Electronic Supplementary Information

From metal-organic frameworks to magnetic nanostructured porous carbon composites: Towards highly efficient dye removal and degradation

Cong Zhang, Fanggui Ye,* Shufen Shen, Yuhao Xiong, Linjing Su, Shulin Zhao Key Laboratory for the Chemistry and Molecular Engineering of Medicinal Resources (Ministry of Education of China), College of Chemistry and Pharmaceutical Science of Guangxi Normal University, Guilin 541004, P. R. China.

1. The equation of the adsorption model.

The Langmuir equation is as follows:

$$q_e = \frac{q_{max}K_LC_e}{1 + K_LC_e}$$
 Eq. S1

where K_L is the Langmuir constant, qmax is a constant related to the maximum amount of adsorbed adsorbate (mg·g⁻¹), q_e is the extent of sorption at equilibrium (mg·g⁻¹), and C_e is the equilibrium concentration of MG (mg·g⁻¹).

The linear form of the Langmuir equation is

$$\frac{C_e}{q_e} = \frac{1}{K_L q_{max}} + \frac{C_e}{q_{max}}$$
 Eq. S2

The Freundlich equation can be written as follows:

$$q_e = K_F C_e^{1/}$$
 Eq. S3

where K_F and 1/n represent the Freundlich constants that correspond to the adsorption capacity and adsorption intensity, respectively. Equation (5) can be rearranged into a linear form as follows:

$$\log q_e = \log K_F + \frac{1}{n} \log C_e$$
 Eq. S4

2. The equation of the kinetics model.

The linear form of the pseudo-first-order model is generally expressed as follows:

$$\ln\left(q_e - q_t\right) = \ln q_e - k_1 t$$
 Eq. S5

where k_1 is the equilibrium rate constant of pseudo–first-order kinetics (min⁻¹). The linear fit between the log(q_e – q_t) and contacttime (t) at 30 °C can be approximated as pseudo–first-order kinetics.

The linear form of the pseudo-second-order model is as follows:

$$\frac{t}{q_t} = \frac{1}{kq_e^2} + \frac{t}{q_e}$$
Eq. S6

where k_2 is the equilibrium rate constant of pseudo-second-order kinetics $(g \cdot mg^{-1} \cdot min^{-1})$.

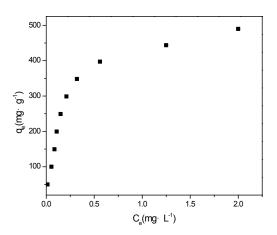


Fig.S1 Standard adsorption curve for MG onto γ -Fe₂O₃/C at the larger volume with lower concentration of MG at 30 °C. The concentrations of MG were 10, 20, 30, 40, 50, 60, 70, 80, 90, 100 mg·L⁻¹; the dosages of adsorbent: 10 mg; the volume: 50 mL.

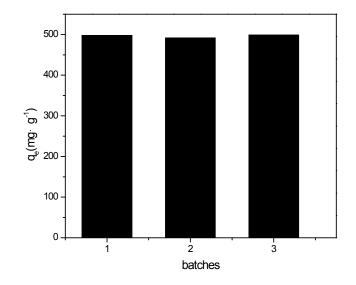


Fig.S2 The adsorption capacity of different batches of the $\gamma\text{-}Fe_2O_3/C.$

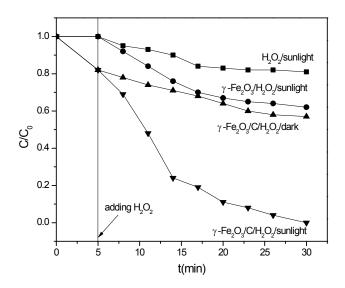


Fig.S3 Removal efficiency of MG under different condition within 30 min, 5 min adsorption/desorption equilibrium in the dark, and then adding H_2O_2 and put the glass bottle under the sunlight. Reaction condition: initial MG concentration, 500 mg·L⁻¹; H_2O_2 , 30%, 20 µL; catalyst, 10 mg; room tempreture.