

Supporting information

Calculation of TOF for NiP catalysts

Calculation of turn over frequencies utilised the surface areas of the catalysts determined by BET and the assumption that each Nitrogen molecule covers 0.162 nm². Both Ni and P sites are considered, and hence each N₂ molecule is assumed to cover two sites. The turnover numbers were calculated as follows.

Material	Density / g cm ⁻³	Molar mass / g mol ⁻¹	Molar volume / cm ³ mol ⁻¹	Surface site density / cm ⁻³
Ni ₂ P	7.35	148.36	20.19	2.00x10 ¹⁵
Ni ₁₂ P ₅	7.53	859.19	114.14	6.31x10 ¹⁴

Surface site density

$$\#atoms \text{ in } 1 \text{ cm}^3 = N(\text{atoms in formula}) \times N_A / V_M$$

$$\# \text{ atoms in } 1 \text{ cm}^2 = ((\#atoms)^{1/3})^2 = (\#atoms)^{2/3}$$

Roughness Factor of electrode

$$R_f \left(\frac{\text{cm}^2}{\text{cm}^2} \right) = \text{Loading} \left(\frac{\text{mg}}{\text{cm}^2} \right) \times 0.001 \left(\frac{\text{g}}{\text{mg}} \right) \times \text{Specific area} \left(\frac{\text{m}^2}{\text{g}} \right) \times 10000 \left(\frac{\text{cm}^2}{\text{m}^2} \right)$$

Specific current density

$$j_{sp} \left(\frac{\text{mA}}{\text{cm}^2} \right) = j_{obs} \left(\frac{\text{mA}}{\text{cm}^2} \right) R_f \left(\frac{\text{cm}^2}{\text{cm}^2} \right)$$

Specific molecular production rate

For the reaction $2\text{H}^+ + 2\text{e}^- \rightarrow \text{H}_2$, $n=2$

$$\text{Prod}_{sp} \left(\frac{\text{molecule}}{\text{cm}^2 \cdot \text{s}} \right) = j_{sp} \left(\frac{\text{mA}}{\text{cm}^2} \right) 0.001 \left(\frac{\text{A}}{\text{mA}} \right) \frac{1}{\text{Faraday}} \left(\frac{1}{\text{C} \cdot \text{mol}^{-1}} \right) \frac{1}{n} (\text{unitless}) N_A \left(\frac{\text{molecule}}{\text{mol}} \right)$$

Site density per specific area

$$\text{AtomsIncc} \left(\frac{1}{\text{cm}^3} \right) = \frac{N(\text{atoms in formula}) N_A (\text{mol}^{-1})}{V_M (\text{cm}^3 \text{mol}^{-1})}$$

$$\text{Sites}_{sp} \left(\frac{1}{\text{cm}^2} \right) = \left(\text{AtomsIncc} \left(\frac{1}{\text{cm}^3} \right) \right)^{2/3}$$

Turnover frequency

$$TOF\left(\frac{\text{molecules}}{s}\right) = \frac{Prod_{sp}\left(\frac{\text{molecules}}{cm^2 \cdot s}\right)}{Sites_{sp}\left(\frac{1}{cm^2}\right)}$$

Catalyst	Loading /mg cm ⁻²	SA /m ² g ⁻¹	Rf	Site density /cm ⁻³	-j _{-0.10V,sp} /μA cm ⁻²	-j _{-0.20V,sp} /μA cm ⁻²	TOF _{-0.1V} /s ⁻¹	TOF _{-0.2V} /s ⁻¹	Ref
Ni ₂ P _{as recv}	0.15	1	1.5	2.00×10 ¹⁵	89	673	0.140	1.051	this work
Ni ₂ P _(6hr)	0.15	1.18	1.8	2.00×10 ¹⁵	85	1110	0.132	1.737	this work
Ni ₂ P _(9hr)	0.15	1.38	2.1	2.00×10 ¹⁵	62	1270	0.096	1.975	this work
Ni ₁₂ P ₅	0.15	16.1	24.1	6.30×10 ¹⁴	4	16	0.019	0.081	this work
Ni ₂ P	1.0	32.8	328	2.00×10 ¹⁵	10	320	0.015	0.500	1
CoP ^b	0.9	59.1	532	2.45×10 ¹⁵	48	NR	0.061	NR	2
MoS ^a	NR	NR	90	1.11×10 ¹⁵	NR	111	NR	0.312	3

(a) loading not provided in text, but roughness factor provided in supplementary materials; NR: not reported

Bode plot of Ni₂P (6hr ball milled) as a function of the applied overpotential. Symbols: Data, line: fit. Frequency range: 100 kHz to 0.2Hz at 10 points/decade. A sinusoidal perturbation of 10 mV_{pp} was used.

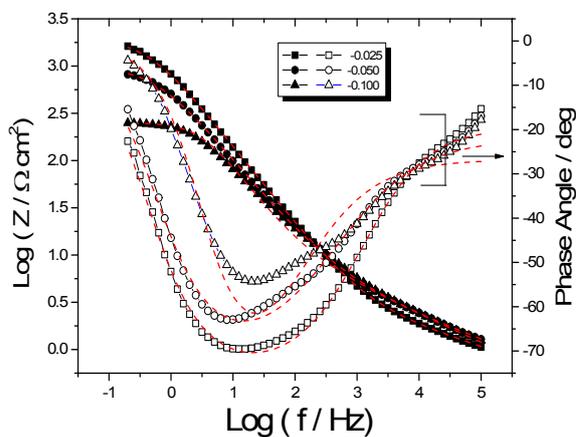


Table giving the equivalent circuit parameters derived using the 2TP model and 2TS model used respectively for Ni₂P and Ni₁₂P₅ based electrodes as a function of the applied overpotential. For Ni₂P based electrodes, R_s corresponds to the solution resistance associated with the electrolyte used and R_{CT}&CPE_{DL} with n₁ and R₂ &CPE₂ with n₂ represent the two time constant associated with the *her* reaction in acidic medium.

Catalyst	η / V vs. RHE	R _s / Ω	R _{ct} / Ω cm ²	R ₂ / Ω cm ²	CPE _{DL} / Fcm ⁻² s ⁿ⁻¹	CPE ₂ / Fcm ⁻² s ⁿ⁻¹	n _{DL}	n ₂
Bulk Ni ₂ P	-0.1	4.5	1.51E+03	7.60E+02	2.33E-11	1.15E-05	0.89	1
	-0.15	4.5	9.09E+02	2.90E+02	2.36E-11	2.01E-05	0.7	1
	-0.2	4.5	5.06E+02	1.97E+02	2.40E-11	3.13E-05	0.83	1
	-0.25	4.5	3.36E+02	2.88E+01	2.36E-11	3.47E-05	0.82	1
	-0.3	4.5	2.17E+02	2.16E+01	2.29E-11	7.29E-05	0.81	1
	-0.35	4.5	1.52E+02	1.16E+01	2.33E-11	1.39E-04	0.8	1
6 hr ball milled Ni ₂ P	-0.4	4.5	1.28E+02	6.60E+00	2.26E-11	2.34E-04	0.8	1
	-0.025	4.5	3.45E+03	2.53E+03	1.24E-10	1.32E-06	0.84	0.55
	-0.05	4.5	1.67E+03	1.19E+03	1.47E-10	5.00E-06	0.86	0.35
	-0.1	4.5	4.44E+02	3.47E+02	1.27E-10	8.68E-06	0.95	0.3
	-0.2	4.5	4.69E+01	2.38E+02	1.32E-10	1.63E-05	0.9	0.27
	-0.3	4.5	1.49E+01	8.50E+01	1.47E-10	2.35E-05	0.7	0.21
9 hr ball milled Ni ₂ P	-0.4	4.5	9.03E+00	3.40E+01	1.32E-10	4.68E-05	0.66	0.14
	-0.1	4.5	6.57E+02	5.17E+02	1.59E-10	8.05E-06	0.87	0.3
	-0.15	4.5	2.54E+02	1.79E+02	1.43E-10	1.58E-05	0.85	0.23
	-0.2	4.5	4.57E+01	3.97E+01	1.64E-10	3.67E-05	0.71	0.18
	-0.3	4.5	1.72E+01	7.25E+00	1.61E-10	2.26E-05	0.7	0.17
	-0.35	4.5	1.43E+01	3.93E+00	1.64E-10	6.79E-05	0.63	0.03
Catalyst	η / V vs. RHE	R _s / Ω	R ₁ / Ω cm ²	R ₂ / Ω cm ²	CPE ₁ / 10 ⁻³ Fcm ⁻² s ⁿ⁻¹	CPE ₂ / 10 ⁻⁶ Fcm ⁻² s ⁿ⁻¹	n ₁	n ₂
Ni ₁₂ P ₅ (series model)	-0.1	4.5	1.77E+04	6.25E+02	8.32E-12	5.64E-06	0.9	0.73
	-0.15	4.5	8.87E+03	2.32E+02	4.06E-12	5.70E-06	0.87	0.75
	-0.2	4.5	4.47E+03	1.16E+02	1.71E-12	5.75E-06	0.9	0.74
	-0.25	4.5	2.34E+03	4.59E+01	7.68E-13	5.72E-06	0.9	0.71
	-0.3	4.5	1.28E+03	1.93E+01	4.25E-13	5.66E-06	0.9	0.69
	-0.35	6.5	6.59E+02	9.66E+00	4.10E-13	5.78E-06	0.95	0.75
	-0.4	6.1	4.27E+02	7.25E+00	3.99E-13	5.72E-06	0.9	0.87

References

1. E. J. Popczun, J. R. McKone, C. G. Read, A. J. Biacchi, A. M. Wiltrout, N. S. Lewis and R. E. Schaak, *Journal of the American Chemical Society*, 2013, **135**, 9267-9270.
2. E. J. Popczun, C. G. Read, C. W. Roske, N. S. Lewis and R. E. Schaak, *Angew. Chem.-Int. Edit.*, 2014, **53**, 5427-5430.
3. J. D. Benck, Z. B. Chen, L. Y. Kuritzky, A. J. Forman and T. F. Jaramillo, *ACS Catalysis*, 2012, **2**, 1916-1923.