

Electronic Supplementary Information

Conversion of Biomass-derived Ethyl Levulinate into γ -Valerolactone via Hydrogen Transfer from Supercritical Ethanol over ZrO_2 Catalyst

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Table S1 Conversion of EL into GVL in various alcohol solvents ^a

Entry	Solvent	Pressure ^b (bar)	GVL yield (%)	EL conversion (%)	Other levulinates (%)
1	methanol	98	14.9	72.3	39.9 (ML) ^b
2	ethanol	70	62.5	81.5	
3	isopropanol	64	93.4	97.2	IPL ^c
4	1-butanol	26	84.4	95.5	2.9 (BL) ^d

^a Reaction conditions: EL, 2 g; ZrO_2 -573 catalyst, 1 g; alcohol, 38 g; reaction time, 1 h; reaction temperature, 523 K. ^b ML means methyl levulinate. ^c IPL means isopropyl levulinate, a very small quantity of IPL was detected. ^d BL means butyl levulinate.

Table S2 The specific surface area of ZrO_2 -573 before reaction and after multiple reactions

Cycle	S_{BET}^a (m^2g^{-1})
fresh	157.2
1	126.9
4	129.1
regeneration ^b	130.7

^a Determined by BET analysis of N_2 adsorption isotherms. ^b ZrO_2 -573 calcination at 573 K for 4 h after cycle 4.

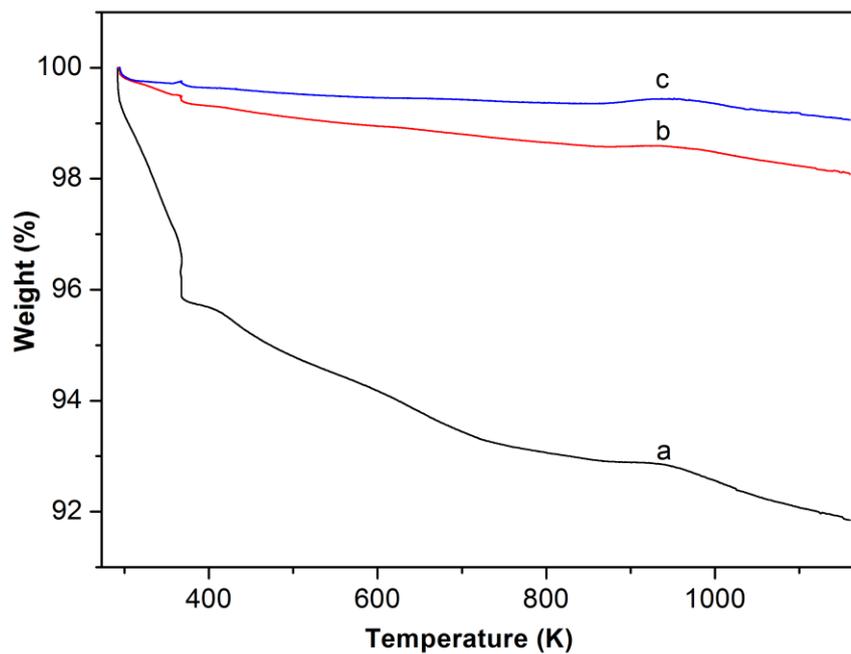


Fig. S1 TGA profiles for (a) ZrO₂-573, (b) ZrO₂-773 and (c) ZrO₂-973.

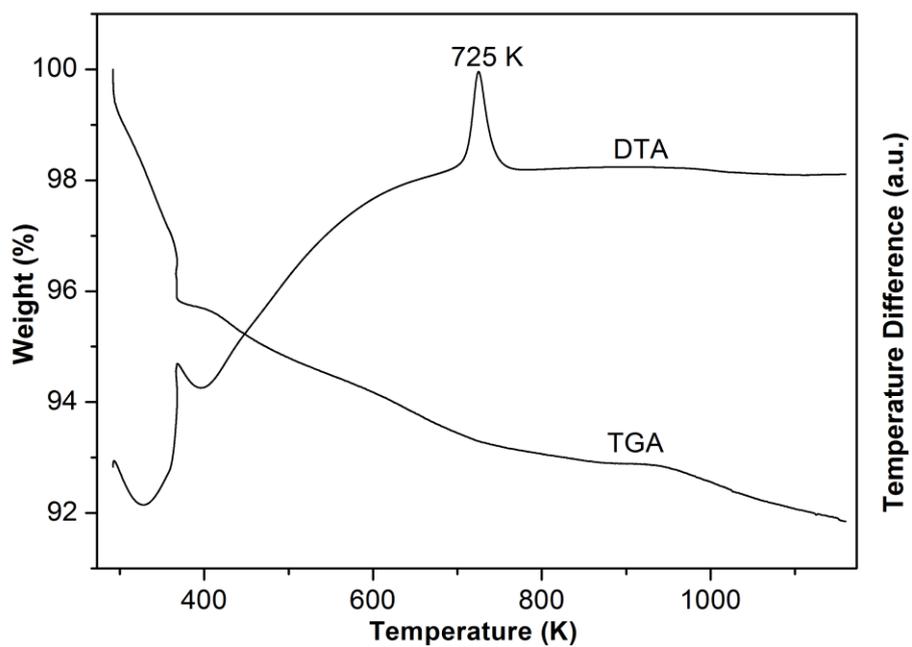


Fig. S2 TGA and DTA curves of the ZrO₂-573 catalyst.

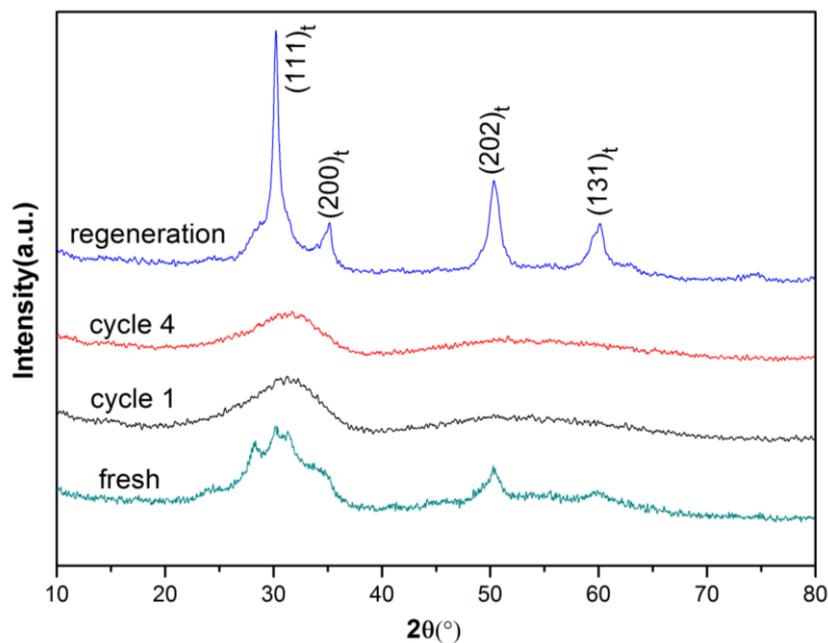


Fig. S3 X-Ray diffraction (XRD) patterns for ZrO₂-573 before and after reaction. Catalyst was regenerated at 573 K for 4 h.

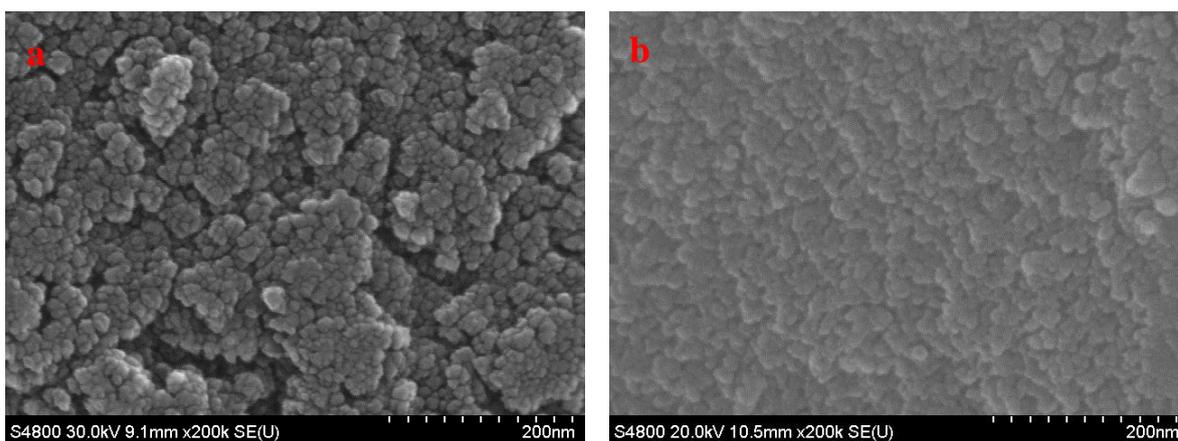
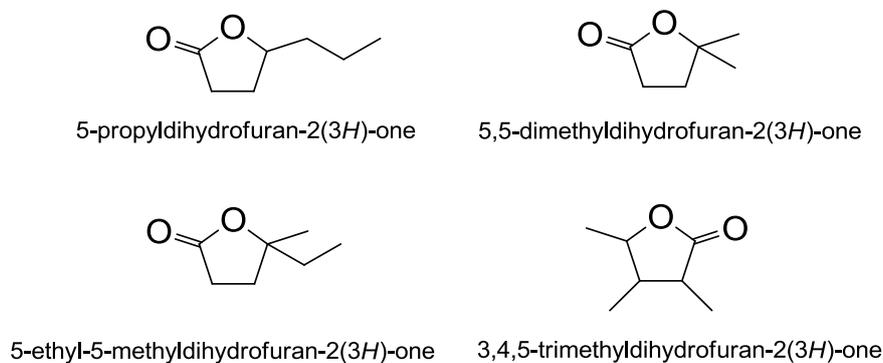


Fig. S4 SEM images for ZrO₂-573 after cycle 4 (a) and regeneration (b).



Scheme S1 By-products derived from GVL were detected by GC-MS analysis.