

Supporting Information for “Nitroxide mediated controlled synthesis of glycidyl methacrylate-rich copolymers enabled by SGI-based alkoxyamines bearing succinimidyl ester groups”

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In Figure 3, the apparent rate constants ($k_p[\text{P}\cdot]$ where k_p is the propagation rate constant and $[\text{P}\cdot]$ is the concentration of propagating macroradicals) determined experimentally from the $\ln[1/(1-X)]$ versus time plots (X = monomer conversion) were plotted as a function of initial monomer feed composition ($f_{\text{GMA}} = 1 - f_{\text{ST}}$) for glycidyl methacrylate (GMA)/styrene (ST) mixtures. The apparent rate constants dramatically increase at high GMA feed compositions and an expression was derived for $k_p[\text{P}\cdot]$ in an attempt to predict the experimental observations. Below is how a predictive expression for $k_p[\text{P}\cdot]$ was derived and compared to the experimental data.

First, the k_p is actually an average k_p for the mixture and is denoted herein as $\langle k_p \rangle$. Expressions for $\langle k_p \rangle$ have been derived using terminal or penultimate kinetic copolymerization models¹. Here, we use the penultimate model as such a model can better describe most copolymerization kinetic systems, even though the copolymer composition can be predicted well by a terminal model¹. For an implicit penultimate model, $\langle k_p \rangle$ is given by:

$$\langle k_p \rangle = \frac{r_{\text{ST}}f_{\text{ST}}^2 + 2f_{\text{ST}}f_{\text{GMA}} + r_{\text{GMA}}f_{\text{GMA}}^2}{r_{\text{ST}}\frac{f_{\text{ST}}}{k_{p,\text{ST}}} + r_{\text{GMA}}\frac{f_{\text{GMA}}}{k_{p,\text{GMA}}}} \quad [1]$$

where r_{ST} and r_{GMA} are the monomer reactivity ratios for ST and GMA, respectively, f_{ST} and f_{GMA} ($f_{\text{GMA}} = 1 - f_{\text{ST}}$) are the feed compositions of ST and GMA, respectively. Also, $\overline{k_{p,\text{ST}}}$ and $\overline{k_{p,\text{GMA}}}$ are given by:

$$\overline{k_{p,\text{ST}}} = k_{p,\text{ST}} \frac{r_{\text{ST}}f_{\text{ST}} + f_{\text{GMA}}}{r_{\text{ST}}f_{\text{ST}} + \frac{f_{\text{GMA}}}{s_{\text{ST}}}} \quad [2a]$$

$$\overline{k_{p,\text{GMA}}} = k_{p,\text{GMA}} \frac{r_{\text{GMA}}f_{\text{GMA}} + f_{\text{ST}}}{r_{\text{GMA}}f_{\text{GMA}} + \frac{f_{\text{ST}}}{s_{\text{GMA}}}} \quad [2b]$$

where $k_{p,\text{ST}}$ and $k_{p,\text{GMA}}$ are the homopolymerization propagation rate constants of ST and GMA, respectively and s_{ST} and s_{GMA} are the radical reactivity ratios. All of the monomer and radical reactivity ratios were taken from Wang and Hutchinson² while the propagation rate constants were taken from the appropriate literature^{3,4}. All of the parameters used for the estimation of $k_p[\text{P}\cdot]$ are summarized in Table S1.

Next, we need to evaluate $[P\cdot]$ for a nitroxide mediated controlled radical polymerization. For this, we use the expression derived by Fischer⁵. It assumes that irreversible termination is not omitted from the polymerization mechanism.

$$[P\cdot] = \left(\frac{\langle K \rangle [I]_0}{3 \langle k_t \rangle} \right)^{1/3} t^{-1/3} \quad [3]$$

In Equation [3] above, $\langle K \rangle$ is the average equilibrium constant, $[I]_0$ is the initial concentration of nitroxide, $\langle k_t \rangle$ is the average termination rate constant and t is the time. For the implicit penultimate model, Charleux and co-workers derived the following expression for $\langle K \rangle$ ⁶.

$$\langle K \rangle = \frac{\frac{r_{ST} f_{ST}}{k_{p,ST}} + \frac{r_{GMA} f_{GMA}}{k_{p,GMA}}}{\frac{r_{ST} f_{ST}}{k_{p,ST} K_{ST}} + \frac{r_{GMA} f_{GMA}}{k_{p,GMA} K_{GMA}}} \quad [4]$$

Note that the individual equilibrium constant for ST is available from experimental data⁷ but that of GMA is not available and was estimated by the available data from the related methyl methacrylate (MMA)⁸. Finally, $\langle k_t \rangle$ was taken for the penultimate model using the following expression⁹:

$$\langle k_t \rangle = \left(p_{ST} k_{t,ST}^{1/2} + p_{GMA} k_{t,GMA}^{1/2} \right)^2$$

where $k_{t,ST}$ and $k_{t,GMA}$ are the homo-termination rate constants for ST and GMA, respectively. Furthermore, p_{ST} and p_{GMA} were given by:

$$p_{ST} = \frac{\frac{r_{ST} f_{ST}}{k_{p,ST}}}{\frac{r_{ST} f_{ST}}{k_{p,ST}} + \frac{r_{GMA} f_{GMA}}{k_{p,GMA}}} \text{ and } p_{GMA} = 1 - p_{ST}.$$

$k_{t,ST}$ was taken from Beuermann and Buback⁴ while $k_{t,GMA}$ was not available from the literature and thus the termination rate constant for MMA was substituted in its place¹⁰. Thus, the product of $\langle k_p \rangle [P\cdot]$ can be determined. Note however, that due to the $[P\cdot]$ term, the expression is time dependent. To account for this, $[P\cdot]$ at each composition was plotted as a function of time. $[P\cdot]$ dramatically decreased and leveled to nearly a constant value after only a few minutes (Fig. S1). The concentration at 10 minutes was then taken as the steady value for $[P]$, which would have been reasonable during the time-scale of the experiments. Table S2 lists the $[P\cdot]$ after 10 minutes as a function of feed composition. The $[P\cdot]$ values were then multiplied by the expression for $\langle k_p \rangle$ and plotted in Figure 3 of the manuscript along with the experimental data.

Table S1: List of parameters used for the estimation of the apparent rate constants for the nitroxide mediated copolymerization of styrene/glycidyl methacrylate mixtures at 90 °C.

Parameter	Value
r_{ST}	0.292 ^{ref. 2}
r_{GMA}	0.528 ^{ref. 2}
s_{ST}	0.278 ^{ref. 2}
s_{GMA}	1.046 ^{ref. 2}
$k_{p,ST}$ (L mol ⁻¹ s ⁻¹)	900 ^{ref. 3}
$k_{p,GMA}$ (L mol ⁻¹ s ⁻¹)	3000 ^{ref. 4}
K_{ST} (mol L ⁻¹)	4.0 x 10 ⁻¹⁰ ref. 7
K_{GMA} (mol L ⁻¹)	1.0 x 10 ⁻⁷ ref. 8,a
$k_{t,ST}$ (L mol ⁻¹ s ⁻¹)	1.3 x 10 ⁸ ref. 4
$k_{t,GMA}$ (L mol ⁻¹ s ⁻¹)	2.6 x 10 ⁷ ref. 10,b
$[I]_0$ ((mol L ⁻¹))	0.020 ^c

^a Since K_{GMA} was not available, the equilibrium constant for methyl methacrylate, K_{MMA} , was used in its place.

^b Since $k_{t,GMA}$ was not available, the termination rate constant for methyl methacrylate, $k_{t,MMA}$, was used in its place.

^c $[I]_0$ is the initial alkoxyamine concentration.

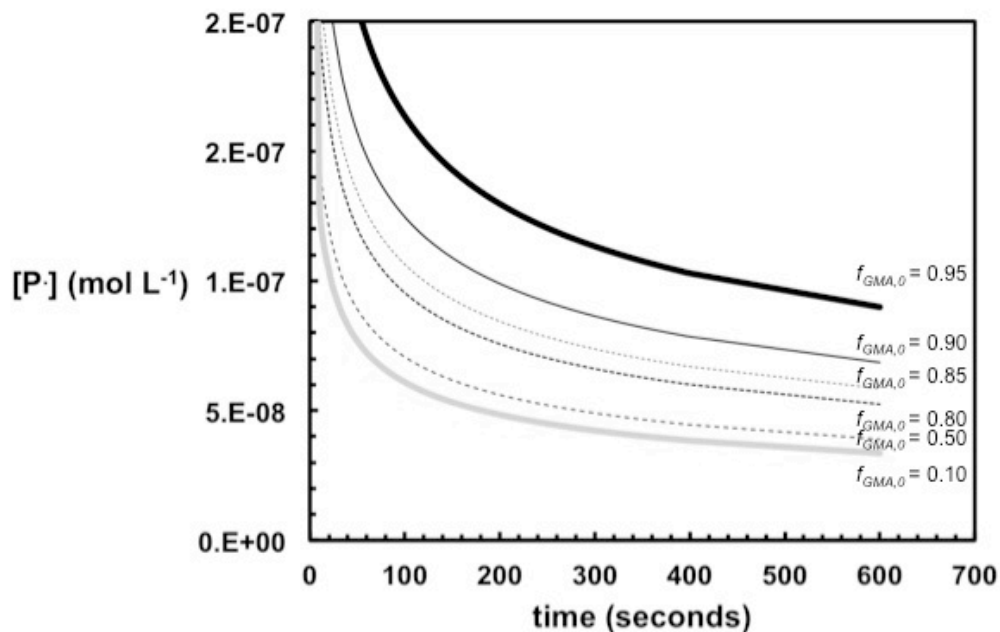


Fig S1. Plot of concentration of propagating radicals $[P\cdot]$ as a function of time (using Equation 3).

Table S2: Estimates of the propagating radical concentration $[P\cdot]$ as a function of feed glycidyl methacrylate (GMA)/styrene (ST) feed compositions.

<i>GMA feed composition</i> $f_{GMA,0}$	$[P\cdot]_{t=10 \text{ min}}$ (mol L ⁻¹)
0	3.2×10^{-8}
0.1	3.4×10^{-8}
0.2	3.5×10^{-8}
0.3	3.6×10^{-8}
0.4	3.7×10^{-8}
0.5	3.9×10^{-8}
0.6	4.1×10^{-8}
0.7	4.5×10^{-8}
0.8	5.2×10^{-8}
0.85	5.8×10^{-8}
0.9	6.9×10^{-8}
0.95	9.0×10^{-8}
1	3.5×10^{-7}

References

1. T. Fukuda, Y.-D. Ma and H. Inagaki, *Macromolecules*, 1985, **18**, 17-26.
2. W. Wang and R. A. Hutchinson, *Macromolecules*, 2008, **41**, 9011-9018.
3. M. Buback, R. G. Gilbert, R. A. Hutchinson, B. Klumperman, F. D. Kutchta, B. G. Manders, K. F. O'Driscoll, G. T. Russell and J. Schweer, *Macromol. Chem. Phys.* 1995, **196**, 3267-3280.
4. S. Beuermann and M. Buback, *Prog. Polym. Sci.*, 2002, **27**, 191-254.
5. H. Fischer, *J. Polym. Sci. Part A: Polym. Chem.*, 1999, **37**, 1885-1901.
6. B. Charleux, J. Nicolas and O. Guerret, *Macromolecules*, 2005, **38**, 5485-5492.
7. D. Benoit, S. Grimaldi, S. Robin, J. P. Finet, P. Tordo and Y. Gnanou, *J. Am. Chem. Soc.*, 2000, **122**, 5929-5939.
8. G. S. Ananchenko, M. Souaille, H. Fischer, C. Le Mercier and P. Tordo, *J. Polym. Sci. Part A: Polym. Chem.*, 2002, **40**, 3264-3283.
9. Y.-D. Ma, K.-S. Sung, Y. Tsujii and T. Fukuda, *Macromolecules*, 2001, **34**, 4749-4756.
10. M. S. Matheson, E. E. Auer, E. B. Bevilacqua, E. J. Hart, *J. Am. Chem. Soc.*, 1949, **71**, 497-504.