

## Tunable Pt nanocatalysts for the aerobic selox of cinnamyl alcohol

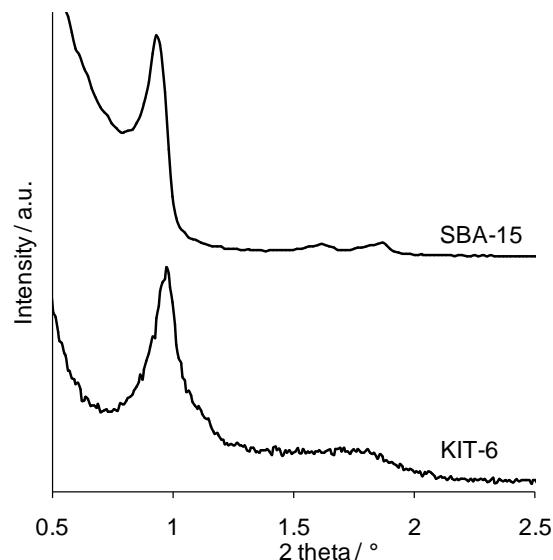
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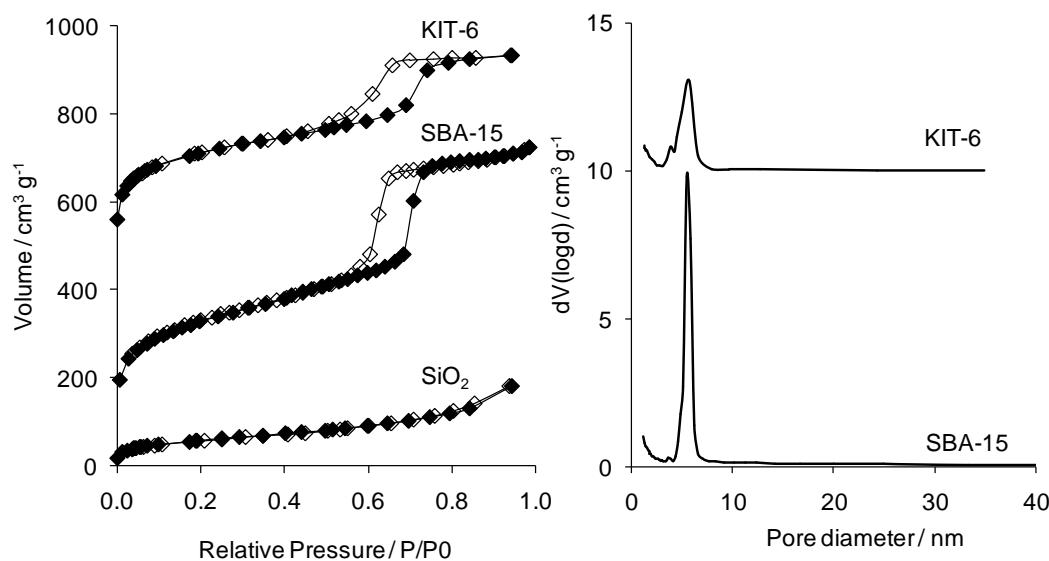
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### Structural and catalytic properties of silicas and Pt/silicas

#### *Parent silica supports*



**Figure S1.** Low Angle XRD patterns for parent mesoporous silica supports. Offset for clarity.

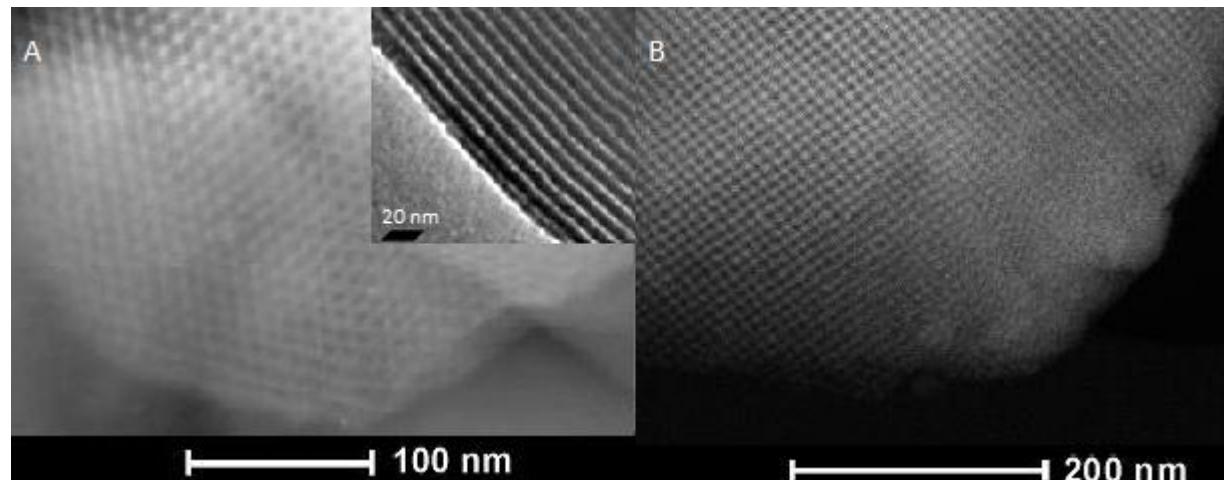


**Figure S2.** Nitrogen adsorption-desorption isotherms and associated BJH pore size distributions for parent mesoporous silica supports. Offset for clarity.

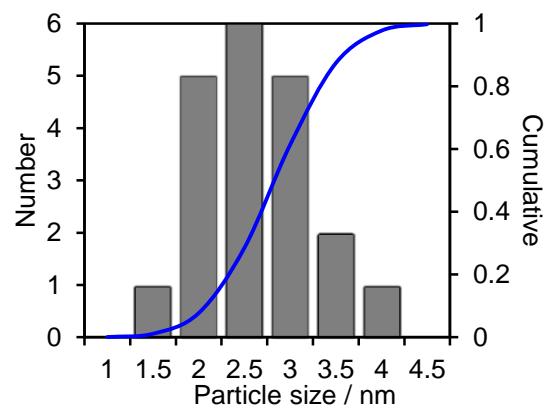
**Table S1.** Textural properties of parent silica supports

Sample	Surface area / m <sup>2</sup> g <sup>-1</sup> <sup>(a)</sup>	Mesopore Diameter / nm <sup>(b)</sup>	Lattice Parameter / nm <sup>(c)</sup>	Pore Separation / nm <sup>(c)</sup>
SiO <sub>2</sub> (S5505)	208.2	31.3	n/a	n/a
SBA-15	1031.9	5.8	9.0	10.4
KIT-6	1144.1	6.6	22.2	22.2

<sup>a</sup>N<sub>2</sub> BET, <sup>b</sup>BJH desorption isotherm, <sup>c</sup>Low angle XRD via Bragg's law

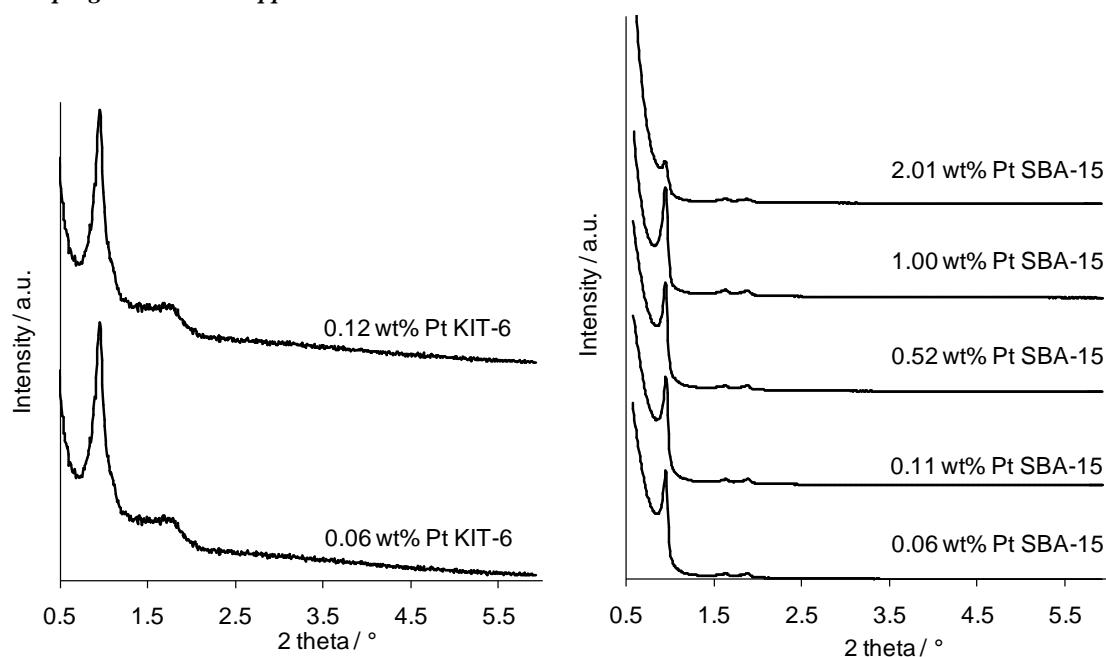


**Figure S3a.** High-resolution TEM (HRTEM) dark field images of parent (a) SBA-15 and (b) KIT-6 supports

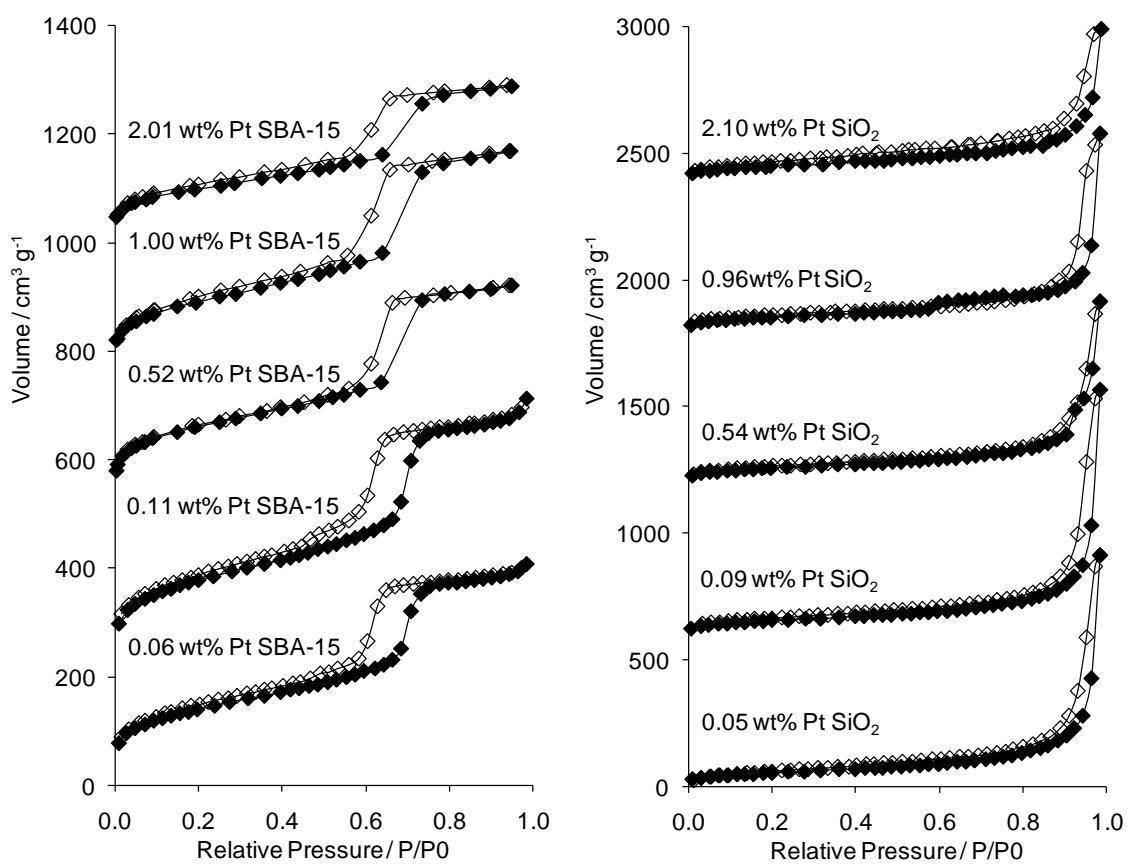


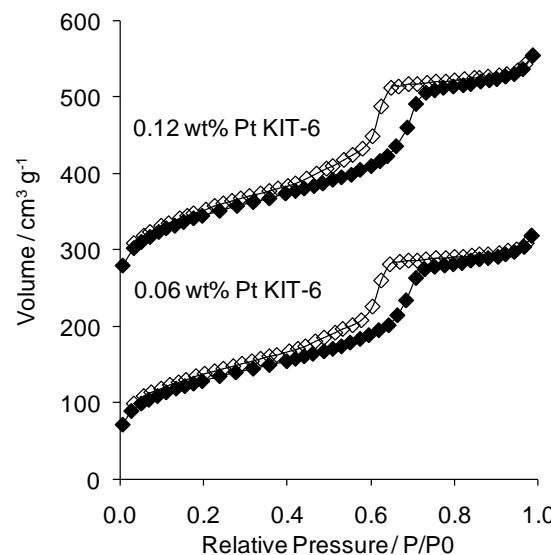
**Figure S3b.** HRTEM particle size distribution for 0.1 wt% Pt/SBA-15

Pt-impregnated silica supports

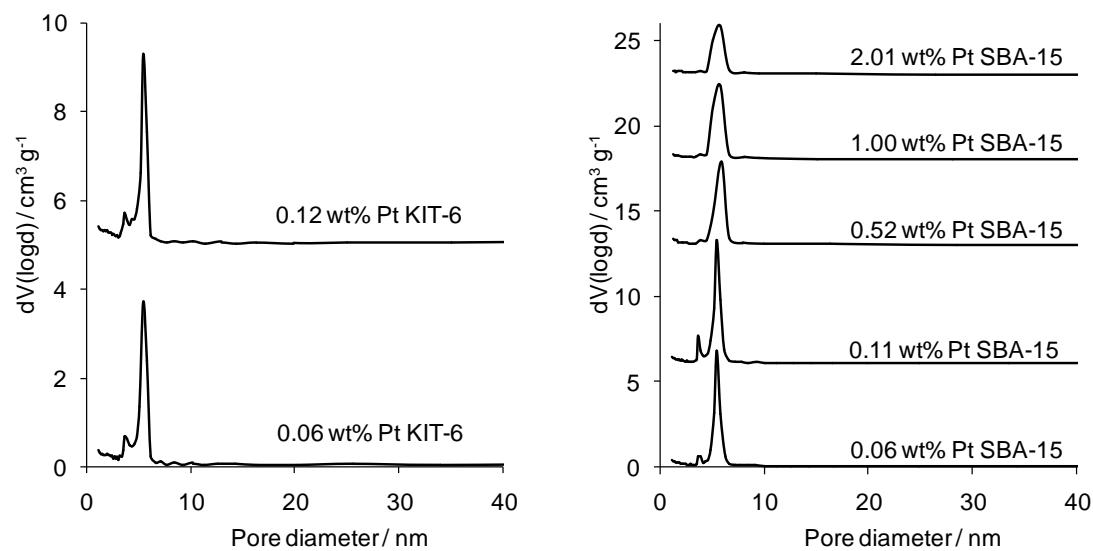


**Figure S4.** Low angle XRD for Pt-impregnated KIT-6 (left) and SBA-15 (right). Pore structure is preserved following impregnation. Offset for clarity.





**Figure S5.** Nitrogen adsorption-desorption isotherms for Pt impregnated KIT-6 (bottom), SBA-15 (top left) and commercial fumed silica (top right). Offset for clarity.



**Figure S6.** BJH pore size distributions for Pt impregnated KIT-6 (left) and SBA-15 (right). Offset for clarity.

**Table S2.** Physico-chemical properties of Pt/silicas

Support	Pt loading / wt% <sup>(a)</sup>	Pt dispersion / % <sup>(b)</sup>	Pt particle size / nm <sup>(c)</sup>	PtO <sub>2</sub> content / % <sup>(d)</sup>	Surface area / m <sup>2</sup> g <sup>-1</sup> <sup>(e)</sup>	Mesopore diameter / nm <sup>(f)</sup>
SiO <sub>2</sub>	2.10	10.0	15.6 (16.6)	7.7	176.16	n/a
SiO <sub>2</sub>	0.96	14.7	9.7 (9.5)	10.1	188.25	n/a
SiO <sub>2</sub>	0.54	20.0	7.7 (8.4)	16.2	192.50	n/a
SiO <sub>2</sub>	0.09	44.4	3.4	23.2	194.36	n/a
SiO <sub>2</sub>	0.05	52.4	3.0	26.7	189.93	n/a
SBA-15	2.01	14.9	14.3 (15.1)	13.8	610.69	5.8
SBA-15	1.00	18.3	7.9 (9.0)	14.8	638.45	5.8
SBA-15	0.52	31.8	3.8 (5.4)	18.1	679.22	5.8
SBA-15	0.11	70.9	2.6	33.8	702.19	5.8
SBA-15	0.06	82.5	2.3	36.0	734.20	5.8
KIT-6	0.12	80.6	1.8	34.7	822.02	6.7
KIT-6	0.06	84.1	1.7	38.1	861.47	6.7

<sup>a</sup>SEM/EDX; <sup>b</sup>from CO chemisorption assuming a CO:Ptsurface stoichiometry of 0.68<sup>1, 2</sup>; <sup>c</sup>From CO chemisorption with parenthesis values from XRD via Scherrer analysis; <sup>d</sup>XPS; <sup>e</sup>N<sub>2</sub> BET; <sup>f</sup>BJH desorption isotherm

Determination of platinum oxide distribution via two different photoelectron excitation sources: a constant Pt<sup>0</sup> XP intensity implies homogeneous particles, a varying Pt<sup>0</sup> intensity implies a core-shell structure.

- The Pt<sup>0</sup> 4f XP intensity for a 0.1 wt% Pt/SiO<sub>2</sub> catalyst, using Mg K<sub>α</sub> X-rays, for which the inelastic mean free path of Pt 4f<sub>7/2</sub> photoelectrons  $\lambda_{\text{Pt}} = 1.11 \text{ nm}^3$  is given by:

$$\text{Intensity}_{\text{Pt}}^{\text{Actual Mg Ka}} = \text{Intensity}_{\text{Pt}}^{\text{Bulk Pt}} \times \exp^{-\left[\frac{(\text{number of layers} \times \text{layer thickness})}{1.11}\right]} = 36.5 \text{ arb. units} \text{ (experimental value)}$$

- The Pt 4f XP intensity for a 0.1 wt% Pt/SiO<sub>2</sub> catalyst, using Al K<sub>α</sub> X-rays, for which the inelastic mean free path of Pt 4f<sub>7/2</sub> photoelectrons  $\lambda_{\text{Pt}} = 1.27 \text{ nm}^3$  is given by:

$$\text{Intensity}_{\text{Pt}}^{\text{Actual Al Ka}} = \text{Intensity}_{\text{Pt}}^{\text{Bulk Pt}} \times \exp^{-\left[\frac{(\text{number of layers} \times \text{layer thickness})}{1.27}\right]} = 57 \text{ arb. units} \text{ (experimental value)}$$

Since the proportion of metallic Pt is a function of escape depth, the nanoparticles most likely comprise a platinum(0) core buried beneath a capping PtO<sub>2</sub> film, from which the oxide film thickness may be estimated as follows:

$$\frac{\text{Intensity}_{\text{Pt}}^{\text{Actual Mg Ka}}}{\text{Intensity}_{\text{Pt}}^{\text{Actual Al Ka}}} = \exp^{-\left[\frac{(\text{number of layers} \times \text{layer thickness})}{1.11} - \frac{(\text{number of layers} \times \text{layer thickness})}{1.27}\right]}$$

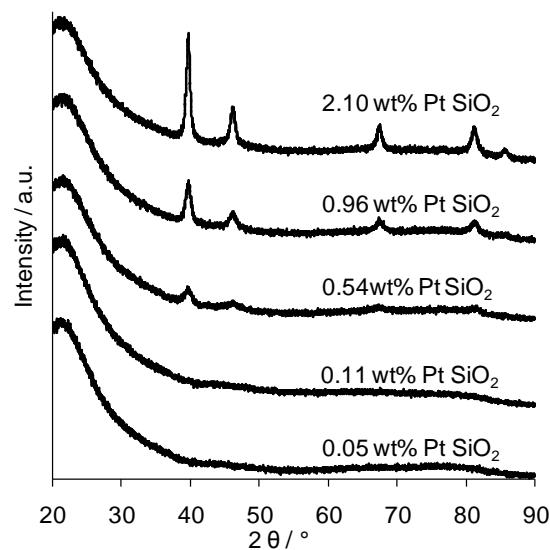
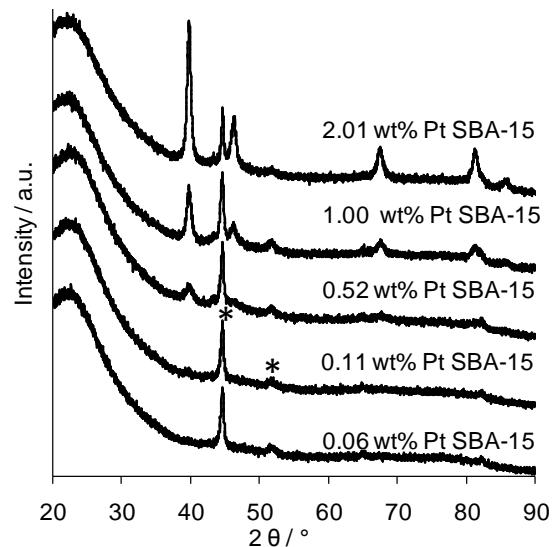
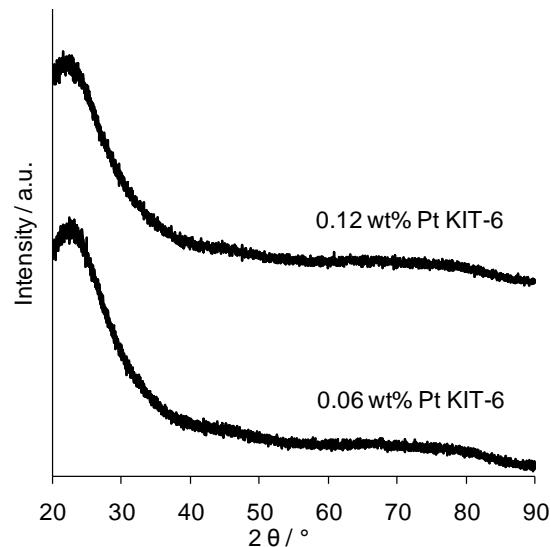
or

$$\ln \frac{36.5}{57} = - \left[ \frac{(\text{number of layers} \times \text{layer thickness})}{1.11} - \frac{(\text{number of layers} \times \text{layer thickness})}{1.27} \right]$$

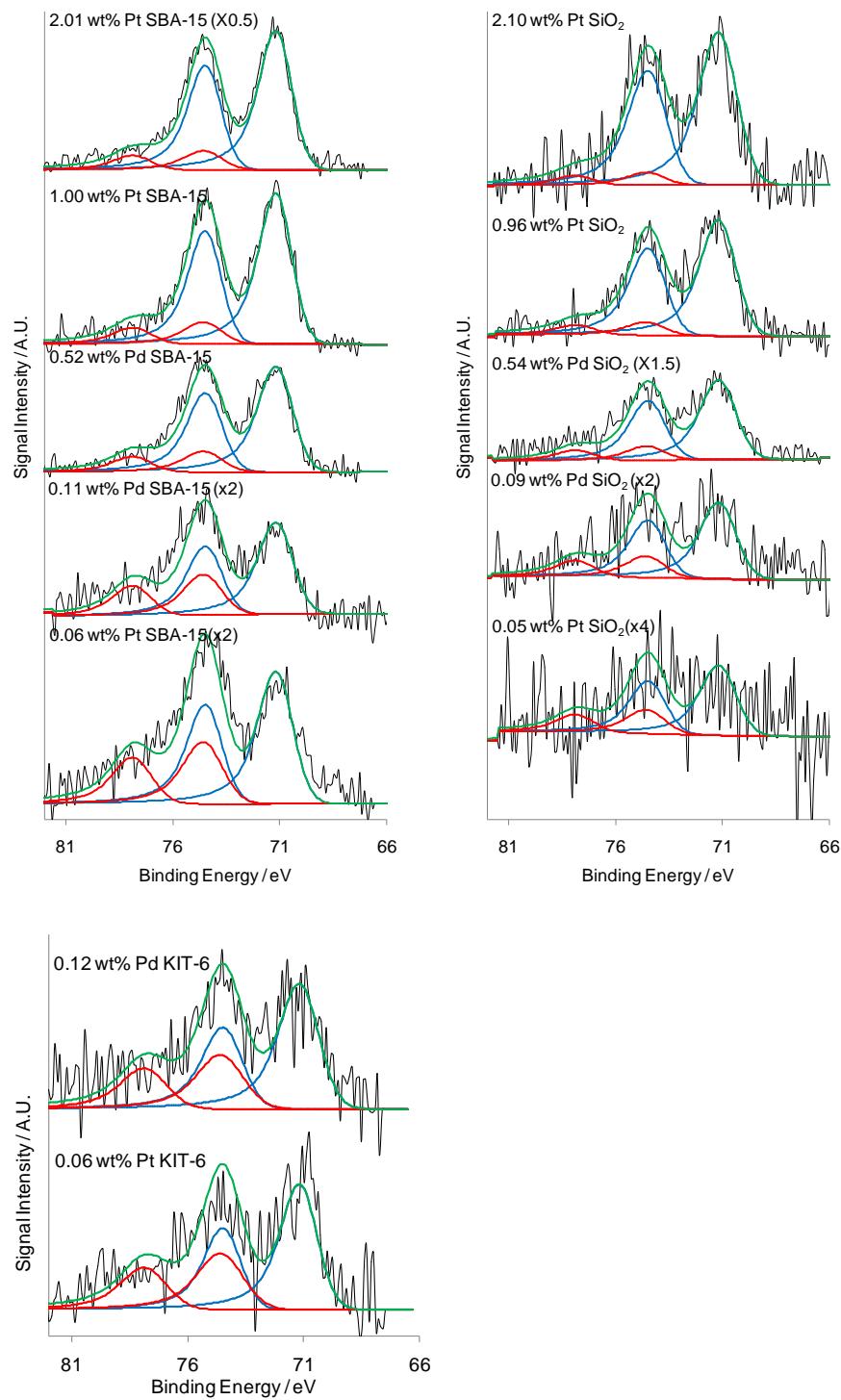
Assuming a mean PtO<sub>2</sub> interlayer spacing of 0.255 nm this yields:

$$\ln \frac{36.5}{57} = - \text{number of layers} \times \left[ \frac{(1.27 \times 0.255) - (1.11 \times 0.255)}{1.11 \times 0.255} \right]$$

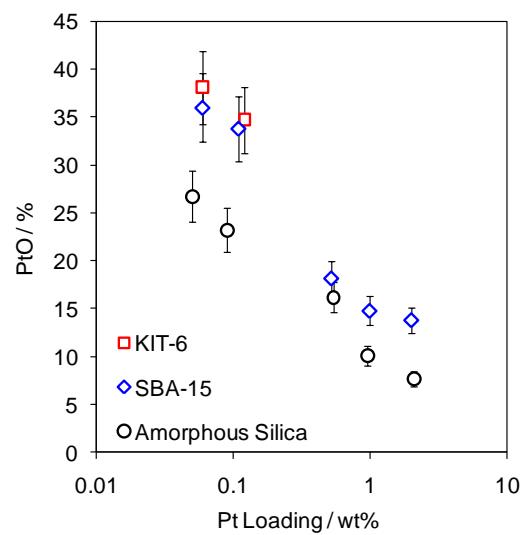
which on rearrangement gives:  $\text{Number of PtO}_2 \text{ layers} = \frac{0.45}{0.144} = 3$



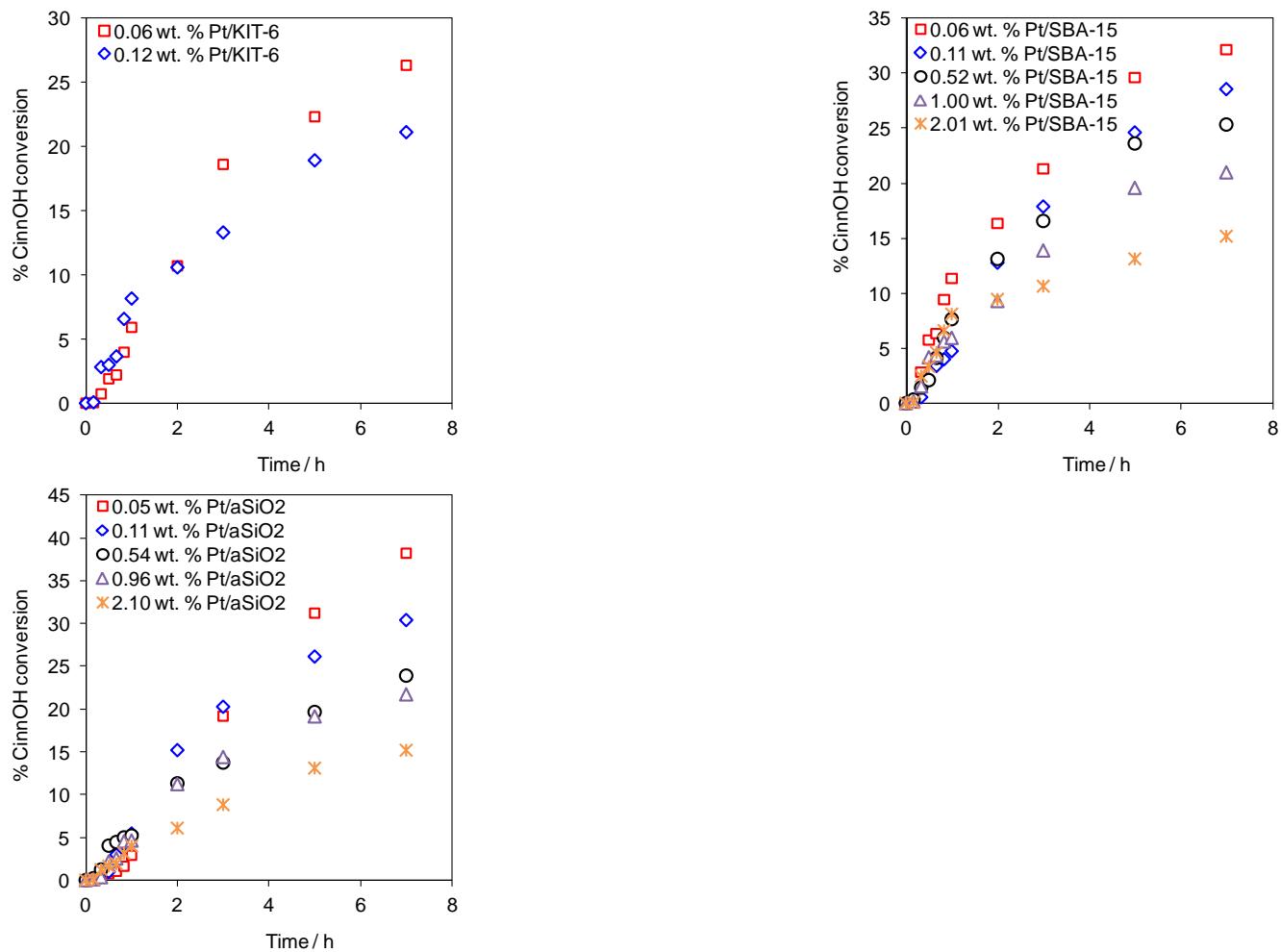
**Figure S7.** Wide angle XRD for Pt-imregnated KIT-6, SBA-15 and commercial fumed silica. Offset for clarity.



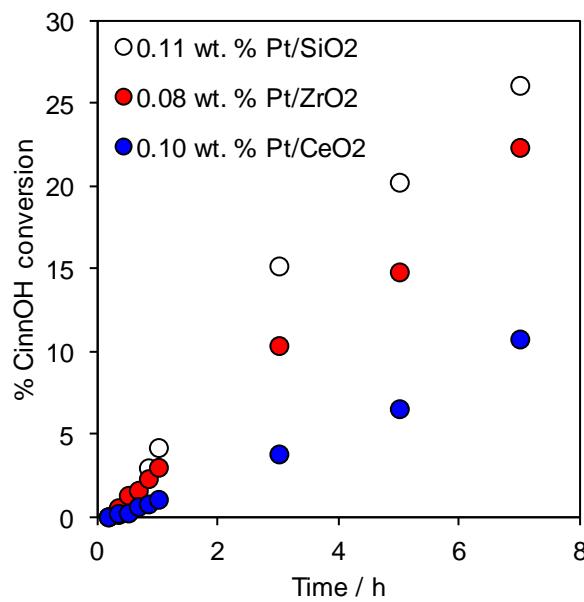
**Figure S8.** Fitted Pt 4f XP spectra for Pt impregnated KIT-6 (bottom), SBA-15 (top left) and commercial fumed silica (top right). Offset for clarity.



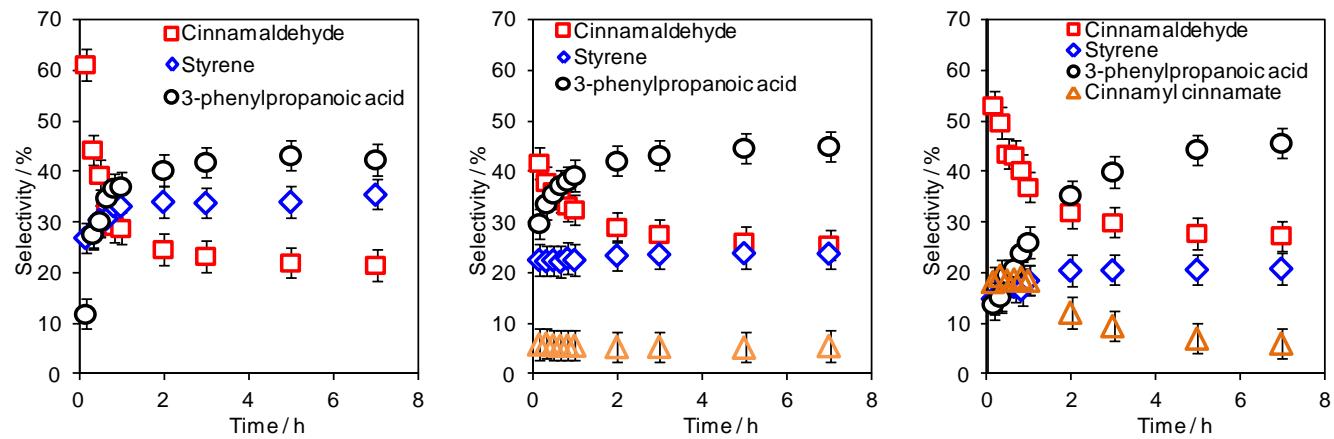
**Figure S9.** Effect of both metal loading and support on  $\text{PtO}_2$  content



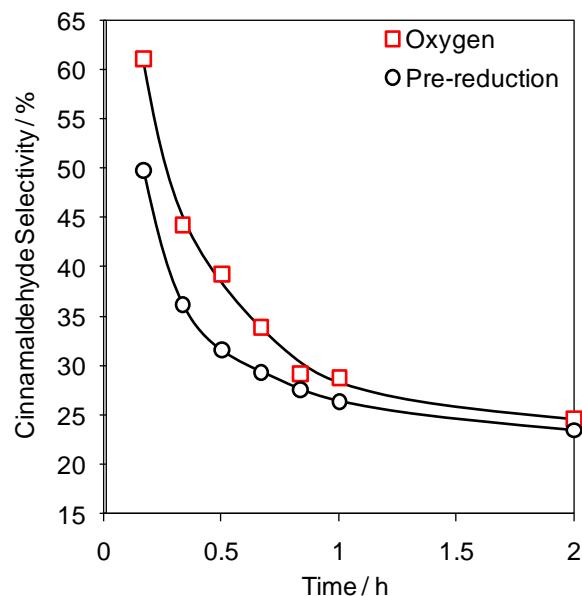
**Figure S10.** Cinnamyl alcohol selox reaction profiles for KIT-6 (left), SBA-15 (right) and commercial silica (bottom) series.



**Figure S11.** Cinnamyl alcohol selox reaction profiles for 0.11 wt% Pt/SiO<sub>2</sub> versus 0.08 wt% Pt/ZrO<sub>2</sub> versus 0.1 wt% Pt/CeO<sub>2</sub>.



**Figure S12.** Selectivity profiles during cinnamyl alcohol selox over: (left) 0.11 wt% Pt/SiO<sub>2</sub>; (middle) 0.08 wt% Pt/ZrO<sub>2</sub>; and (right) 0.1 wt% Pt/CeO<sub>2</sub>.



**Figure S13.** Effect of in-situ catalysts reduction\* on 0.05 wt% Pt/SiO<sub>2</sub> selectivity towards cinnamaldehyde

\* In situ pre-reduction protocol: Catalysts (50 mg) in toluene (7.5 mL) was treated under flowing H<sub>2</sub> (1 bar, 10 mL min<sup>-1</sup>) at 90°C. After 1 h, the solution was purged with N<sub>2</sub> for 0.5 h prior to initiating reaction by addition of a solution comprising toluene (2.5 mL), mesitylene (0.1 mL), and cinnamyl alcohol (1.123 g) under flowing oxygen (5 mL min<sup>-1</sup>).

1. R. Chen, Z. Chen, B. Ma, X. Hao, N. Kapur, J. Hyun, K. Cho and B. Shan, *Computational and Theoretical Chemistry*, 2012, 987, 77-83.
2. S. R. Longwitz, J. Schnadt, E. K. Vestergaard, R. T. Vang, E. Laegsgaard, I. Stensgaard, H. Brune and F. Besenbacher, *Journal of Physical Chemistry B*, 2004, 108, 14497-14502.
3. P.J.Cumpson and M.P. Seah, *Surface and Interface Analysis* **1997**, 25, 430.