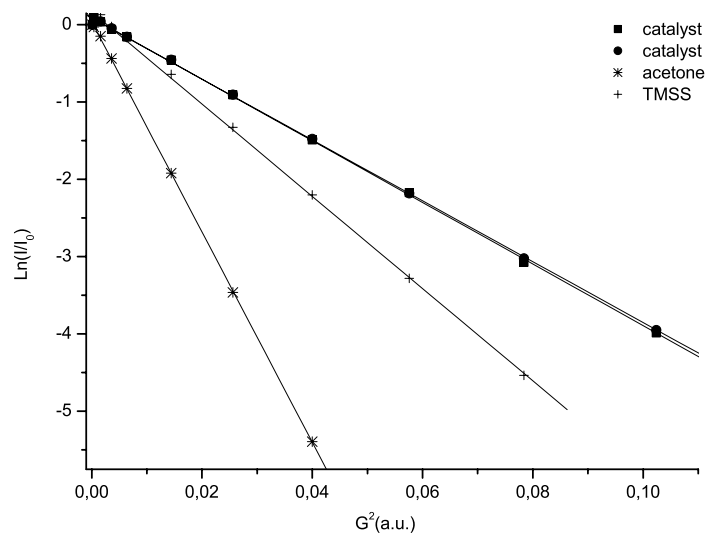


**Table 10S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **1** in acetone- $d_6$  at 296 K using TMSS as internal standard (entry 9)

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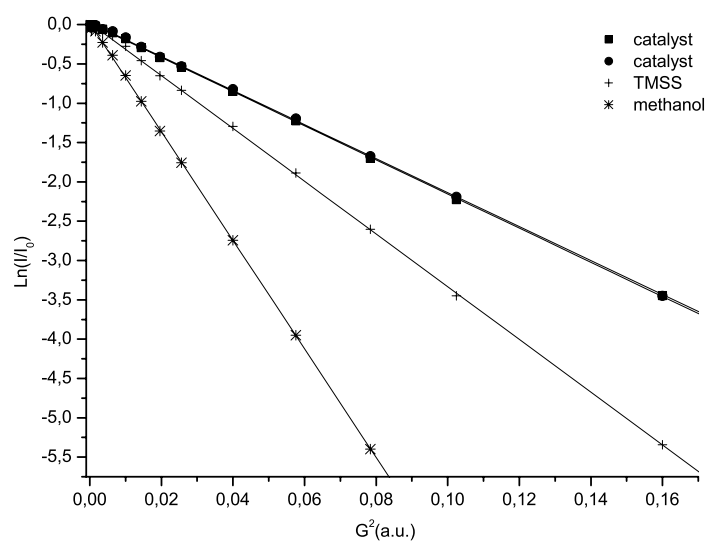
$G^2$	catalyst	$2 \cdot 10^{-3}$ M. $\Delta = 90$ ms catalyst	acetone	TMSS
1.00E-04	0	0	0	0
4.00E-04	1.15E-01	5.32E-02	-2.99E-02	0.10968
0.0016	3.65E-02	0.04287	-0.14919	0.12967
0.0036	-0.058	-0.0448	-0.4347	-0.02354
0.0064	-0.15953	-0.15493	-0.82201	-0.16727
0.0144	-0.45575	-0.45417	-1.92052	-0.64068
0.0256	-0.90498	-0.90128	-3.46093	-1.32701
0.04	-1.48751	-1.47456	-5.39326	-2.20225
0.0576	-2.17205	-2.18044	-	-3.28098
0.0784	-3.07313	-3.02152	-	-4.53595
0.1024	-3.98588	-3.94766	-	-

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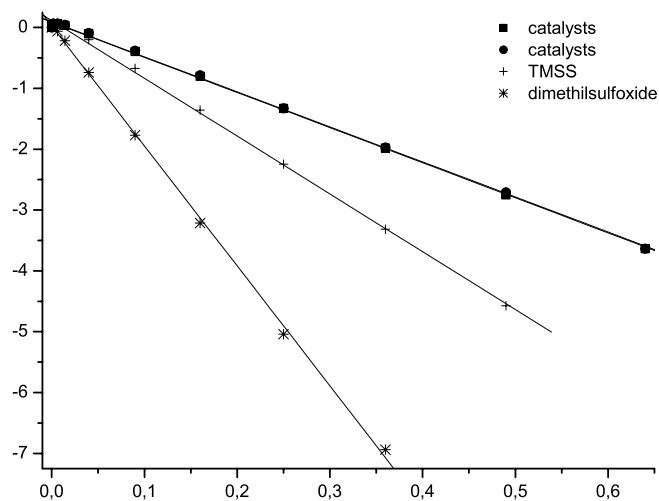
**Table 11S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **1** in methanol- $d_4$  at 296 K using TMSS as internal standard (entry 10)

$G^2$	$2 \cdot 10^{-3}$ M. $\Delta = 90$ ms			
	catalyst	catalyst	TMSS	methanol
1.00E-04	0	0	0	0
4.00E-04	-9.14E-03	-3.66E-02	-7.81E-02	-0.04423
0.0016	-1.82E-02	-0.0052	-0.01807	-0.08428
0.0036	-0.05859	-0.05837	-0.10735	-0.22752
0.0064	-0.10312	-0.08298	-0.14042	-0.38961
0.01	-0.17865	-0.16171	-0.27499	-0.64738
0.0144	-0.29297	-0.28339	-0.45861	-0.97484
0.0196	-0.41797	-0.40797	-0.65112	-1.35386
0.0256	-0.53906	-0.52902	-0.83677	-1.75785
0.04	-0.84791	-0.81788	-1.29297	-2.74322
0.0576	-1.2216	-1.19174	-1.887	-3.94996
0.0784	-1.69967	-1.6723	-2.60275	-5.39856
0.1024	-2.22433	-2.18915	-3.44864	-
0.16	-3.44615	-3.44823	-5.34343	-



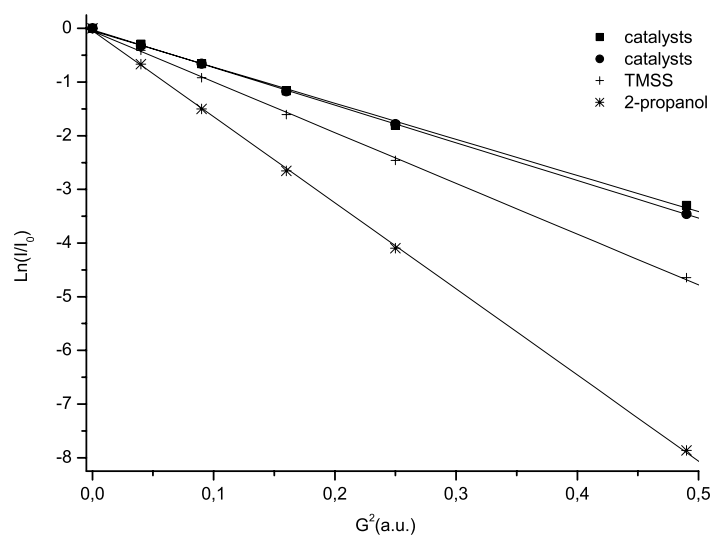
**Table 12S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **1** in dimethylsulfoxide- $d_6$  at 296 K using TMSS as internal standard (entry 11)

$G^2$	catalyst	$2 \cdot 10^{-3}$ M. $\Delta = 90$ ms catalyst	TMSS	DMSO
1.00E-04	0	0	0	0
4.00E-04	3.10E-02	3.32E-02	2.75E-02	0.01734
0.0016	6.34E-02	0.06529	0.07482	0.01796
0.0064	0.05928	0.06691	0.07266	-0.06161
0.0144	0.03405	0.04253	0.03403	-0.2154
0.04	-0.1026	-0.09222	-0.19903	-0.74035
0.09	-0.39336	-0.38209	-0.67179	-1.7712
0.16	-0.80046	-0.78624	-1.35968	-3.21406
0.25	-1.32988	-1.3271	-2.24403	-5.04055
0.36	-1.97863	-1.97101	-3.31671	-6.93813
0.49	-2.74908	-2.71056	-4.57379	-
0.64	-3.63552	-3.63568	-	-



**Table 13S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **2** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 12)

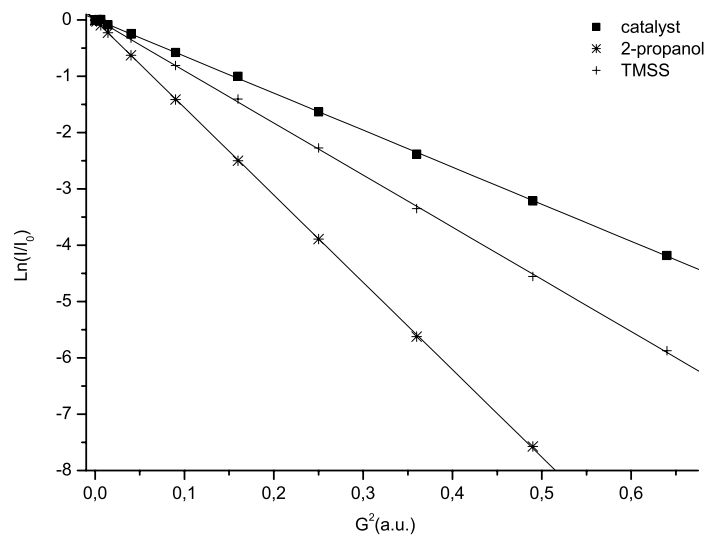
$G^2$	catalyst	$0.5 \cdot 10^{-3}$ M. $\Delta = 90$ ms catalyst	TMSS	2-propanol
1.00E-04	0	0	0	0
0.04	-2.95E-01	-0.32045	-0.40843	-0.66379
0.09	-0.65768	-0.65636	-0.91983	-1.50288
0.16	-1.1623	-1.172	-1.60662	-2.65472
0.25	-1.80352	-1.78212	-2.46123	-4.09429
0.49	-3.29725	-3.45511	-4.64449	-7.86385





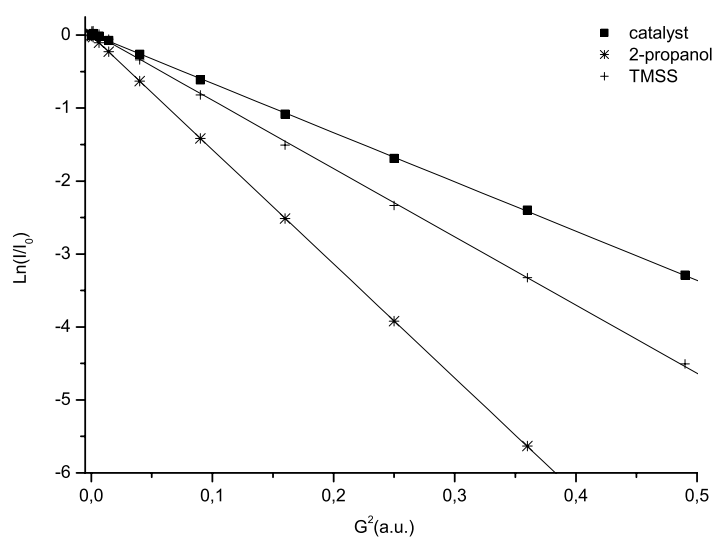
**Table 14S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **2** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 13).

$G^2$	$1.5 \cdot 10^{-3}$ M. $\Delta = 90$ ms		
	catalyst	2-propanol	TMSS
1.00E-04	0	0	0
4.00E-04	-9.21E-03	-0.0074	-0.01837
0.04	-0.24015	-0.62881	-0.32349
0.0064	0.00776	-0.09621	0.00719
0.0144	-0.08803	-0.22582	-0.11198
0.49	-3.21254	-7.5717	-4.55423
0.09	-0.57691	-1.41198	-0.80809
0.16	-0.99958	-2.49904	-1.40483
0.25	-1.63157	-3.88923	-2.27444
0.36	-2.38045	-5.62307	-3.34894
0.0016	-0.00211	-0.02512	-0.01273
0.64	-4.18106	-	-5.87202



**Table 15S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **2** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 14)

$G^2$	$4 \cdot 10^{-3}$ M. $\Delta = 90$ ms		
	catalyst	2-propanol	TMSS
1.00E-04	0	0	0
4.00E-04	8.26E-03	-0.01177	0.05636
0.0016	0.02344	-0.02665	0.06001
0.0064	-0.01146	-0.10489	0.01505
0.0144	-0.0722	-0.22848	-0.05467
0.04	-0.26049	-0.63157	-0.3396
0.09	-0.61388	-1.4168	-0.82006
0.16	-1.08435	-2.51535	-1.50613
0.25	-1.68967	-3.91953	-2.33362
0.36	-2.39849	-5.6327	-3.32341
0.49	-3.28996	-	-4.50527

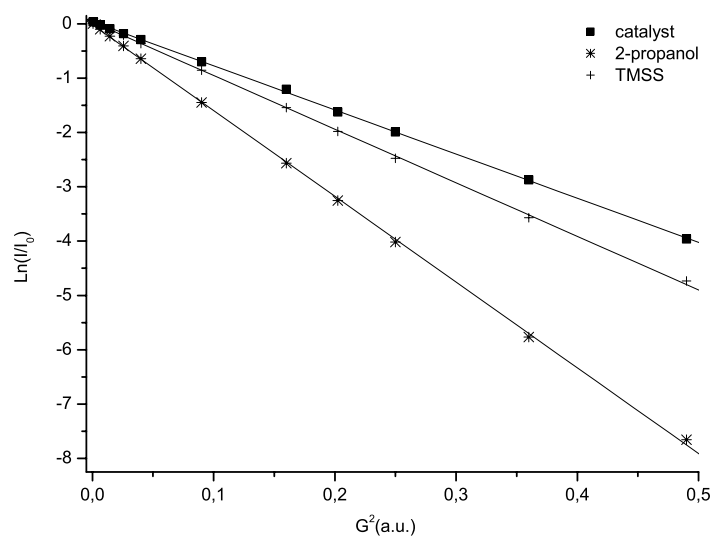


**Table 16S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **3** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 15)

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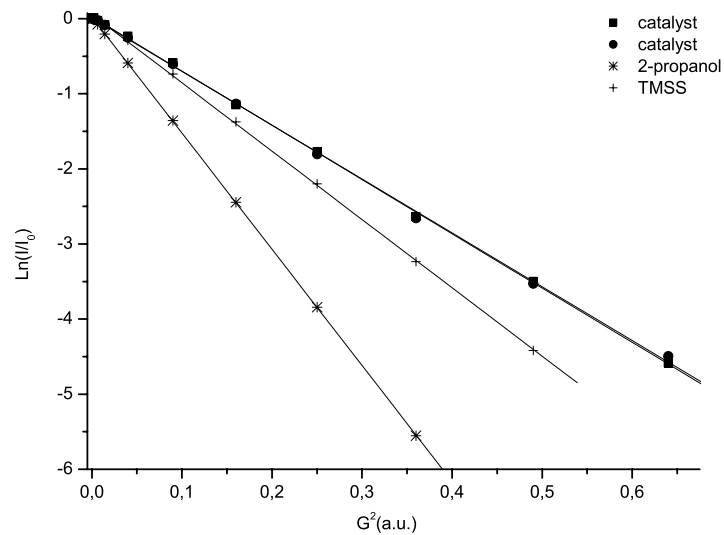
$G^2$	$0.2 \cdot 10^{-3} \text{ M. } \Delta = 90 \text{ ms}$		
	catalyst	2-propanol	TMSS
4.00E-04	3.63E-02	0.00425	0.03279
0.04	-0.28686	-0.64287	-0.36375
0.16	-1.20191	-2.56746	-1.54071
0.49	-3.96063	-7.65503	-4.73396
0.0064	-0.01464	-0.09966	-0.00267
0.0144	-0.09221	-0.22769	-0.09327
0.0256	-0.18094	-0.40628	-0.20906
0.09	-0.69712	-1.44566	-0.85309
0.2025	-1.62176	-3.2527	-1.97863
0.25	-1.98961	-4.01784	-2.47542
0.36	-2.87146	-5.76652	-3.57125

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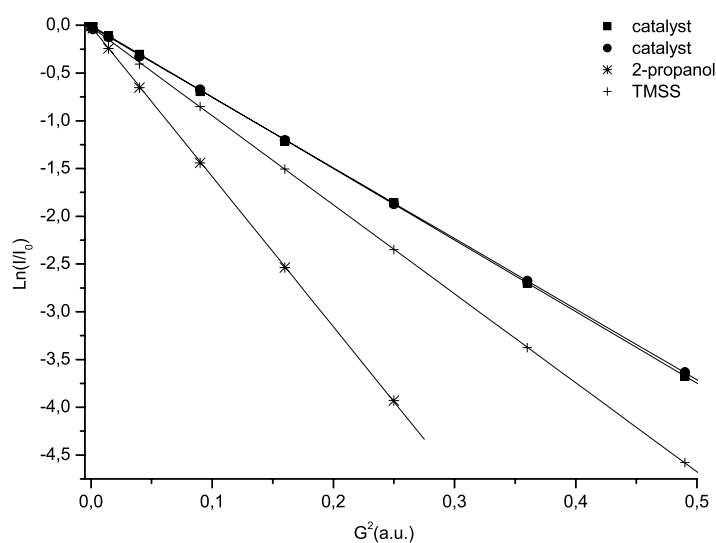
**Table 17S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **3** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 16)

$G^2$	4 $10^{-3}$ M. $\Delta = 90$ ms			
	catalyst	catalyst	2-propanol	TMSS
1.00E-04	0	0	0	0
4.00E-04	0.0117	0.02	0.01484	0.05361
0.0016	0.02232	0.01776	9.93E-04	0.04796
0.0064	-0.02545	-0.02116	-0.07583	-0.01325
0.0144	-0.08027	-0.08195	-0.20417	-0.08378
0.04	-0.23044	-0.25381	-0.58847	-0.28967
0.09	-0.5858	-0.60402	-1.35571	-0.73496
0.16	-1.14392	-1.13103	-2.44361	-1.37239
0.25	-1.7684	-1.8024	-3.84162	-2.19771
0.36	-2.63611	-2.65684	-5.55453	-3.23372
0.49	-3.49875	-3.52919	-	-4.41864
0.64	-4.58626	-4.49371	-	-



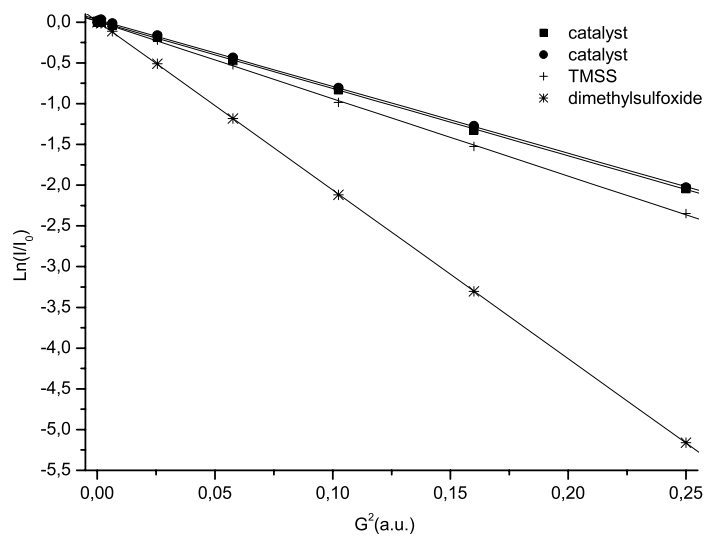
**Table 18S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **3** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 17)

$G^2$	7 $10^{-3}$ M. $\Delta = 90$ ms			
	catalyst	catalyst	2-propanol	TMSS
1.00E-04	0	0	0	0
4.00E-04	0.00355	0.00242	-0.01045	-0.00354
0.0016	-0.00584	-0.04012	-3.19E-02	-0.04507
0.0144	-0.10859	-0.12315	-0.24353	-0.15427
0.04	-0.30432	-0.32607	-0.6529	-0.40707
0.09	-0.69354	-0.67196	-1.4398	-0.85048
0.16	-1.212	-1.20221	-2.5372	-1.5054
0.25	-1.85751	-1.87098	-3.92912	-2.3498
0.36	-2.69951	-2.67577	-	-3.37442
0.49	-3.67303	-3.63206	-	-4.57756
0.64	-	-	-	-



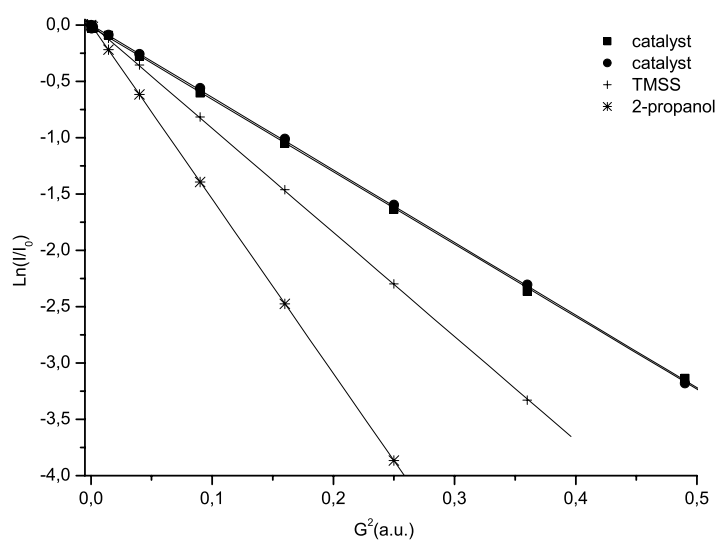
**Table 19S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **3** in dimethylsulfoxide- $d_6$  at 296 K using TMSS as internal standard (entry 18)

$G^2$	$2.6 \cdot 10^{-3} \text{ M. } \Delta = 90 \text{ ms}$			
	catalyst	catalyst	TMSS	DMSO
1.00E-04	0	0	0	0
4.00E-04	0.01197	0.02169	0.01309	0.005
0.0016	0.00284	0.03285	-0.00216	-0.01323
0.0064	-0.03984	-0.01163	-0.04267	-0.11094
0.0256	-0.18179	-0.16021	-0.22165	-0.51071
0.0576	-0.46177	-0.43303	-0.52342	-1.1824
0.1024	-0.83166	-0.80543	-0.98507	-2.11852
0.16	-1.32473	-1.27471	-1.52421	-3.30232
0.25	-2.04391	-2.02674	-2.34735	-5.16049



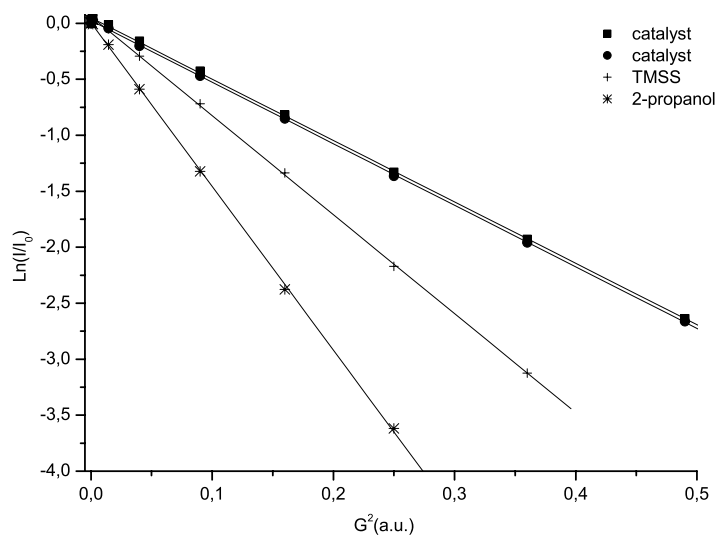
**Table 20S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **4** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 19)

$G^2$	catalyst	$9 \cdot 10^{-3}$ M. $\Delta = 90$ ms catalyst	TMSS	2-propanol
1.00E-04	0	0	0	0
4.00E-04	-0.02739	-0.02912	-0.00513	-0.00947
0.0016	-0.0303	-0.01752	-0.02005	-0.01695
0.0144	-0.08983	-0.08584	-0.11826	-0.21733
0.04	-0.27531	-0.25702	-0.35437	-0.61488
0.09	-0.60164	-0.55979	-0.81672	-1.39221
0.16	-1.048	-1.0095	-1.46155	-2.47399
0.25	-1.63339	-1.59438	-2.29688	-3.86593
0.36	-2.36364	-2.30559	-3.33015	-
0.49	-3.13711	-3.17842	-	-



**Table 21S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **4** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 20)

$G^2$	$5.0 \cdot 10^{-2}$ M. $\Delta = 90$ ms			
	catalyst	catalyst	TMSS	2-propanol
1.00E-04	0	0	0	0
4.00E-04	0.03077	0.03153	0.05432	0.01017
0.0016	0.06332	0.02578	0.07239	-0.00724
0.0144	-0.0115	-0.04322	-0.04815	-0.19104
0.04	-0.15896	-0.20246	-0.29321	-0.58747
0.09	-0.42511	-0.46889	-0.71866	-1.32158
0.16	-0.81606	-0.85039	-1.33693	-2.37598
0.25	-1.32974	-1.36302	-2.16976	-3.61863
0.36	-1.928	-1.9583	-3.12368	-
0.49	-2.63792	-2.6632	-	-



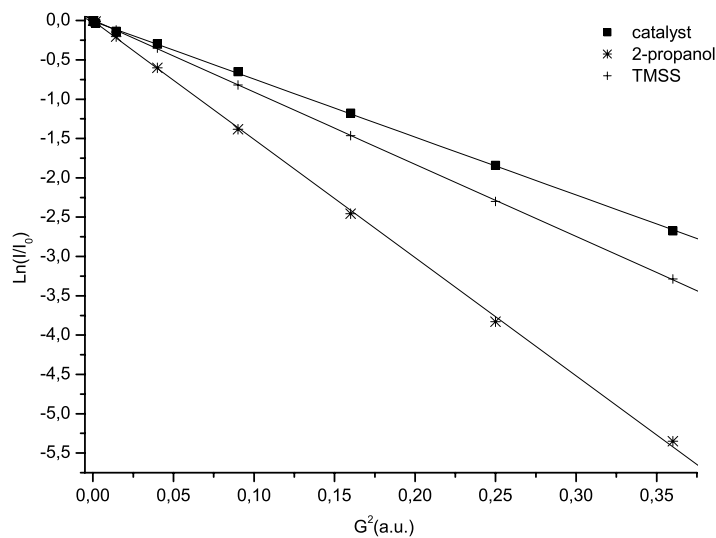


**Table 22S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **5** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 21)

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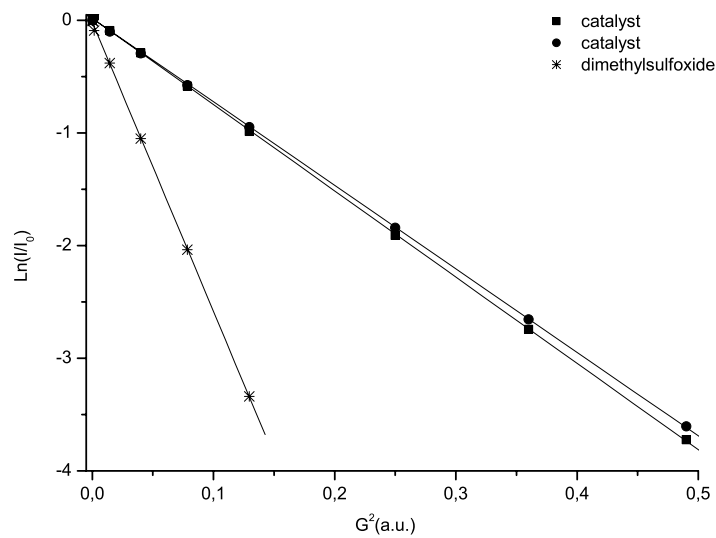
$G^2$	$0.5 \cdot 10^{-3} \text{ M. } \Delta = 90 \text{ ms}$		
	catalyst	2-propanol	TMSS
1.00E-04	0	0	0
4.00E-04	-0.01328	4.25E-04	0.00195
0.0016	-0.03588	-0.01096	-0.00174
0.0144	-0.13687	-0.20493	-0.12053
0.04	-0.29662	-0.60209	-0.34971
0.09	-0.64848	-1.38342	-0.81798
0.16	-1.17806	-2.45591	-1.46401
0.25	-1.84147	-3.83025	-2.29938
0.36	-2.6753	-5.35123	-3.28736

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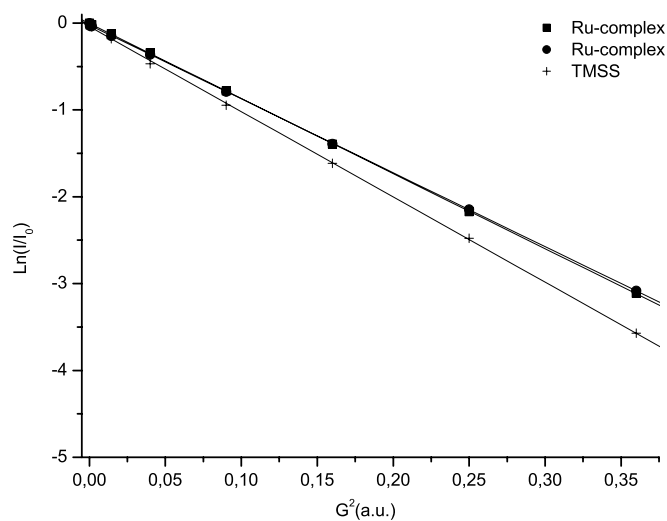
**Table 23S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **5** in dimethylsulfoxide- $d_6$  at 296 K using TMSS as internal standard (entry 22)

$G^2$	$6.0 \cdot 10^{-2}$ M. $\Delta = 90$ ms		DMSO
	catalyst	catalyst	
1.00E-04	0	0	0
4.00E-04	0.0149	1.57E-02	-0.00585
0.0016	0.0386	0.0632	-0.09195
0.0144	-0.09136	-0.09978	-0.38019
0.04	-0.28866	-0.29336	-1.05069
0.0784	-0.5846	-0.57481	-2.03604
0.1296	-0.98645	-0.94799	-3.33862
0.25	-1.90846	-1.84193	-
0.36	-2.74425	-2.6556	-
0.49	-3.72207	-3.60368	-



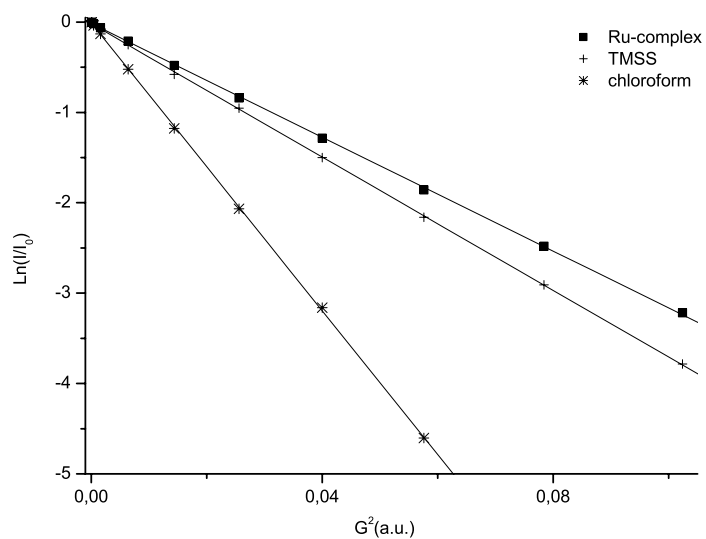
**Table 24S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **6** in 2-propanol- $d_8$  at 296 K using TMSS as internal standard (entry 23)

$G^2$	$2 \cdot 10^{-3}$ M. $\Delta = 90$ ms		
	Ru-complex	Ru-complex	TMSS
1.00E-04	0	0	0
4.00E-04	-0.02057	-0.03239	-0.04151
0.0016	-0.01819	-0.0364	-0.04554
0.0144	-0.12369	-0.14715	-0.17865
0.04	-0.34057	-0.36363	-0.46962
0.09	-0.77973	-0.78923	-0.94449
0.16	-1.39279	-1.39173	-1.61328
0.25	-2.17166	-2.14406	-2.4769
0.36	-3.11238	-3.08225	-3.57111



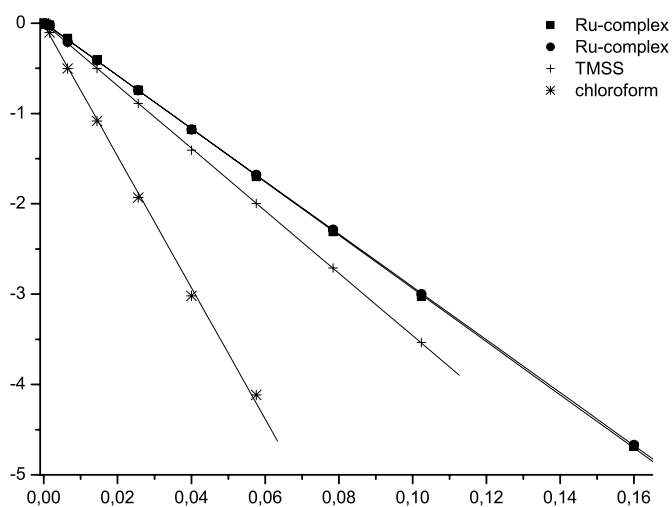
**Table 25S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **6** in chloroform-d at 296 K using TMSS as internal standard (entry 24)

$G^2$	$2 \cdot 10^{-3}$ M. $\Delta = 90$ ms		
	Ru-complex	TMSS	chloroform
1.00E-04	0	0	0
4.00E-04	-0.01753	-0.03378	-0.03878
0.0016	-0.06305	-0.07464	-0.13081
0.0064	-0.2111	-0.24904	-0.5233
0.0144	-0.47876	-0.5795	-1.17798
0.0256	-0.83847	-0.95295	-2.06708
0.04	-1.28493	-1.50077	-3.16109
0.0576	-1.85822	-2.16118	-4.60439
0.0784	-2.47985	-2.90973	-
0.1024	-3.21744	-3.78372	-



**Table 26S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **6** in chloroform-d at 296 K using TMSS as internal standard (entry 25)

$G^2$	$1.6 \cdot 10^{-2} \text{ M. } \Delta = 90 \text{ ms}$			
	Ru-complex	Ru-complex	TMSS	chloroform
1.00E-04	0	0	0	0
4.00E-04	-0.01532	-0.00298	-0.0164	-0.01729
0.0016	-0.02145	-0.01774	-0.04443	-0.10407
0.0064	-0.16716	-0.20883	-0.22007	-0.50216
0.0144	-0.40696	-0.41237	-0.50278	-1.08323
0.0256	-0.74034	-0.74384	-0.88859	-1.93148
0.04	-1.17639	-1.17729	-1.40614	-3.01977
0.0576	-1.69966	-1.67812	-1.99621	-4.11522
0.0784	-2.30865	-2.28608	-2.70991	-
0.1024	-3.02291	-2.99872	-3.53476	-
0.16	-4.68471	-4.6671	-	-

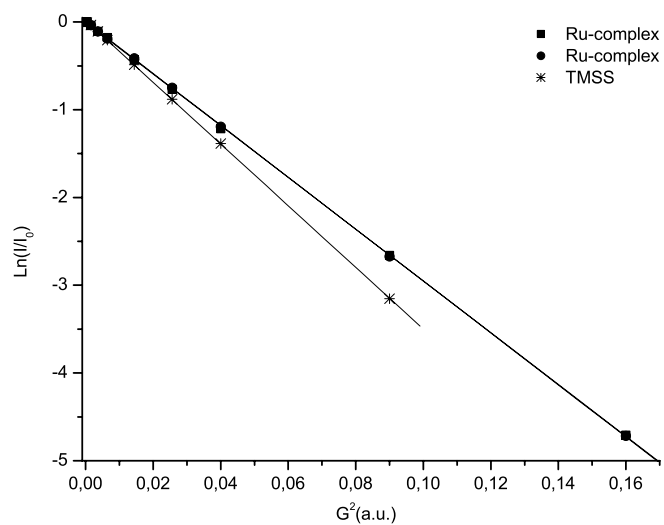


**Table 27S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **6** in methanol- $d_4$  at 296 K using TMSS as internal standard (entry 26)

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$G^2$	$2 \cdot 10^{-3}$ M. $\Delta = 90$ ms		
	Ru-complex	Ru-complex	TMSS
1.00E-04	0	0	0
4.00E-04	-0.00408	0.01387	-0.00751
0.0016	-0.04098	-0.03396	-0.03479
0.0036	-0.10661	-0.10621	-0.10818
0.0064	-0.17785	-0.18957	-0.20754
0.0144	-0.43163	-0.41323	-0.48804
0.0256	-0.76641	-0.75008	-0.88013
0.04	-1.21573	-1.19296	-1.3851
0.09	-2.65972	-2.67297	-3.15293
0.16	-4.70842	-4.71575	-

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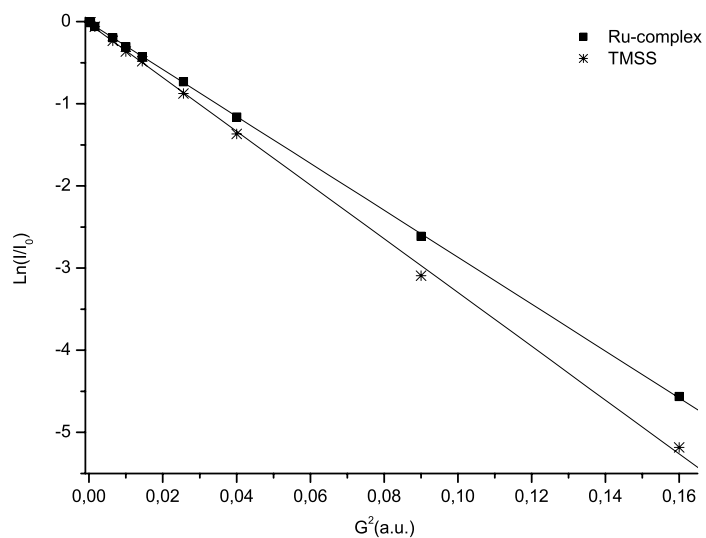


**Table 28S**  $\ln(I/I_0)$  vs.  $G^2$  for solution of **6** in benzene- $d_6$  at 296 K using TMSS as internal standard (entry 27)

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$G^2$	$2 \cdot 10^{-3}$ M. $\Delta = 90$ ms Ru-complex	TMSS
1.00E-04	0	0
4.00E-04	-0.01157	-0.0073
0.0016	-0.05848	-0.0619
0.0064	-0.19709	-0.23489
0.01	-0.30418	-0.36486
0.0144	-0.42857	-0.48246
0.0256	-0.73144	-0.87475
0.04	-1.16132	-1.36738
0.09	-2.61135	-3.09297
0.16	-4.56239	-5.18187

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<sup>1</sup> K.-J. Haack, S. Hashiguchi, A. Fujii, T. Ikariya, R. Noyori, *Angew. Chem., Int. Ed. Engl.*, 1997, **36**, 285.

<sup>2</sup> D. F. Dersnah, M. C. Baird, *J. Organomet. Chem.*, 1977, **127**, C55; R. Krämer, K. Polborn, H. Wanjek, I. Zahn, W. Beck, *Chem. Ber.*, 1990, **123**, 767; D. Carmona, A. Mendoza, F. J. Lahoz, L. A. Oro, M. P. Lamata, E. San José, *J. Organomet. Chem.*, 1990, **396**, C17.

<sup>3</sup> G. Bellachioma, G. Cardaci, V. Gramlich, A. Macchioni, L. M. Venanzi, *J. Chem. Soc., Dalton Trans.*, 1998, 947.

<sup>4</sup> M. A. Benneth, A. K. Smith, A., *K. J. Chem. Soc., Dalton Trans.*, 1974, 233.

<sup>5</sup> M. Valentini, H. Rügger, P. S. Pregosin, *Helv. Chim. Acta* 2001, **84**, 2833 and references therein.

<sup>6</sup> H. J. W. Tyrrell, K. R. Harris, *Diffusion in Liquids*; Butter-worth: London, 1984.

<sup>7</sup> A. Gierer, A.; K. Wirtz, *Z. Naturforsch. A*, 1953, **8**, 522. A. Spornol, K. Wirtz, *Z. Naturforsch. A* **1953**, 8, 532. P. J. Espinosa, J. G. de la Torre, *J. Phys. Chem.*, 1987, **91**, 3612. H. -C. Chen, S. -H. Chen, *J. Phys. Chem.*, 1984, **88**, 5118.

<sup>8</sup> D. Zuccaccia, S. Sabatini, G. Bellachioma, G. Cardaci, E. Clot, A. Macchioni, *Inorg. Chem.*, 2003, **42**, 5465.