## Supporting Information

## Macromolecular prodrugs of ribavirin: <br> Towards a treatment for co-infection with HIV and HCV.

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Polymer synthesis. A Chemspeed Swing-SLT automated synthesizer was used for the parallel synthesis. ${ }^{16}$ The reactions were performed in a glass reactor block of 16 reactors ( 13 mL ) with thermal jackets. These were connected in series to a Hüber thermoregulation system $\left(-90^{\circ} \mathrm{C}\right.$ to $140^{\circ} \mathrm{C}$ ). The reactors were equipped with cold-finger reflux condensers and mixing was done by vortex agitation. The liquid transfers were performed by a 4 -needle head, which was washed in between each transfer with dimethyl sulfoxide (DMSO). The DMSO reservoir was degassed by continuous nitrogen sparging. The needle head and tubing lines were also primed with DMSO prior to the transfers. The reaction vessels were heated to $135^{\circ} \mathrm{C}$ and subjected to 10 cycles of vacuum and subsequent nitrogen filling prior to the experiments as to remove oxygen. The reaction mixtures were degassed through an automated parallel freeze-evacuatethaw degassing method. All stock solutions were degassed by sparging with nitrogen for 15 min before being put in the Chemspeed. The desired aliquots of stock solutions and solvent from the reservoir were transferred to the reactors with the automated liquid handling system. Penultimately, the reactors were degassed through three automated freeze-evacuate-thaw cycles, before the reactors were heated to $70^{\circ} \mathrm{C}$ while subjected to vortex agitation for the duration of the polymerization.

The polymerizations were performed with a monomer to RAFT ratio of 500, 250, 50, 35 and 20 . These were done with a ribavirin methacrylate feed varying from $0-20 \mathrm{~mol} \%$. The following stock solutions in DMSO were prepared; HPMA $0.5 \mathrm{~g} / \mathrm{mL}$, ribavirin methacrylate $0.38 \mathrm{~g} / \mathrm{mL}, 4$-cyano-4-[(dodecylsulfanylthiocarbonyl)sulfanyl]pentanoic acid $50 \mathrm{mg} / \mathrm{mL}$ with 4,4 '-azobis(4-cyanovaleric acid) $8.7 \mathrm{mg} / \mathrm{mL}$ as a mixture. Fluorescent duplicates of the polymers with the monomer to RAFT ratios of 500,250 and 50 were made by adding two equivalents of fluorescein methacrylate (with respect to RAFT agent) to the RAFT-initiator stock solution mixture.

These stock solutions were aliquoted into the reaction vessels according to the following table :

## Polymer synthesis

The table below details the reagent compositions for the polymerizations with monomer to RAFT ratios of 500,250 and 50 , these polymerizations were run at $70^{\circ} \mathrm{C}$ for 12 hours.

|  | HPMA $(\mathrm{mL})$ | RBV-MA $(\mathrm{mL})$ | Initiator + RAFT $(\mathrm{mL})$ | Solvent $(\mathrm{mL})$ |
| :--- | :---: | :---: | :---: | :---: |
| Reactor 1 | 0.900 | 0.000 | 0.051 | 1.049 |
| Reactor 2 | 0.856 | 0.129 | 0.051 | 0.964 |
| Reactor 3 | 0.810 | 0.258 | 0.051 | 0.881 |
| Reactor 4 | 0.765 | 0.387 | 0.051 | 0.797 |
| Reactor 5 | 0.720 | 0.517 | 0.051 | 0.712 |
| Reactor 6 | 0.900 | 0.000 | 0.102 | 0.998 |
| Reactor 7 | 0.856 | 0.129 | 0.102 | 0.914 |
| Reactor 8 | 0.810 | 0.258 | 0.102 | 0.831 |
| Reactor 9 | 0.765 | 0.387 | 0.102 | 0.746 |
| Reactor 10 | 0.720 | 0.517 | 0.102 | 0.661 |
| Reactor 11 | 0.900 | 0.000 | 0.510 | 0.592 |
| Reactor 12 | 0.856 | 0.129 | 0.510 | 0.507 |
| Reactor 13 | 0.810 | 0.258 | 0.510 | 0.425 |
| Reactor 14 | 0.765 | 0.387 | 0.510 | 0.340 |
| Reactor 15 | 0.720 | 0.517 | 0.510 | 0.255 |

This scheme corresponds to the following amounts being added to each reactor:

|  | HPMA <br> $(\mathrm{mmol})$ | RBV- <br> Methacrylate <br> $(\mathrm{mmol})$ | RAFT $(\mu \mathrm{mol})$ | Initiator <br> $(\mu \mathrm{mol})$ | Fluorescein <br> methacrylate <br> $(\mu \mathrm{mol})$ |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Reactor 1 | 3.14 | 0.00 | 6.29 | 1.57 | 12.58 |
| Reactor 2 | 2.99 | 0.16 | 6.29 | 1.57 | 12.58 |
| Reactor 3 | 2.83 | 0.31 | 6.28 | 1.57 | 12.58 |
| Reactor 4 | 2.67 | 0.47 | 6.29 | 1.57 | 12.58 |
| Reactor 5 | 2.52 | 0.63 | 6.29 | 1.57 | 12.58 |
| Reactor 6 | 3.14 | 0.00 | 12.58 | 3.15 | 25.15 |
| Reactor 7 | 2.99 | 0.16 | 12.58 | 3.15 | 25.15 |
| Reactor 8 | 2.83 | 0.31 | 12.58 | 3.15 | 25.15 |
| Reactor 9 | 2.67 | 0.47 | 12.58 | 3.15 | 25.15 |
| Reactor 10 | 2.52 | 0.63 | 12.58 | 3.15 | 25.15 |
| Reactor 11 | 3.14 | 0.00 | 62.90 | 15.73 | 125.78 |
| Reactor 12 | 2.99 | 0.16 | 62.90 | 15.73 | 125.78 |
| Reactor 13 | 2.83 | 0.31 | 62.90 | 15.73 | 125.78 |
| Reactor 14 | 2.67 | 0.47 | 62.90 | 15.73 | 125.78 |
| Reactor 15 | 2.52 | 0.63 | 62.90 | 15.73 | 125.78 |

The same procedure is done for the reactions with the monomer to RAFT ratios of 35 and 20, these polymerizations were run at $70^{\circ} \mathrm{C}$ for 24 hours.

|  | HPMA $(\mathrm{mL})$ | RBV-MA $(\mathrm{mL})$ | Initiator + RAFT <br> $(\mathrm{mL})$ | Solvent $(\mathrm{mL})$ |
| :--- | :---: | :---: | :---: | :---: |
| Reactor 1 | 0.675 | 0.000 | 0.389 | 0.736 |
| Reactor 2 | 0.642 | 0.097 | 0.389 | 0.673 |
| Reactor 3 | 0.607 | 0.194 | 0.389 | 0.611 |
| Reactor 4 | 0.574 | 0.291 | 0.389 | 0.547 |
| Reactor 5 | 0.540 | 0.388 | 0.389 | 0.483 |
| Reactor 6 | 0.675 | 0.000 | 0.680 | 0.445 |
| Reactor 7 | 0.542 | 0.388 | 0.680 | 0.192 |

Corresponding to the following amounts:

|  | HPMA (mmol) | RBV-Methacrylate <br> $(\mathrm{mmol})$ | RAFT $(\mu \mathrm{mol})$ | Initiator <br> $(\mu \mathrm{mol})$ |
| :--- | :---: | :---: | :---: | :---: |
| Reactor 1 | 2.36 | 0.00 | 67.40 | 16.84 |
| Reactor 2 | 2.24 | 0.12 | 67.40 | 16.84 |
| Reactor 3 | 2.12 | 0.24 | 67.40 | 16.84 |
| Reactor 4 | 2.00 | 0.35 | 67.40 | 16.84 |
| Reactor 5 | 1.89 | 0.47 | 67.40 | 16.84 |
| Reactor 6 | 2.36 | 0.00 | 117.90 | 29.48 |
| Reactor 7 | 1.89 | 0.47 | 117.90 | 29.48 |

## Polymer characterization

The analysis of the polymerizations (SEC and ${ }^{1} \mathrm{H}$ NMR) revealed the following characteristics
(Polymer highlighted in bold were used in further cell experiments, see Main text)
The non-fluorescent polymers with M:RAFT 500-50

| Series | RBV feed | RBV <br> content | M:RAFT | Conversion | Mn (kDa, <br> calc) | Mn (kDa, <br> GPC) | $\oplus$ | DP <br> (GPC) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| I-1 | $\mathbf{0 \%}$ | $\mathbf{0 \%}$ | $\mathbf{5 0 0}$ | $\mathbf{4 9 \%}$ | $\mathbf{3 5 . 3}$ | $\mathbf{3 4 . 6}$ | $\mathbf{1 . 2 8}$ | $\mathbf{2 4 2}$ |
| I-2 | $\mathbf{5 \%}$ | $\mathbf{7 \%}$ | $\mathbf{5 0 0}$ | $\mathbf{4 8 \%}$ | $\mathbf{3 7 . 8}$ | $\mathbf{4 0 . 6}$ | $\mathbf{1 . 2 3}$ | $\mathbf{2 6 1}$ |
| I-3 | $\mathbf{1 0 \%}$ | $\mathbf{1 5 \%}$ | $\mathbf{5 0 0}$ | $\mathbf{5 5 \%}$ | $\mathbf{4 6 . 8}$ | $\mathbf{4 8 . 6}$ | $\mathbf{1 . 1 9}$ | $\mathbf{2 8 4}$ |
| $\mathbf{I - 4}$ | $\mathbf{1 5 \%}$ | $\mathbf{2 0 \%}$ | $\mathbf{5 0 0}$ | $\mathbf{5 2 \%}$ | $\mathbf{4 6 . 8}$ | $\mathbf{4 2 . 8}$ | $\mathbf{1 . 2 8}$ | $\mathbf{2 3 6}$ |
| $\mathbf{I - 5}$ | $\mathbf{2 0 \%}$ | $\mathbf{2 2 \%}$ | $\mathbf{5 0 0}$ | $\mathbf{5 2 \%}$ | $\mathbf{4 7 . 0}$ | $\mathbf{5 2 . 9}$ | $\mathbf{1 . 2 1}$ | $\mathbf{2 8 6}$ |
| $\mathbf{I I - 1}$ | $\mathbf{0 \%}$ | $\mathbf{0 \%}$ | $\mathbf{2 5 0}$ | $\mathbf{5 4 \%}$ | $\mathbf{1 9 . 6}$ | $\mathbf{2 0 . 0}$ | $\mathbf{1 . 2 6}$ | $\mathbf{1 4 0}$ |
| $\mathbf{I I - 2}$ | $\mathbf{5 \%}$ | $\mathbf{7 \%}$ | $\mathbf{2 5 0}$ | $\mathbf{6 2 \%}$ | $\mathbf{2 4 . 4}$ | $\mathbf{2 4 . 9}$ | $\mathbf{1 . 1 8}$ | $\mathbf{1 5 8}$ |
| $\mathbf{I I - 3}$ | $\mathbf{1 0 \%}$ | $\mathbf{1 3 \%}$ | $\mathbf{2 5 0}$ | $\mathbf{6 2 \%}$ | $\mathbf{2 6 . 0}$ | $\mathbf{2 7 . 8}$ | $\mathbf{1 . 1 5}$ | $\mathbf{1 6 5}$ |
| $\mathbf{I I - 4}$ | $\mathbf{1 5 \%}$ | $\mathbf{1 5 \%}$ | $\mathbf{2 5 0}$ | $\mathbf{6 1 \%}$ | $\mathbf{2 6 . 3}$ | $\mathbf{2 7 . 2}$ | $\mathbf{1 . 1 5}$ | $\mathbf{1 5 8}$ |
| $\mathbf{I I - 5}$ | $\mathbf{2 0 \%}$ | $\mathbf{1 9 \%}$ | $\mathbf{2 5 0}$ | $\mathbf{6 6 \%}$ | $\mathbf{2 9 . 1}$ | $\mathbf{2 5 . 5}$ | $\mathbf{1 . 1 3}$ | $\mathbf{1 4 2}$ |
|  | $0 \%$ | $0 \%$ | 50 | $80 \%$ | 6.1 | 6.7 | 1.16 | 47 |
|  | $5 \%$ | $7 \%$ | 50 | $82 \%$ | 6.7 | 7.6 | 1.12 | 49 |
|  | $10 \%$ | $12 \%$ | 50 | $79 \%$ | 6.9 | 7.8 | 1.10 | 47 |
|  | $15 \%$ | $16 \%$ | 50 | $81 \%$ | 7.3 | 8.4 | 1.07 | 48 |
|  | $20 \%$ | $22 \%$ | 50 | $81 \%$ | 7.7 | 8.8 | 1.06 | 47 |

The non-fluorescent polymers with M:RAFT 35-20

| Reaction | RBV <br> feed | RBV content | M:RAFT | Conversion | Mn (kDa, <br> calc) | Mn (kDa, <br> GPC) | $D$ | DP |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| III-1 | $\mathbf{0}$ | $\mathbf{0}$ | $\mathbf{3 5}$ | $\mathbf{9 9 \%}$ | $\mathbf{5 . 0}$ | $\mathbf{8 . 1}$ | $\mathbf{1 . 2 0}$ | $\mathbf{5 7}$ |
| III-2 | $\mathbf{5 \%}$ | $\mathbf{6 \%}$ | $\mathbf{3 5}$ | $\mathbf{9 9 \%}$ | $\mathbf{5 . 3}$ | $\mathbf{6 . 1}$ | $\mathbf{1 . 1 2}$ | $\mathbf{3 9}$ |
| III-3 | $\mathbf{1 0 \%}$ | $\mathbf{1 2 \%}$ | $\mathbf{3 5}$ | $\mathbf{9 9 \%}$ | $\mathbf{5 . 6}$ | $\mathbf{7}$ | $\mathbf{1 . 0 6}$ | $\mathbf{4 2}$ |
| III-4 | $\mathbf{1 5 \%}$ | $\mathbf{1 7 \%}$ | $\mathbf{3 5}$ | $\mathbf{9 9 \%}$ | $\mathbf{5 . 8}$ | $\mathbf{6 . 9}$ | $\mathbf{1 . 0 7}$ | $\mathbf{3 9}$ |
| III-5 | $\mathbf{2 0 \%}$ | $\mathbf{2 3 \%}$ | $\mathbf{3 5}$ | $\mathbf{9 9 \%}$ | $\mathbf{6 . 0}$ | $\mathbf{6 . 4}$ | $\mathbf{1 . 0 9}$ | $\mathbf{3 4}$ |
| IV-1 | $\mathbf{0 \%}$ | $\mathbf{0 \%}$ | $\mathbf{2 0}$ | $\mathbf{9 9 \%}$ | $\mathbf{2 . 8}$ | $\mathbf{3 . 7}$ | $\mathbf{1 . 1 2}$ | $\mathbf{2 6}$ |
| IV-2 | $\mathbf{2 0 \%}$ | $\mathbf{2 2 \%}$ | $\mathbf{2 0}$ | $\mathbf{9 9 \%}$ | $\mathbf{3 . 3}$ | $\mathbf{4 . 1}$ | $\mathbf{1 . 0 3}$ | $\mathbf{2 2}$ |

The fluorescent polymers with M:RAFT 500-50

| Reaction | $\begin{aligned} & \hline \text { RBV } \\ & \text { feed } \\ & \hline \end{aligned}$ | RBV content | M:RAFT | Conversion | $\begin{gathered} \mathrm{Mn}(\mathrm{kDa}, \\ \text { calc) } \end{gathered}$ | $\begin{gathered} \mathrm{Mn}(\mathrm{kDa}, \\ \mathrm{GPC}) \\ \hline \end{gathered}$ | $\oplus$ | DP |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| I-1 | 0\% | 0\% | 500 | 24\% | 17.4 | 92.1 | 1.24 | 643 |
| I-2 | 5\% | 8\% | 500 | 24\% | 18.9 | 77.7 | 1.14 | 498 |
| I-3 | 10\% | 20\% | 500 | 29\% | 25.9 | 67.8 | 1.21 | 381 |
| I-4 | 15\% | 24\% | 500 | 38\% | 35.1 | 65.7 | 1.18 | 358 |
| I-5 | 20\% | 25\% | 500 | 53\% | 49.7 | 67.7 | 1.19 | 363 |
| II-1 | 0\% | 0\% | 250 | 50\% | 17.9 | 20.0 | 1.29 | 140 |
| II-2 | 5\% | 7\% | 250 | 60\% | 23.3 | 21.1 | 1.28 | 136 |
| II-3 | 10\% | 13\% | 250 | 64\% | 26.5 | 22.2 | 1.25 | 134 |
| II-4 | 15\% | 17\% | 250 | 66\% | 28.3 | 23.4 | 1.21 | 135 |
| II-5 | 20\% | 20\% | 250 | 64\% | 28.3 | 22.0 | 1.13 | 124 |
| III-1 | 0\% | 0\% | 50 | 80\% | 5.7 | 4.9 | 1.31 | 34 |
| III-2 | 5\% | 4\% | 50 | 82\% | 6.1 | 6.4 | 1.19 | 43 |
| III-3 | 10\% | 9\% | 50 | 83\% | 6.6 | 6.1 | 1.21 | 38 |
| III-4 | 15\% | 14\% | 50 | 81\% | 6.8 | 6.5 | 1.14 | 39 |
| III-5 | 20\% | 17\% | 50 | 80\% | 6.8 | 6.9 | 1.07 | 40 |

## Additional graphs



Figure SI 1. Haemolysis of erythrocytes upon incubation with macromolecular prodrugs at $100 \mu \mathrm{~g} / \mathrm{mL}$ concentration over 24 h at $37{ }^{\circ} \mathrm{C}$. Shown results are the average $\pm$ SD of three independent experiments ( $\mathrm{n}=3$ ). Depicted RBV content is for illustrative purposes only, for actual numerical values see the tables above.


Figure SI 2. Top panel, microscope pictures illustrating PBS treated erythrocytes and PLL treated cells, the latter introducing aggregation of RBCs. Bottom panel, dot-plots from flow cytometry analysis of erythrocytes incubated with PBS and PLL ( $10 \mathrm{~g} / \mathrm{L}$ ) during 24 h at $37^{\circ} \mathrm{C}$.


FSC (a.u.)
Figure SI 3. Dot-plots from flow cytometry analysis of erythrocytes incubated with MPs at $100 \mu \mathrm{~g} / \mathrm{mL}$ during 24 h at $37{ }^{\circ} \mathrm{C}$, with erythrocytes treated with PHPMA of similar $M_{\mathrm{n}}$, with and without RBV: Top three panels showing $0 \%, 92$ $\mathrm{kDA}, 0 \%, 20 \mathrm{kDa}$, and $0 \%, 5 \mathrm{kDa}$. Bottom panels showing $20 \%, 68 \mathrm{kDa}, 20 \%, 22 \mathrm{kDa}$, and $17 \%, 7 \mathrm{kDa}$.

