

Selective hydrogenation of levulinic acid to γ -valerolactone over Ru/Mg-LaO catalyst

V. Swarna Jaya,* M. Sudhakar, S. Naveen Kumar and A. Venugopal

**Inorganic and Physical Chemistry Division, CSIR-Indian Institute of Chemical Technology, Hyderabad- 500 007, India.*

Corresponding address

Tel.: +91-40-27193510; fax: +91-40-27160921;

E-mail address: swarnajv@gmail.com

Table S1. CO Chemisorption studies of different Ru catalysts

Entry	Catalyst	Metal dispersion (%)	Metal surface area (m ² /g) sample/metal
1	RMO	1.4	0.3356/6.8
2	RMA	1.6	0.375/8.175
3	RML	1.7	0.4/8.7

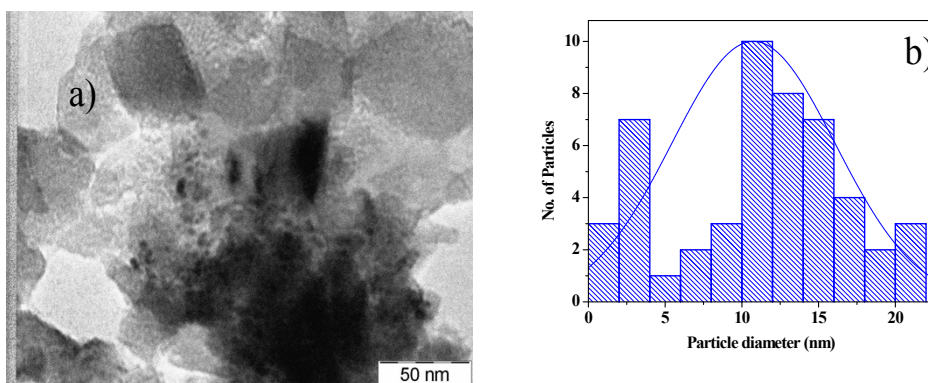


Figure S1. TEM images of a) reduced Ru/MgO, b) particle analysis (avg. particle size ~12 nm)

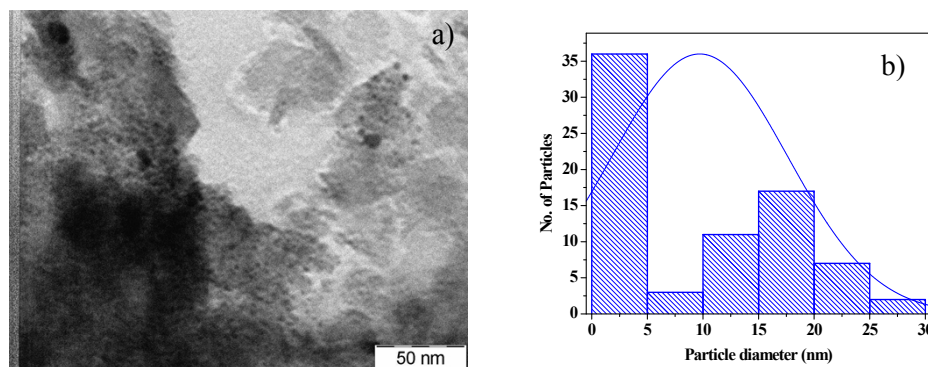


Figure S2. TEM images of a) reduced Ru/MgAlO, b) particle analysis (avg. particle size ~10nm)

The normalized rate is calculated as per the formula

$$\text{Rate} = \frac{\text{Fractional yield} \times [\text{Substrate}]_{\text{moles}} \times [\text{Room Temperature}]_{\text{Kelvin}} \times 1}{[\text{Catalyst}]_{\text{moles}} \times [\text{Reaction Temperature}]_{\text{Kelvin}} \times [\text{Pressure}]_{\text{bar}}}$$

1

$$\text{Yield} = \frac{\text{Conversion} \times \text{Selectivity}}{100} = Y$$

$$\text{Fractional Yield} = Y / 100$$