1 2	Supplementary Material (ESI) for Journal of Materials Chemistry A This journal is (c) The Royal Society of Chemistry 2012
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4	Supporting Information:
5	Direct synthesis of c-axis oriented ZSM-5 nanoneedles from acid-treated
6	kaolin clay
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9 10	Experimental Section
11 12	1. Preparation of c-axis oriented ZSM-5 nanoneedles
13	In a typical synthesis of c-axis oriented ZSM-5 nanoneedles sample (denoted as HZS-18; 18 was the Si/Al
14	ratios), the precursor of Kaolin was firstly calcinated at 1073 K for 3 hrs and then treated with 3 M $H_2SO_4$ (5 g
15	$H_2SO_4/1$ g kaolin clay) for 2 hrs to get the suitable ratio of Si/Al for the ZSM-5 synthesis. Then 6 g acid-treated
16	kaolin clay was mixed with 120 g deionized water, 0.6 g NaOH and 3 g ethylene diamine (EDA). The suspension
17	was aged with stirring for 12-24 hr at room temperature. Then the mixture was transferred into the stainless-steel
18	autoclave lined with polytetrafluoroethylene (PTFE) and was heated to 453 K for 3 days with continuous
19	stirring. After cooling to room temperature, the products were filtrated and washed thoroughly with deionized
20	water. Then the samples were dried at 383 K overnight and subsequently calcined in air at 823 K for 6 h to
21	remove the template (EDA). Using 3 g acid-treated kaolin clay instead of 6 g as the alumina source and silica
22	source, 100 nm i.d monodispersed ZSM-5 nanoneedles were also synthetized under the same conditions. For
23	comparison, the conventional ZSM-5 zeolites with Si/Al ratio of 19, in H <sup>+</sup> ion-exchanged form, was purchased
24	from Nankai university catalyst factory (designated as CZS-19; 19 is the Si/Al ratios).
25	2. Preparations of Zn-modified ZSM-5
26	The Zn-modified HZSM-5 with mass loading of Zn of 3% was prepared by traditional incipient wetness
27	impregnation of HZS-18 using aqueous solutions of Zn (NO <sub>3</sub> ) <sub>2</sub> . 6H <sub>2</sub> O. After drying overnight and calcinating in

air at 823 K for 5 h, the resultant catalyst was designated as Zn/HZS-18. To compare catalytic performances,

29 CZS-19 was also impregnated with the same Zn content and manner (designated as Zn/CZS-19).

30 *3. Characterization* 

31 X-ray diffractions (XRD) were recorded on a Rigaku D/Max-RB diffractometer with Cu KαRadiation at 40

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kV and 120 mA. Scanning electron microscope (SEM) images were obtained by a high-resolution scanning 1 2 electron microscope (JEOL, JSM-7401) at 3.0 kV. Energy-dispersive X-ray (EDX) analysis was performed using a JSM-7401F apparatus at 15.0 kV with the analytical software INCA.TEM experiments were performed 3 on a high-resolution transmission electron microscope (JEOL, JEM-2010, exited at 120kV) equipped with 4 selected area electron diffraction (SAED). Brunauer-Emmett-Teller (BET) surface area were recorded in a 5 6 Quantachrome automated surface area and porosity analyzer with N<sub>2</sub> as the adsorption gas. Thermogravimetric 7 analysis (TGA) was carried out using a thermo gravimetric analyzer (TGA/DSC-1) from 30-900 °C at a heating rate of 10 °C min<sup>-1</sup> in air. NH<sub>3</sub>-TPD analysis was completed in a Quantachrome automated chemisorption 8 analyzer from room temperature to 850°C with a ramp of 10°C/min. Brønsted acid sites and Lewis acid sites 9 10 were determined by pyridine adsorption. The samples were first dried, in situ, by heating to 723 K under vacuum, and then were cooled to 323 K. At this temperature, the samples were exposed to pyridine vapour using 11 12 an equilibration time of 30 min. After physically adsorbed pyridine molecules were removed by outgassing at 423 K for 1 h, IR spectra were collected at 423 K with 4  $cm^{-1}$  resolution using a Nicolet FTIR spectrometer. 13

## 14 4. Catalytic Activity Testing

The MTA reaction were performed at the conditions of 1 atm, 748 K and WHSV =  $0.79 \text{ h}^{-1}$ (under N<sub>2</sub> flow (10 mL min<sup>-1</sup>) in a conventional fixed bed stainless steel reactor (13.0 mm i.d) equipped with a thermocouple in the middle of the catalyst bed. 1 g of catalyst was placed in the fixed bed reactor. The flow rate of pure methanol and N<sub>2</sub> were controlled using a dual micro-plunger pump and the mass flow controllers, respectively. The product (hydrocarbons) was analyzed using two flame ionization detector (FID). The conversion of methanol and the selectivity of different products were calculated (carbon base) accordingly.



Fig.S1 SEM image of the kaolin clay, showing that the Kaolin clay had a nano-sized laminated structure.



9 Fig.S2 SEM image of the CZS-19. The particle sizes of the coffin-shaped or inter grown CZS-19 was about 3μm.



Fig. S3 NH<sub>3</sub>-TPD adsorption of Zn/HZS-18 and Zn/CZS-19. The low temperature desorption peak (400-650 K)
indicates weak adsorption sites and the high temperature peak (650-800 K) was interpreted to be caused by ammonia
desorption from strong Brønsted acid sites and strong Lewis acid sites.





L=Lewis acid sites.



Fig.S6 SEM image of the needle-like ZSM-5 polycrystalline obtained by regulating synthetic conditions.

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Table S1 Physical properties of the HZS-18 and the CZS-19 and product selectivities of MTA reactions over the 

Zn/HZS-18 and the Zn/CZS-19 after 50 minutes reaction <sup>a</sup>.

	Si/Al	BET surface	Total pore	Micropore	Mesopore	Average pore	Selectivity (%)			6)		
Catalyst	atomic	area	volume	volume	volume	diameter	$C_1-C_4$	$C_2-C_4$	C <sub>5+</sub>	Total		
	ratio <sup>b</sup>	$(m^2g^{-1})$	$(cm^{3}g^{-1})$	$(cm^{3} g^{-1})^{c}$	$(\rm cm^3 g^{-1})^d$	(nm) <sup>e</sup>	alkanes	olefins	etc	aromatics		
HZS-18	18.3	374	0.39	0.12	0.27	3	27.8	11.9	3.8	56.5		
CZS-19	19.8	345	0.18	0.14	0.04	-	26.1	17.5	6.3	50.1		
<sup>a</sup> Reaction conditions: Reaction temperature, 748K; $W_{cat} = 1g$ ; GHSV = 0.79 h <sup>-1</sup> .												
<sup>b</sup> Determined by Energy-dispersive X-ray (EDX) analysis.												
<sup>c</sup> T-plot method; ${}^{d}V_{meso} = V_{tot} - V_{micro}$ ; <sup>e</sup> BJH method.												